



# Extraction of Valuable Materials from Reverse Osmosis Concentrate

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# The WateReuse Research Foundation

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- There is 1 (one) Professional Development Hour available.
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# Today's Moderator



Arash Shahmansouri  
*PhD Candidate, Clarkson University*



# Today's Presenter



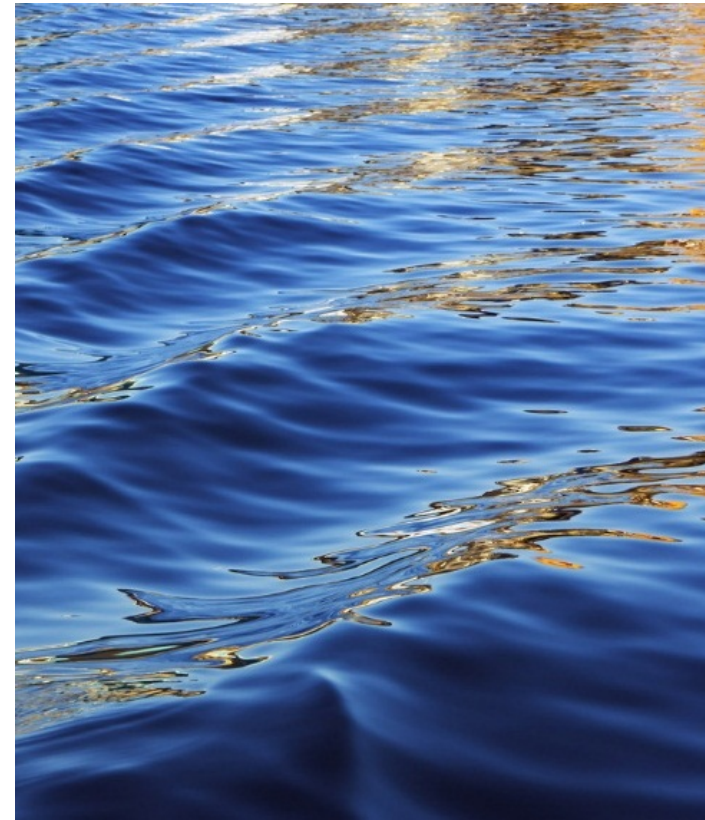
Dr. Christopher Bellona  
*Assistant Professor, Clarkson University*

# Webinar Outline

- Historical Perspective
- Project Introduction
- Economic Evaluations
- Other Options
- Conclusions

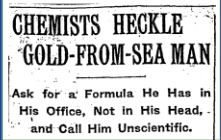


# Historical Perspectives



# Historical Perspective

- The ocean has long been viewed as an inexhaustible resource
- Magnesium and bromine once exclusively produced from seawater in the U.S.
- Large interest in uranium and lithium recovery from seawater
- Various minerals extracted from aqueous resources

2200 BC	Chinese extract salt from SW	<sup>11</sup> Na	<sup>17</sup> Cl
ca. 600-900 BC	Mayan salt works active, Yucatan		
1872	First analysis of SW for gold	<sup>79</sup> Au	
1911	Austrian chemist laughed out of ACS meeting		
World War 1	War with Germany leads Dow to develop Mg production from brine		<sup>12</sup> Mg
1918	Gold from SW proposed to pay German war debt		
1926	Br first produced from SW		<sup>35</sup> Br
1933	Dow-Ethyl Br plant opens at Kure Beach, NC		
World War 2	UK develops magnesia production		
1941	Dow opens Freeport, TX, Mg plant		
1950s	UK starts uranium from SW research	<sup>92</sup> U	
1960s	Japan researches U		
1970s	Li extraction studied at Brookhaven	<sup>3</sup> Li	
1990s on	Increased interest in extracting salts from RO brine		



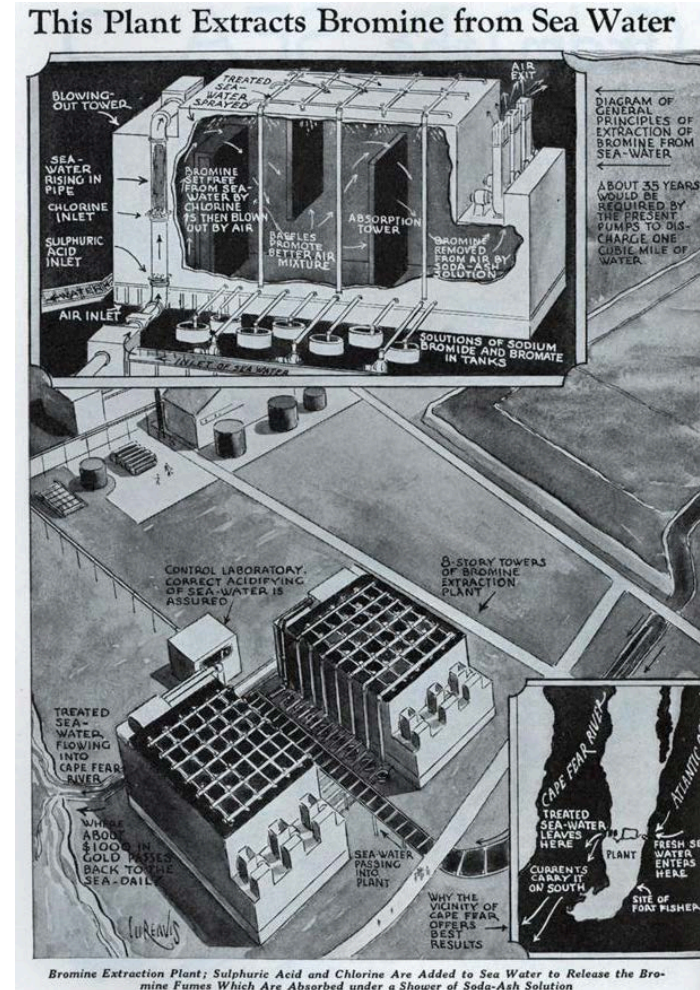
# Historical Perspective – Sodium Chloride

- Extracted from seawater in significant quantities for thousands of years
- Commonly produced in solar salt works – successive precipitation steps
- Byproducts of solar salt include bromide, iodide, potassium, nitrate and sulfate containing salts
- Japan produces food grade salt from seawater using electrodialysis followed by evaporation



# Historical Perspective – Bromine

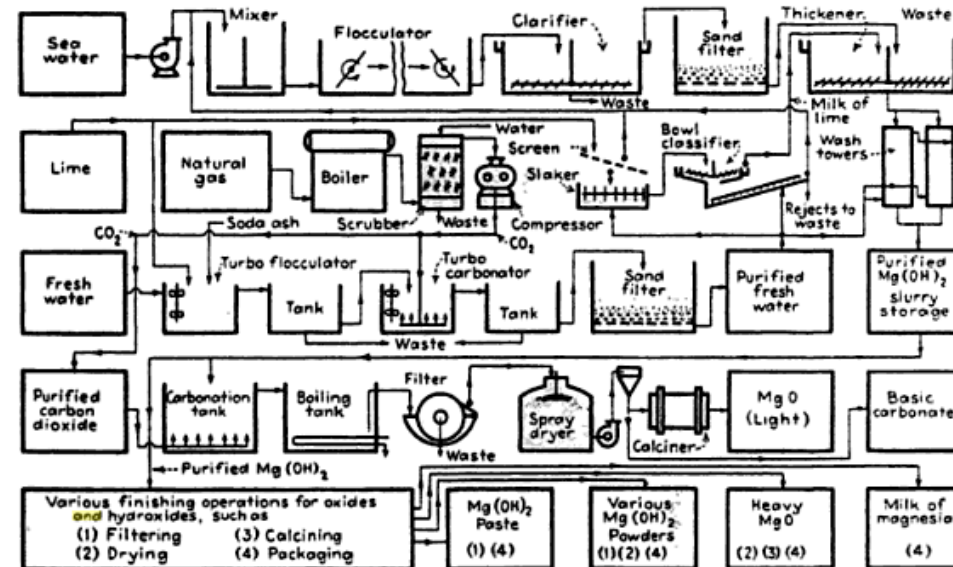
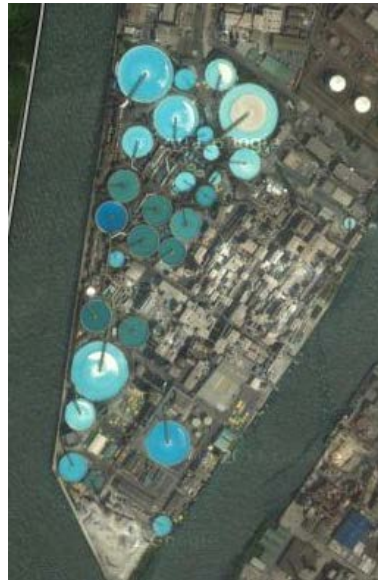
- Ethyl Gasoline Corporation developed process for producing tribromoaniline from seawater in 1920's
- Dow Chemical Company refined process and built a large-scale bromine from seawater plant in North Carolina in 1933
- Both companies eventually turned to underground brines for a source of bromine
- Currently, a small percentage of bromine is produced from byproducts of solar salt operations





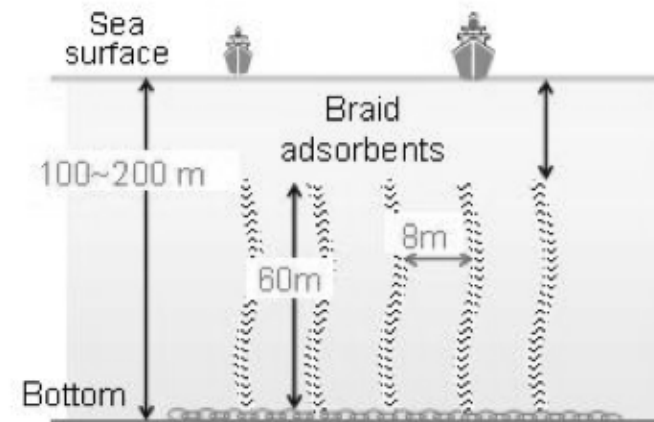
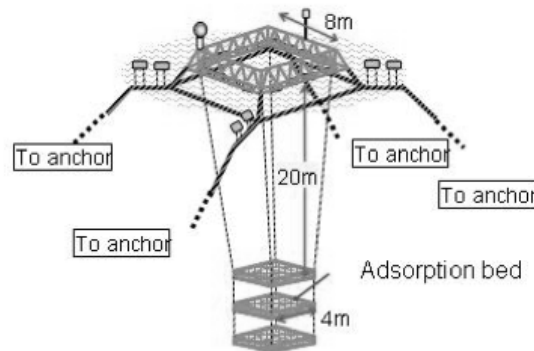
# Historical Perspective – Magnesium

- Second most abundant cation in seawater ( $\sim 1.28$  g/L)
- Dow produced magnesium metal and compounds from seawater for  $\sim 50$  years
- Several seawater magnesium compound ( $\text{MgOH}_2$ ,  $\text{MgO}$ ) extraction facilities in operation worldwide
- Utilize staged lime precipitation process



# Historical Perspective – Uranium

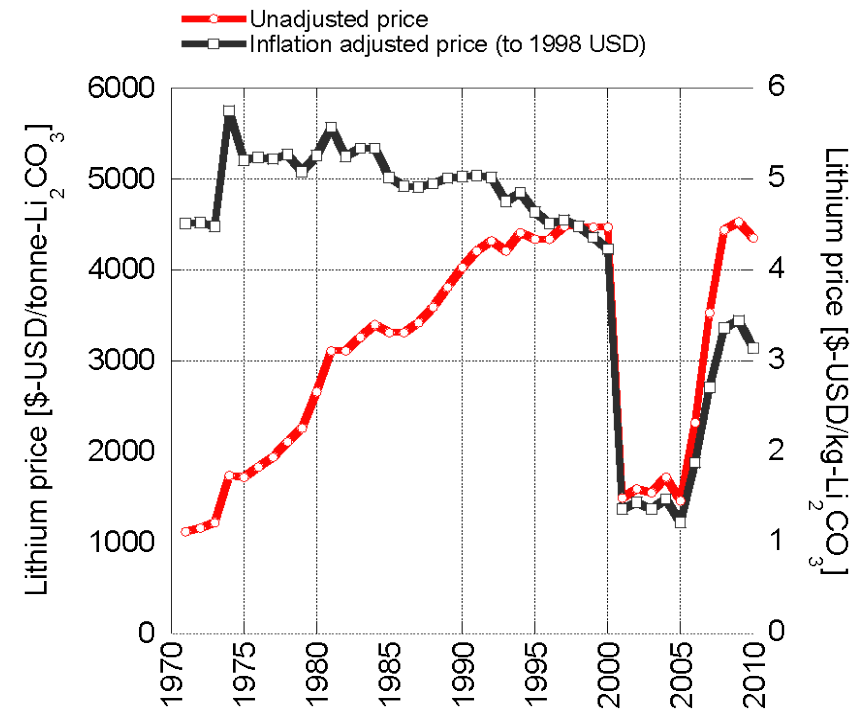
- Uranium found at  $\sim 3 \text{ ug/L}$  in surface seawater
- Research on uranium extraction from the sea likely started in the United Kingdom in the 1950's (abandoned in 1970)
- Japan began researching uranium extraction in the 1960's and researchers have evaluated or developed a number of adsorbent materials
- Researchers at the Japanese Atomic Energy Agency and India's Bhabha Atomic Research Center have begun developing technology for large-scale uranium from sea production





# Historical Perspective – Lithium

- Found in seawater at  $\sim 173.5 \text{ ug/L}$
- Increase in Li-ion battery (LIB) use has brought attention to lithium supply and demand
- Around 90% of lithium resources controlled by 4 major producers, which are not near LIB manufacturers
- Lithium extraction from seawater has received attention for 40-years
- Detailed cost analyses indicate the seawater lithium extraction costs are btw \$16 – 22/kg- $\text{Li}_2\text{CO}_3$



# Historical Perspective – Desalination

- Postulated by John Mero<sup>1</sup> in 1964 that desalination brine would be mined in the not so distant future:

*‘By using these brines for the extraction of minerals, several important advantages are gained; the cost of pumping is carried by the conversion plant, the brine temperature is relatively high, and the concentrations are increased as high as four.’*

- Others<sup>2</sup> have more recently raised the question:

*‘Where it [seawater] has to be used to produce fresh water, why not try to obtain as many byproducts as are economically viable?...Or why not place a minerals industry in a region where byproduct water would be desirable?’*

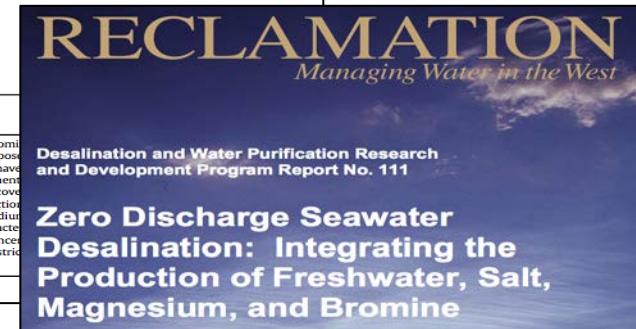
<sup>1</sup>Mero, J.L., *The mineral resources of the sea*. Vol. 1. 1965, Amsterdam: Elsevier.

<sup>2</sup>Petersen, U., *Mining the hydrosphere*. *Geochimica et Cosmochimica Acta*, 1994. **58**(10): p. 2387-2403.



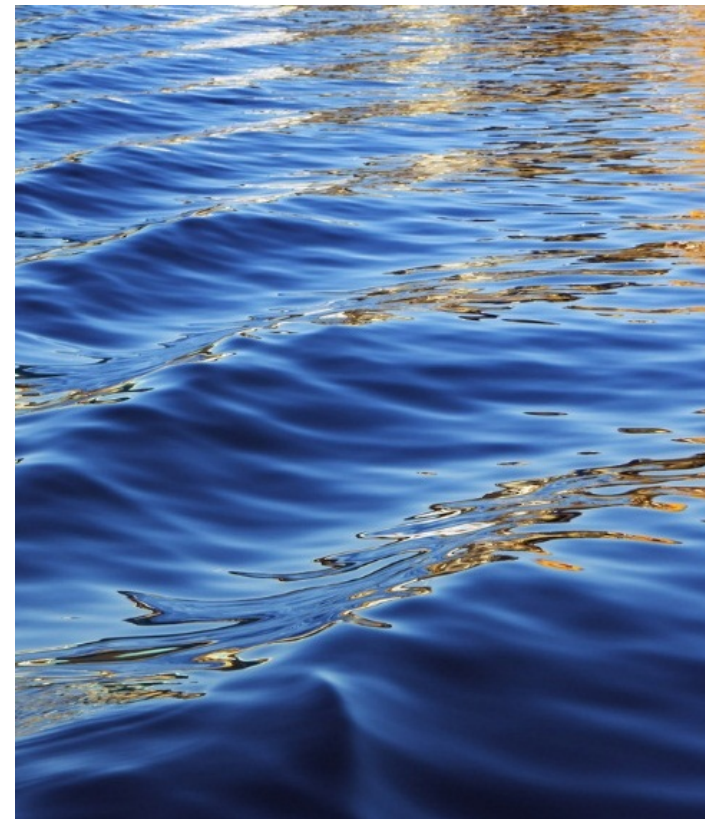
## A vertical photograph of tall, green reeds or grasses growing in a body of water. The water is a deep blue, and the reeds are reflected in it, creating a symmetrical pattern. The reeds are thin and pointed, with some showing signs of being cut or broken.

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# Project Introduction





# Project Introduction

- Solicited project funded by the WaterReuse Research Foundation
- Goal of investigating the feasibility of extracting materials for economic gain from desalination brine/concentrate
- Objective of conducting a review of past and present work focused on commodity recovery from aqueous solutions
- Final report title will be 'Guidance for Selection of Selective Salt, Metal, Radionuclide, and Other Valuable Material Recovery Approaches'

# Project Introduction

- Goal: evaluate feasibility of material extraction from desalination brine/concentrate by:
  - Conducting comprehensive literature review
  - Conducting comprehensive patent review
  - Summarizing case studies
  - Performing economic analyses



# Literature Review

- A variety of literature types screened and categorized:
  - Commodity information
  - Sources of water quality information
  - Patented technologies for extraction
  - Peer-reviewed literature
  - Book chapters
  - Reports
  - Grey literature
- Significant amount of research conducted on extracting commodities from aqueous solutions over the past 100-years
- All information compiled into searchable EndNote database

▶ REVIEWED	746	•	Bennett, R.C.	2002	Crystallizer selection and design
▶ RELEVANCE	693	•	C.M. Bethke	2008	Geochemical and Biogeochemical Reaction Modeling
▶ TECHNOLOGY TYPE	512	•	Biello, D.	2008	Cement from CO2: A concrete cure for global warming?
▶ WATER TYPE	464	•	Birnhack, Liat; Lahav, Ori	2007	A new post-treatment process for attaining Ca2+, Mg2+,
		•	Blaney, Lee M.; Cinar, Suna;...	2007	Hybrid anion exchanger for trace phosphate removal fro
		•	Bond, R.; Batchelor, B.; Davi...	2011	Zero liquid discharge desalination of brackish water with



# Findings from Literature and Patent Reviews

- Patents were not generally useful unless associated with a published paper or report
- Commodity information often indicated that markets for extracted materials are either competitive, limited or difficult to enter
- Research has been conducted on the extraction of a wide variety of substances or elements from water using a wide range of technologies
- Most studies conducted at a very fundamental level – not near demonstration level
- Very few studies were identified that physically evaluated the technical feasibility of extracting and purifying commodities from desalination brine/concentrate



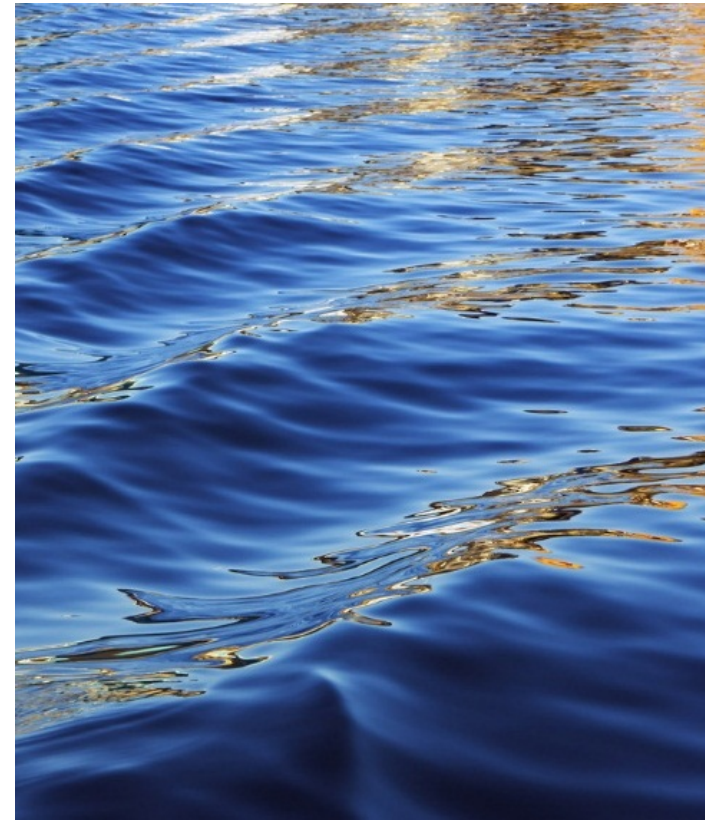
# Findings from Literature and Patent Reviews

- Significant amount of research on extraction of commodities from desalination brine/concentrate streams
- Many studies conclude that extraction is feasible and would produce a profit
- Very few demonstration studies
- Very few studies that analyzed energy requirements, chemical consumption, and costs

Desal. System	Constituent(s)	Processes	Level of Investigation	Cost and Energy Requirements
SWRO	Br <sub>2</sub> , Mg(OH) <sub>2</sub> , salt	ED/EDR, precipitation, evaporation, blowout tower	Lab-scale tests conducted	Preliminary costs presented indicate potential profits
SWRO	NaCl	ED/EDR, MSF, crystallization	Lab-scale tests conducted	Cost analysis presented indicates sale of salts reduces water cost
SWRO	NaCl	ED/EDR, MED, crystallization	Simulation only	Energy analysis indicates NaCl production from SWRO brine 80% more efficient than from seawater
SWRO	CaCO <sub>3</sub> , MgSO <sub>4</sub> , NaCl, KCl, Li, Cl <sub>2</sub> , NaOH	NF, RO, precipitation, evaporation, ion-exchange	Proposed only	Not evaluated
BWRO, WWRO	CaCO <sub>3</sub> , CaSO <sub>4</sub> , Mg(OH) <sub>2</sub> , Na <sub>2</sub> SO <sub>4</sub> , K <sub>2</sub> Na(SO <sub>4</sub> ) <sub>2</sub>	Precipitation, RO, Evaporation	Mostly simulation, bench-scale tests conducted	Not evaluated
Thermal desal.	Na <sub>2</sub> SO <sub>4</sub> , Br <sub>2</sub> , NaCl	Eutectic freezing, crystallization, blowout tower	Simulation	Not evaluated
SWRO	Cs, Rb, In, Ge, Mg, NaCl, KCl	Evaporation, IX, solvent extraction, liquid membranes	Proposed only	Not evaluated
SWRO, BWRO	NaCl, Mg, Cl <sub>2</sub> , NaOH, CaCO <sub>3</sub>	ED/EDR, MSF, MVC precipitation, NF, MCr	Proposed only	Performed cost analysis, claim that extraction is economical
Thermal desal.	NaCl, Na <sub>2</sub> SO <sub>4</sub> , Cl <sub>2</sub> , NaOH	MED, electrolysis, eutectic freezing	Proposed only	Performed cost analysis: NaOH produced for \$149/t, \$ high capital costs
BWRO	CaSO <sub>4</sub> , Mg(OH) <sub>2</sub> , NaCl, CaCl <sub>2</sub> , Na <sub>2</sub> SO <sub>4</sub> , CaCO <sub>3</sub>	SAL-PROC process, precipitation, evaporation	Proposed only	Not evaluated
MSF	Mg, NaCl	MSF	Proposed only	Not evaluated
BWRO	CaCO <sub>3</sub>	FBC, clarification	Demonstration	Not reported
WWRO	HCl, NaOH, Cl <sub>2</sub> , P	Electrolysis, ED, IX	Lab-scale tests conducted	Not reported
WWRO	P, struvite	IX	Lab-scale tests conducted	Only calculated the potential revenue from struvite sales
SWRO	NaCl	Evaporation ponds	Full-scale	Not presented, produce food grade salt in a arrangement with a salt company
MED	NaCl	Solar evaporator	Simulation	Not evaluated
SWRO	Cl <sub>2</sub> , NaOH	Precipitation, clarification, filtration, evaporation, IX, electrolysis	Simulation	Claim that production of NaOH requires 2150 kWh/t-NaOH – unclear if this is only for electrolysis
SWNF	CaCO <sub>3</sub> , NaCl, MgSO <sub>4</sub>	NF, precipitation, MCr	Laboratory-scale study	Not evaluated



# Economic Evaluations



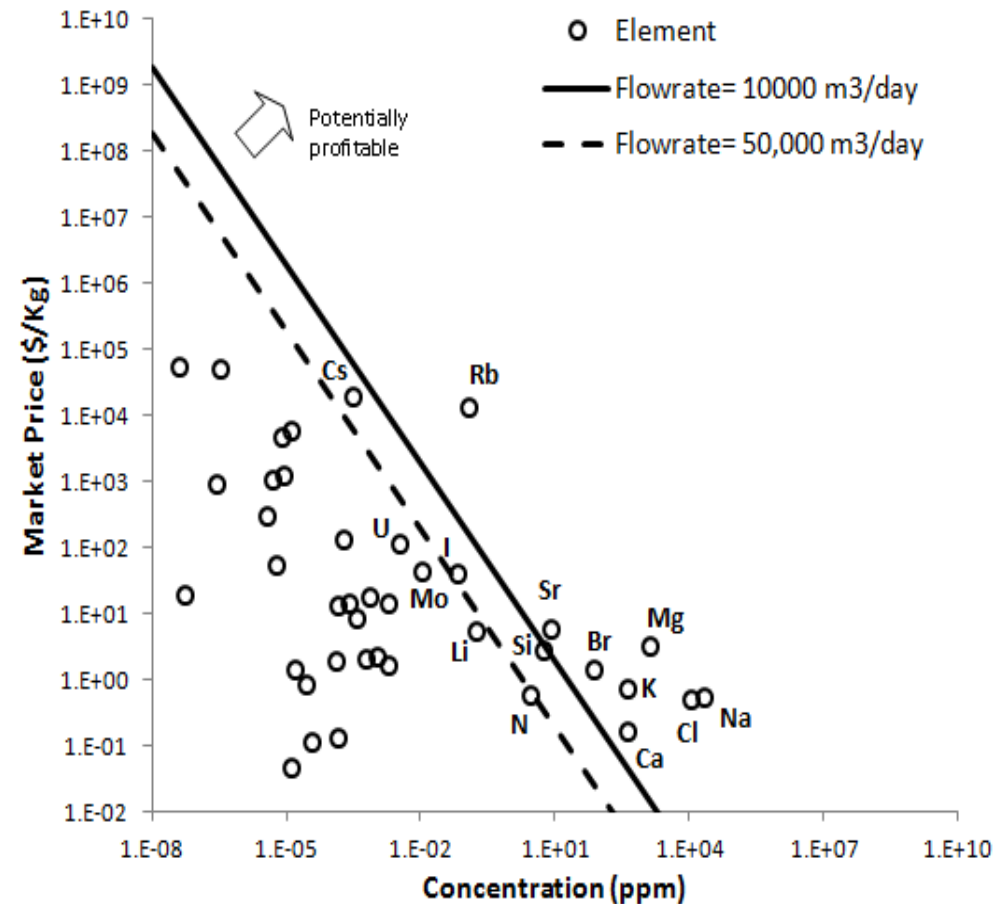
# Screening for Constituents of Interest

- USGS Mineral Commodity Summaries (and other sources when necessary) used to:
  - Obtain commodity pricing
  - Understand commodity trends and potential lucrative materials
- Concentrations of ions and metals in seawater, brackish water and wastewater compiled
- Minimum operational cost (\$33,000) used to identify salable constituents
- Potentially economically viable substances must meet the following criteria :

$$\text{Price} * \text{Concentration} * \text{Flowrate} > \text{Annual Cost}$$

# Screening for Constituents of Interest

- Indicates that Br, Ca, K, Mg, NaCl, Rb, and Sr could potentially be extracted for profit
- Other researchers have concluded that  $\text{Cl}_2$  and NaOH production feasible and lucrative
- Extraction procedures analyzed to evaluate feasibility





# Economic Evaluations – Rubidium and Strontium

- Rubidium is a valuable commodity with very low demand
- Rubidium is not traded commercially in the U.S.
- Neither rubidium or strontium commodities produced in the U.S.
- Both extremely difficult to separate and purify from aqueous solutions
- Further evaluation not performed for rubidium and strontium



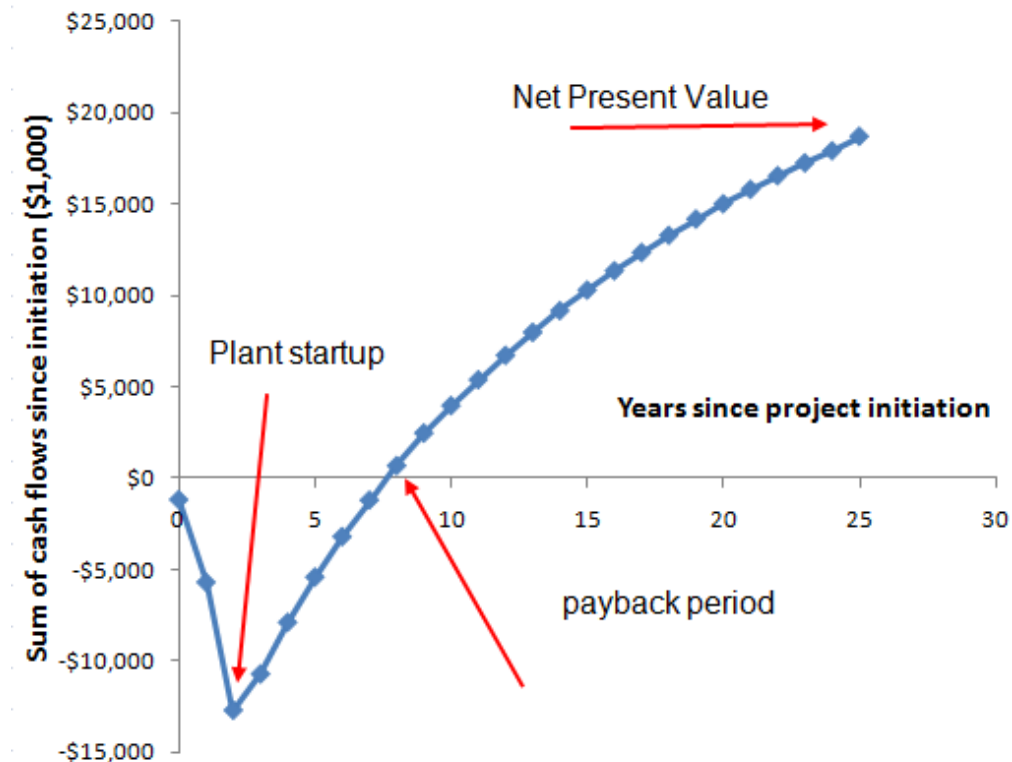
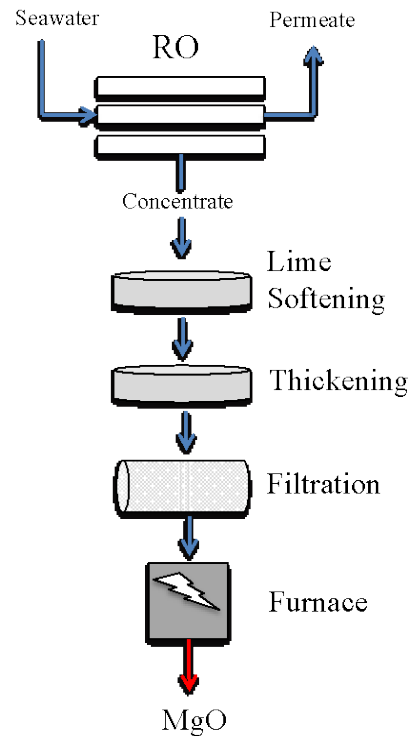
# Economic Evaluations

- Viable extraction schemes identified from literature
- Cost analysis performed for 20 MGD seawater desalination facility operating at 50% recovery
- Assumed 25-year facility lifespan, 6% interest rate and 80% extraction efficiency
- Approach assumes that local commodity market exists
- Payback period and net present value (NPV) calculated

Plant	Product	Plant efficiency (%)	Unit price (\$/metric ton)	Revenue (M\$/yr)
Mg(OH) <sub>2</sub> , Br <sub>2</sub> , NaCl	NaCl	80%	55	16.32
	Br <sub>2</sub>	80%	1390	0.49
	Mg(OH) <sub>2</sub>	80%	275	8.45
NaCl	NaCl	80%	55	16.32
MgO	MgO	80%	539	11.42
Cl <sub>2</sub> , NaOH	Cl <sub>2</sub>	80%	550	99.01
	NaOH	80%	500	101.56

# Economic Evaluations – Magnesium Oxide

- Payback period estimated at 8-years
- Net present value of \$19 million at 25-years



# Economic Evaluations – Chlorine and Sodium Hydroxide

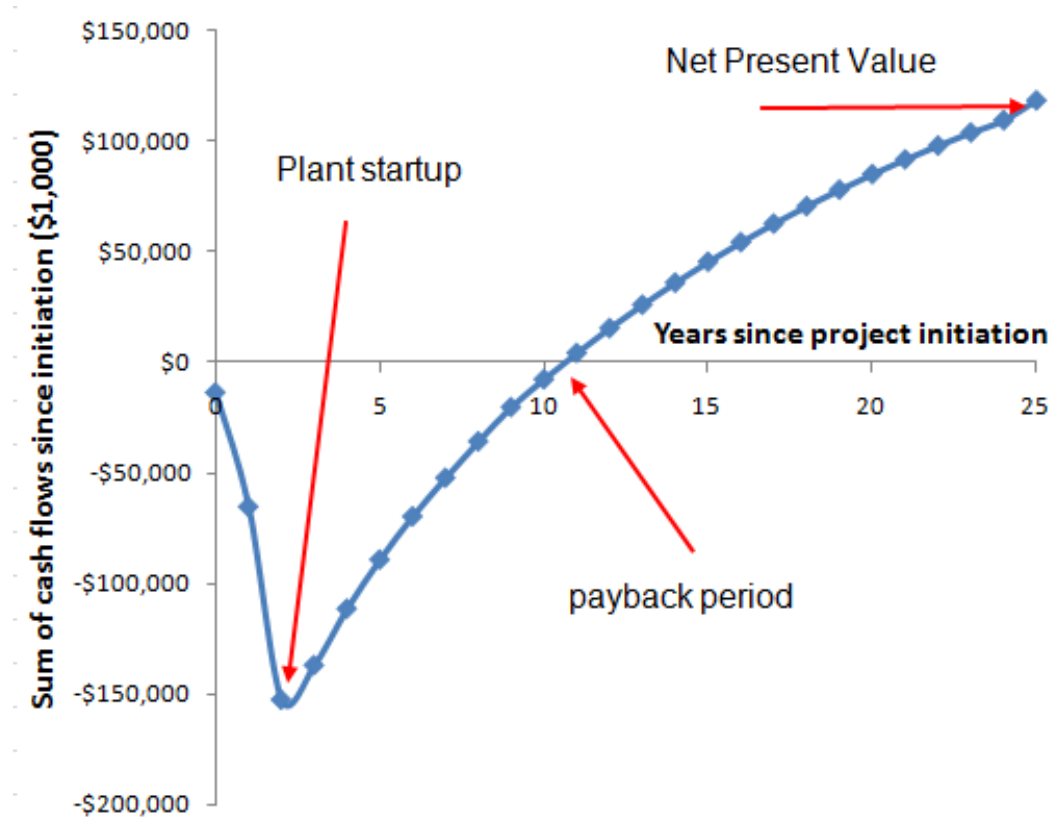
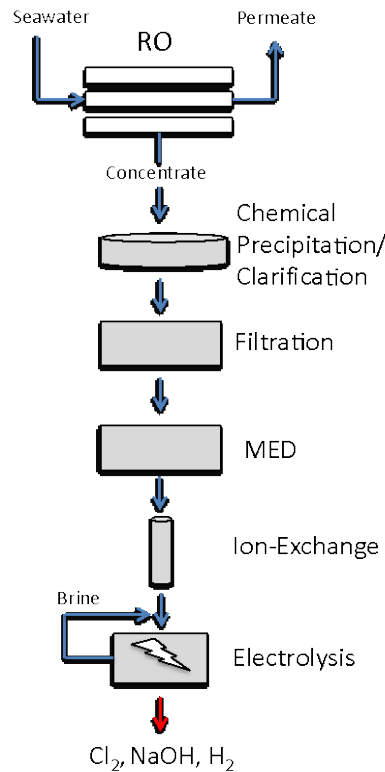
- Chlorine is produced from seawater in small quantities
- Chlorine is one of the largest production industries in the U.S.
- Chlor-alkali industry uses purified and nearly saturated sodium chloride solutions as feed stock
- Efficient electrolytic production from desalination brine would likely require significant pretreatment and concentration





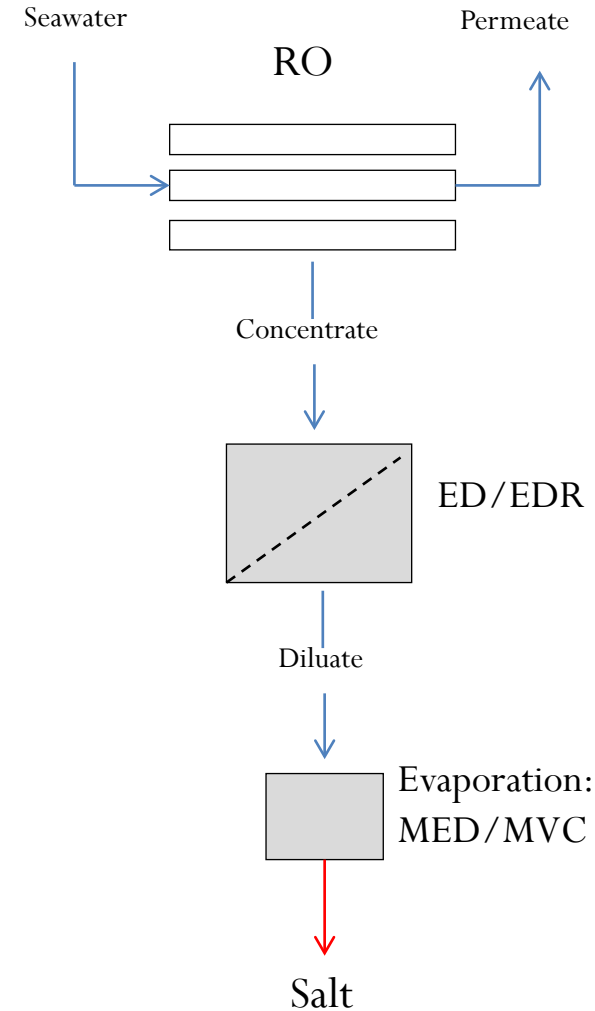
# Economic Evaluations – Chlorine and Sodium Hydroxide

- Payback period estimated at 11-years
- Net present value of \$118 million at 25-years



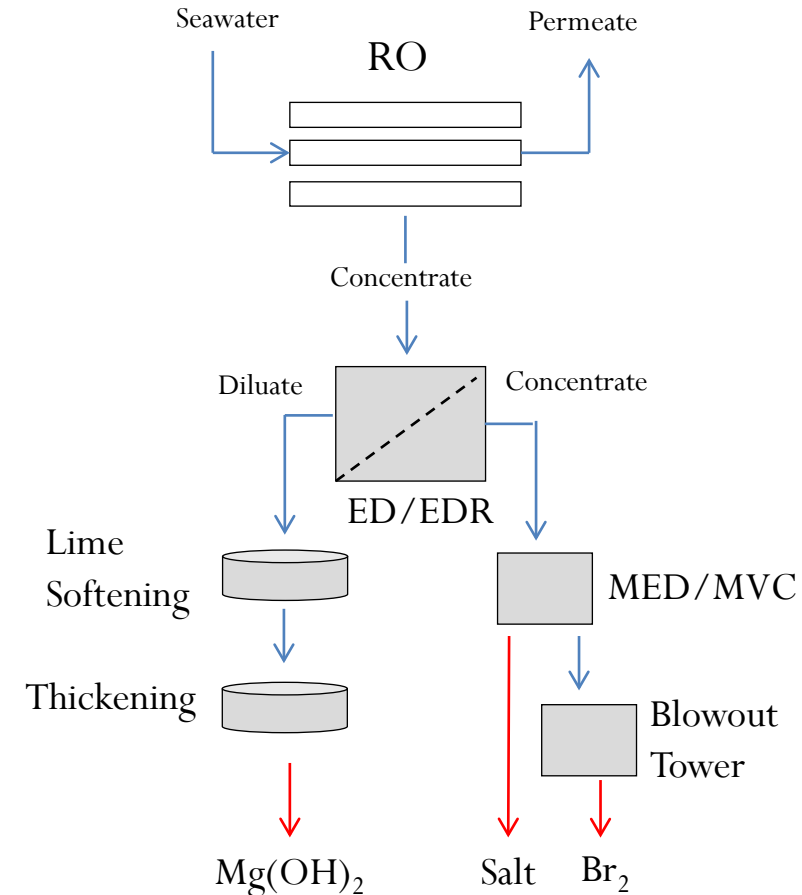
# Economic Evaluations – Sodium Chloride

- Feasibility dependent on final price of salt produced
- Economically unfeasible at solar salt price of \$55/ton
- Potentially profitable after 8-years for salt price of \$100/ton for MED scenario



# Economic Evaluations – Bromine, Magnesium, and Sodium Chloride

- Examined zero discharge desalination process developed by Thomas Davis<sup>3</sup> for simultaneous production of bromine, magnesium and sodium chloride
- Found cost of bromine extraction inhibited profit in developed scenario
- NPV analysis indicated that extraction would not be profitable



<sup>3</sup>Davis, T.A., *Zero discharge seawater desalination: Integrating the production of freshwater, salt, magnesium, and bromine, in U.S.*  
Bureau of Reclamation Research Report No. 1112006.

# Economic Evaluations – Summary

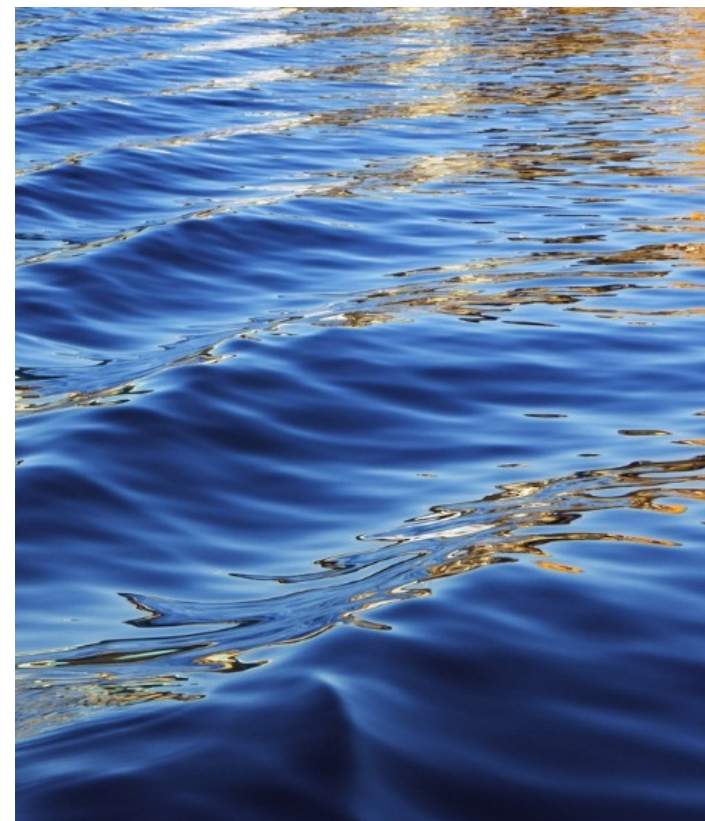
- From a profit standpoint, it appears that only the extraction of magnesia (MgO) and NaOH-Cl<sub>2</sub> feasible
- Assumes that high-purity products can be produced from desalination brine and a buyer exists

Plant	Capital Cost	O&M cost	NPV	Payback period
	(M\$)	(M\$/yr)	(M\$)	(years)
Mg(OH)-Br-Salt-MED	93	18 ~ 19	-24.7	-
Mg(OH)-Br-Salt-MVC	76	21 ~ 24	-58.3	-
NaCl-MED	84 ~ 86	6 ~ 7	-14.5	-
NaCl-MVC	64 ~ 76	12 ~ 13	-40.2	-
MgO	12	7	18.7	8
NaOH-Cl <sub>2</sub>	137	158	118.6	11





# Other Options



# Extraction to Alleviate Brine/Concentrate Disposal Issues

- Desalination brine/concentrate management is a highly divisive issue
- Extraction of valuable materials could offset costs associated with disposal
  - Allowing for higher system recoveries
  - Production of chemicals used within the plant
  - Potentially providing an additional revenue stream
- Two real world examples identified
- Several novel approaches identified



# Example 1 – Sodium Chloride

- Mekorot Water Company entered into a partnership with the Israel Salt Company to produce high-quality NaCl from the brine of seawater and brackish water RO in Eilat, Israel
- In 2007, reportedly 150,000 tons of table and industrial grade salt was produced annually from solar salt ponds
- The two parties share the cost of seawater intake pumping and maintenance
- Challenges included preventing algal growth in evaporation ponds and producing brine with ideal chemistry



## Example 2 – Calcium Carbonate

- Push towards zero liquid discharge for inland desalination benefits from production of salable materials
- Several studies evaluated secondary RO with intermediate softening<sup>4,5</sup>
- Recent Chino II Desalter (Southern California) expansion required concentrate minimization
- Designed to produce salable calcium carbonate material to reduce costs
- Results in increased overall system recovery and reduction of brine discharge costs

<sup>4</sup>Bond, R. and S. Veerapaneni, *Zero liquid discharge for inland desalination*, 2007, Black and Veatch. p. 1 - 233.

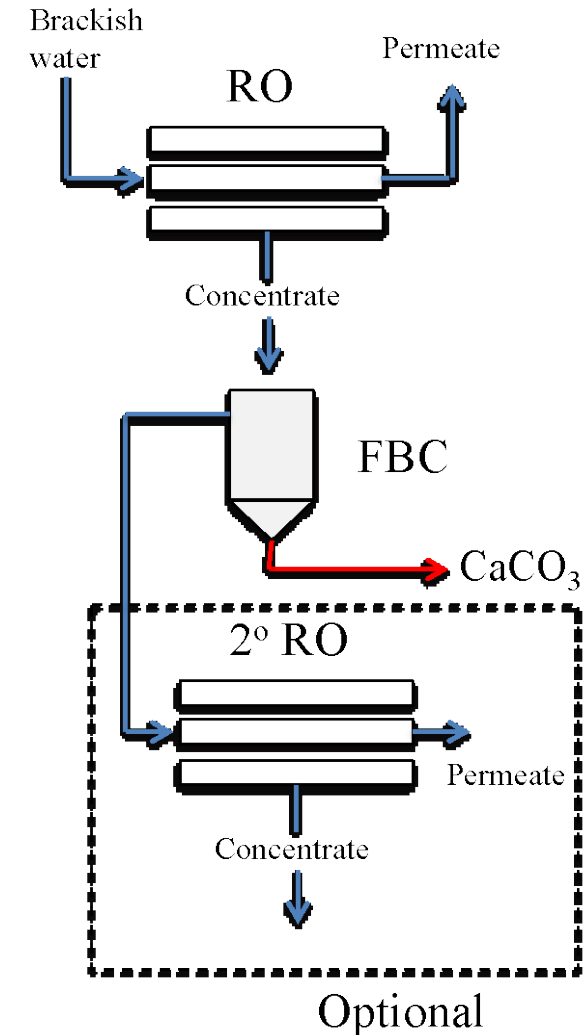
<sup>5</sup>Shih, W., Brandon Yallaly, Matthew Marshall, Don DeMichele, . *Chino II Desalter Concentrate Management Via Innovative Byproduct*. in *American Membrane Technology Association*. 2013. San Antonio, Texas.





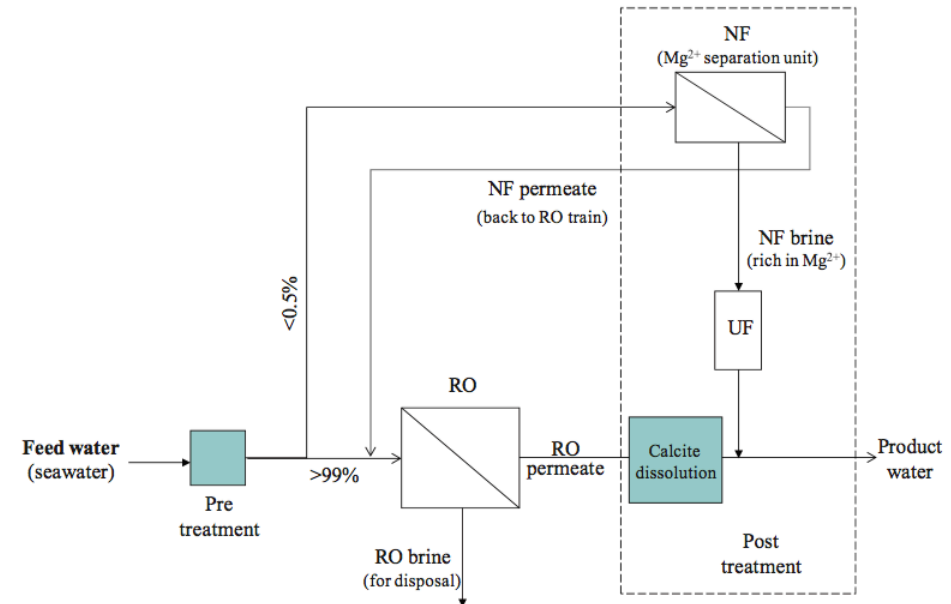
## Example 2 – Calcium Carbonate

- Economics of extraction difficult to assess due to benefits from concentrate minimization
- Scenario based on 5 MGD concentrate flow rate with 800 mg/L calcium
- Assumed  $\text{CaCO}_3$  price of \$30/ton
- Could generate ~\$130,000/yr



## Other Processes – Alternative Stabilization

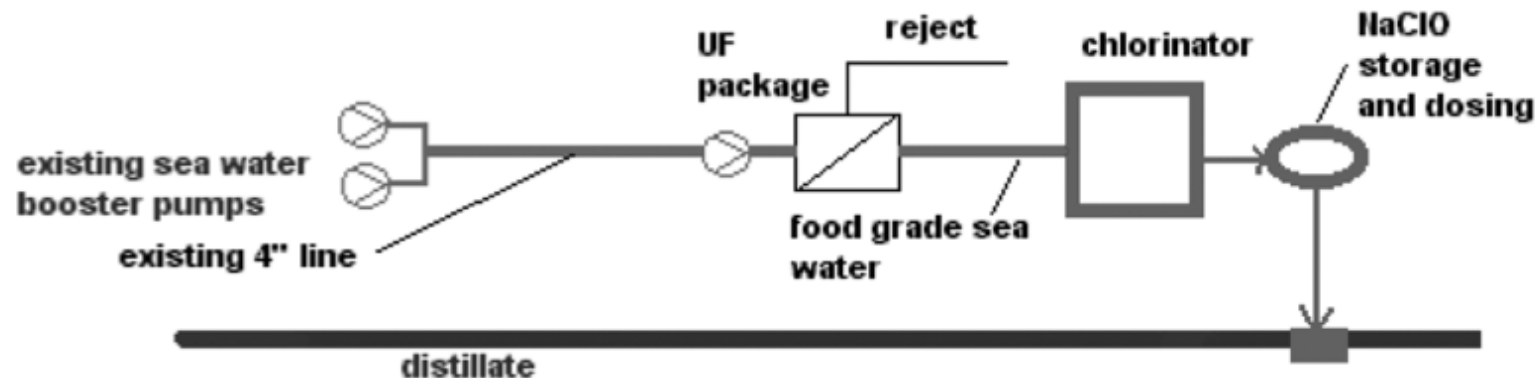
- Telzhensky et al. proposed a concept where nanofiltration would be used to separate out magnesium ions for post RO stabilization
- Alternatively, NF concentrate could be used for struvite precipitation from municipal wastewater



<sup>6</sup>Telzhensky, M., L. Birnhack, O. Lehmann, E. Windler and O. Lahav (2011). "Selective separation of seawater Mg<sup>2+</sup> ions for use in downstream water treatment processes." Chemical Engineering Journal **136**: 136-143.

## Other Processes – Chlorine Production

- Chlorine currently produced from seawater for a variety of industries
- Can be produced from seawater or desalination brine and used for finished water disinfection
- Desalination brine may not be the most effective feed stock for chlorine production
- Currently a need to evaluate cost effectiveness versus purchasing chlorine



## Other Processes – Electrodialysis Metathesis

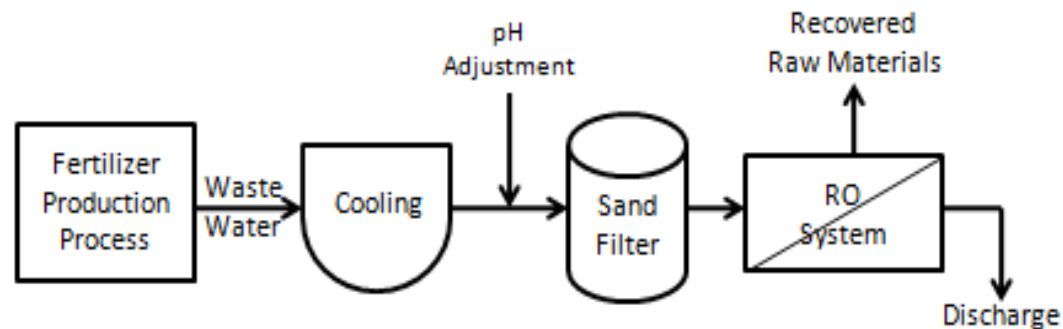
- Electrodialysis process that uses a mix of ion exchange membranes to achieve high recovery on moderately brackish water
- Produces two streams of mixed salts differing in composition
- Can purportedly sequentially precipitate minerals
- Not included in economic evaluations due to lack of specific information





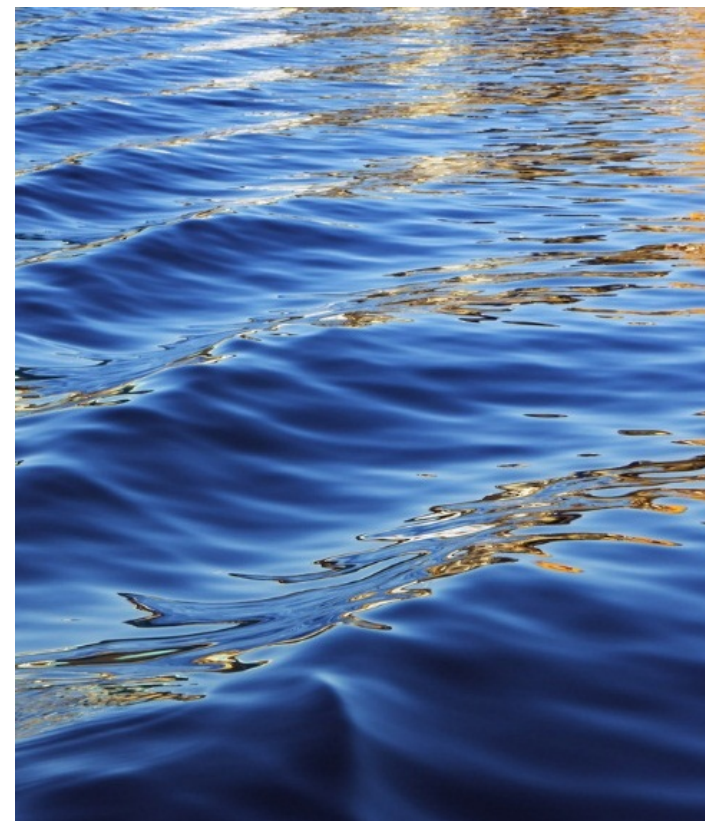
# Case Studies

- Identified a number of industries where extraction is currently being or close to being implemented:
  - Nutrient recovery from municipal waste streams
  - Utilizing membranes for improving bioethanol production
  - Copper recovery from electroplating industries
  - Amino acid recovery from fermentation broth
  - Silica recovery for geothermal brines





# Conclusions



# Conclusions

- Extraction of many materials from desalination brine is technically feasible
- Economics of extraction currently impede material recovery from seawater desalination brine
- Other factors include facility siting, product purity, staffing, safety, material handling and storage
- Push towards inland desalination increasing research on and application of material extraction approaches and technologies



# Research Needs

- One of the main findings of this study was that although a significant amount of extraction research has been performed, very little demonstration-scale research has been performed
- There is a clear need to evaluate not only the technical and economic feasibility of extraction schemes, but also product purity, process efficiency, life cycle costs, and the real benefits of incorporating an extraction scheme into desalination





# Project Report

- This presentation provided a summary of major findings
- The final report was written to be a resource for anyone interested in the extraction of materials from aqueous solutions
- The report includes an in-depth analysis of research conducted towards the extraction of a wide variety of elements and compounds

# Acknowledgements

- WateReuse Research Foundation
- Bureau of Reclamation
- Joon Min, PhD – BKT
- Liyan Jin, PhD – BKT
- Arash Shahmansouri – Clarkson
- Ashley Waldron – Clarkson

# Questions

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# Upcoming Events

- November 13, 2014

## **Enhancing the Soil Aquifer Treatment Process for Potable Reuse**

- December 11, 2014

## **Formation of Nitrosamines and Perfluorochemicals during Ozonation in Water Reuse Applications**

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