Comparing the Sustainability and Effectiveness of RO- and Non-RO Based Potable Reuse Schemes

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Arizona Water Reuse 2016 Symposium



#### **Presentation Overview**

- Introduction
- Types of Potable Reuse
- RO and Non-RO Advanced Treatment Schemes
- Treatment Cost Comparison
- Greenhouse Gas Emissions Comparison
- Pathogen and Trace Organic Removal
- Conclusions

#### Introduction

- Increased interest in and implementation of potable reuse in U.S. as a means to meet water supply challenges
- Trend has been to use MF/RO/UV-AOP as default advanced treatment scheme driven by the broad contaminant removal capability of RO, particularly for bulk organics (TOC)
- RO produces a high salinity waste stream (concentrate) that can be challenging to dispose of
- Are other advanced treatment schemes capable to satisfying the pathogen, bulk and trace organic removals required for potable reuse but in a more cost-effective and sustainable manner

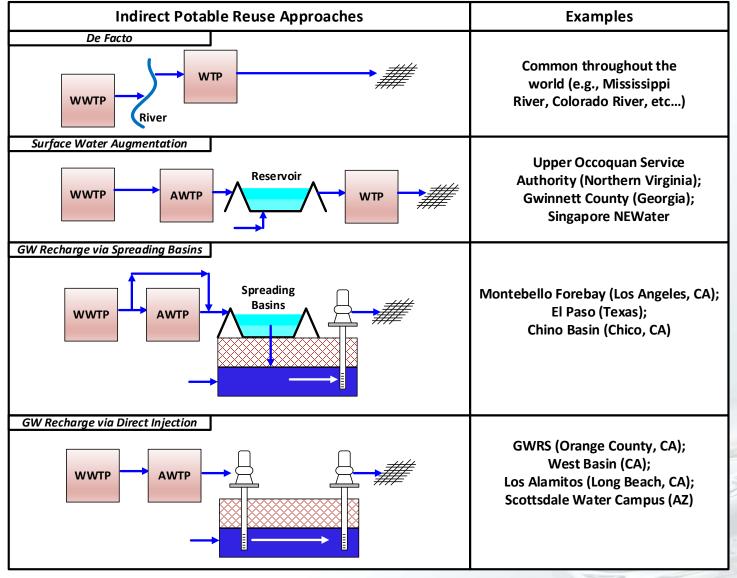


## Approach

- Compare and contrast two distinctly different advanced treatment schemes employed at full-scale facilities designed to produce a high-quality water from secondary effluent -- suitable for indirect, and possibly, direct, potable reuse
- Illustrate how each scheme is tailored to meet treated water requirements based on influent and regulatory requirements
- Assess the ability of each scheme to meet pathogen removal requirements and provide a high level of trace organic compound (TrOC) removal
- Compare the cost and carbon footprint of each scheme

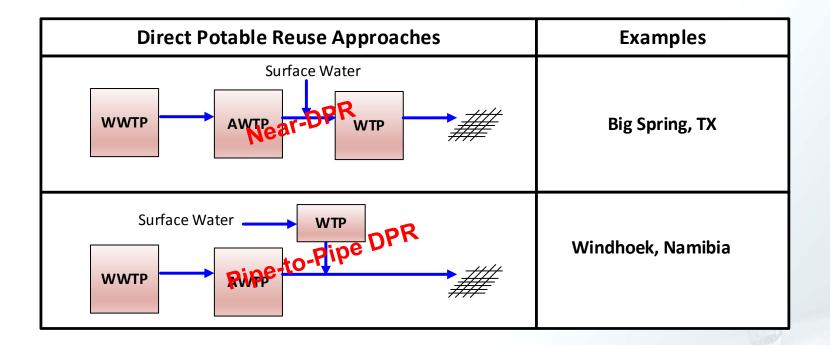


#### **Indirect Potable Reuse**



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#### **Direct Potable Reuse**





#### **Operational Potable Reuse Plants**

Project	Location	Type of Potable Reuse	<u>Year in</u> Operation	<b>Capacity</b>	Current Advanced Treatment Process
Montebello Forebay, CA	Coastal	GW recharge via spreading basins	1962	44 mgd	GMF + $Cl_2$ + SAT (spreading basins)
Windhoek, Namibia	Inland	Direct potable reuse	1968	5.5 mgd	$O_3$ + Coag + DAF + GMF + $O_3/H_2O_2$ + BAC + GAC + UF + $Cl_2$
UOSA	Inland	Surface water augmentation	1978	54 mgd	Lime + GMF + GAC + $Cl_2$
Hueco Bolson, El Paso, TX	Inland	GW recharge via direct injection and spreading basins	1985	10 mgd	Lime + GMF + Ozone + GAC + $Cl_2$
Clayton County, GA	Inland	Surface water augmentation	1985	18 mgd	$Cl_2$ + UV disinfection + SAT (wetlands)
West Basin, El Segundo, CA	Coastal	GW recharge via direct injection	1993	12.5 mgd	MF + RO + UVAOP
Scottsdale, AZ	Inland	GW recharge via direct injection	1999	20 mgd	MF + RO + Cl2
Gwinnett County, GA	Inland	Surface water augmentation	2000	60 mgd	Coag/floc/sed + UF + Ozone + GAC + Ozone
NEWater, Singapore	Coastal	Surface water augmentation	2000	146 mgd (5 plants)	MF + RO + UV disinfection
Los Alamitos, CA	Coastal	GW recharge via direct injection	2006	3.0 mgd	MF + RO + UV disinfection
Chino GW Recharge, CA	Inland	GW recharge via spreading basins	2007	18 mgd	GMF + $Cl_2$ + SAT (spreading basins)
GWRS, Orange County, CA	Coastal	GW recharge via direct injection and spreading basins	2008	100 mgd	MF + RO + UVAOP + SAT (spreading basins for a portion of the flow)
Queensland, Australia	Coastal	Surface water augmentation	2009	66 mgd	MF + RO + UVAOP
Arapahoe County, CO	Inland	GW recharge via spreading	2009	9 mgd	SAT (via RBF) + RO + UVAOP
Loudoun County, VA	Inland	Surface water augmentation	2009	11 mgd	MBR + GAC + UV
Aurora, CO	Inland	Surface water augmentation	2010	50 mgd	SAT (via RBF) + Soft + UVAOP + GMF +GAC
Big Spring ,TX	Inland	Direct potable	2013	1.8 mgd	MF + RO + UVAOP

ARR = Aquifer Recharge and Recovery; BAC = Biological Activated Carbon filtration;  $CI_2$  = Chlorine Disinfection; Coag = Coagulation; DAF = Dissolved Air Flotation; GAC = Granular Activated Carbon; GMF = granular media filtration; GW = groundwater;  $H_2O_2$  = Hydrogen Peroxide; MF = Microfiltration;  $O_3$  = Ozone; RBF = riverbank filtration; RO = Reverse Osmosis; SAT = Soil Aquifer Treatment; UF = Ultrafiltration; UV = Ultraviolet; UVAOP = UV Advanced Oxidation

## Why Not MF/RO/UV-AOP for AZ

#### • The scheme is:

- High CAPEX and OPEX
- Has high power consumption and carbon footprint
- Produces a waste stream that is challenging and costly to dispose (concentrate)

#### **AWT Plant Locations**



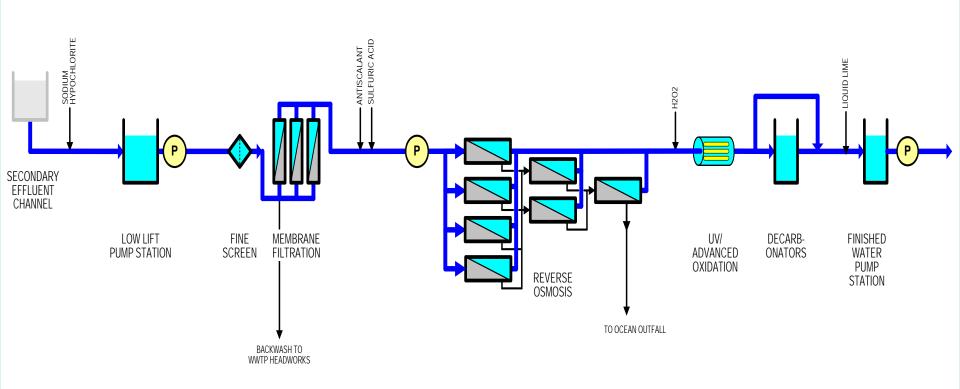
#### **Indirect Potable Reuse Schemes**

Facility	IPR Method	Treatment
Gwinnett County F. Wayne Hill Water Resources Center	Reservoir augmentation	Chemical clarification <sup>1</sup> , screening, UF, O <sub>3</sub> , BAC, $O_3$
Oxnard Advanced Water Purification Facility	Groundwater recharge	Micro-screening, chloramination <sup>2</sup> , MF, RO, UV/AOP

<sup>1</sup> Ferric addition, rapid mix, flocculation, high-rate plate settling <sup>3</sup> Chlorine addition

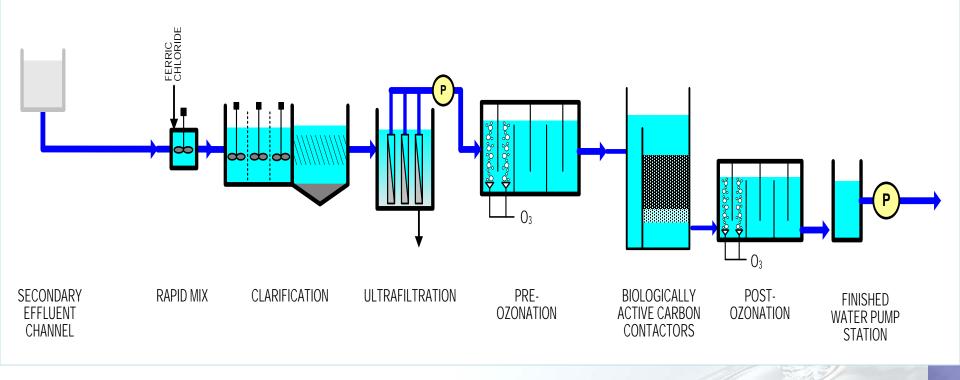


## Oxnard AWPF Process Schematic (6.25 mgd Phase 1)





## Advanced Treatment at FWHWRC, Gwinnett County





# **Representative AWT Feed Water Quality**

mg/L	Gwinnett County	Oxnard
BOD		16
COD	25	
TOC	6	16.6
TSS	9	6.4
Turbidity, NTU	2.0	4.0
TDS	300	1,750
NH3-N	0.2	23.3
NO3-N	6.5	2.6
Total N	8.0	25.9
Total P	0.2	1.24

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## **AWT Treated Water Quality Requirements**

mg/L or as shown	Gwinnett C	Oxnard	
	Req'd	Actual	Req'd
COD	18	10	NR
TOC	NR	3.5	0.5 <sup>a</sup>
TSS	3	<1	NR
Turbidity, NTU	0.5	<0.1	0.2
TDS	NR		500
NH3-N	0.4		NR
Total N	<10		<10 (5)
Total P	0.08		NR

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NR = Not regulated

<sup>a</sup> Assumes 100% treated water injection

# **AWT Treated Water Quality Requirements**

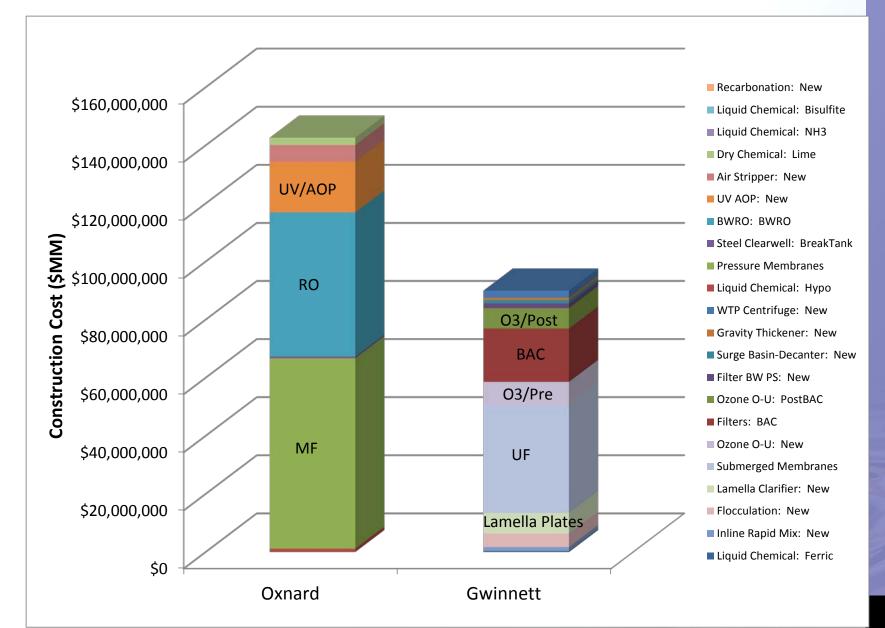
mg/L or as shown	Gwinnett County	Oxnard
	Req'd	Req'd
NDMA, ng/L	NR	1.2 LR <sup>b</sup>
1,-4 dioxane, ng/L	NR	0.5 LR <sup>b</sup>
NR = Not regulated <sup>b</sup> Log reduction by H <sub>2</sub> O <sub>2</sub> /UV		



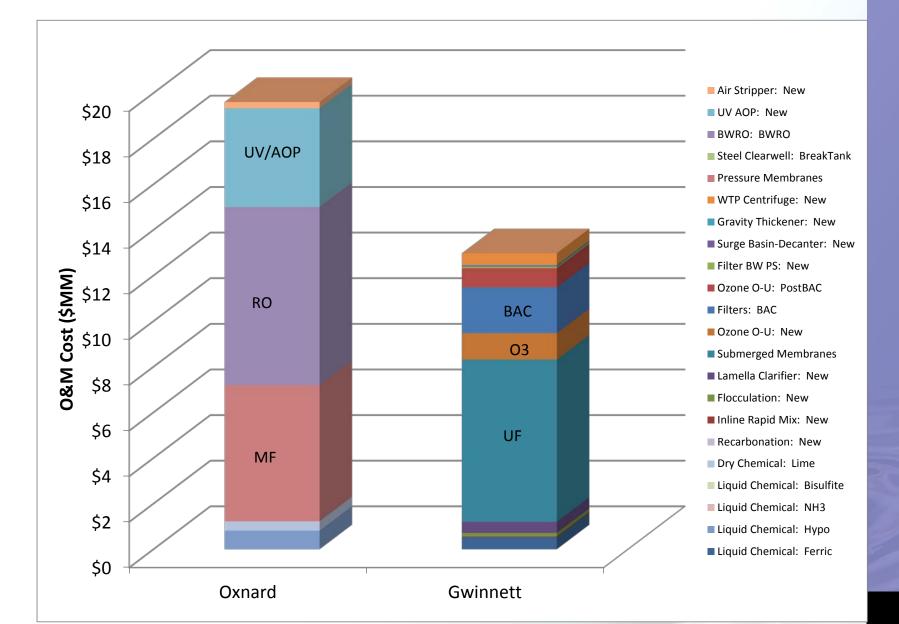
#### Construction and O&M Cost Estimates – AWT Schemes at 25 mgd capacity

- Developed using CH2MHILL's proprietary cost estimating program (CPES)
  - Parametric-based, uses detailed quantity take-offs and extensive database of constructed facility costs
- Both AWTPs sized at 25 mgd using design criteria from full-scale plant
- All unit processes and operations included except finished water pumping
- O&M costs include power, chemicals, residuals but excludes labor
- No costs included for RO concentrate disposal from Oxnard AWTP; concentrate discharged to river or ocean

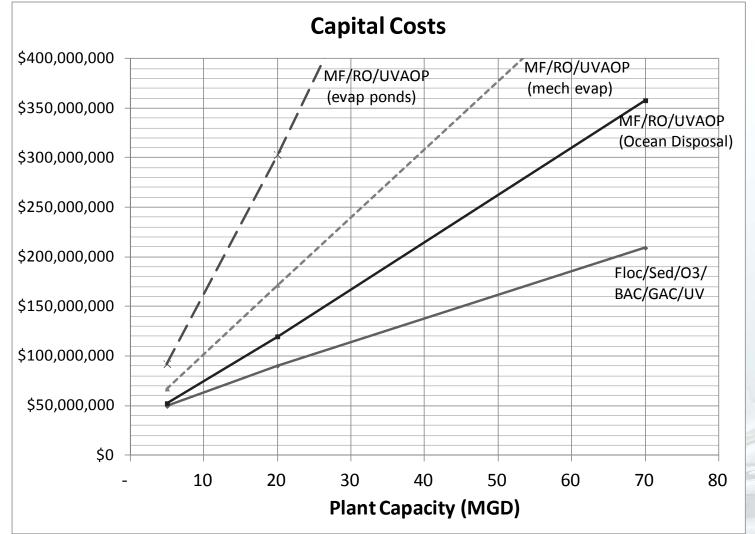
#### **Estimated Construction Costs (25 mgd)**



## Estimated Annual O&M Costs (25 mgd)



# **Cost Impact of Zero Liquid Discharge of RO Concentrate**



From WRRF-10-01, Fit for Purpose Water: The Cost of Overtreating Reclaimed Water

#### **Greenhouse Gas Emissions Estimates**

- Similar to Water Research Foundation Project 4156: Greenhouse Gas Emission Inventory and Management Strategy Guidelines for Water Utilities
- Evaluation is predictive based on specific design criteria and GHG production data
- Carbon dioxide, methane, nitrous oxide in carbon dioxide equivalents (CO2e)
- Accurate development and understanding of the facility and associated physical footprint, energy and chemical use, and residuals production is critical
  - CPES use provides foundation for estimates



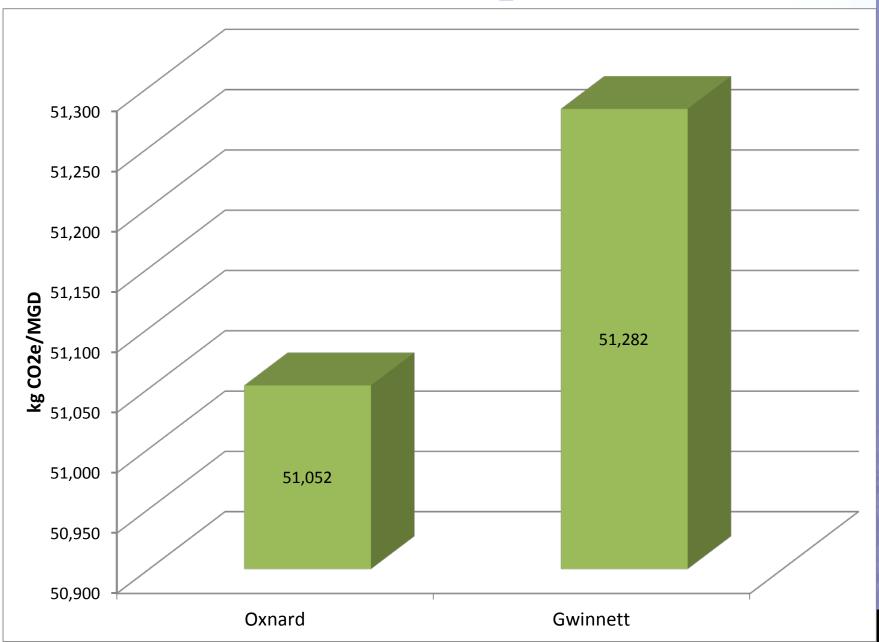
## **GHG Production Bases**

Component	Emission Value	Emission Unit
GAC Media <sup>1</sup>	368	Lbs CO <sub>2</sub> e/ton GAC
Electricity		
Gwinnett County (Southeast USA) <sup>2</sup>	1,294	Lbs CO <sub>2</sub> e/MWh
Oxnard (California) <sup>2</sup>	879	Lbs CO <sub>2</sub> e/MWh
Fuel Use <sup>3</sup>	21.96	Lbs CO <sub>2</sub> e/gal

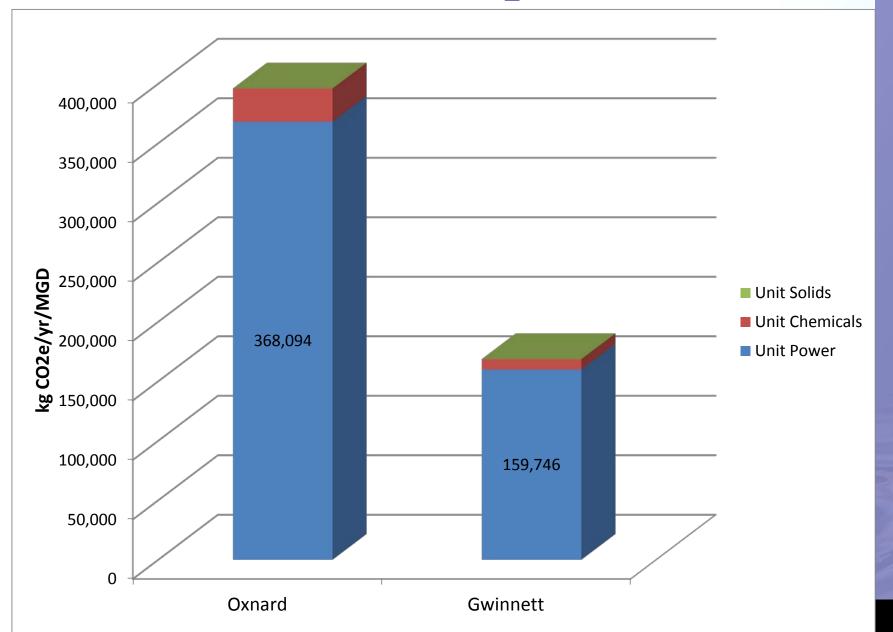
<sup>1</sup>Liu, P. and Wagner, N. Thermal Regeneration of Activated Carbon. Environmental Progress. May 1985.
<sup>2</sup> USEPA. Indirect Emissions from Purchaces/Sales of Electricity and Stream. June 2008.
<sup>3</sup> California Climate Action Registry General Reporting Protocol, Version 2.2. California Climate Action Registry. 2007 (based on diesel fuel)



#### **Construction-Related CO<sub>2</sub> Emissions**



#### **Annual O&M-Related CO<sub>2</sub> Emissions**



# Pathogen Log Removals – DPR (1)

Oxnard AWPF	Crypto	Giardia	Virus
MF	4	4	0.5
RO	1.5 - 3	1.5 - 3	1.5 - 3
UV-AOP	6	6	6
Total	11.5 - 13	11.5 - 13	8-9.5*
DPR Req'mt	10	10	12
FWH WRC AWT	Crypto	Giardia	1
Coag-Sed			2
UF	4	4	Z
Pre-O3	0	0	0
BAC	0	0	0
Post-O3	1.5	3	6
Total	5.5	7	8
DPR Req'mt	10	10	12

(1) No downstream WTP \*Add'I 6 log virus through aquifer storage

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UV-AOP	6	6	6
Total	11.5 - 13	11.5 - 13	8-9.5*
DPR Req'mt	10	10	12
FWH WRC AWT	Crypto	Giardia	Virus
Coag-Sed			0
UF	4	4	2
Pre-O3	0	0	0
BAC	0	0	0
Post-O3	1.5	3	6
UV-AOP	6	6	6
Total	11.5	13	12
DPR Req'mt	10	10	12
) No downstream WTP *Add'l	6-log removal through	aquifer storage	ch2n

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# Pathogen Log Removals – DPR (2)

Oxnard AWPF	Crypto	Giardia	Virus
MF	4	4	0.5
RO	1.5 - 3	1.5 - 3	1.5 - 3
UV-AOP	6	6	6
Total	11.5 - 13	11.5 - 13	8-9.5
N-DPR	8	7	8
FWH WRC AWT	Crypto	Giardia	Virus
Coag-Sed			0
UF	4	4	2
Pre-O3	0	0	0
BAC	0	0	0
Post-O3	1.5	3	6
UV	4	4	2
Total	9.5	11	10
N-DPR	8	7	8
2) ATW to downstream WTP			ch2m

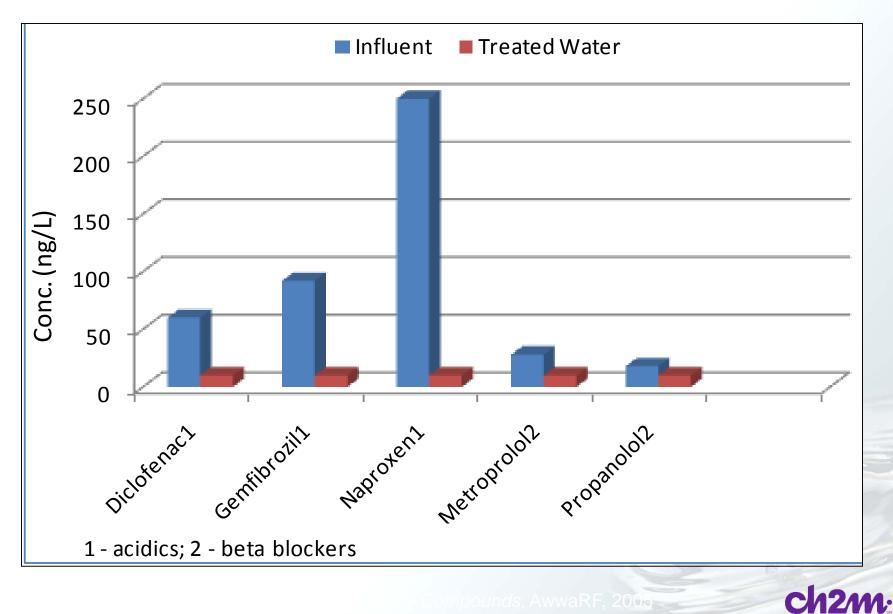
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## Trace Organic Compound (TrOC) Removal

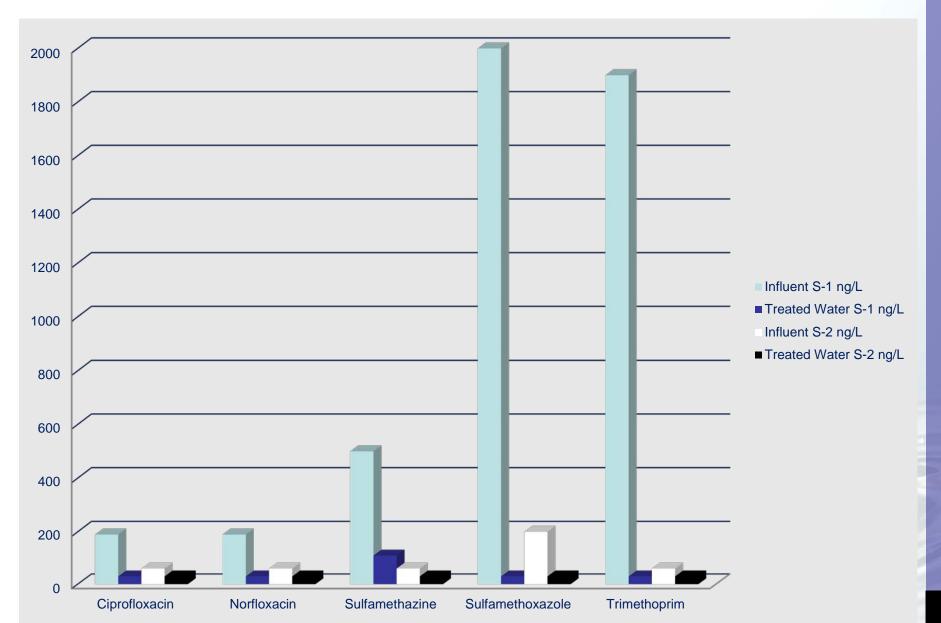
- Oxnard AWT designed specifically to achieve high level of removal of two TrOCs (NDMA and 1,4-dioxane) per California recycled water regulations for subsurface injection.
- RO and UV-AOP combination provides excellent removal of all classes of TrOCs as demonstrated by full-scale potable reuse facilities
- Gwinnett County AWT isn't specifically designed to achieve TrOC removal, but O<sub>3</sub>/BAC/O<sub>3</sub> provides good-to-excellent removal of most TrOCs, confirmed through research conducted on pharmaceutically-active compounds (PhACs)



## **PhAC Removal - Gwinnett County**



### **Antibiotic Removal – Gwinnett County**



## Conclusions

- RO- and non RO-based treatment schemes are both capable of meeting or exceeding pathogen log removal requirements, whether for direct or near-direct potable reuse – a key requirement for any potable reuse facility
- Although RO provides better bulk organics (TOC) removal, both schemes are capable of providing a high level of TrOC removal
- The non RO-based treatment scheme has significant lower CAPEX, OPEX and life-cycle costs, even where a low-cost concentrate disposal option is available
- The non RO-based treatment scheme has significantly lower GHG emissions
- If some demineralization and improved TOC removal is required, the non-RO based scheme can be adapted by incorporating nanofiltration, and soil aquifer treatment (SAT) and/or GAC.



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## **Questions?**

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