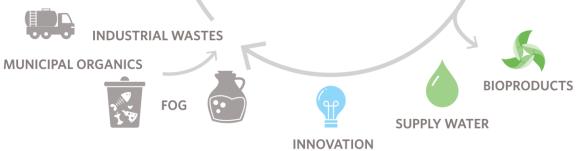






INNOVATION PLATFORM

A collaborative research program transforming waste into resources to support a circular economy.



MABR Technology for Secondary Treatment **Process Intensification** **BLACK & VEATCH:** SANDEEP SATHYAMOORTHY

YUEYUN TSE

KELLY GORDON SAMIK BAGCHI

(CURRENTLY WITH DIGESTED ORGANICS)

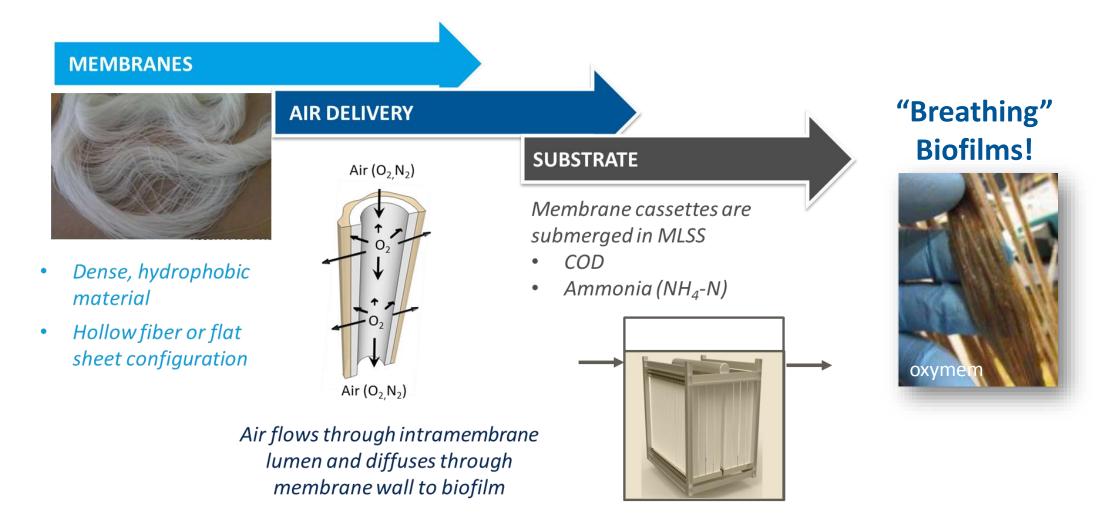
DWIGHT HOUWELING SUEZ:

DAN COUTTS



BUILDING A WORLD OF DIFFERENCE®

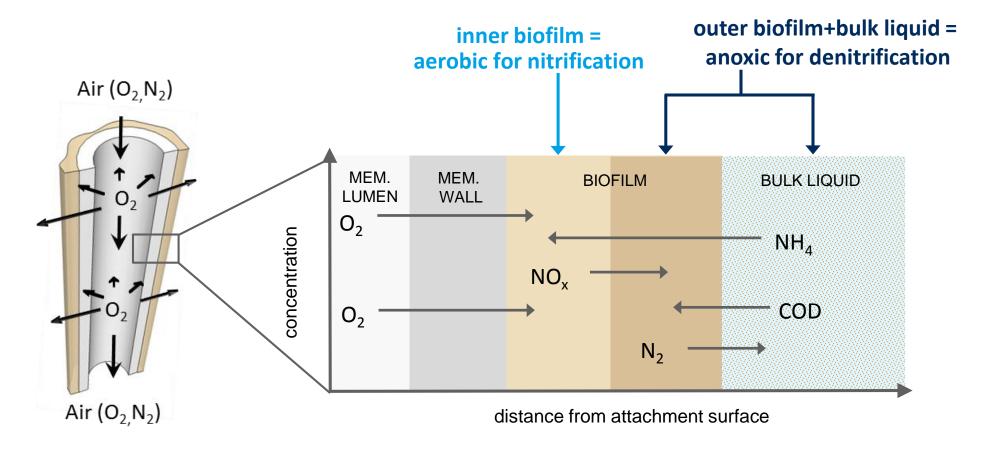
An MABR is...



Passive delivery of oxygen results in high oxygen transfer efficiencies.



THE MABR SUPPORTS COUNTER-DIFFUSIONAL SUBSTRATE DELIVERY.



Counter-diffusional substrate delivery supports total nitrogen removal in a single biofilm and basin.

BENEFITS OF AN MABR

a Bubbleless Aeration Device

Fine aeration control



a Biofilm Technology

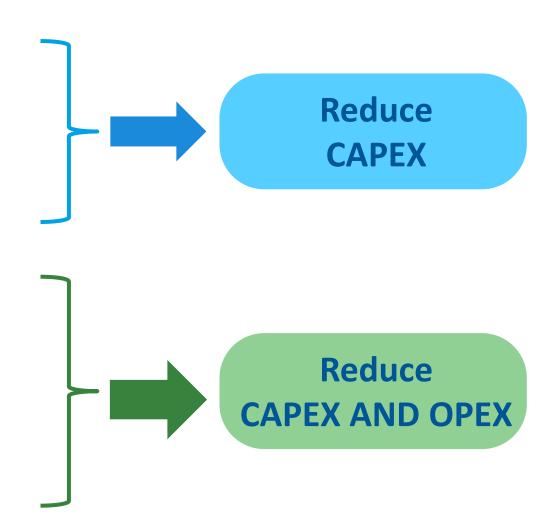
- Intensified treatment
- Support slow growing organisms

SYNERGY

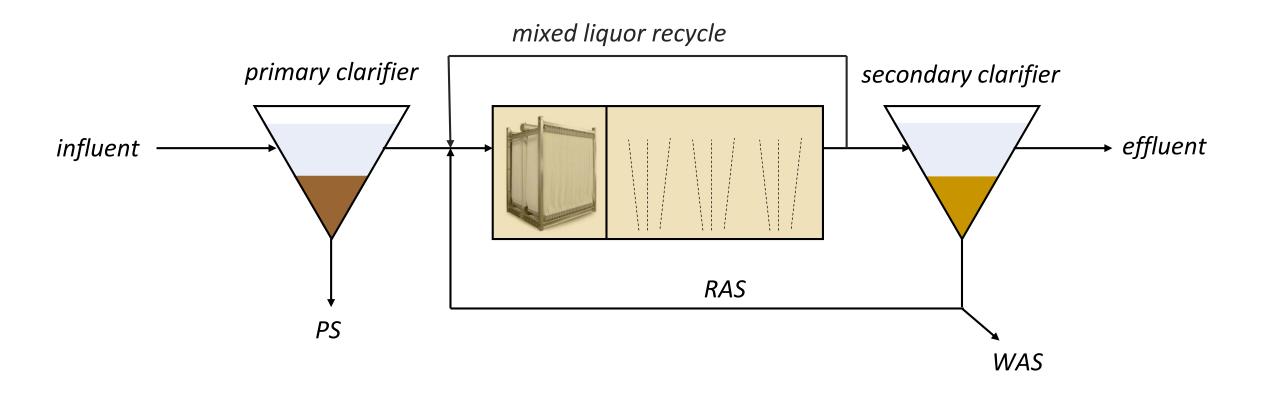
- Efficient aeration driven by biofilm activity
- High abundance of nitrifying organisms in biofilm
- Total nitrogen removal in a single reactor

VALUE PROPOSITION OF MABR TECHNOLOGY

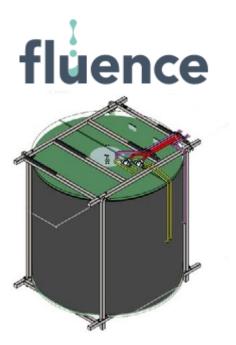
- Support total nitrogen removal in the same tank
- Retrofit existing aeration tanks and achieve process intensification
- Achieve efficient oxygen transfer rates
- Reduce internal recycle pumping
- Reduce supplemental biodegradable organic carbon requirements for denitrification



MABR achieves nitrification/denitrification in the anoxic zone.



TECHNOLOGY PROVIDERS











KNOWLEDGE GAPS OF MABR

Fundamental Understanding

- Microbial Community Structure
- AOB/NOB ratio

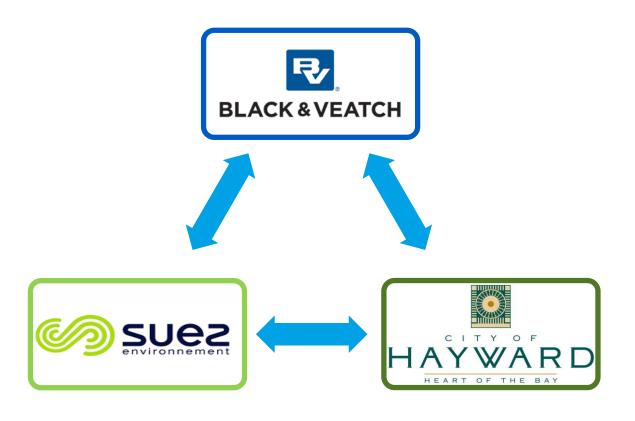
Operational Challenges

- Optimal SRT
- Impact of C:N ratio
- Biofilm Management

Scale up Challenges

- No of cassettes
- Nitrification Rate

MABR Research Collaborative

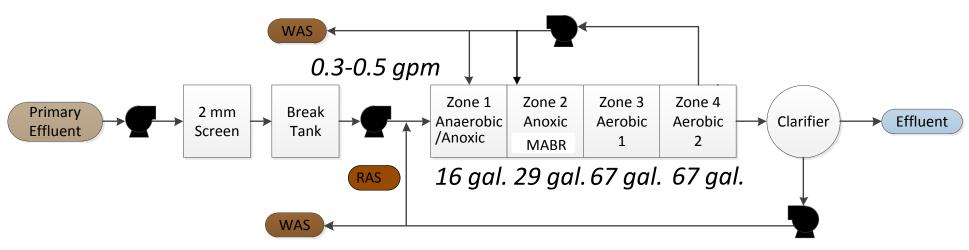




MABR Pilot @ Hayward WPCF



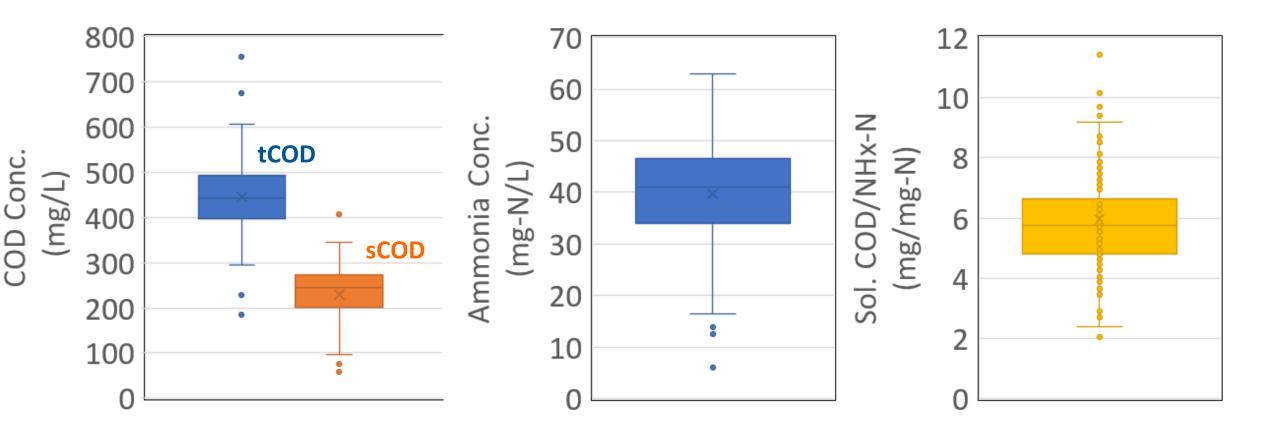
Pilot Overview







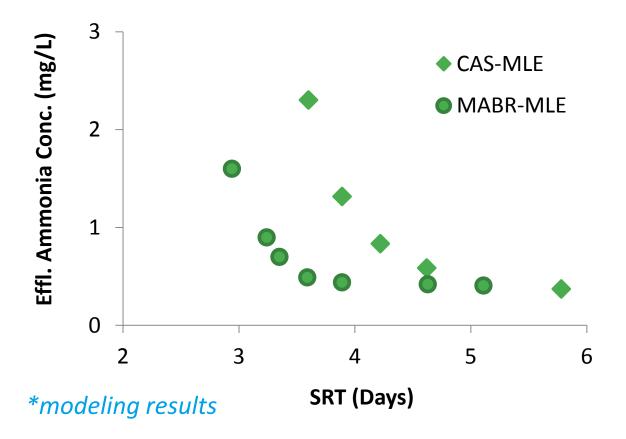
An introduction to the pilot influent/Hayward PE



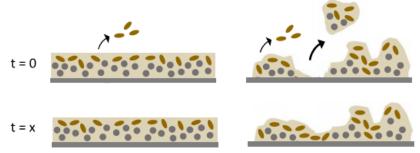
- Grab samples
- Samples typically collected ∼9 11 am

MABR Pilot Research Question # 1

Evaluate the aerobic solids retention time (SRT) required to achieve nitrification in an MABR configuration compared with a Suspended Growth BNR configuration



- 1. Lower nitrification "work" required by suspended sludge
- 2. "Seeding" effect by the biofilm.



SRT & Suspended SRT (S.SRT)

Suspended Growth (SG) process:

MABR-SG Hybrid process:

Suspended

Suspended SRT [T] =

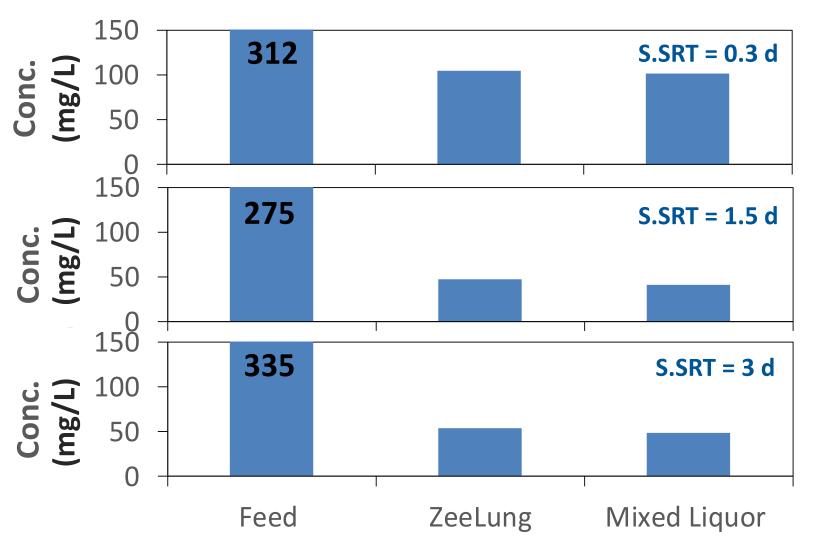
Wasted Biomass [M/T] =

$$X_{ML} [M/L^3] \times V_{BIO} [L^3]$$
 $Q_{WAS} [L^3/T] \times X_{WAS} [M/L^3]$

Wasted Biomass [M/T]

There's also ADDITIONAL BIOMASS ON THE BIOFILM AT A "BIOFILM SRT" MABR ADDS ~1-5 g-biomass/m²-MABR Surface Area (In the pilot – MABR SA = $10 \text{ m}^2 => 10 - 50 \text{ g biomass added} \cong 15 - 80 \text{ mg/L SS}$

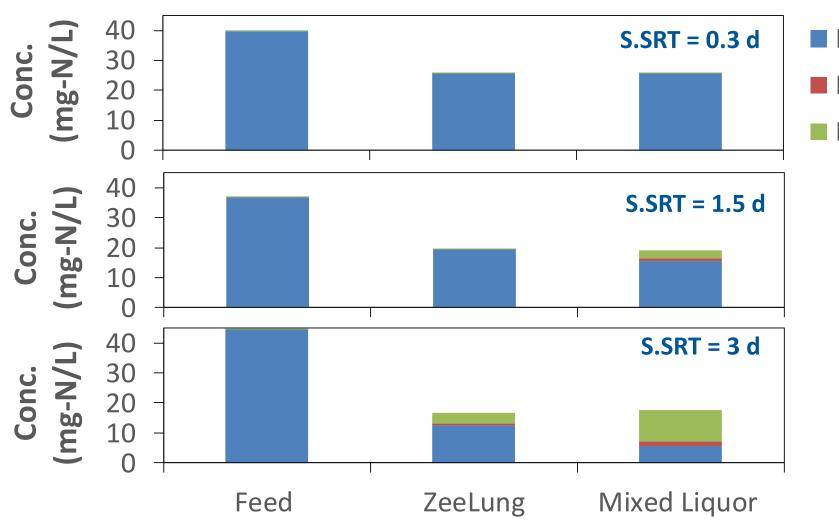
Pilot (MABR+ Sus. Growth) Performance At Different SRTs



Soluble COD

- **Each SRT Condition** tested for > 5X SRT
- Flow-weighted average from duplicate 24-h intensive sampling (2h interval) results

Pilot (MABR+ Sus. Growth) Performance At Different SRTs



- NHx-N
- NO2-N
- NO3-N

- **Each SRT Condition** tested for > 5X SRT
- Flow-weighted average from duplicate 24-h intensive sampling (2h interval) results

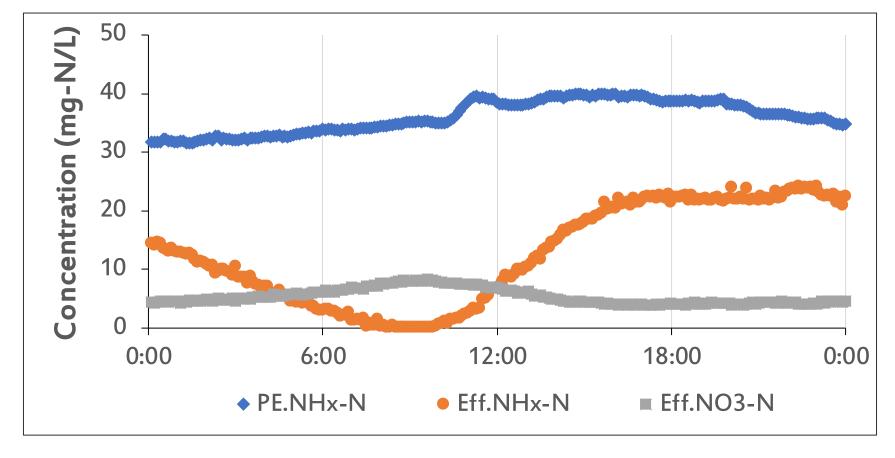
Typical Performance with Diurnal Flow

Influent = Diurnal Flow (matching Hayward WPCF pattern (avg. = 0.4 gpm)

60%xQ_{INF} RAS =

200% x Q_{INF} MLR =

Temp. ~ 18-19 °C MLSS ~ 1,340 mg/L Aerobic SRT_{SUSP.GR} ~ 1.5 d



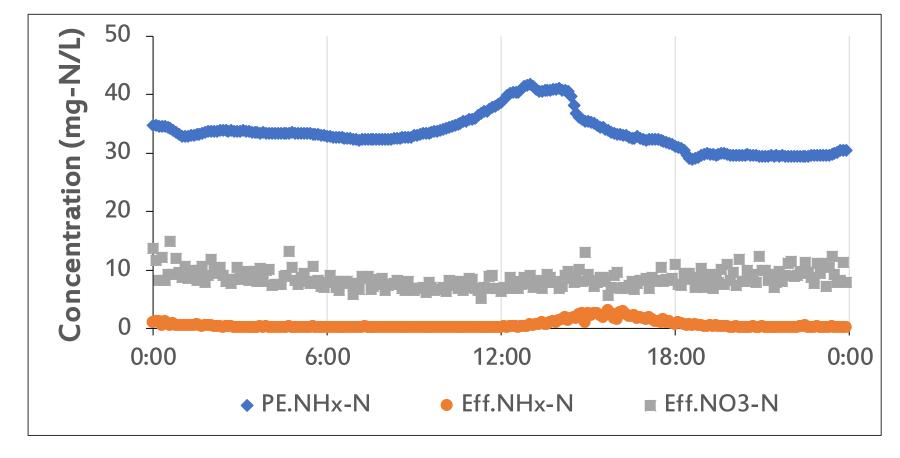
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Influent = Diurnal Flow (matching Hayward WPCF pattern (avg. = 0.4 gpm)

 $RAS = 60\% \times Q_{INF}$

 $MLR = 200\% \times Q_{INF}$

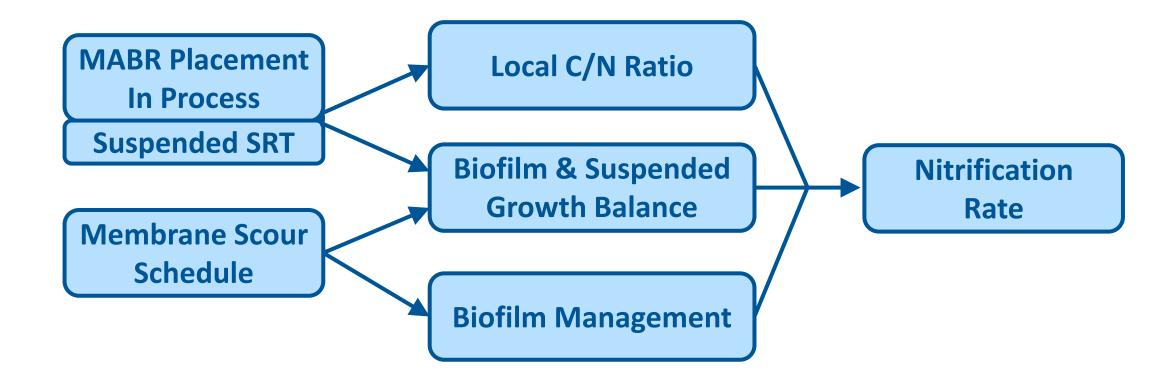
Temp. ~ 18-19 °C MLSS ~ 1,600 mg/L Aerobic SRT_{SUSP.GR} ~ 3d



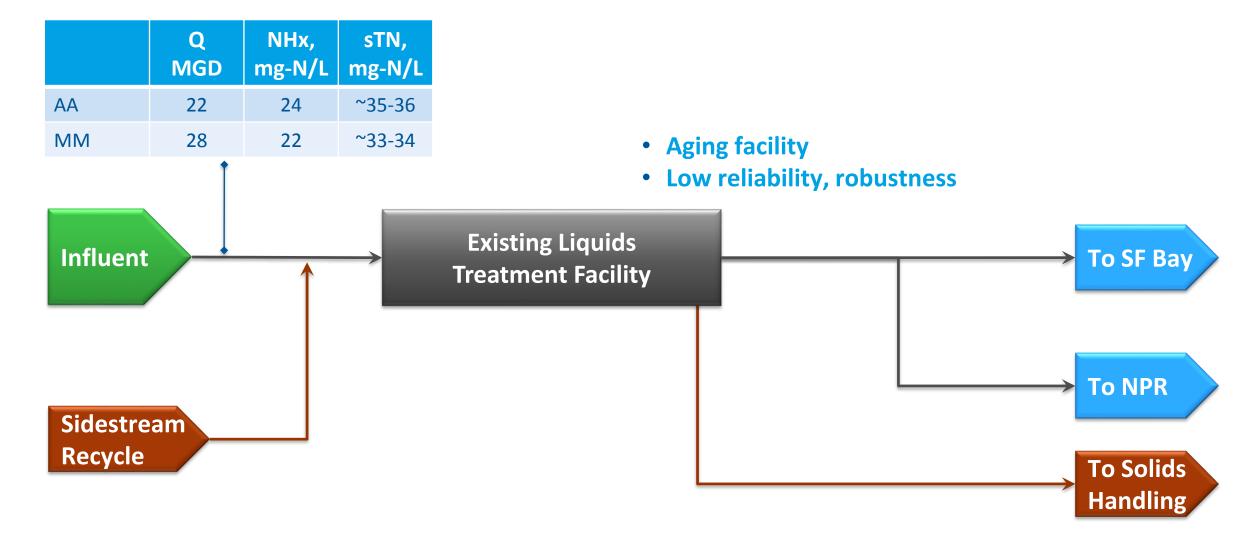
Preliminary Conclusions

- The counter-diffusional substrate delivery scheme leads to TN removal in one Tank.
- TN removal can be achieved at suspended SRTs lower than conventionally required/designed through MABR intensification
- Biofilm Management, C/N Ratio, Balance between Biofilm and Suspended **Growth** are critical to efficient MABR Design.

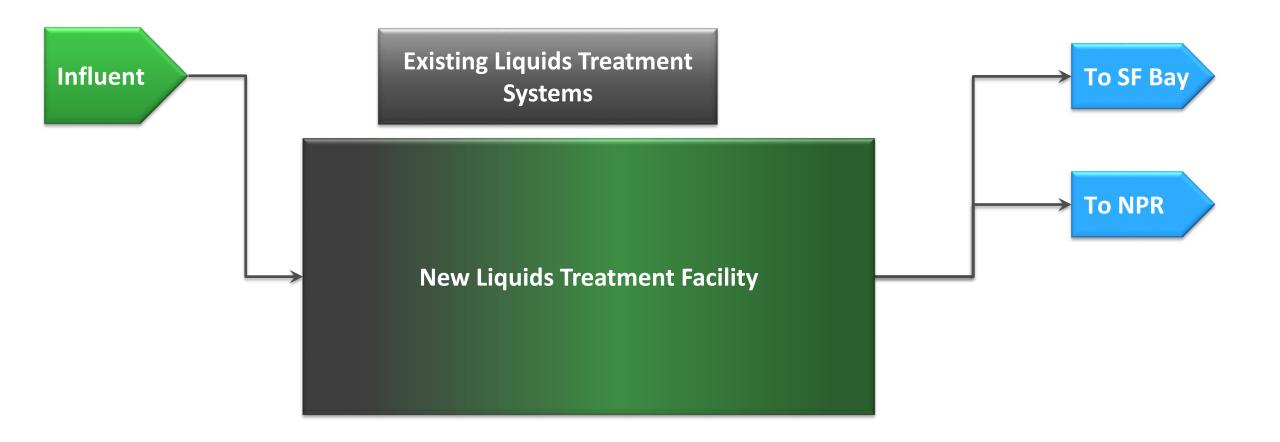
Key Factors to Consider for MABR Design



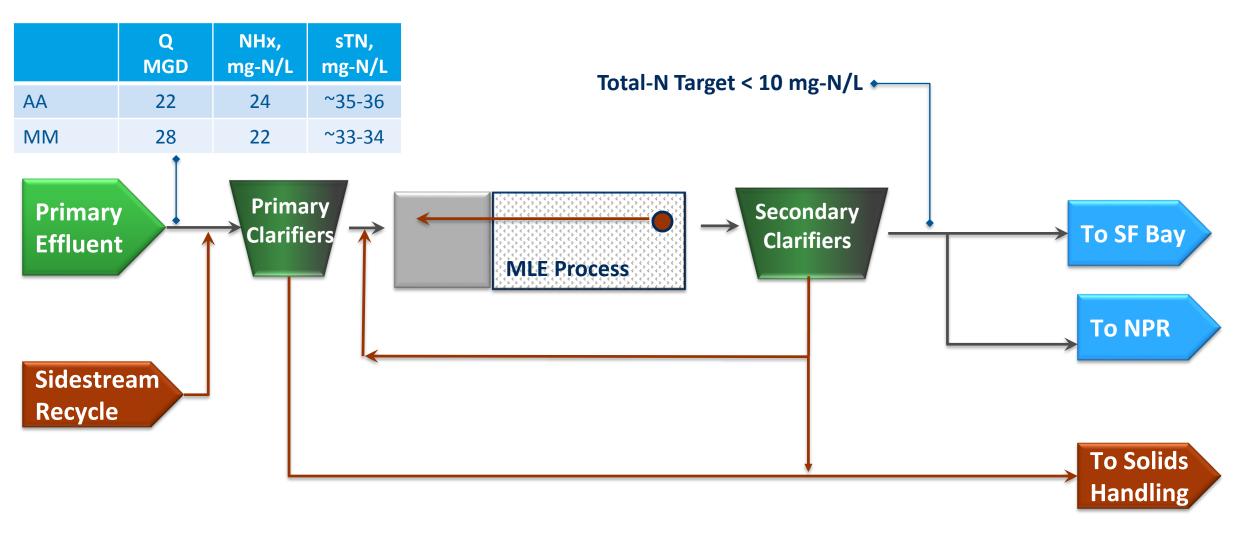
Consider expansion of an existing WRRF at an adjacent site



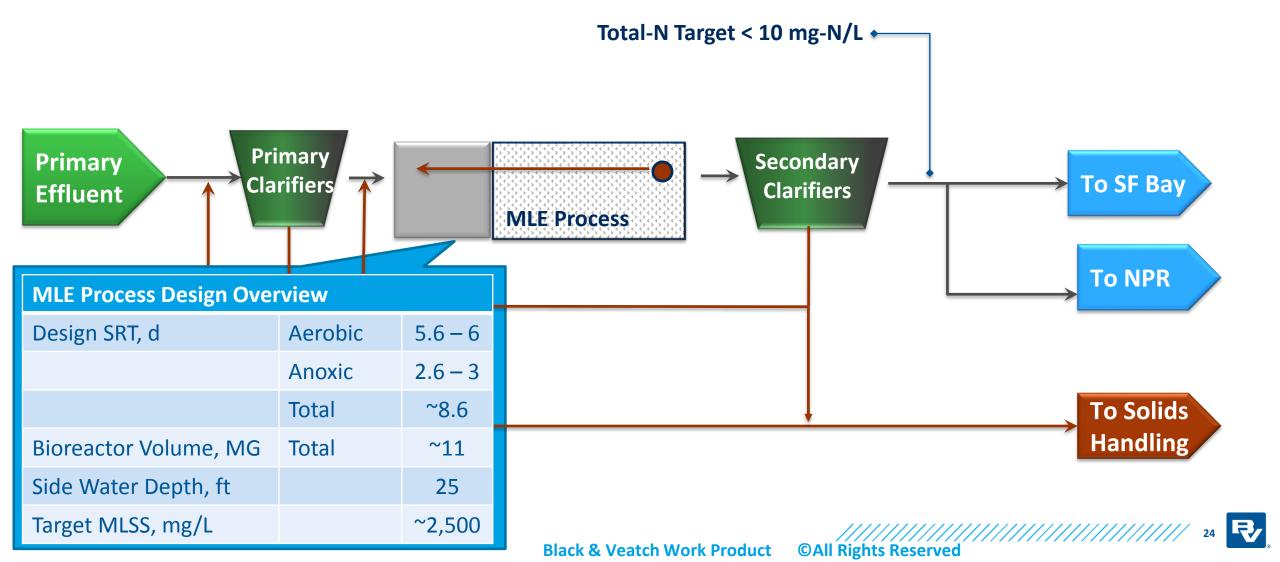
Consider expansion of an existing WRRF at an adjacent site



New WRRF Design (at "greenfield" site)



New WRRF Design (at "greenfield" site) Process Design Summary

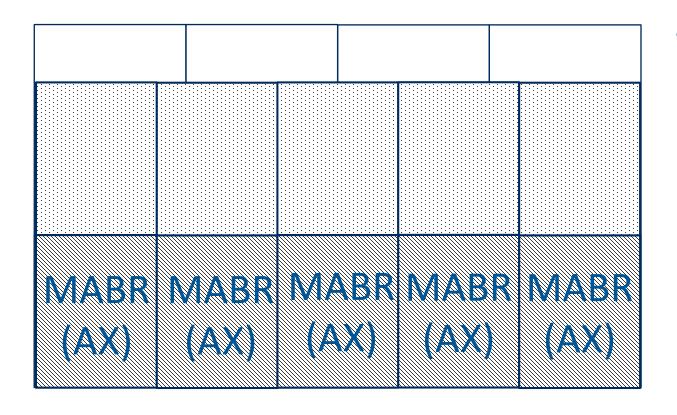


Can Process Intensification Help Enhance the Process Design?

What is the potential suspended SRT (and resulting volume) reduction?

What are some trade-offs to consider?

Incorporation of MABRs into the MLE design



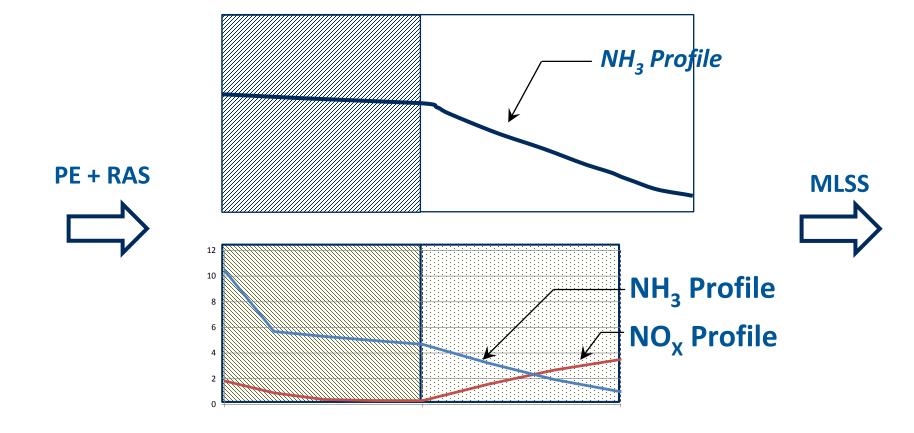
Current CAS Design

- ~ 11 MG
- ~35% AX, 65% AE
- MLSS_{MAX,MONTH} ~ 2,500 mg/L

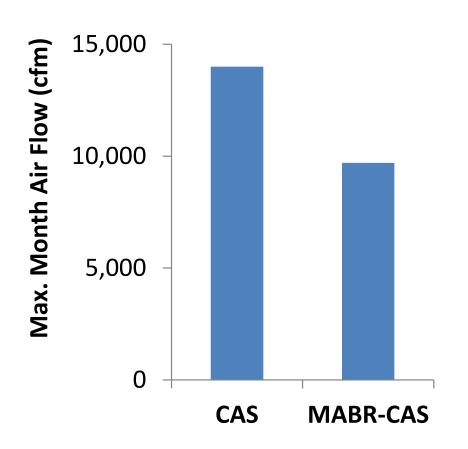
MABR-AS Design

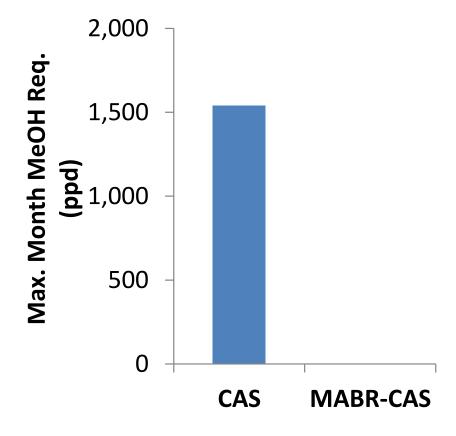
- ~ 8 MG
- ~ 50% AX
- MLSS_{MAX.MONTH} ~ 2,500 mg/L

Where is ammonia removal occurring?



Aeration & Chemical Use Benefits



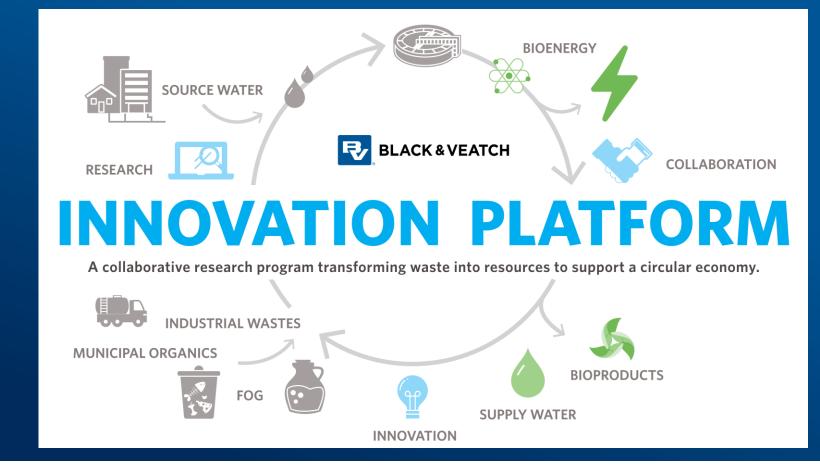


Tradeoffs

- Replacing potentially expensive concrete with equipment
 - More detailed tradeoff analyses required including LCC, etc.
- But are there benefits of reducing the SWD and overall tank depth?
 - Safety, operability, etc.

- Can this not be planned for as part of a future "plug-and-play" solution?
 - Yes...& No
 - Overall plant design/integration and system design are critical
 - (any) technology needs to be "best positioned" for success
 - For MABRs hydraulics are key: shortcuiting, bypassing, best use of membrane area, etc.

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Sandeep Sathyamoorthy

+1.925.949.5913
SathyamoorthyS@bv.com

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