



Low-Cost Treatment Technologies for Small-Scale Water Reclamation Plants

WateReuse Research Foundation

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About the WateReuse Research Foundation

The mission of the WateReuse Research Foundation is to conduct and promote applied research on the reclamation, recycling, reuse, and desalination of water. The Foundation's research advances the science of water reuse and supports communities across the United States and abroad in their efforts to create new sources of high quality water through reclamation, recycling, reuse, and desalination while protecting public health and the environment.

The Foundation sponsors research on all aspects of water reuse, including emerging chemical contaminants, microbiological agents, treatment technologies, salinity management and desalination, public perception and acceptance, economics, and marketing. The Foundation's research informs the public of the safety of reclaimed water and provides water professionals with the tools and knowledge to meet their commitment of increasing reliability and quality.

The Foundation's funding partners include the Bureau of Reclamation, the California State Water Resources Control Board, the California Energy Commission, and the California Department of Water Resources. Funding is also provided by the Foundation's Subscribers, water and wastewater agencies, and other interested organizations.

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Andrew Salveson
Carollo Engineers, P.C.

Zhi Zhou
Carollo Engineers, P.C.

Brad A. Finney
Humboldt State University

Mary Burke
Humboldt State University

Jong Chan Ly
Humboldt State University

Cosponsor
Bureau of Reclamation



WateReuse Research Foundation
Alexandria, VA

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For more information, contact:

WateReuse Research Foundation
1199 North Fairfax Street, Suite 410
Alexandria, VA 22314
703-548-0880
703-548-5085 (fax)
www.WateReuse.org/Foundation

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CONTENTS

List of Figures	vii
List of Tables.....	ix
List of Acronyms.....	x
Foreword.....	xi
Acknowledgments	xii
Executive Summary	xv
 Chapter 1. Introduction	1
 Chapter 2. Reclaimed Water Regulations and Uses	3
 Chapter 3. Treatment Process Overview	5
3.1 Identification of Treatment Processes and Package Systems.....	5
3.2 Conventional Customized Plants	6
3.2.1 Activated Sludge	6
3.2.2 Extended Aeration.....	7
3.2.3 Biological Nutrient Removal (BNR) Processes	7
3.2.4 Trickling Filter and RBCs	7
3.3 Conventional Package Plants	7
3.3.1 Activated Sludge Package Plant.....	7
3.3.2 SBR	8
3.3.3 OD	9
3.3.4 Biological Filtration	9
3.4 Membrane Customized Plants	10
3.5 Natural Systems	11
3.6 Alternative Treatment Systems.....	12
 Chapter 4. Cost Analysis	15
4.1 Data Gathering and Processing.....	15
4.1.1 Data Sources.....	15
4.1.2 Cost Factors.....	18
4.1.3 Filtration and Disinfection.....	19
4.1.4 Normalization of Data	20
4.2 Comparisons of Treatment Processes and Package Systems	22
4.2.1 General Trend of Construction Costs and Capacities.....	22
4.2.2 Unit Construction Cost–Capacity Curves of Selected Processes	24
4.2.3 Comparison of Unit Construction Costs.....	31
4.2.4 General Trend of O&M Costs and Capacities	34
4.2.5 Comparison of Unit O&M Costs.....	36

4.2.6	Comparison of Unit Present Value Costs	38
4.2.7	Comparison of Effluent Water Quality.....	41
Chapter 5. The WAWTTAR Model.....		43
5.1	Introduction to WAWTTAR	43
5.2	WAWTTAR Components.....	44
5.3	WAWTTAR Operation.....	45
5.4	WAWTTAR Output.....	46
5.5	WAWTTAR Application	47
5.6	Incorporating New Treatment Process Cost Data into WAWTTAR	47
Chapter 6. Conclusions		49
References.....		51
Appendices		
Appendix A.	Summarized State Guidelines and Regulations for Reclaimed Water	53
Appendix B.	Websites of State Guidelines and Regulations for Reclaimed Water	62
Appendix C.	Uses of Reclaimed Water in Selected States.....	65
Appendix D.	Suggested Guidelines for Water Reuse by USEPA and USAID	82
Appendix E.	Recommended Limits for Constituents in Reclaimed Water for Irrigation by USEPA and USAID	88
Appendix F.	Recommended Minimum Verification Monitoring of Microbial Performance Targets for Wastewater and Excreta Use in Agriculture and Aquaculture by the WHO	90
Appendix G.	Regulations for Operator Certification in California	91
Appendix H.	Additional Alternative Treatment Systems.....	107
Appendix I.	Utility Survey.....	109
Appendix J.	Data.....	114

FIGURES

3.1	Flow diagram of conventional activated sludge system	6
3.2	Sample picture of an aeration tank in an activated sludge system	6
3.3	Flow diagram of SBR system.....	8
3.4	SBR system by Siemens (OMNIFLO)	8
3.5	Process flow diagram of OD.	9
3.6	Multichannel OD by U.S. Filter (Siemens)	9
3.7	AdvanTex system by Orenco Systems, Inc.	10
3.8	Process flow diagram of MBR	10
3.9	Sample pictures of MBR systems.....	11
3.10	Constructed wetland system for Arcata, CA	12
3.11	Flow chart of a sample LM	13
4.1	Locations of surveyed plants and systems in the U.S.....	15
4.2	Capacities of surveyed plants	16
4.3	Data type of surveyed plants	17
4.4	Construction dates of surveyed plants	17
4.5	Open-channel UV disinfection system by Trojan Technologies.....	20
4.6	Total construction costs.....	23
4.7	Unit construction costs	23
4.8	Raw data of unit construction costs.....	24
4.9	Unit construction costs of activated sludge plants.....	25
4.10	Unit construction costs of extended aeration plants	25
4.11	Unit construction costs of Bardenpho plants.....	26
4.12	Unit construction costs of MLE plants	26
4.13	Unit construction costs of ICEAS plants	27
4.14	Unit construction costs of package plants	27
4.15	Unit construction costs of SBR plants	28
4.16	Unit construction costs of ODs.....	28
4.17	Unit construction costs of MBRs	29
4.18	Unit construction costs of ponds	29
4.19	Unit construction costs of lagoons	30
4.20	Unit construction costs of wetlands.....	30
4.21	Unit construction costs of LMs	31
4.22	Comparison of unit construction costs of conventional customized plants and conventional package plants	32

4.23	Comparison of unit construction costs of conventional customized plants and membrane customized plants	32
4.24	Comparison of unit construction costs of conventional customized plants and natural systems	33
4.25	Comparison of unit construction costs of conventional customized plants and alternative treatment systems	33
4.26	Comparison of unit construction costs of membrane customized plants and alternative treatment systems.....	34
4.27	Total annual O&M costs	35
4.28	Unit O&M costs	35
4.29	Comparison of unit O&M costs of conventional customized plants and conventional package plants	36
4.30	Comparison of unit O&M costs of conventional customized plants and membrane customized systems	37
4.31	Comparison of unit O&M costs of conventional customized plants and natural systems	37
4.32	Comparison of unit O&M costs of conventional customized plants and alternative treatment systems.....	38
4.33	Comparison of unit present value costs of conventional customized plants and conventional package plants	39
4.34	Comparison of unit present value costs of conventional customized plants and membrane customized plants	39
4.35	Comparison of unit present value costs of conventional customized plants and natural systems	40
4.36	Comparison of unit present value costs of conventional customized plants and alternative treatment systems	40
4.37	Comparison of effluent water quality.....	41
4.38	Detailed comparison of effluent water quality of each subcategory	41
4.39	Comparison of removal efficiency	42
4.40	Detailed comparison of removal efficiency of each subcategory.....	42
5.1	Screening process used to identify feasible treatment trains in WAWTTAR	46

TABLES

2.1	Summary of Most Stringent Regulations for Reclaimed Water in Each Surveyed State.....	4
3.1	Categories of Treatment Trains and Processes.....	5
4.1	Levels of Engineering Accuracy for Cost Estimation	18

ACRONYMS

A/O	Anaerobic/aerobic
A2/O	Anaerobic/anoxic/aerobic
AS	Activated sludge
BNR	Biological nutrient removal
BOD	Biochemical oxygen demand
CCI	Construction cost index
COD	Chemical oxygen demand
ENR	Engineering News Record
HAAs	Heterocyclic aromatic amines
ICEAS	Intermittent cycle extended aeration system
HRT	Hydraulic retention time
IFAS	Integrated fixed film activated sludge
LM	Living Machine®
MBBR	Moving bed biological reactor
MBR	Membrane bioreactor
MF	Microfiltration
mgd	Millions of gallons per day
MLE	Modified Ludzak-Ettinger
MPN	Most probable number
Schreiber N&D	Schreiber nitrification and denitrification system
NPDES	National Pollutant Discharge Elimination System
NTU	Nephelometric turbidity unit
O&M	Operation and maintenance
OD	Oxidation ditch
RBC	Rotating biological contactor
RO	Reverse osmosis
SBR	Sequencing batch reactor
TDS	Total dissolved solids
SRT	Solid retention time
THMs	Trihalomethanes
TMDL	Total maximum daily loads
TN	Total nitrogen
TOC	Total organic carbon
TOX	Total organic halogen
TP	Total phosphorus
TSS	Total suspended solids
UF	Ultrafiltration
USAID	U.S. Agency for International Development
USEPA	U.S. Environmental Protection Agency
UV	Ultraviolet
WAWTTAR	Water and Wastewater Treatment Technologies Appropriate for Reuse
WHO	World Health Organization

FOREWORD

The WateReuse Research Foundation, a nonprofit corporation, sponsors research that advances the science of water reclamation, recycling, reuse, and desalination. The Foundation funds projects that meet the water reuse and desalination research needs of water and wastewater agencies and the public. The goal of the Foundation's research is to ensure that water reuse and desalination projects provide high-quality water, protect public health, and improve the environment.

An Operating Plan guides the Foundation's research program. Under the plan, a research agenda of high-priority topics is maintained. The agenda is developed in cooperation with the water reuse and desalination communities including water professionals, academics, and Foundation Subscribers. The Foundation's research focuses on a broad range of water reuse research topics including:

- Defining and addressing emerging contaminants;
- Public perceptions of the benefits and risks of water reuse;
- Management practices related to indirect potable reuse;
- Groundwater recharge and aquifer storage and recovery;
- Evaluation and methods for managing salinity and desalination; and
- Economics and marketing of water reuse.

The Operating Plan outlines the role of the Foundation's Research Advisory Committee (RAC), Project Advisory Committees (PACs), and Foundation staff. The RAC sets priorities, recommends projects for funding, and provides advice and recommendations on the Foundation's research agenda and other related efforts. PACs are convened for each project and provide technical review and oversight. The Foundation's RAC and PACs consist of experts in their fields and provide the Foundation with an independent review, which ensures the credibility of the Foundation's research results. The Foundation's Project Managers facilitate the efforts of the RAC and PACs and provide overall management of projects.

The Foundation's primary funding partners include the Bureau of Reclamation, California State Water Resources Control Board, the California Energy Commission, Foundation Subscribers, water and wastewater agencies, and other interested organizations. The Foundation leverages its financial and intellectual capital through these partnerships and funding relationships.

This study identifies and evaluates established and innovative technologies that provide treatment of flows of less than 1 million gal per day. A range of conventional treatment processes, innovative treatment processes, and package systems were evaluated as part of this project. The primary value of this work is the extensive cost database, where the cost and operation data from existing small-scale wastewater treatment and water reuse facilities have been gathered and synthesized.

David L. Moore
Chair
WateReuse Research Foundation

G. Wade Miller
Executive Director
WateReuse Research Foundation

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Principal Investigator

Andrew T. Salveson, *P.E., Carollo Engineers, P.C.*

Co-Principal Investigator

Brad A. Finney, *Ph.D., Humboldt State University*

Research Project Team

Dr. Zhi Zhou, *Carollo Engineers, P.C.*

Rod Reardon, *Carollo Engineers, P.C.*

Lisa Prieto, *formerly of Camp Dresser & McKee Inc.*

Dr. Robert Gearheart, *Humboldt State University*

Mary Burke, *Humboldt State University*

Jong Chan Ly, *Humboldt State University*

Dr. Kara L. Nelson, *University of California, Berkeley*

Contributors

Bill Vineyard, *ABP Engineers Inc.*

Patrick Bollman, *Aquionics*

Alan Rimer, *Black & Veatch*

Michael Shafer, *Black & Veatch*

Allan Briggs, *Carollo Engineers, P.C.*

Aniruddha Bhagwat, *Carollo Engineers, P.C.*

Courtney Eaton, *Carollo Engineers, P.C.*

Lori Kennedy, *Carollo Engineers, P.C.*

Lydia Holmes, *Carollo Engineers, P.C.*

Nitin Goel, *Carollo Engineers, P.C.*

Rick Chan, *Carollo Engineers, P.C.*

Roderick D. Reardon, *Carollo Engineers, P.C.*

Steve Swanback, *Carollo Engineers, P.C.*

Ted Downen, *Carollo Engineers, P.C.*

Jamie McCullough, *City of El Mirage*

Scott Hamby, *City of Scotts Valley*

Lew Nelson, *City of Tulare*

Kathleen Carroll, *City of Yuma*

Frank Ferguson, *Curriculum Associates*

Tony Giordano, *Curriculum Associates*

Dennis Livingston, *Enviroquip, Inc.*

Andrew Ball, *Enviroquip, Inc.*

Paul Schuler, *GE Water and Process Technologies (Zenon)*

Steven Mullerheim, *Great Circle Water*

Matthias Boeker, *ITT Wedeco, Inc.*
Brenda Osterhaug, *King County*
Susan McDonough, *Lakeside Equipment Corporation*
Donald L. Safrit, *McKim & Creed*
Chris Shuster, *Miller-Leaman Inc.*
Michael Tooley, *MISCO*
Sandy Clarke, *MISCO*
Olivenhain Municipal Water District
Tristian Bounds, *Orenco Inc.*
Darrell Fitzpatrick, *Parks Canada*
Bruce Coyle, *Paulding County*
R. Wayne Ramey, *Ramey Environmental Compliance, Inc.*
Joseph Zuback, *Siemens Water Technologies Corporation*
Robert F. Newton, *Siemens Water Technologies Corporation*
Wayne Lem, *Trojan Technologies*
Aaron Winer, *Veolia Water North America*
Craig L. Riley, *Washington State Department of Health*
Brian Walker, *Water and Wastewater Services*
Robert Scott, *Water's Edge Resort*
David Boucher, *WhiteWater Inc.*

Project Managers

Caroline Sherony, *WateReuse Research Foundation*
Joshua M. Dickinson, *WateReuse Research Foundation*

Project Advisory Committee

Shane Trussell, *Trussell Technologies, Inc.*
James R. Mihelcic, *University of South Florida*
Yuliana Porras, *Bureau of Reclamation*
Alan Rimer, *Black & Veatch*

EXECUTIVE SUMMARY

The shortage of freshwater is a severe problem for many areas of the world. Water reclamation and reuse provide promising opportunities to ease freshwater shortage problems. However, data and technical information for low-cost treatment technologies for small-scale water reuse projects are often unavailable, especially to communities with limited financial and technical resources in rural areas and in developing countries.

In response to this need, this study identifies and evaluates established and innovative technologies that provide treatment of flows of less than 1 million gal per day. A range of conventional treatment processes, innovative treatment processes, and package systems were evaluated as part of this project. The primary value of this work is the extensive cost database, where the cost and operation data from existing small-scale wastewater treatment and water reuse facilities have been gathered and synthesized. From these data, the costs and maintenance issues for the various types of treatment technology are compared and contrasted.

The selection of small-scale reclamation systems will depend on many factors, such as regulations, availability of land, the budget, and trained staff. Based on the results of this project, natural systems (ponds plus wetlands) are the best economic alternative for small communities if inexpensive land is available and if effluent water quality can satisfy the local regulations. If high water quality is desired and a budget is available, nonmembrane systems can be used. Membrane-based systems can be used if even higher water quality is needed and if the budget allows.

The results from this project have been incorporated into the Water and Wastewater Treatment Technologies Appropriate for Reuse (WAWTTAR) model for dissemination to rural communities and developing countries. The WAWTTAR model is available on the Internet for download at no cost and can be found at <http://firehole.humboldt.edu/wawttar/>.

Please note that this is not a comprehensive list of treatment technologies or systems that could be used for treatment of wastewater to reclaimed standards, as it represents the data that could be gathered within the time frame and budget of this project.

CHAPTER 1

INTRODUCTION

The shortage of freshwater is a severe problem for many areas of the world. Water reclamation and reuse provide promising opportunities to ease freshwater shortages. Satellite and small-scale reclamation has become synonymous with membrane bioreactors (MBRs). While MBRs produce a high-quality effluent, they also come at a high capital cost. Rural communities often don't have engineering or operation staff experienced in advanced membrane treatment. Further, the high quality of MBR effluent is not required for most applications. Many utilities are now looking for the optimal balance between effluent quality and cost to maximize reclamation efforts. However, data and technical information for treatment technologies for small-scale water reuse projects are often unavailable, especially to communities with limited financial and technical resources in rural areas and in developing countries.

In response to this need, the WateReuse Research Foundation (WRF) contracted Carollo Engineers and Humboldt State University to lead "Low-Cost Treatment Technologies for Small-Scale Water Reclamation Plants", WRF-06-008. The main goal of this study is to identify and evaluate established and innovative technologies that provide economical treatment for flows of fewer than 1 million gal per day (mgd). A range of conventional treatment processes, innovative unit treatment processes, and package systems were evaluated. The cost and operability data from existing small-scale water reuse facilities have been gathered and synthesized. From this analysis, the costs and maintenance issues for the various types of treatment technologies are compared and contrasted.

Specific objectives of this project included the following:

- Identify a range of conventional and innovative unit treatment processes and package systems to be evaluated.
- Gather and synthesize cost and operability data from existing small-scale (<1 mgd) wastewater treatment and water reuse facilities.
- Incorporate the results into the Water and Wastewater Treatment Technologies Appropriate for Reuse (WAWTTAR) model for dissemination to rural and developing countries. The WAWTTAR model (<http://firehole.humboldt.edu/wawttar/>) is available on the Internet for download at no cost.

The results can help identify treatment trains suitable for small-scale operation that will minimize capital, operating, and maintenance costs; minimize staffing requirements through automation and simplicity of operation; minimize waste streams while maintaining high product water quality; and be utilized by communities with limited financial and technical resources in rural areas and developing countries.

CHAPTER 2

RECLAIMED WATER REGULATIONS AND USES

The reclaimed water regulations and uses have been summarized at the state level, national level, and international level. These regulations and uses, included in Appendices A to F and in the WAWTTAR model, are the baseline of what level of treatment is required for a particular application. There is no need, for example, to go to the expense of an MBR when a particular application does not require filtration and may require only 23 MPN of coliform per 100 mL of effluent. Thus, the reader is encouraged to use the regulatory summaries in this document to define the minimum acceptable water quality criteria and then to review the data from this report with those criteria in mind when selecting potential treatment systems.

At the state level, the guidelines and regulations for reclaimed water in 34 states in the United States are summarized in Appendix A. A summary of the most stringent regulations for reclaimed water in each surveyed state is shown in Table 2.1, which is sorted by the stringency of disinfection requirements and treatment requirements. Details can be found in Appendix A. The guidelines and regulations for reclaimed water of the other 16 states in the United States are not available as of December 2008. The titles and websites for the guidelines and regulations and related environmental protection departments in other states are listed in Appendix B. The uses of reclaimed water in 12 states in the United States are summarized in Appendix C. All of the information presented is considered current as of December 2008. The uses of reclaimed water govern the effluent quality, with some states such as California having an extensive list of uses, water quality standards, and treatment technologies that are proven to meet the effluent quality standards.

At the national level, the U.S. Environmental Protection Agency (USEPA) and U.S. Agency for International Development (USAID) published a report, EPA/625/R-04/108 (Guidelines, 2004), that summarized reclaimed water regulations and uses through 2002. This information is listed in Appendix D and Appendix E.

At the international level, the World Health Organization (WHO) guidelines of microbial performance targets for wastewater and excreta use in agriculture and aquaculture are shown in Appendix F.

While this project does not evaluate the relative public health impacts of using the different indicator organisms and disinfection targets, it is worth noting that there are substantial differences among some states. Many states have limited regulations or guidelines with limited categories of water reuse, such as crop and turf irrigation. Some states use fecal coliform as an indicator organism, and other states (such as California) use a more inclusive indicator: total coliform, which is about 10 times more sensitive than fecal coliform. In some cases, a subset of fecal coliform, *Escherichia coli*, is used as an indicator organism.

One further regulatory item must be considered for reclaimed water treatment: the training and certification requirements of operations staff. Should a utility, for example, convert from a natural system to an MBR, such a facility may be required to find or train staff to the appropriate level prior to operation. The example of operator regulations in California is included as Appendix G.

Table 2.1. Summary of Most Stringent Regulations for Reclaimed Water in Each Surveyed State^a

State	Indicator Organism(s)	Disinfection Requirements (per 100 mL)	Turbidity (NTU)	Nitrogen (mg/L)	TSS (mg/L)	BOD ₅ (mg/L)
Utah	<i>E. coli</i>	ND (daily), < 9	< 2		< 5	< 10
Massachusetts	fecal coliform	ND (7 days), < 14	<= 2	< 10	< 5	<= 10
Indiana	fecal coliform	ND, < 14			< 5	< 10
Florida	fecal coliform	ND		< 10	< 5	< 20
Colorado	<i>E. coli</i>	ND in 75% of samples	<= 3		< 30	
Arizona	fecal coliform	ND in 4 of last 7 samples	<= 2	< 10		
Alabama	total coliform	< 1		< 10		
Nevada	total coliform	< 2.2				
New Jersey	fecal coliform	< 2.2		< 10	< 5	
Vermont	<i>E. coli</i>	< 2.2	< 2	< 5	< 5	< 10
California	total coliform	< 2.2	< 2 or < 0.2			
Washington	total coliform	< 2.2	<= 2		< 30	< 30
Wyoming	fecal coliform	< 2.2				
Oregon	total coliform	< 2.2	< 2			
Idaho	total coliform	< 2.2				
Hawaii	fecal coliform	< 2.2				
Maryland	fecal coliform	< 3			< 10	< 10
New Mexico	fecal coliform	< 5		< 3		< 10
Virginia	fecal coliform, <i>E. coli</i> , enterococci	<= 14; <= 11; <= 11		< 2		<= 10
N. Carolina	fecal coliform	<= 14		<= 4	<= 5	<= 10
Texas	fecal coliform	< 20		< 3		< 5
Delaware	fecal coliform	< 20		< 5		< 10
Georgia	fecal coliform	< 23		<= 3		< 5
Montana	fecal coliform	< 23				< 10
Ohio	fecal coliform	< 23				< 10
South Carolina	fecal coliform	< 200			< 5	< 5
North Dakota	fecal coliform	< 200			< 30	< 25
Tennessee	fecal coliform	< 200			<= 30	
Nebraska	fecal coliform	< 200				
Missouri	fecal coliform	< 200				
South Dakota	total coliform	< 200				
Alaska					< 30	< 30
Wisconsin				< 10		< 50

^aND: not detected. TSS: total suspended solids. BOD₅: 5-day biochemical oxygen demand.

CHAPTER 3

TREATMENT PROCESS OVERVIEW

3.1. IDENTIFICATION OF TREATMENT PROCESSES AND PACKAGE SYSTEMS

The treatment trains reviewed for this project include a range of conventional, advanced, and alternative technologies. Two types of engineering approaches are included in this analysis, one being the use of pre-engineered “package” plants and the other being that of nonpackage “customized” plants. As shown in Table 3.1, there are five subcategories of treatment plants evaluated as part of this project: A) conventional (nonmembrane) customized plants, B) conventional package plants, C) membrane customized plants, D) natural systems, and E) alternative treatment systems. Some limited descriptions of the predominant treatment processes compiled for this project are also included here. The lack of inclusion of specific technologies within this report is based upon a lack of collected information on such technologies by the project team and does not reflect a negative judgment on those technologies.

Table 3.1. Categories of Treatment Trains and Processes

Treatment Trains	Processes
A) Conventional Customized Plants	A.1) conventional activated sludge (AS) A.2) extended aeration A.3) intermittent aeration A.4) anaerobic/aerobic (A/O) A.5) anaerobic/anoxic/aerobic (A2/O) A.6) Bardenpho A.7) biological nutrient removal (BNR) A.8) modified Ludzak-Ettinger (MLE) A.9) Schreiber nitrification and denitrification (Schreiber N&D) A.10) in-channel denitrification A.11) intermittent cycle extended aeration system (ICEAS) A.12) trickling filter A.13) rotating biological contactor (RBC)
B) Conventional Package Plants	B.1) activated sludge package plants B.2) sequencing batch reactor (SBR) B.3) oxidation ditches (ODs) B.4) biological filtration
C) Membrane Customized Plants	C.1) MBR
D) Natural Systems	D.1) pond D.2) lagoon D.3) constructed wetland
E) Alternative Treatment Systems	E.1) living machines (LMs)

3.2. CONVENTIONAL CUSTOMIZED PLANTS

Most conventional customized processes are developed based on the conventional activated sludge process and modified for specific purposes such as nutrient removal. Details of subcategories of conventional customized plants are discussed in the following section.

3.2.1 Activated Sludge

The flow diagram of a typical activated sludge system is shown in Figure 3.1. Figure 3.2 is a picture of an aeration tank in an activated sludge system.

The activated sludge process was first discovered in 1914 (Ritmann and McCarty, 2001). The activated sludge process is a biological wastewater treatment method in which the organic matter in raw wastewater is degraded by dispersed microorganisms. The microorganisms and flocs are called activated sludge. Usually a primary settling process separates solids from raw wastewater before the secondary activated sludge treatment. In the secondary activated sludge treatment process, activated sludge recycles between the aeration tank and the secondary clarifier to control the solid retention time (SRT) in the aeration tank. After sedimentation, the clear effluent is discharged from the top of the secondary clarifier. The activated sludge process is widely used for the treatment of municipal and industrial wastewater (Ritmann and McCarty, 2001).

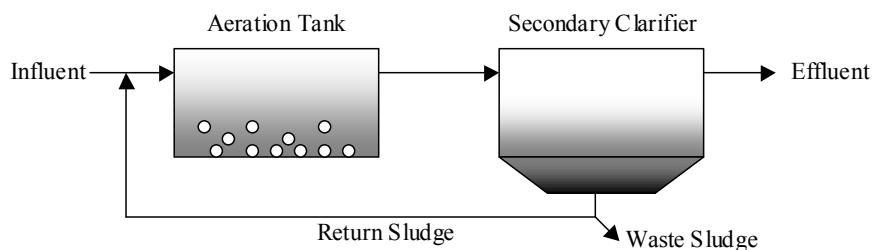


Figure 3.1. Flow diagram of conventional activated sludge system.



Figure 3.2. Sample picture of an aeration tank in an activated sludge system.

3.2.2 Extended Aeration

An extended aeration process is a modification of activated sludge process without primary settling and longer aeration time. Compared to a conventional activated sludge process, an extended aeration process has a higher biochemical oxygen demand removal efficiency and generates less sludge. However, the long aeration time means larger basins due to a long hydraulic residence time (HRT).

3.2.3 Biological Nutrient Reduction (BNR) Processes

Nutrient removal processes such as nitrogen removal and phosphorus removal can be added to the conventional activated sludge process. Nitrogen removal includes nitrification and denitrification. The nitrification process converts ammonia to nitrite and finally to nitrate. Nitrification lowers concentrations of ammonia in wastewater, a substance toxic to aquatic organisms, and controls eutrophication as well (Tchobanoglous et al., 2003). Denitrification includes the reduction of nitrate to nitric oxide, nitrous oxide, and nitrogen gas. Nitrogen removal is important for the protection of surface discharge and groundwater recharge (Tchobanoglous et al., 2003).

Various processes have been developed for BNR, such as intermittent aeration, anaerobic/aerobic (A/O), Bardenpho, modified Ludzak-Ettinger (MLE), Schreiber nitrification and denitrification (N&D), in-channel denitrification, and intermittent cycle extended aeration systems (ICEASs).

3.2.4 Trickling Filter and RBCs

Both rotating biological contractors (RBCs) and trickling filters develop a large biofilm surface and rely on mass transfer of oxygen from bulk liquids to the biofilm (Tchobanoglous et al., 2003).

An RBC consists of a series of closely spaced circular disks that are submerged in wastewater and rotating through it. These disks support the growth of microorganisms for biological degradation of wastewater. The advantages of RBCs are short contact time and short retention time due to a large active surface, low power requirement, and low sludge production. The disadvantage is that shafts within the mechanical process need regular maintenance.

A trickling filter is a nonsubmerged fixed-film biological reactor using rocks or plastic packing to support the growth of biofilms for biodegradation. Wastewater is distributed from the top of the filter beds by a rotary distributor. The advantage of a trickling filter is the high oxygen transfer efficiency due to the large contact area between air and liquids. However, energy costs are also high for trickling filters because wastewater needs to be pumped to the top of the filter.

3.3. CONVENTIONAL PACKAGE PLANTS

3.3.1 Activated Sludge Package Plant

Activated sludge package plants are prepackaged plants utilizing the activated sludge process for small-flow applications. Because such systems are prepackaged, they usually have smaller footprints than conventional activated sludge plants.

3.3.2 SBR

A sequencing batch reactor (SBR) is an activated sludge reactor composed of one or more periodically operated fill-and-draw reactors (Herzbnin et al., 1985).

A typical SBR system has five stages for each cycle: fill, react, settle, draw, and idle. During the anoxic fill stage, microorganisms utilize biochemical oxygen demand (BOD) and remove NO_3^- in influent wastewater. During the aerobic react stage, waste degradation and nitrification are enhanced with the aeration in the reactor. During the settle stage, mixed liquor suspended solids (MLSS) settle in the reactor. The relatively clean supernatant is then removed in the draw stage, and the remaining wastewater settles in the idle stage (Davis and Masten, 2004). SBRs are similar to the five-stage Barnard process, and the only difference is that the SBR process uses carryover NO_3^- from the settle and draw stages to drive pre-denitrification (Ritmann and McCarty, 2001). SBRs can achieve 90% total nitrogen removal. The disadvantage of SBRs is that they need many tanks and relatively long HRTs.

The flow diagram of a typical SBR system is shown in Figure 3.3 (Tchobanoglous et al., 2003). Figure 3.4 is a sample picture of an installed SBR system manufactured by Siemens.

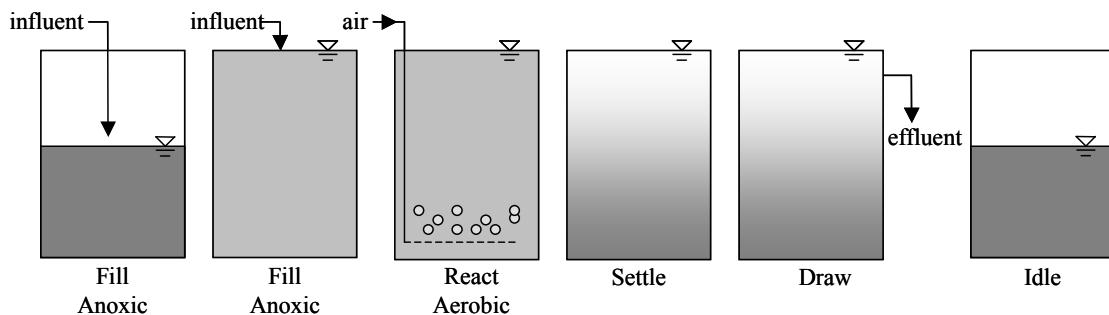


Figure 3.3. Flow diagram of SBR system.



Figure 3.4. SBR system by Siemens (OMNIFLO).

3.3.3 OD

An oxidation ditch (OD) is a modified extended aeration activated sludge treatment process used for long-term aeration and high SRTs. An OD usually has elliptical or circular channels and utilizes aeration rotors to circulate wastewater in the channel to supply oxygen to facilitate biodegradation in channels. ODs are easily maintained, relatively unaffected by load fluctuations, and form relatively less sludge than do conventional activated sludge systems. They are easily controlled by changing the rotation of the rotor and the dipping depth, and such changes require relatively little energy. Furthermore, ODs can perform both N&D in the same structure to save energy. Mixing in ODs is improved compared to results in conventional aeration tanks. However, ODs require a relatively large area.

The flow diagram of a typical OD is shown in Figure 3.5. Figure 3.6 is a sample picture of a modified OD with multiple channels by U.S. Filter (Siemens).

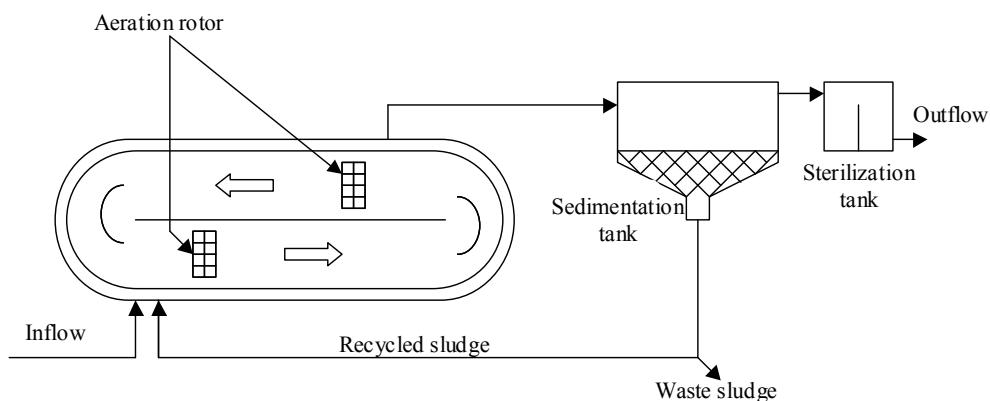


Figure 3.5. Process flow diagram of OD.

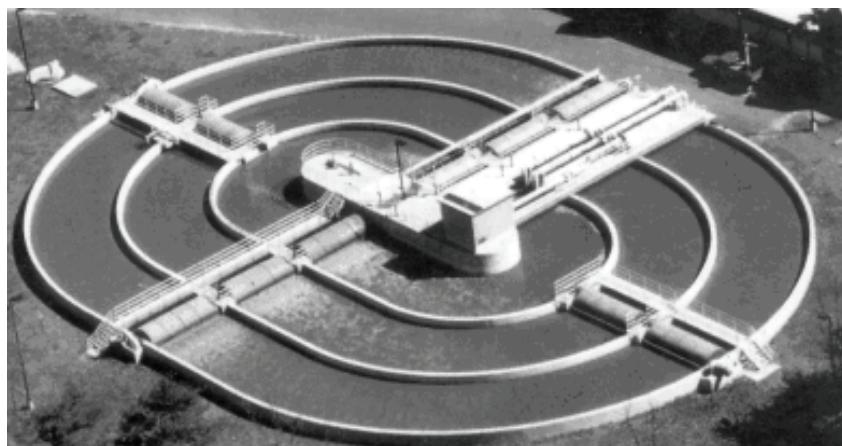


Figure 3.6. Multichannel OD by U.S. Filter (Siemens).

3.3.4 Biological Filtration

A biological filtration system utilizes particulate media or disks to host biological substrate that then treat wastewater, as opposed to seeding wastewater with inoculated return sludge. The media used in biological filtration have large surface areas on the surface of filtration media to support the microbial growth and form biofilms, which are used for the nitrification

process. Without utilizing a recirculating activated sludge process, biological filtration systems eliminate secondary clarifiers and associated costs and space requirements. Figure 3.7 shows an installed package biological filtration system manufactured by Orenco Systems, Inc. In Figure 3.7, the treatment system includes an underground recirculation tank and several pods that contain the textile filter media. Primary tanks are located at each home that feeds the treatment system, and most systems also include a dosing tank for the effluent dispersal field.

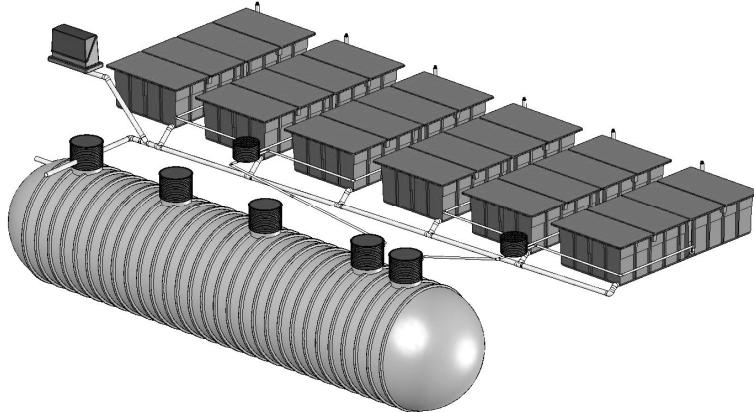


Figure 3.7. AdvanTex system by Orenco Systems, Inc.

3.4. MEMBRANE CUSTOMIZED PLANTS

MBRs integrate membranes (microfiltration [MF] or ultrafiltration [UF]) into activated sludge systems. MBRs use membrane filtration instead of sedimentation, which is used in conventional activated sludge systems, to separate biomass from effluent in secondary clarifiers.

The MLSS concentration in MBRs can reach 10,000 to 15,000 mg/L, which is much higher than MLSS values in conventional activated sludge systems (~3000 to 5000 mg/L). The pores of MBR membranes are smaller than some pathogens such as protozoa, allowing for the effective removal of some pathogens. MBRs have a reduced treatment system footprint due to the lack of clarifiers.

The flow diagram of a typical MBR system is shown in Figure 3.8. Figure 3.9 shows two sample pictures of MBRs manufactured by Zenon (Z-MOD) and Siemens Water Technologies (Xpress).

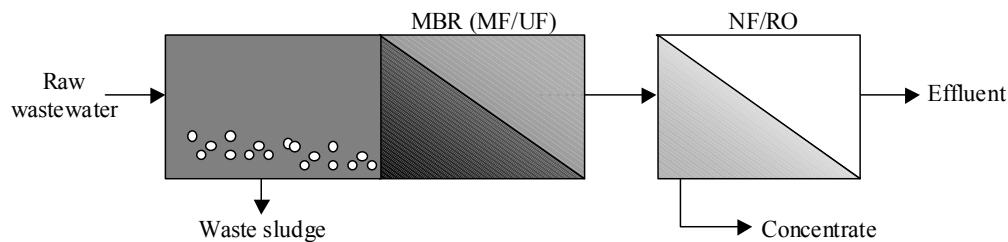


Figure 3.8. Process flow diagram of MBR.

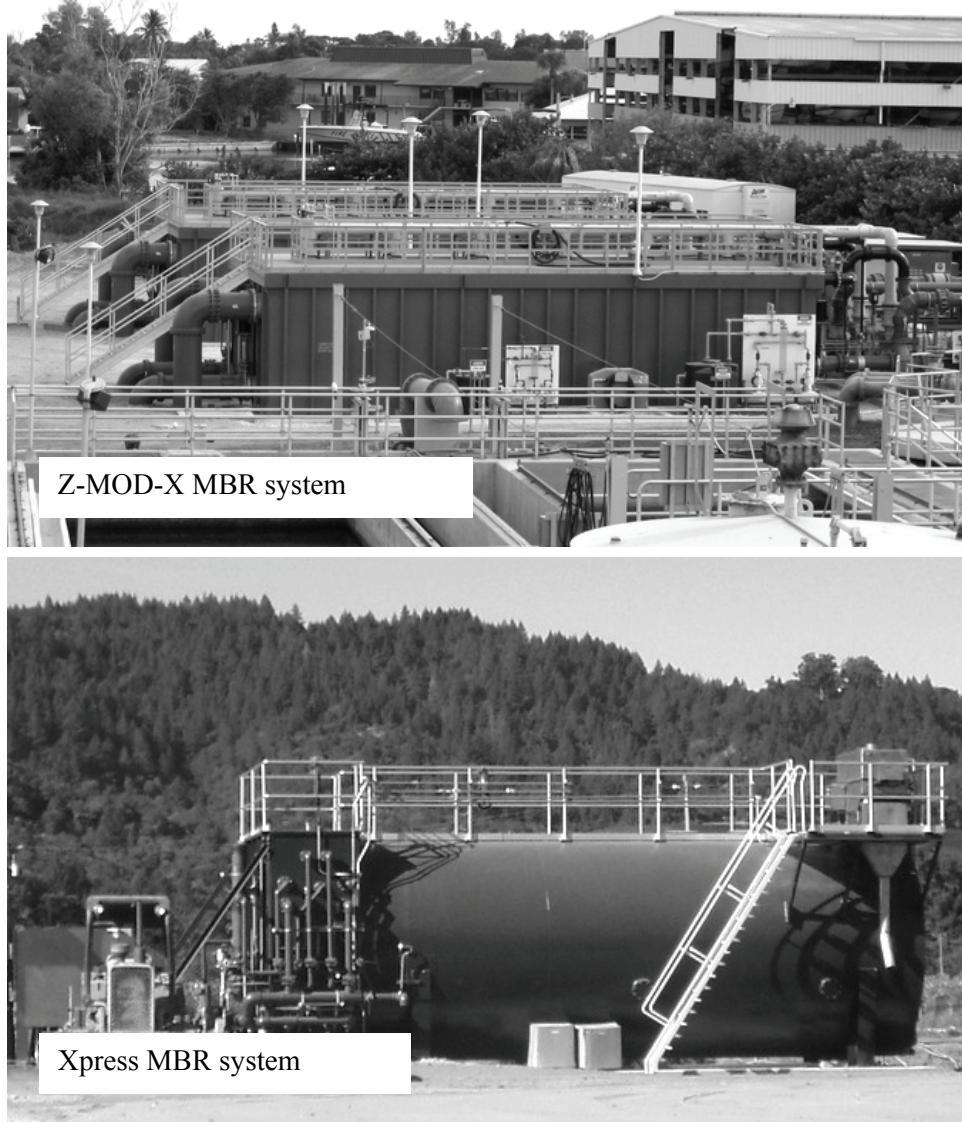


Figure 3.9. Sample pictures of MBR systems.

3.5. NATURAL SYSTEMS

Natural systems rely upon natural microbial, biological, physical, and chemical processes in lagoons, ponds, and wetlands to treat wastewater (Constructed Wetlands, 2000). As there is no need to construct major facilities for natural systems, they are generally cost-effective. The operation and maintenance (O&M) costs are also relatively low. Such systems can provide adequate treatment of organic pollutants (5-day BOD [BOD₅] and total suspended solids [TSS]), nitrogen, and phosphorus. The performance is relatively consistent because of the large area, which acts as a natural filter, and the long retention time. Treatment efficiency of these systems is seasonal, highest in summer or in warm climates. Treatment efficiency is lower in winter and in cold climates. Additionally, natural systems require relative large areas and may produce nuisance insects. Figure 3.10 is a sample picture of a constructed wetland.



Figure 3.10. Constructed wetland system for Arcata, CA.

3.6. ALTERNATIVE TREATMENT SYSTEMS

As the costs detailed further in this report illustrate, larger-flow treatment plants realize economies of scale relative to construction costs. Stated another way, the costs to construct small-scale treatment plants can be prohibitive, limiting the ability to efficiently tap into wastewater supplies for decentralized reuse. This section examines several alternative treatment technologies that may provide lower-cost or lower-maintenance treatment that may be cost-effectively employed.

One such system, the Living Machine® (LM), was evaluated. The LM was developed by Dr. John Todd. It mimics the cleaning functions of wetlands and uses a series of tanks to support vegetation and organisms for wastewater treatment (Wastewater, 2002). The flow diagram of an LM is shown in Figure 3.15 (Wastewater, 2002).

There are advantages to LMs. They can be chemical-, odor-, and noise-free. They can effectively remove BOD, TSS, and total nitrogen (TN) while keeping a small ecological footprint and have reduced maintenance costs. Also, LM systems are aesthetically pleasing and have been incorporated into environmentally friendly locations, such as the Audubon Society's Corkscrew Swamp Nature Reserve in South Florida. However, LM systems are highly tailored to each specific site and thus result in relatively high costs for installation compared to other treatment systems.

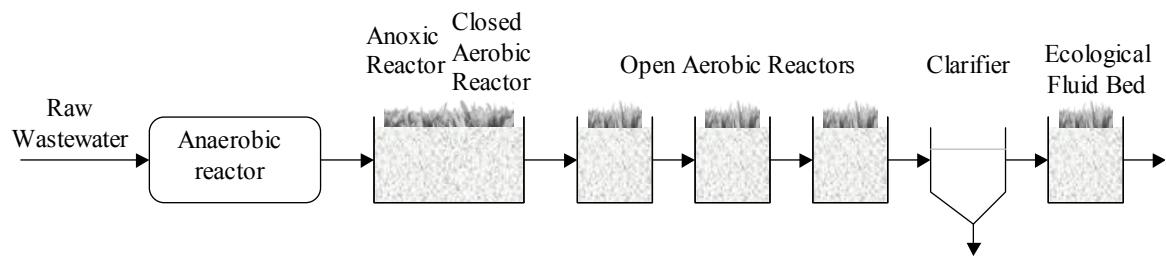


Figure 3.11. Flow chart of a sample LM.

As part of this project, the team reviewed two nonbiological treatment systems, the point-of-need water recycling system (PONWRS) and the Integrated Membrane System (IMANS®). These two systems are relatively unproven. However, they both focus on the same innovative basic premise, leaving the nutrients in and taking the pathogens out. More details for these systems are included in Appendix H.

CHAPTER 4

COST ANALYSIS

This section summarizes the data-gathering and -processing methods for this project. The cost and operation data from over 234 small-scale wastewater treatment and water reuse facilities have been gathered and synthesized.

4.1. DATA GATHERING AND PROCESSING

4.1.1. Data Sources

This project includes four different searches for cost and performance data on wastewater treatment and water reuse treatment technologies. The first search worked directly with equipment manufacturers and targeted various general treatment types. Utilities that own the various types of technologies were then contacted for cost information. A utility survey (Appendix I) was developed and sent out to utilities for information collection. The second search approach used information from USDA Rural Development state office dockets for loans and grants on wastewater projects. This information was requested through the Freedom of Information Act. The third search used a cost database developed by Camp Dresser & McKee Inc. The fourth search used water reuse cost information from Carollo projects.

The treatment trains evaluated for this project include a range of conventional, advanced, and alternative technologies. A total of 234 plants and systems have been surveyed. The locations of these plants and systems in the United States are shown in Figure 4.1. Information collected outside the United States was not used for the data analysis in this report.

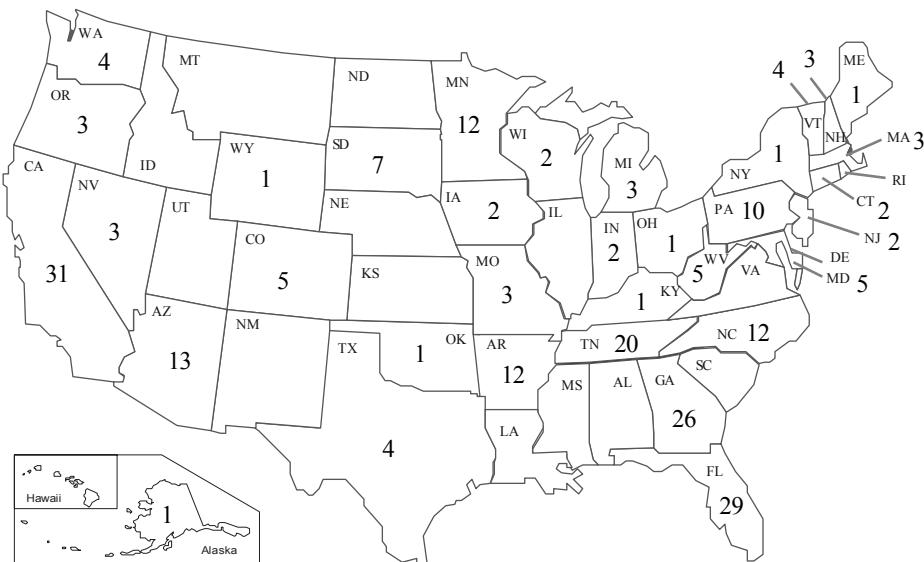


Figure 4.1. Locations of surveyed plants and systems in the U.S.

These plants and systems are divided into five categories:

- A) conventional customized plants (83 plants),
- B) conventional package plants (63 plants),
- C) membrane customized plants (24 plants),
- D) natural systems (58 plants), and
- E) alternative treatment systems (6 plants).

The capacities (flow) of the 234 plants are shown in Figure 4.2. Eighteen percent of the plants were less than 0.1 mgd, 53% between 0.1 and 1 mgd, 11% between 1 and 2 mgd, 9% between 2 and 3 mgd, 6% between 3 and 4 mgd, and 3% between 4 and 5 mgd. The goal of this project was to compile data in the flow range of 0.1 to 1.0 mgd. However, the plants with flows below 5 mgd were included for the value of reference. Plants with flows above 5 mgd were excluded from the following analysis.

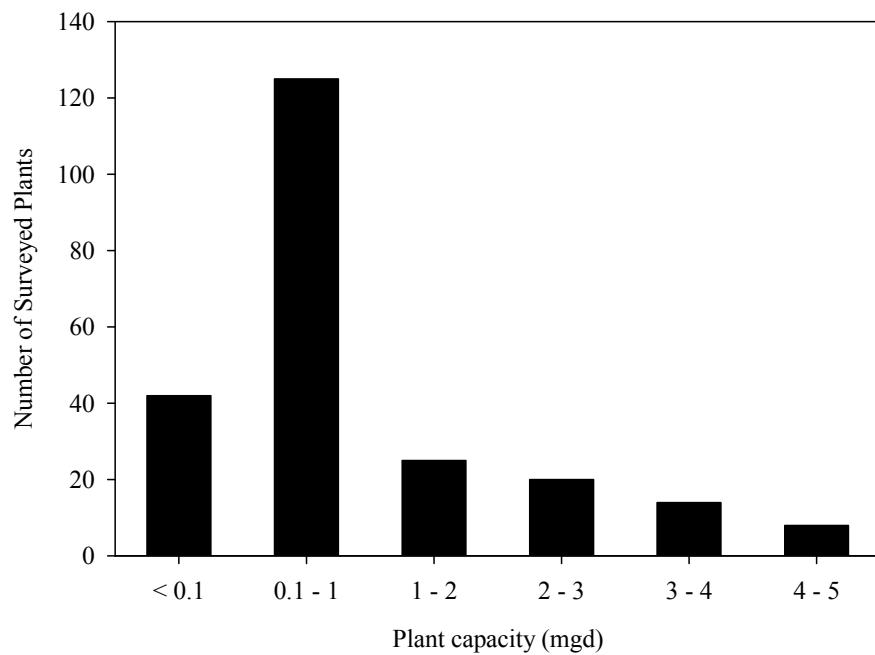


Figure 4.2. Capacities of surveyed plants.

Not all construction costs and O&M costs could be collected in every plant evaluated in this study. Only construction costs were gathered on 93 plants, only O&M costs were collected on 17 plants, and both construction and O&M costs were collected on 124 plants, as shown in Figure 4.3. Plants with only equipment costs are excluded from the analysis in this report.

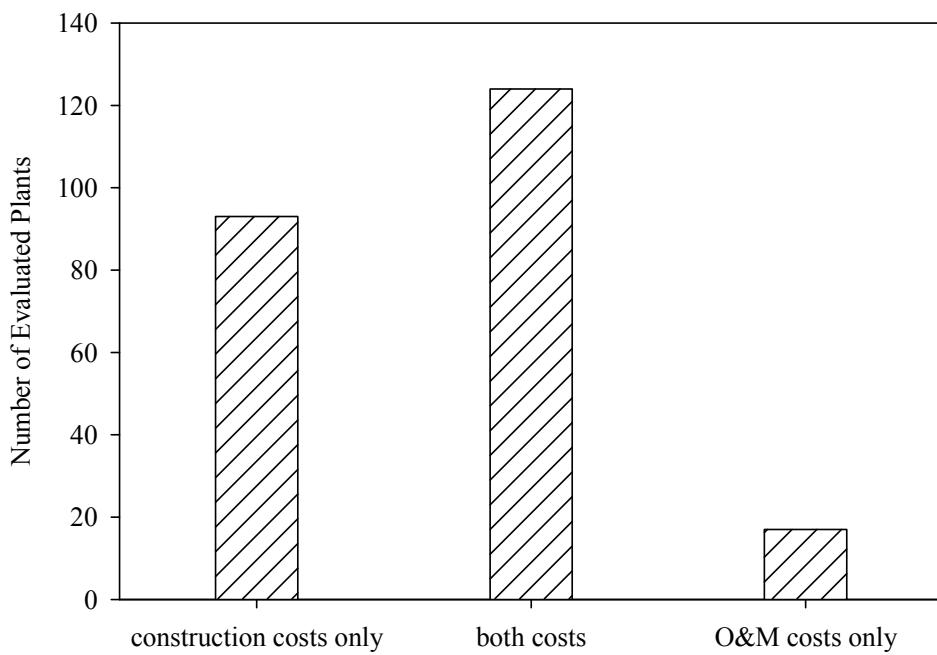


Figure 4.3. Data type of surveyed plants.

The distribution construction dates of evaluated plants are shown in Figure 4.4. Fifty-two percent of the evaluated plants were built or bid after 2000, 28% from 1990 to 1999, 18% from 1980 to 1989, and 2% between 1970 and 1979.

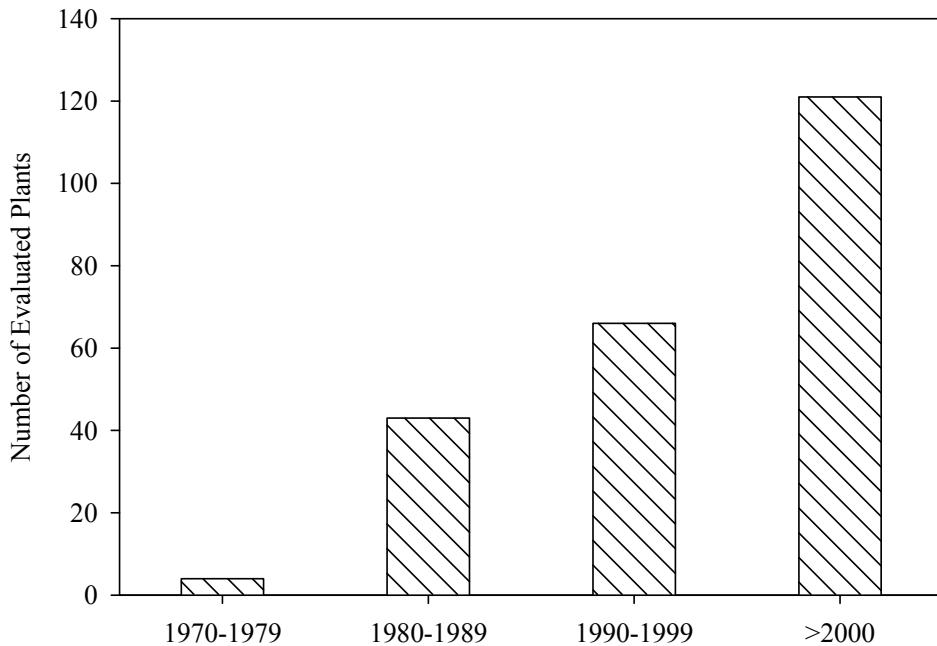


Figure 4.4. Construction dates of surveyed plants.

4.1.2. Cost Factors

There are a number of technology and process decisions that impact cost and add variability to the cost data set, discussed here as “hard” and “soft” costs. Hard costs include the expected equipment and construction costs (engineering and permitting costs are not included in this analysis). These hard costs can be impacted by the current competition for labor and services (available skilled labor, material supplies, and the abundance or absence of projects), which impacts the low bid for these projects. The hard cost will be impacted by the type of use of the reclaimed water and the regulations associated with that use. For example, regulations for certain types of reclaimed water use require higher levels of filtration or disinfection than would be required for other reclaimed water uses. This phenomenon also can be seen with nutrient removal (or lack thereof), which can impact the bottom-line hard cost. If a utility decides to reclaim water as an alternative to discharge to a nutrient-limited waterway, there are avoided costs for not having to reduce nutrients in the treatment train. If a utility decides to provide highly treated, low-nutrient water to supplement a water body (beneficial reuse), then there is an added cost for the nutrient removal. Other items that impact the hard costs include the inclusion of treatment process redundancy and various reliability requirements, as are required particularly in California and Washington for “tertiary recycled water.”

Other issues that may introduce scatter in the cost data are referred to here as “soft” cost components. These soft components include implementation problems such as permitting, lawsuits, funding, user contracts, public perception, and antigrowth efforts that may slow down or halt a project, substantially increasing the project cost. For large projects, these costs may have only a minimal impact on the net budget. For the relatively small projects examined in this project, these added soft costs could extend the total cost well past reasonable levels.

Additional “value” available from reclamation as “soft” costs include reduced potable water infrastructure for new construction, reduced potable water supply management based on smaller distribution and storage requirements for potable water, reduced source capacity requirements to be explored in addition to avoiding investment in water rights purchase, and costs of buying into total-maximum-daily-load trade markets necessary for a new National Pollutant Discharge Elimination System (NPDES) permit. However, the collection or estimation of these costs is beyond the project scope and is not covered in this analysis.

It is important to note the level of engineering accuracy in construction costs that was applied to this project. Currently the American Association of Cost Engineers provides five classes of cost estimation accuracy, as shown in Table 4.1.

Table 4.1. Levels of Engineering Accuracy for Cost Estimation

Class	Expected Accuracy Range for Cost Estimation	
	Low End	High End
5	-20% to -50%	+30% to +100%
4	-15% to -30%	+20% to +50%
3	-10% to 20%	+10% to +30%
2	-5% to -15%	+5% to +20%
1	-3% to -10%	+3% to +15%

While the costs used in this report are real costs encountered by the various utilities, we recommend treating these costs as Class 5 estimates. Further, some of the treatment facilities surveyed as part of this project did not have filtration or disinfection. As part of this project, our team provided construction cost estimations of UV disinfection and filtration.

Typically, cost estimation in Class 5 is used for strategic business planning purposes, such as but not limited to market studies, assessment of initial viability, evaluation of alternate schemes, project screening, project location studies, evaluation of resource needs and budgeting, long-range capital planning, etc. The expectations for the accuracy of the costs found within this report must match the reality of the challenge of providing those estimates based on data from a diverse collection of facilities with various conditions that impact the cost.

4.1.3. Filtration and Disinfection

For all of the treatment trains, the required level of disinfection is dependent upon the reclaimed water use. For some uses, filtration is not required and only minimal disinfection is needed. For other uses, filtration to a high water quality and high-level disinfection is required.

For each treatment plant reviewed under this project, the existence of filtration and disinfection was determined. If there was no noted filtration or disinfection, or if there was no filtration and only minimal disinfection, costs for filtration (using continuous backwash sand filtration) and high-level disinfection (using UV disinfection at 65% UV transmittance) were added to better normalize the cost database. The design of these additional treatment processes is conservatively based upon meeting the turbidity and disinfection criteria required for “tertiary recycled water” under Title 22 of the California Code of Regulations. Again, there are occasions where filtration is not required and disinfection to “tertiary recycled water” standards is not required, and thus treatment costs could be reduced in many circumstances. The full-cost data set in Appendix J includes the added cost columns for filtration and disinfection, if utilized. The user of this report could modify the costs to subtract out filtration and/or high-level disinfection if needed.

The continuous backwash filter was used as the basis for the cost estimation of filtration technologies if the surveyed treatment plant did not include filtration. Parkson's DynaSand® Filter is a continuous backwash, upflow, deep bed, granular medium filter commonly used for reuse applications. The internal washing system cleans filter media and requires no backwash pumps or storage tanks.

If a surveyed utility did not include disinfection, the Trojan UV3000 UV disinfection system costs were included. This low-pressure UV disinfection system is shown in Figure 4.5.



Figure 4.5. Open-channel UV disinfection system by Trojan Technologies.

4.1.4. Normalization of Data

Three types of cost data are calculated or estimated: construction costs, O&M costs, and present value costs. Both construction costs and O&M costs are normalized to December 2008. Present value costs are also based on December 2008.

Construction costs are the costs associated with constructions of the treatment systems. They do not include costs for engineering, permitting, legal services, and general contingency. Land costs and collection system costs, if known, were subtracted from the gathered costs. Construction costs of filtration and disinfection systems are included if no filtration or disinfection systems existed in each treatment plant.

To compare the construction costs of facilities built at different dates and different locations, original costs were normalized to a national average level with the Engineering New Record (ENR) 20-city construction cost indexes (CCIs) and R.S. Means location factors, as shown in Equation 1.

$$\text{Total construction cost}_{\text{normalized}} = \text{Original construction cost} * \frac{\text{CCI}_{\text{current date}}}{\text{CCI}_{\text{built date}}} * \frac{1}{\text{location factor}_{\text{R.S. Means}}}$$

Equation 1

Unit construction costs (\$million/mgd) are calculated as the total construction costs normalized by the treatment flow capacities of their corresponding systems, as shown in Equation 2.

$$\text{Unit construction cost} = \frac{\text{Total construction Costs}_{\text{normalized}}}{\text{Capacity}} \quad \text{Equation 2}$$

O&M costs are the costs associated with O&M. O&M costs at different dates and different locations were normalized to national average levels as well. These costs were broken down into energy, materials, and labor, as shown in Equation 3. The energy costs were normalized with average retail prices of electricity published by the Energy Information Administration at the U.S. Department of Energy, as shown in Equation 4. Material and manpower costs were normalized to ENR material price indexes (Equation 5) and ENR skilled labor indexes (Equation 6). Both ENR material price indexes and skilled labor indexes can be accessed through ENR's website: <http://enr.construction.com/>. Each category of O&M costs was then also normalized to R.S. Means location factors.

$$\text{Annual O & M cost}_{\text{normalized}} = \text{Annual energy cost}_{\text{normalized}} + \text{Annual material cost}_{\text{normalized}} + \text{Annual labor cost}_{\text{normalized}} \quad \text{Equation 3}$$

$$\text{Annual energy cost}_{\text{normalized}} = \text{original energy cost} * \frac{\text{retail price of electricity}_{\text{current date}}}{\text{retail price of electricity}_{\text{built date}}} * \frac{1}{\text{location factor}_{\text{R.S. Means}}} \quad \text{Equation 4}$$

$$\text{Annual material cost}_{\text{normalized}} = \text{original material cost} * \frac{\text{ENR material price index}_{\text{current date}}}{\text{ENR material price index}_{\text{built date}}} * \frac{1}{\text{location factor}_{\text{R.S. Means}}} \quad \text{Equation 5}$$

$$\text{Annual labor cost}_{\text{normalized}} = \text{original labor cost} * \frac{\text{ENR skilled labor index}_{\text{current date}}}{\text{ENR skilled labor index}_{\text{built date}}} * \frac{1}{\text{location factor}_{\text{R.S. Means}}} \quad \text{Equation 6}$$

Unit O&M costs (\$/1000 gal) are calculated as the annual O&M costs normalized by the treatment flow capacities of their corresponding systems and then normalized to 1000 gal, as shown in Equation 7.

$$\text{Unit O & M cost} = \frac{\text{Annual O & M cost}}{\text{Capacity (mgd)} * (365 \text{ days}/1000 \text{ gallons})} \quad \text{Equation 7}$$

Present value costs are the costs in currently valued dollars to be expended over a period of time less the net of any funds to be repaid. In the context of cost analysis of wastewater treatment facilities, present value costs are the total cost of owning and operating a wastewater treatment facility for the life of the system in current dollars. The construction costs are one-time costs at the base year if no payment plans are considered. O&M costs are a series of annually recurring costs that need to be converted to present value costs. For this analysis, engineering and permitting costs are not included in the present value costs. Equation 8 shows the equation for such conversion.

$$\text{Present Value of O \& M Cost} = \text{Annual O \& M cost}_{\text{normalized}} * \sum_{t=1}^n \frac{1}{(1+d)^t} = \text{Annual O \& M cost}_{\text{normalized}} * \frac{(1+d)^n - 1}{d(1+d)^n}$$

Equation 8

In Equation 8, d is the discount rate and n is the number of years. If we assume the water reuse systems can last for 20 years ($n = 20$) and a discount rate of 5% ($d = 0.05$), the present value cost can be estimated using Equation 9 and unit present value costs can be calculated using Equation 10.

$$\text{Present Value Cost} = \text{Construction Costs} + \text{Annual O \& M cost}_{\text{normalized}} * \frac{(1+d)^n - 1}{d(1+d)^n} \quad \text{Equation 9}$$

$$\text{Unit present value cost} = \frac{\text{Present value cost}_{\text{normalized}}}{\text{Capacity}} \quad \text{Equation 10}$$

4.2. COMPARISONS OF TREATMENT PROCESSES AND PACKAGE SYSTEMS

4.2.1. General Trend of Construction Costs and Capacities

The data plots or cost curves of total construction costs and unit construction costs versus capacities are shown in Figures 4.6 and 4.7. Costs and capacities are plotted on log-log graphs. Regression lines, 95% confidence intervals, and 95% prediction intervals are also shown in these figures. The general trend is that small flow systems have higher unit construction costs, possibly due to economies of scale for construction and/or possibly due to “soft” cost issues.

The scaling effect is further shown in the plot of unit construction costs and capacities without log transformation (Figure 4.8). A regression line is also developed. The figure shows that unit construction costs are much higher at small flows (<1 mgd) and relatively low and consistent at large flows (>1 mgd). To conduct the comparisons of treatment processes and systems with different flows, log-transformation and cost-capacity curves are used for all the following analyses.

Please note that the regression lines are developed only to show the general trend of construction costs and capacities for all evaluated technologies in this report. The best value of these data is the database itself, which can be mined for the most relevant data for a particular project. The authors of this report recommend site-specific analysis for the basis for engineering costing of new water reuse facilities.

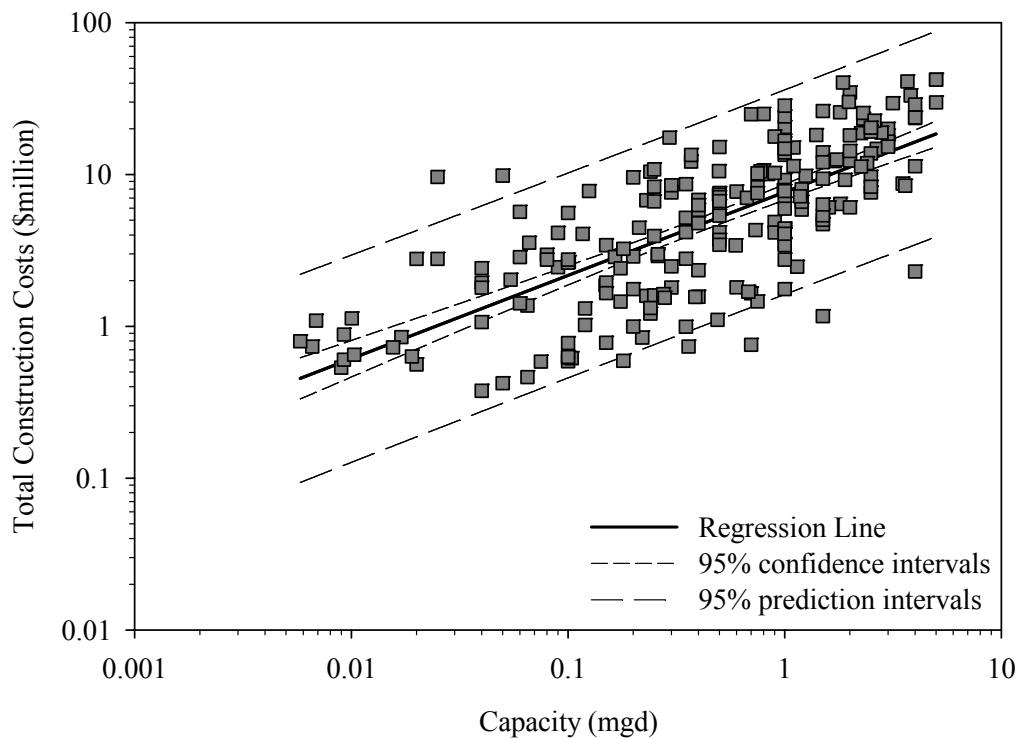


Figure 4.6. Total construction costs.

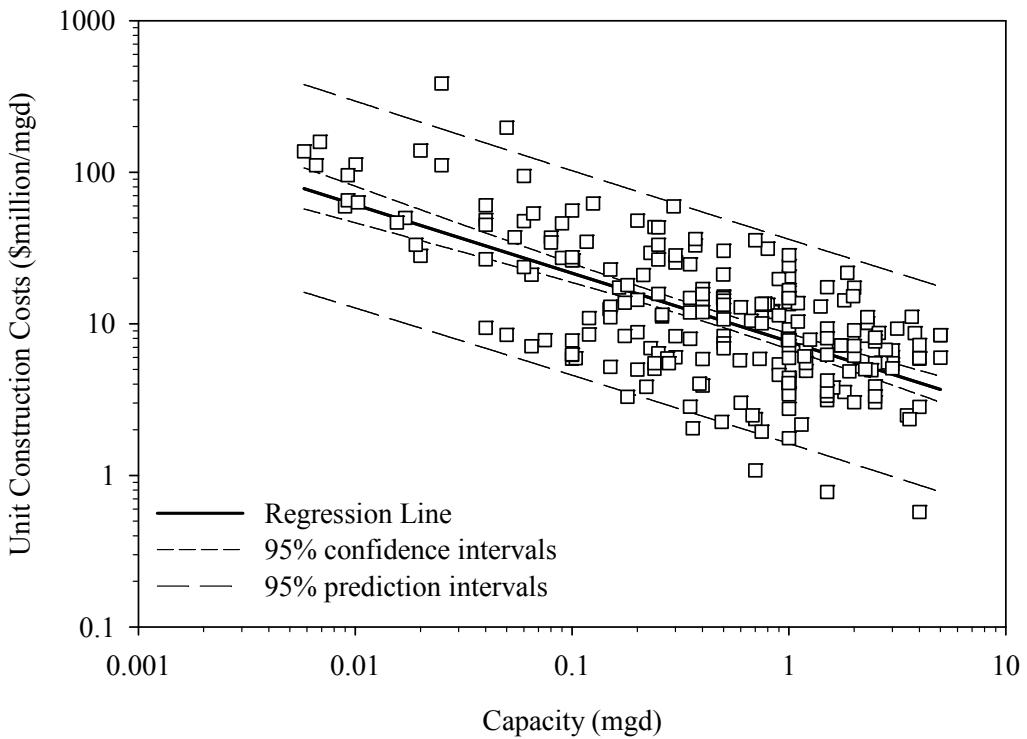


Figure 4.7. Unit construction costs.

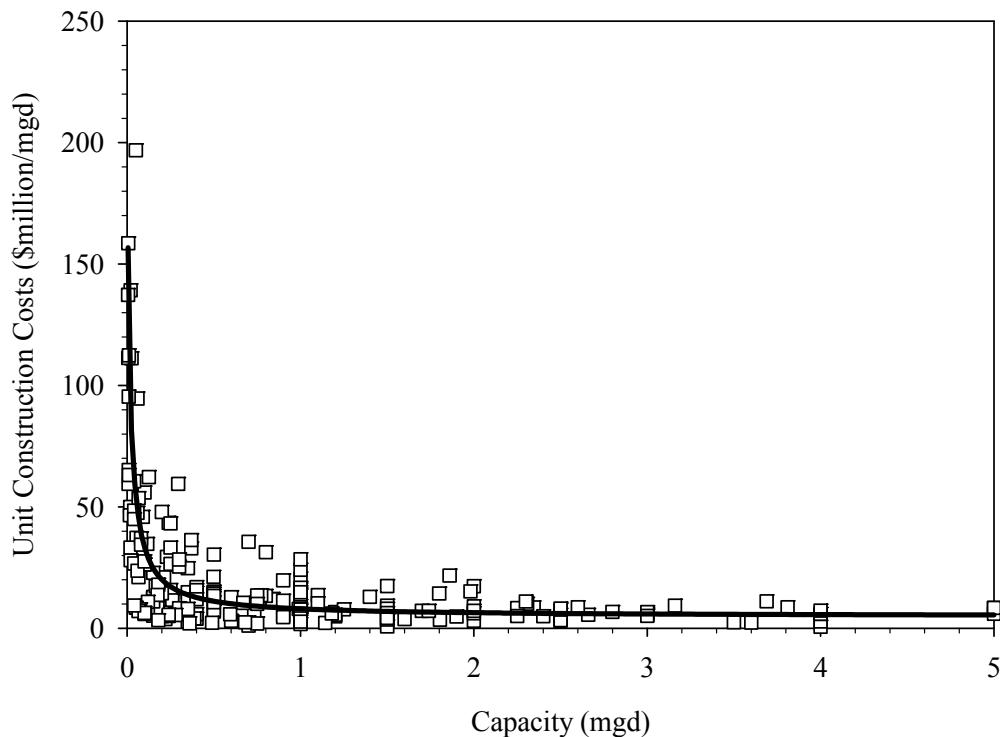


Figure 4.8. Raw data of unit construction costs. Solid line, regression line.

4.2.2. Unit Construction Cost-Capacity Curves of Selected Processes

Unit construction cost-capacity curves were plotted for selected processes.

- Figure 4.9 shows the construction costs of activated sludge plants.
- Figure 4.10 shows the construction costs of extended aeration plants.
- Figure 4.11 shows the construction costs of Bardenpho plants.
- Figure 4.12 shows the construction costs of MLE plants.
- Figure 4.13 shows the construction costs of ICEAS plants.
- Figure 4.14 shows the construction costs of package plants.
- Figure 4.15 shows the construction costs of SBR plants.
- Figure 4.16 shows the construction costs of ODs.
- Figure 4.17 shows the construction costs of MBR plants.
- Figure 4.18 shows the construction costs of ponds.
- Figure 4.19 shows the construction costs of lagoons.
- Figure 4.20 shows the construction costs of wetlands.
- Figure 4.21 shows the construction costs of LMs.

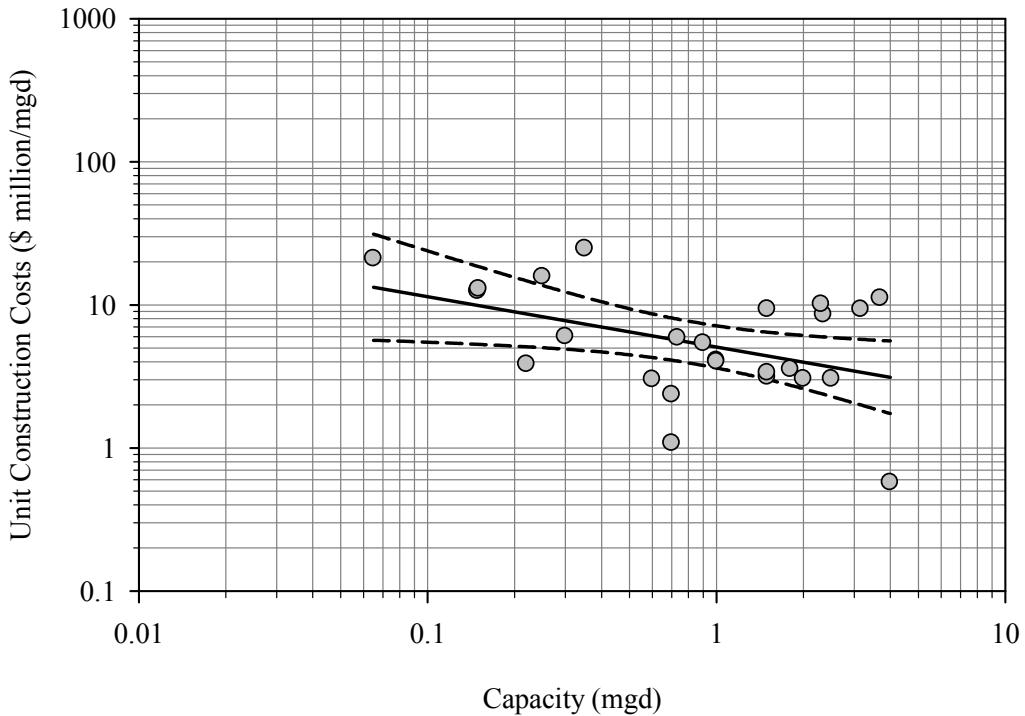


Figure 4.9. Unit construction costs of activated sludge plants.
Solid line, regression line; dash lines, 95% confidence intervals.

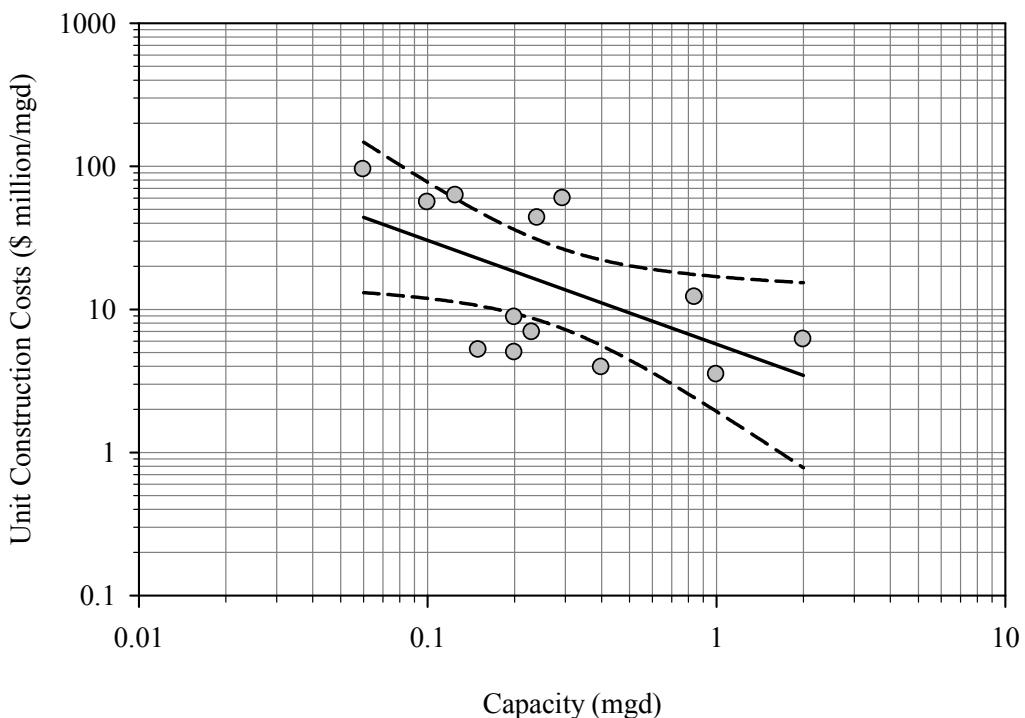


Figure 4.10. Unit construction costs of extended aeration plants.
Solid line, regression line; dash lines, 95% confidence intervals.

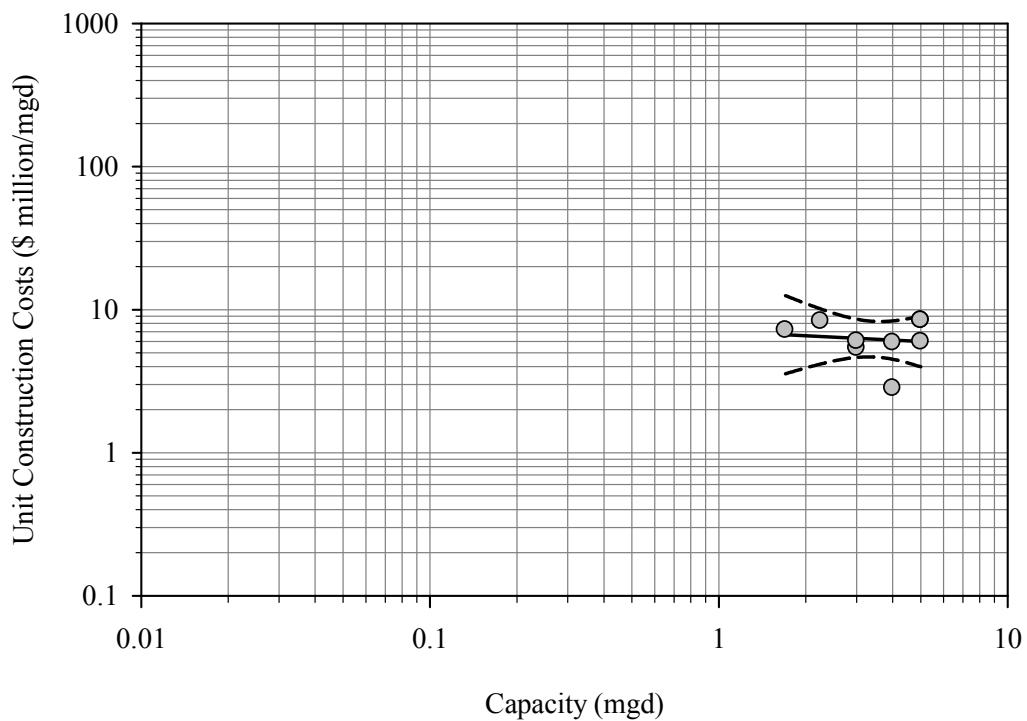


Figure 4.11. Unit construction costs of Bardenpho plants.
Solid line, regression line; dash lines, 95% confidence intervals.

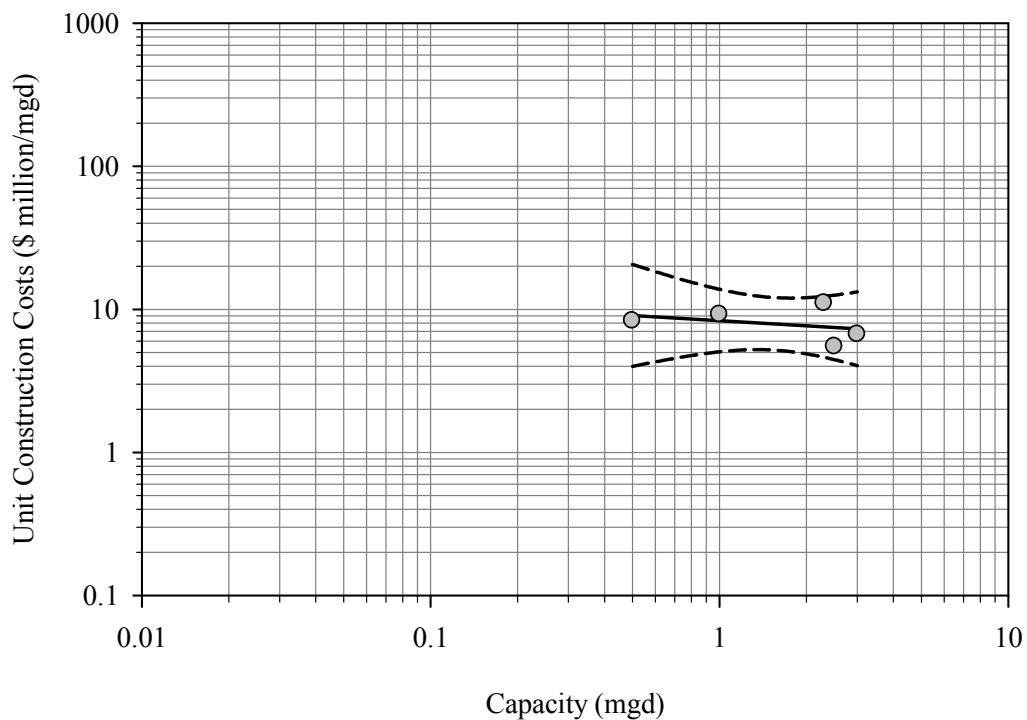


Figure 4.12. Unit construction costs of MLE plants.
Solid line, regression line; dash lines, 95% confidence intervals.

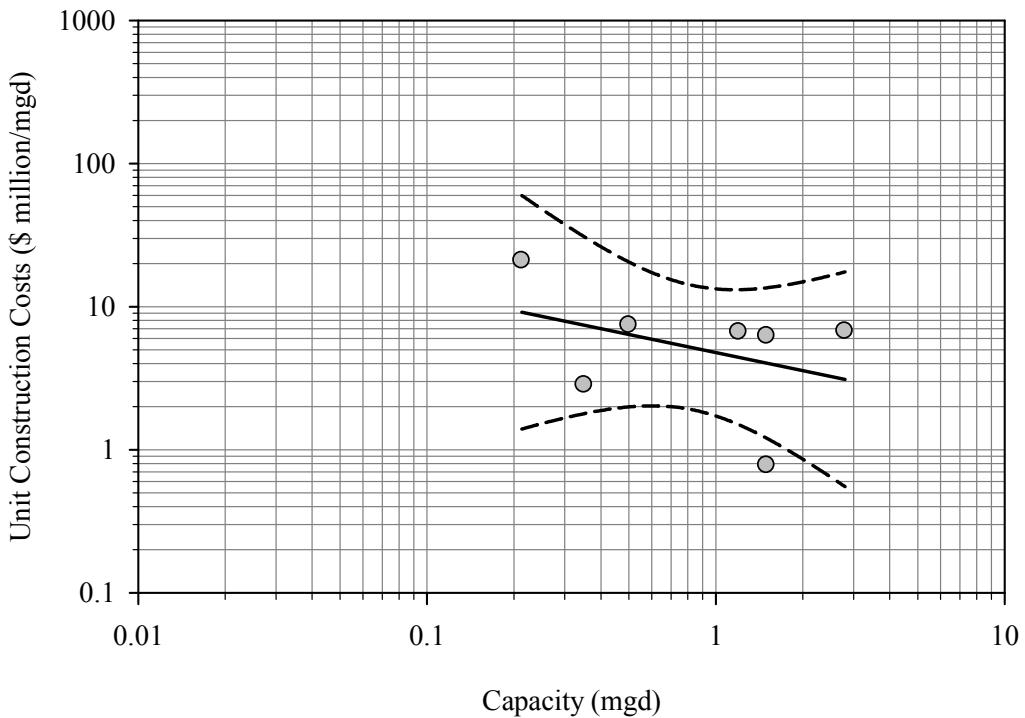


Figure 4.13. Unit construction costs of ICEAS plants.
Solid line, regression line; dash lines, 95% confidence intervals.

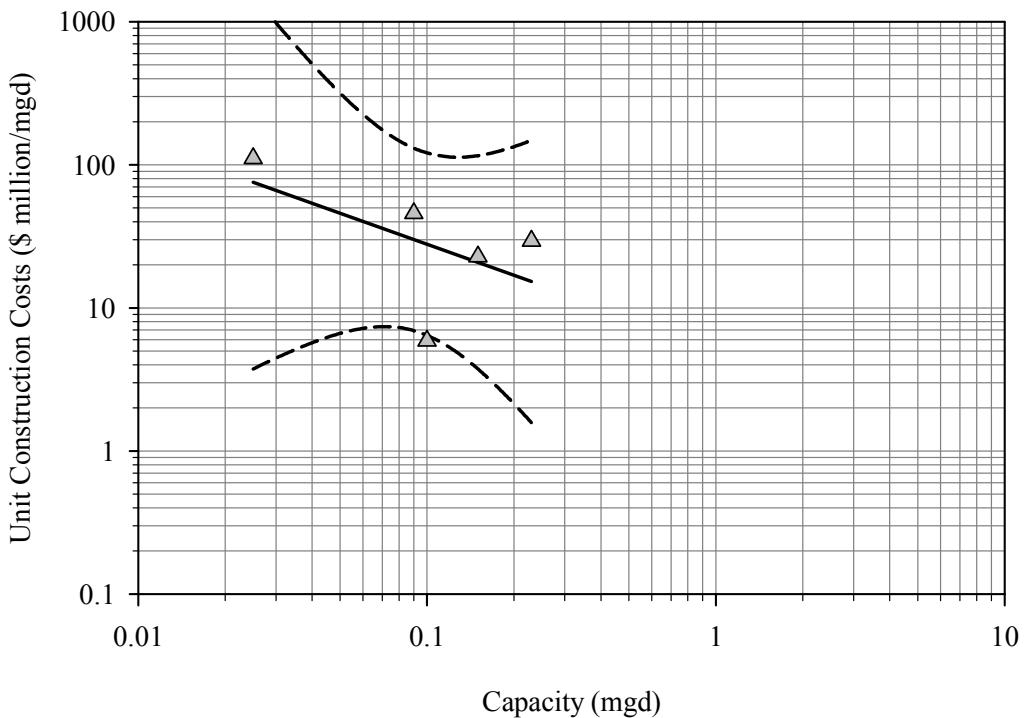


Figure 4.14. Unit construction costs of package plants.
Solid line, regression line; dash lines, 95% confidence intervals.

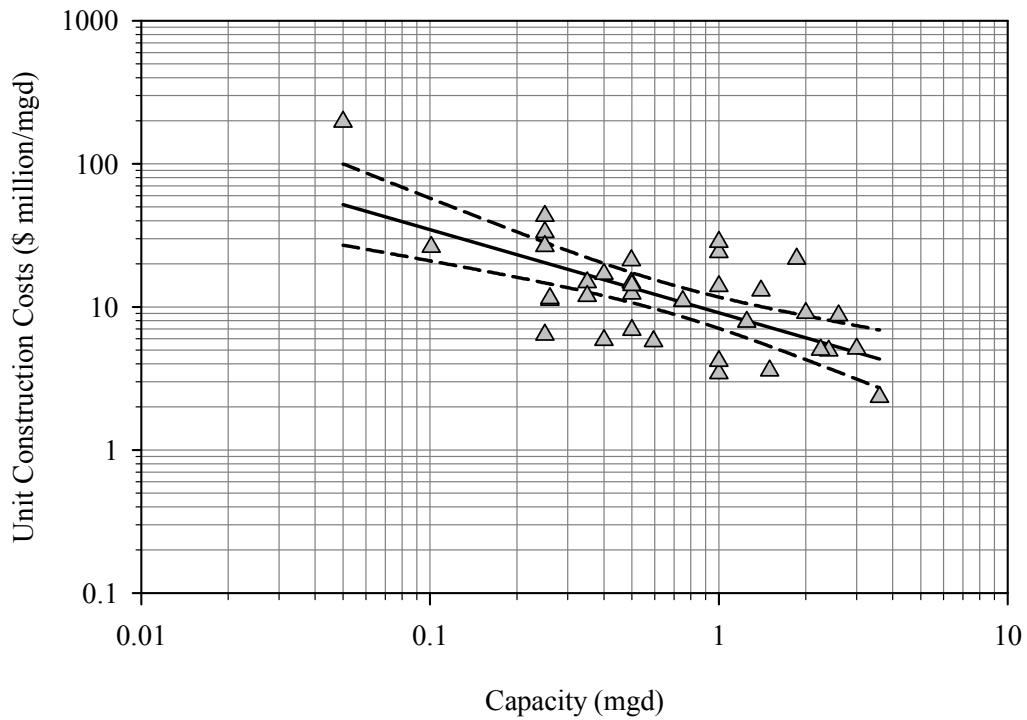


Figure 4.15. Unit construction costs of SBR plants.
Solid line, regression line; dash lines, 95% confidence intervals.

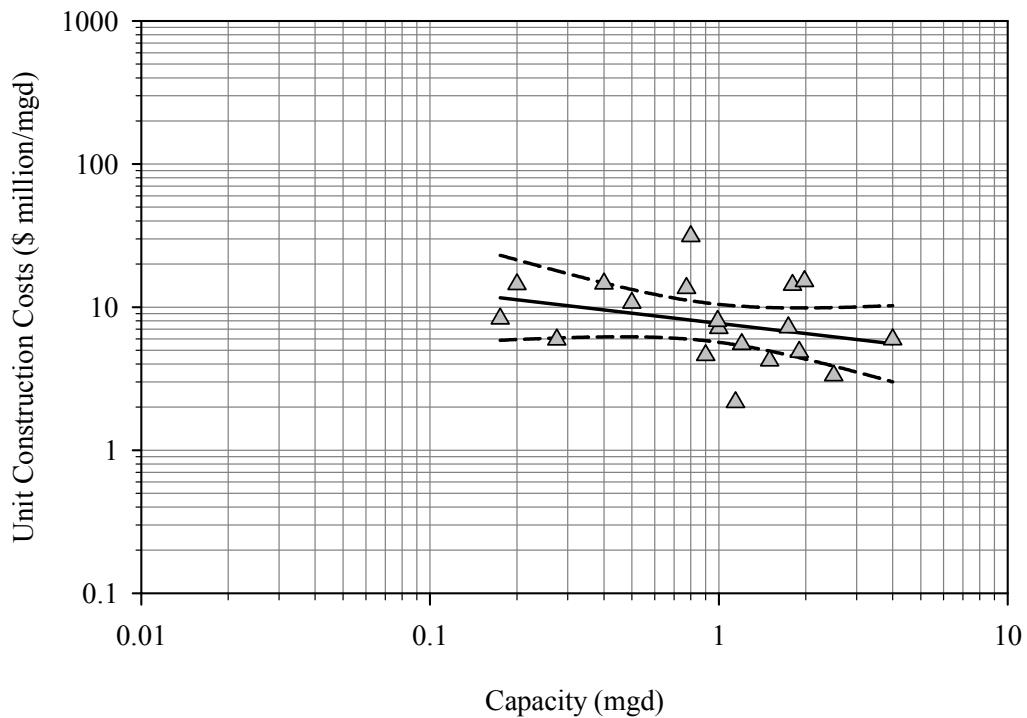


Figure 4.16. Unit construction costs of ODs.
Solid line, regression line; dash lines, 95% confidence intervals.

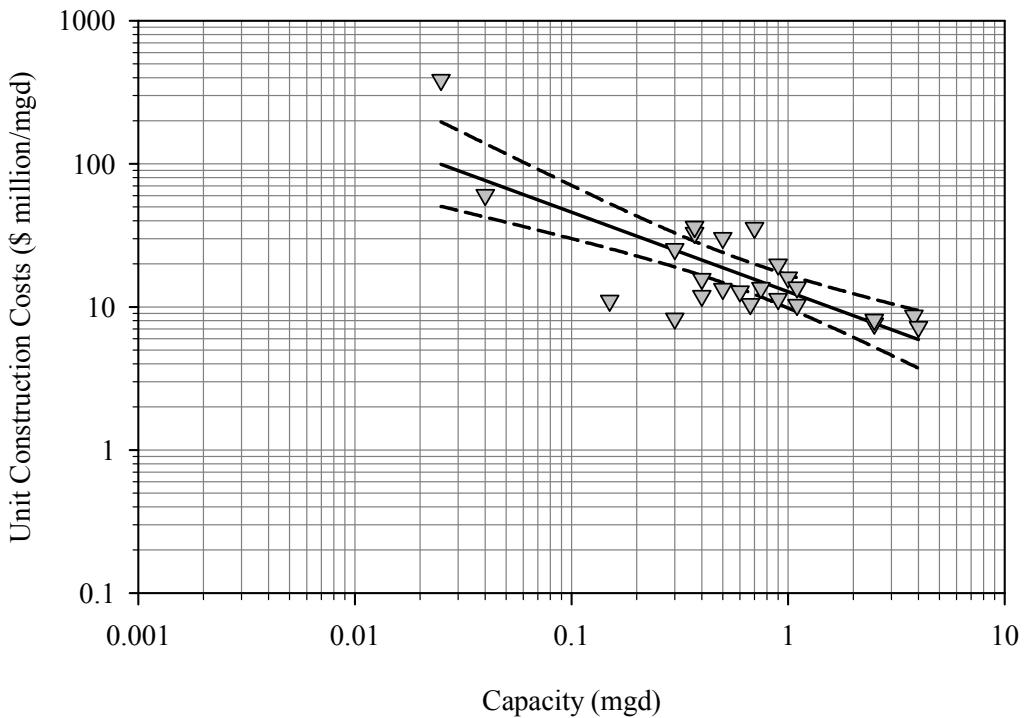


Figure 4.17. Unit construction costs of MBRs.
Solid line, regression line; dash lines, 95% confidence intervals.

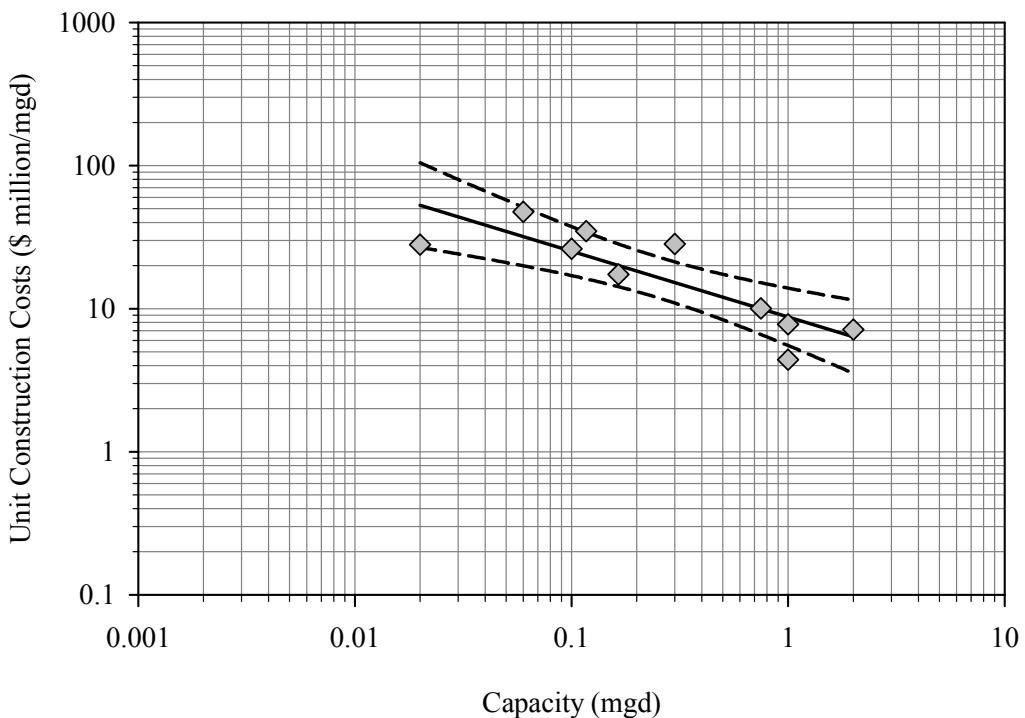


Figure 4.18. Unit construction costs of ponds.
Solid line, regression line; dash lines, 95% confidence intervals.

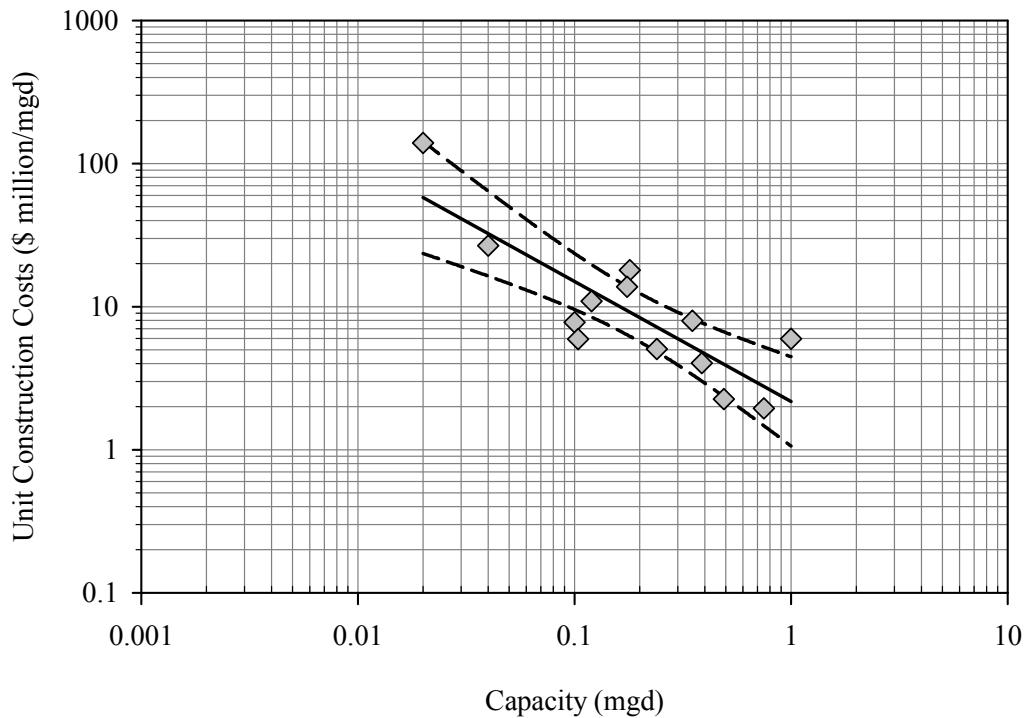


Figure 4.19. Unit construction costs of lagoons.
Solid line, regression line; dash lines, 95% confidence intervals.

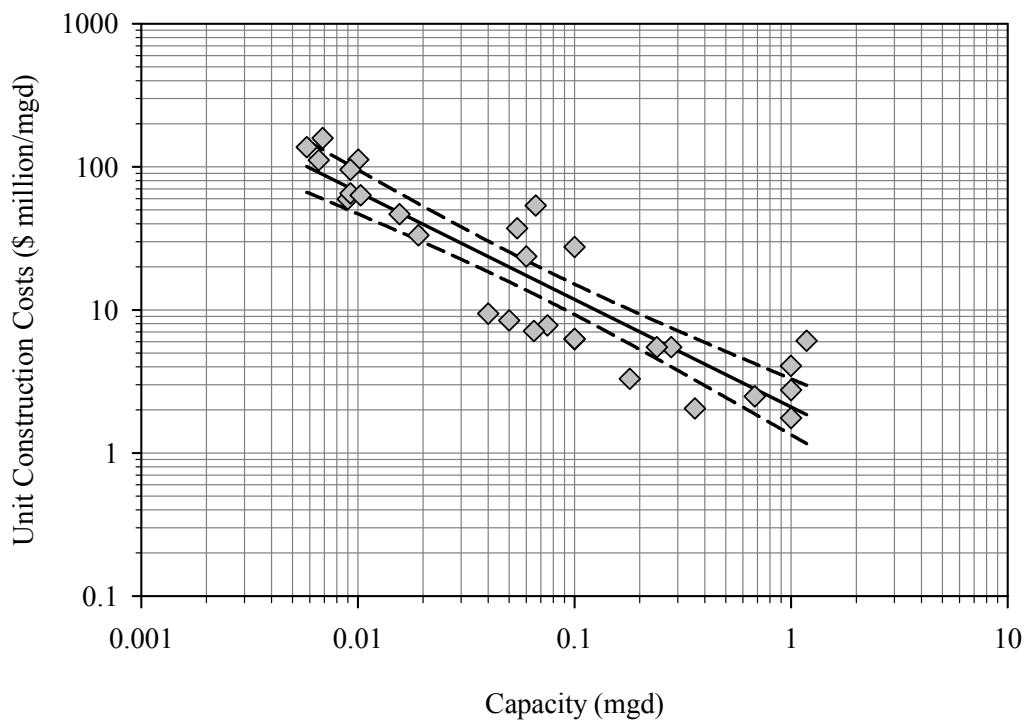


Figure 4.20. Unit construction costs of wetlands.
Solid line, regression line; dash lines, 95% confidence intervals.

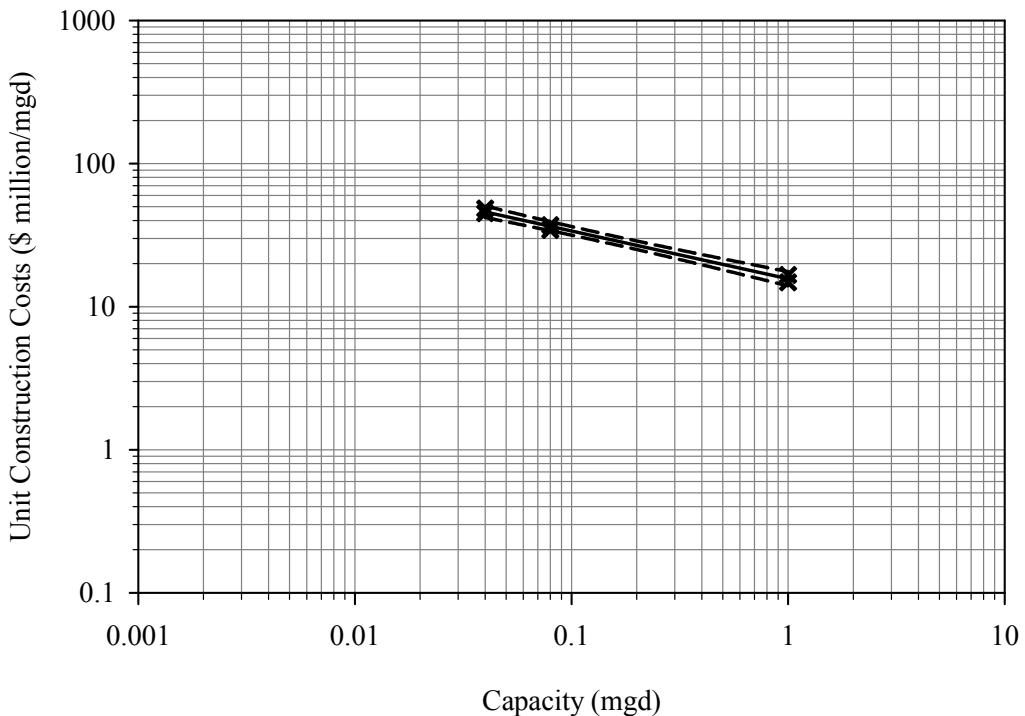


Figure 4.21. Unit construction costs of LMs.
Solid line, regression line; dash lines, 95% confidence intervals.

4.2.3. Comparison of Unit Construction Costs

The cost curves were segregated based upon treatment technology. Unit construction costs were compared for each category.

- Figure 4.22 indicates that conventional customized plants and conventional package plants have similar unit construction costs.
- Figure 4.23 shows that membrane customized plants are more expensive than conventional customized plants.
- Figure 4.24 indicates that natural systems are less expensive than are conventional customized plants.
- Figure 4.25 shows that alternative treatment systems (in this case the LM natural system) are more expensive than conventional customized plants.
- Figure 4.26 indicates that membrane customized plants and alternative treatment systems (in this case, the LM natural system) have similar unit construction costs.

In summary, the unit construction costs of natural systems were the least expensive, followed by similar costs for conventional package plants and conventional customized plants, while alternative treatment systems and membrane customized plants were the most expensive.

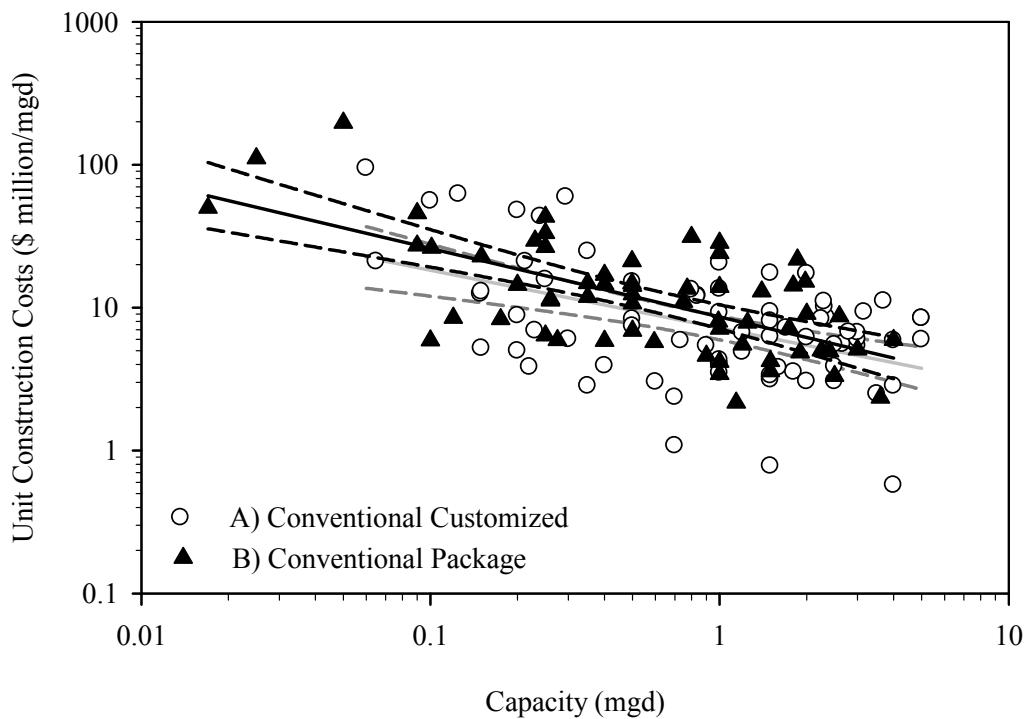


Figure 4.22. Comparison of unit construction costs of conventional customized plants and conventional package plants.
Solid lines, regression lines; dash lines, 95% confidence intervals.

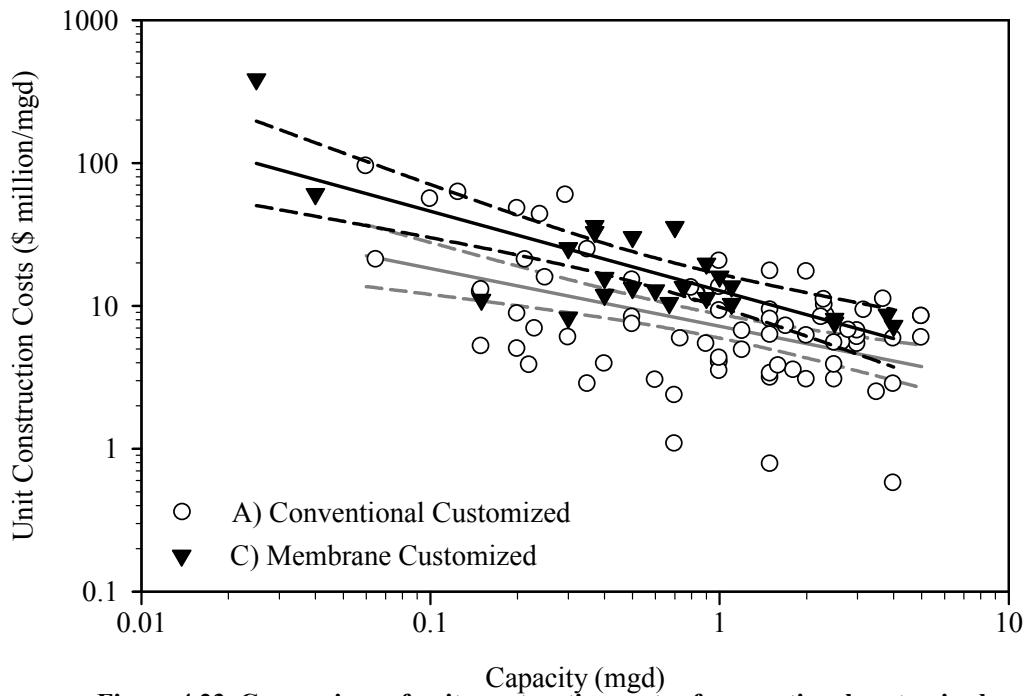


Figure 4.23. Comparison of unit construction costs of conventional customized plants and membrane customized plants.
Solid lines, regression lines; dash lines, 95% confidence intervals.

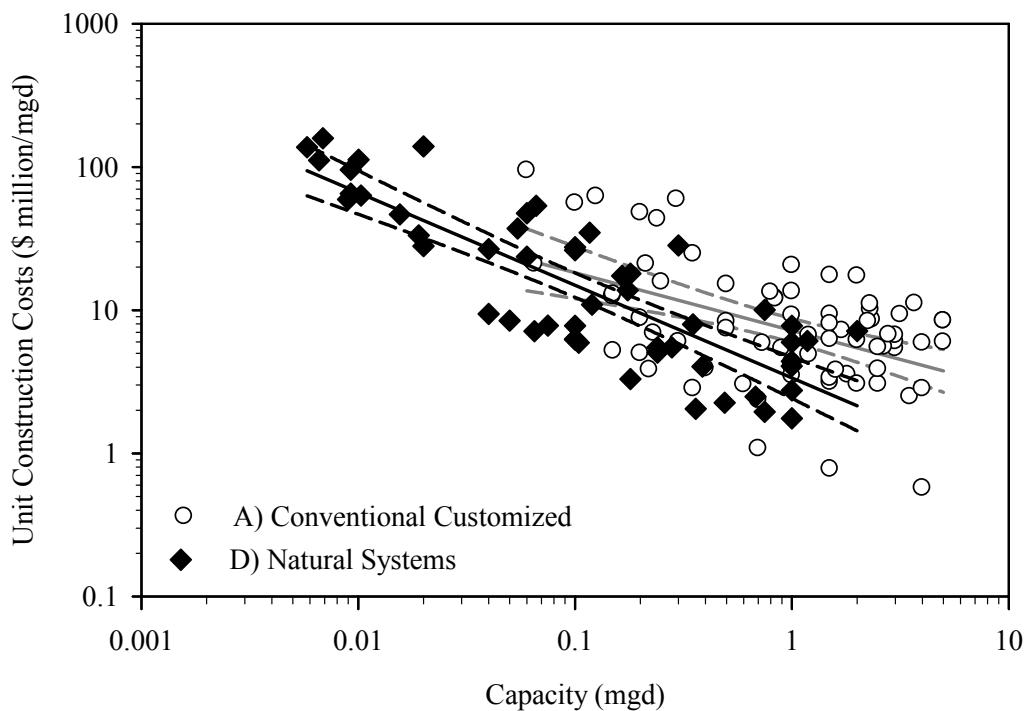


Figure 4.24. Comparison of unit construction costs of conventional customized plants and natural systems.
Solid lines, regression lines; dash lines, 95% confidence intervals.

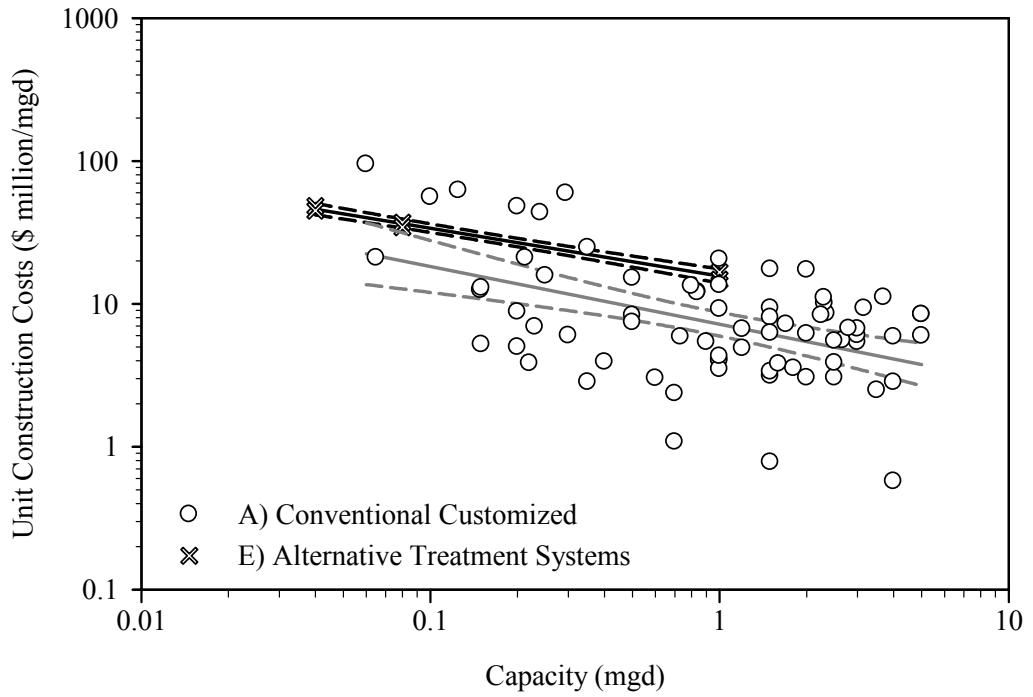


Figure 4.25. Comparison of unit construction costs of conventional customized plants and alternative treatment systems.
Solid lines, regression lines; dash lines, 95% confidence intervals.

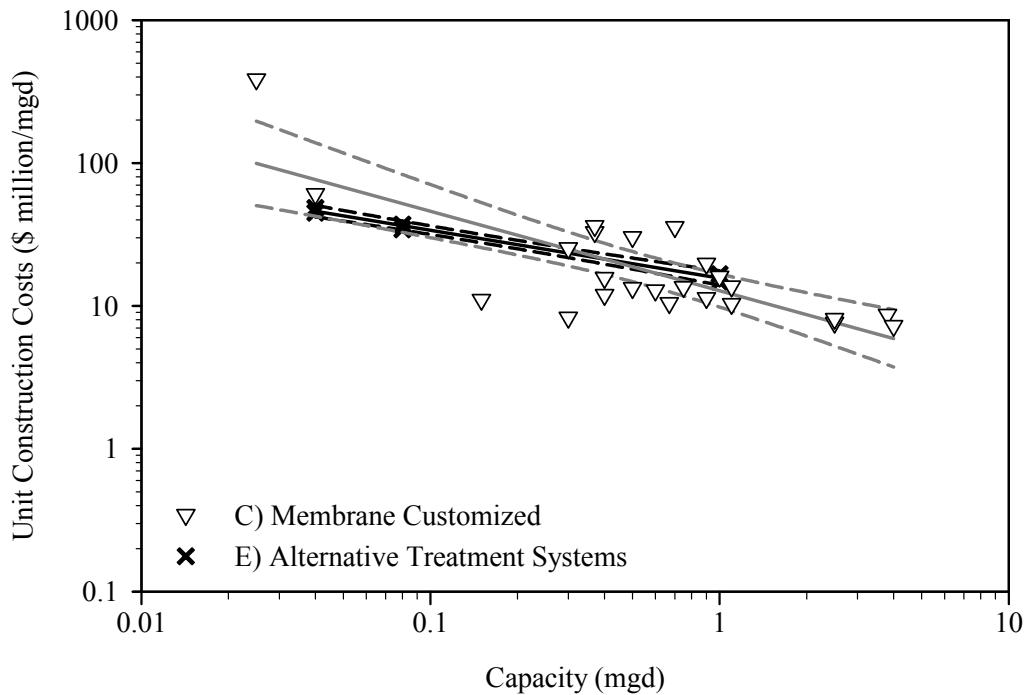


Figure 4.26. Comparison of unit construction costs of membrane customized plants and alternative treatment systems.
Solid lines, regression lines; dash lines, 95% confidence intervals.

4.2.4. General Trend of O&M Costs and Capacities

The data plots or cost curves of total O&M costs and unit O&M costs versus capacity are shown in Figures 4.27 and 4.28. Regression lines, 95% confidence intervals, and 95% prediction intervals are also shown in these figures. Please note that the regression lines are developed only to show the general trend of O&M costs and capacities for all evaluated technologies in this report. The authors of this report recommend site-specific analysis for the basis for engineering costing of new water reuse facilities.

The general trend is that lower-flow systems have a higher unit O&M cost, possibly because of economies of scale for O&M and/or possibly because of “soft” cost issues.

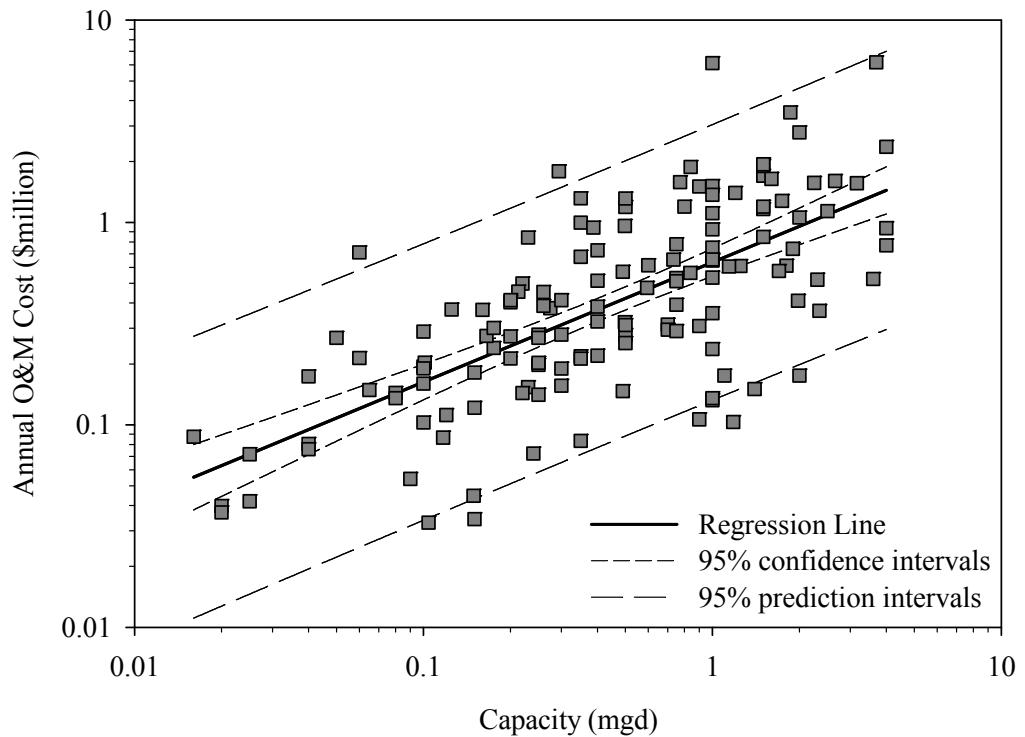


Figure 4.27. Total annual O&M costs.

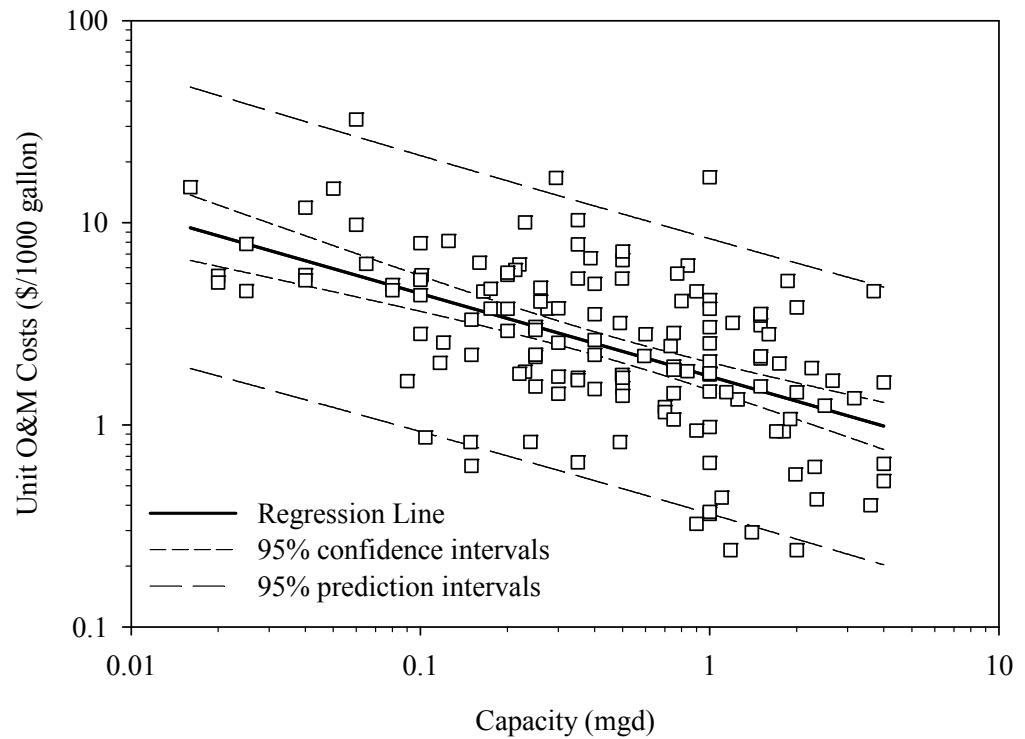


Figure 4.28. Unit O&M costs.

4.2.5. Comparison of Unit O&M Costs

The unit O&M costs are compared among the treatment plants.

- Figure 4.29 indicates that conventional customized plants and conventional package plants have similar unit O&M costs.
- Figure 4.30 shows that conventional customized plants and membrane customized plants also have similar unit O&M costs.
- Figure 4.31 suggests that natural systems and conventional customized plants have similar unit O&M costs.
- Figure 4.32 indicates that conventional customized plants and alternative treatment plants have similar unit O&M costs.

In total, these results show that all systems have similar unit O&M costs.

Please note that the O&M costs include only limited costs for energy consumption, materials, labor, testing, chemicals, and sludge handling. Other specific costs for membrane customized systems such as the costs for replacing membranes and oscillating valves are not available and therefore are not included in this analysis. These additional costs could increase the O&M costs of membrane customized systems significantly, so detailed analysis of these costs is necessary for a more accurate cost estimation.

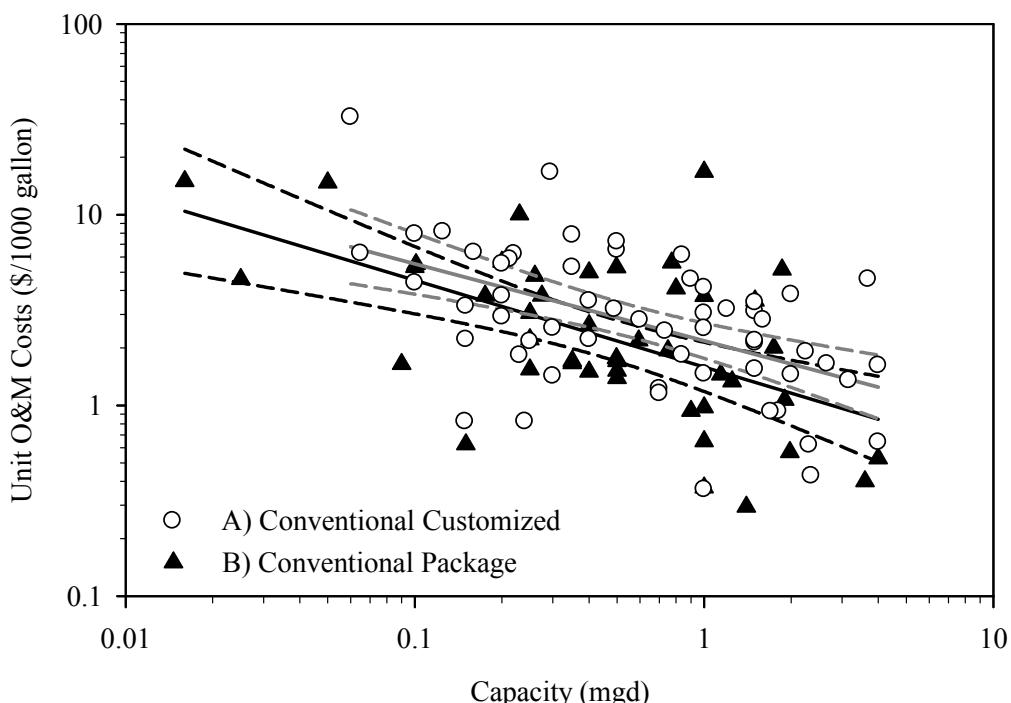


Figure 4.29. Comparison of unit O&M costs of conventional customized plants and conventional package plants.
Solid lines, regression lines; dash lines, 95% confidence intervals.

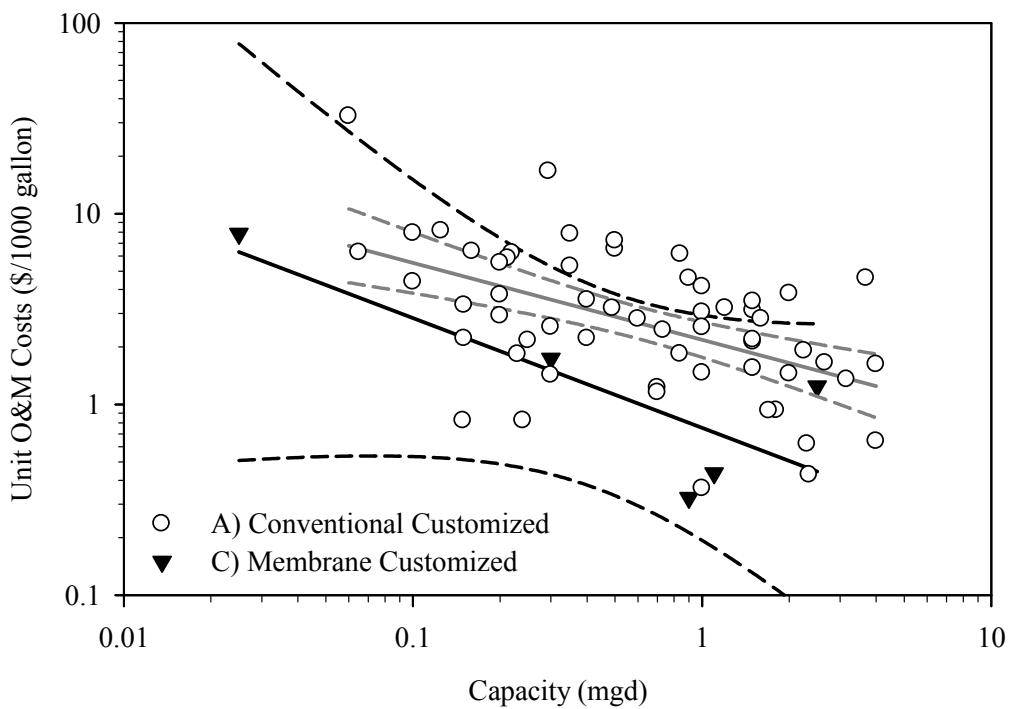


Figure 4.30. Comparison of unit O&M costs of conventional customized plants and membrane customized systems.
Solid lines, regression lines; dash lines, 95% confidence intervals.

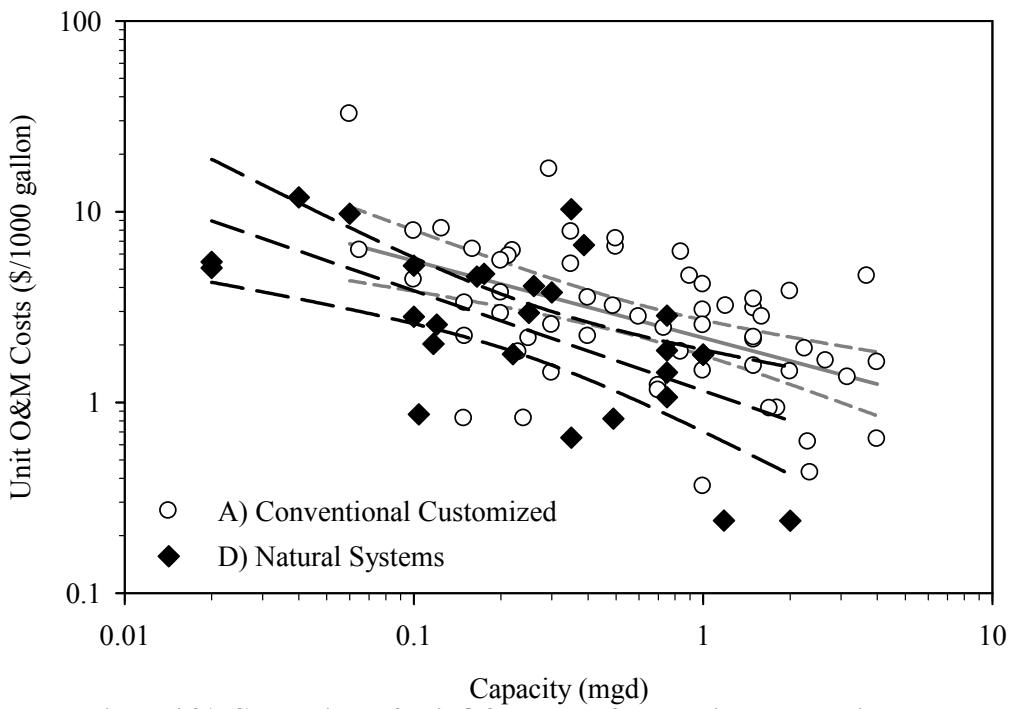


Figure 4.31. Comparison of unit O&M costs of conventional customized plants and natural systems.
Solid lines, regression lines; dash lines, 95% confidence intervals.

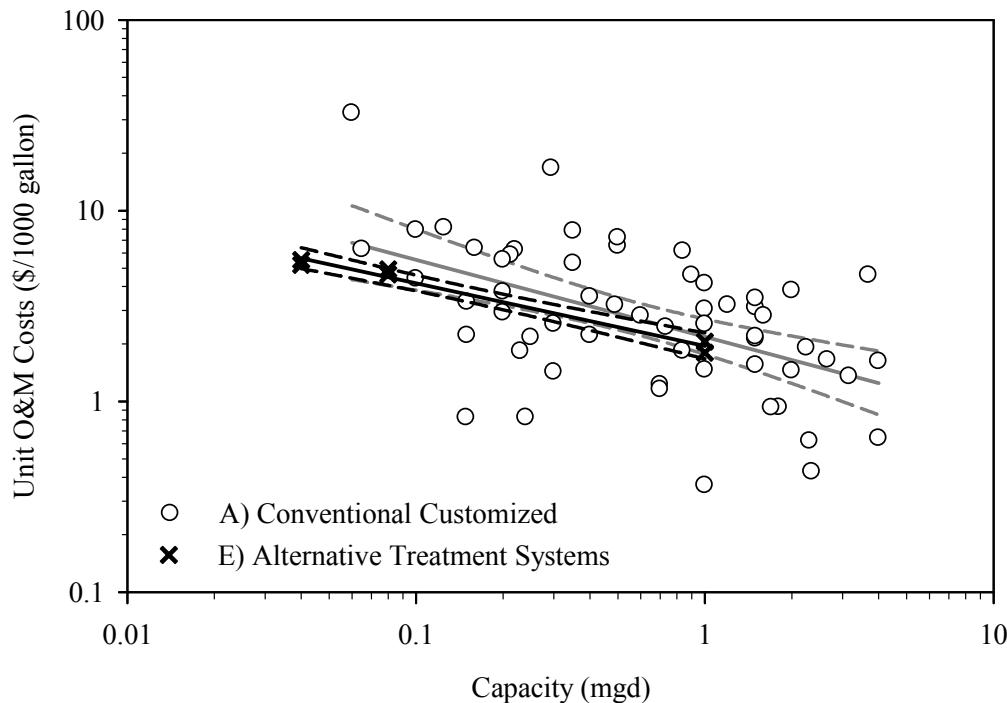


Figure 4.32. Comparison of unit O&M costs of conventional customized plants and alternative treatment systems.
Solid lines, regression lines; dash lines, 95% confidence intervals.

4.2.6. Comparison of Unit Present Value Costs

The unit present value costs of the different treatment systems are compared.

- Figure 4.33 indicates that conventional customized plants and conventional package plants have similar unit present value costs.
- Figure 4.34 shows that conventional customized plants and membrane customized plants also have similar unit present value costs.
- Figure 4.35 indicates that natural systems are less expensive than conventional customized plants.
- Figure 4.36 suggests that conventional customized plants and alternative treatment plants have similar unit present value costs.

These results show that the unit present value costs of natural systems were the lowest, while all other systems have similar unit present value costs.

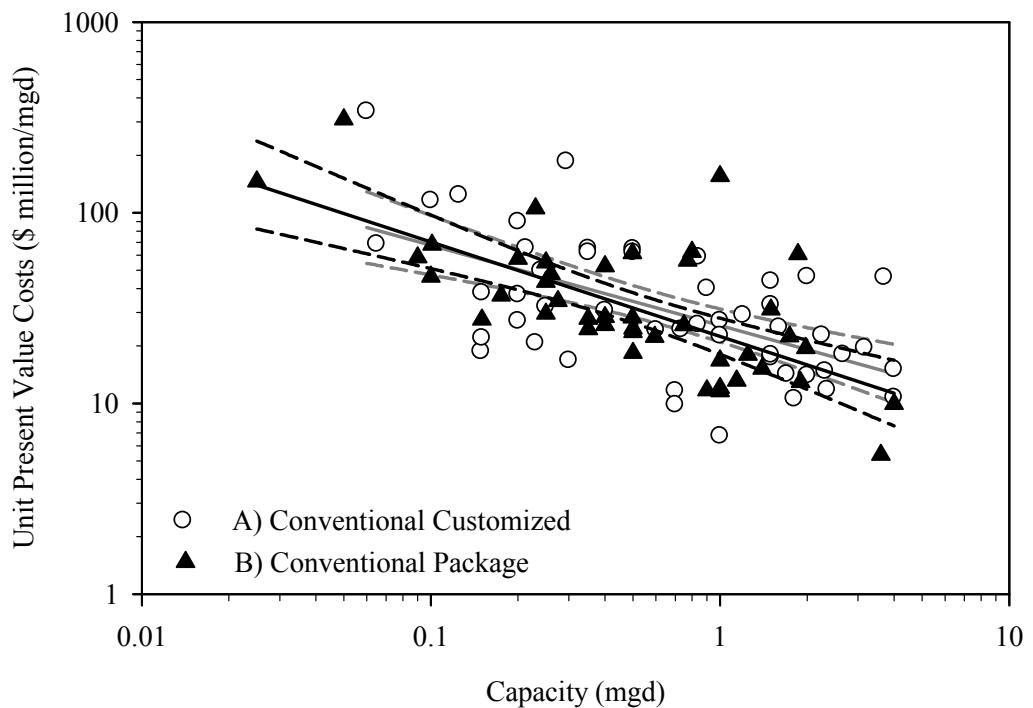


Figure 4.33. Comparison of unit present value costs of conventional customized plants and conventional package plants.
Solid lines, regression lines; dash lines, 95% confidence intervals.

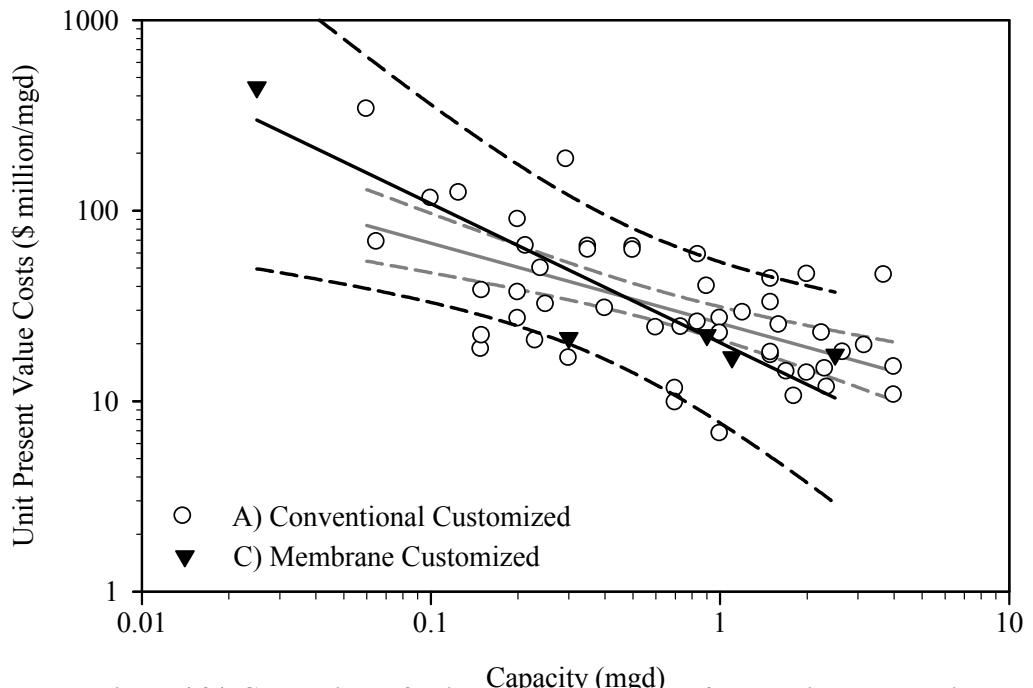


Figure 4.34. Comparison of unit present value costs of conventional customized plants and membrane customized plants.
Solid lines, regression lines; dash lines, 95% confidence intervals.

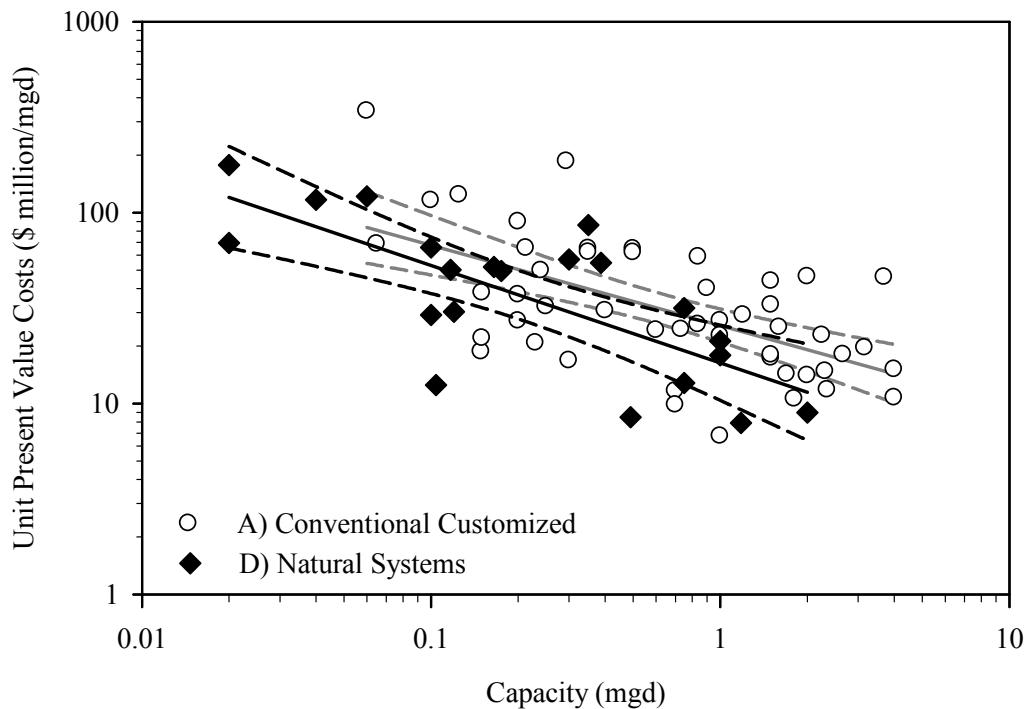


Figure 4.35. Comparison of unit present value costs of conventional customized plants and natural systems.

Solid lines, regression lines; dash lines, 95% confidence intervals.

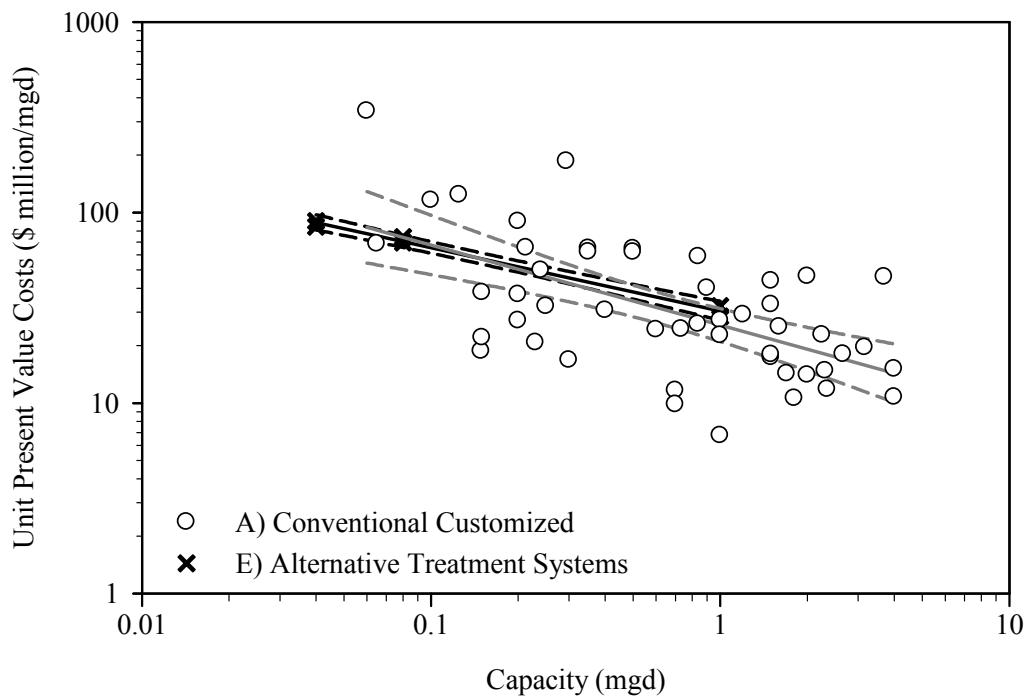


Figure 4.36. Comparison of unit present value costs of conventional customized plants and alternative treatment systems.

Solid lines, regression lines; dash lines, 95% confidence intervals.

4.2.7. Comparison of Effluent Water Quality

The effluent water quality (BOD_5), TSS, TN, and total phosphorus (TP) of natural systems were lower than those of other plants and systems (Figure 4.37). Other systems were similar in effluent water quality, while membrane customized plants were cleaner than conventional systems. A detailed comparison of each subcategory of the treatment processes shows a similar conclusion (Figure 4.38).

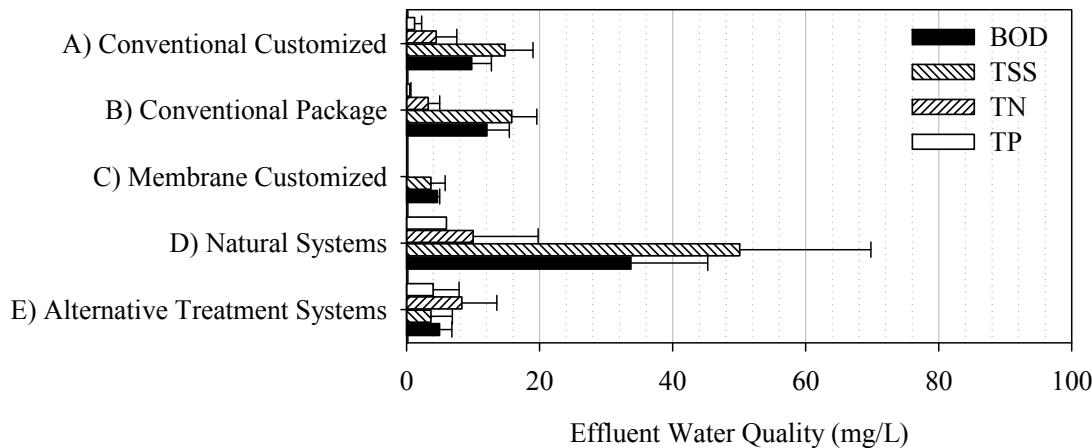


Figure 4.37. Comparison of effluent water quality.

Error bars stand for 95% confidence intervals.

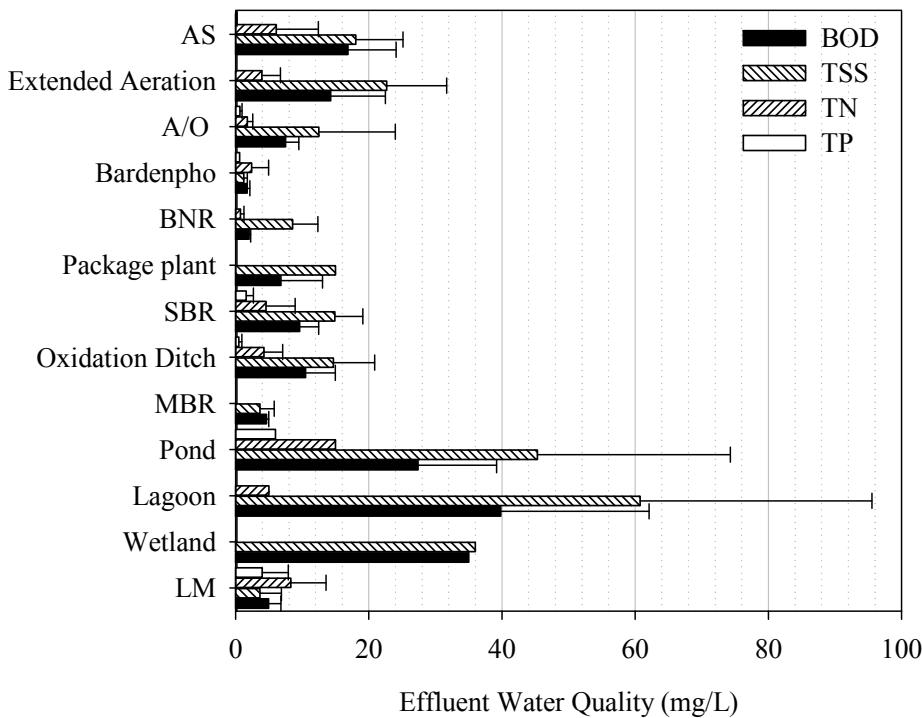


Figure 4.38. Detailed comparison of effluent water quality of each subcategory.

Error bars stand for 95% confidence intervals.

The removal efficiency of natural systems and alternative treatment systems was lower than those of other plants and systems (Figure 4.39). Other systems were similar in removal efficiency. A detailed comparison of each subcategory of the treatment processes shows a similar conclusion (Figure 4.40).

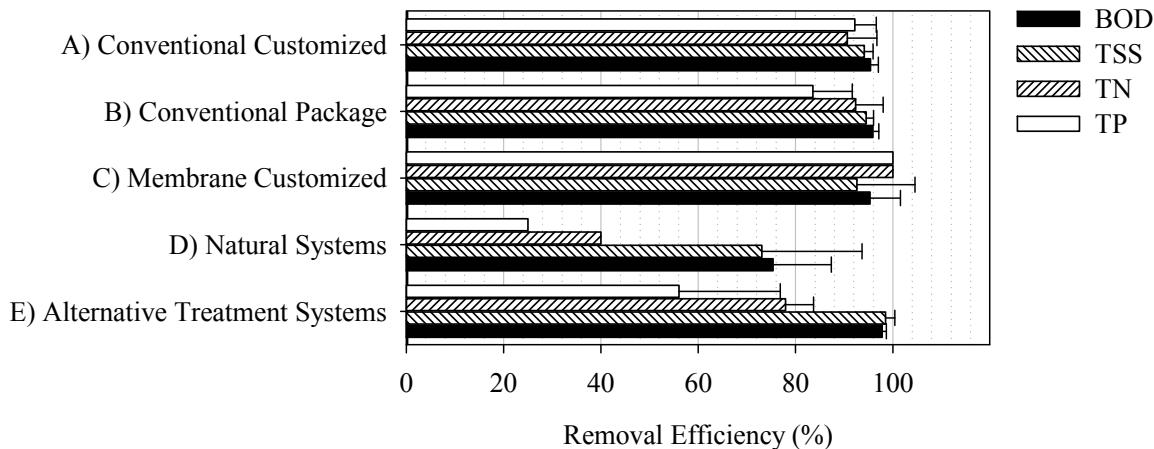


Figure 4.39. Comparison of removal efficiency.
Error bars stand for 95% confidence intervals.

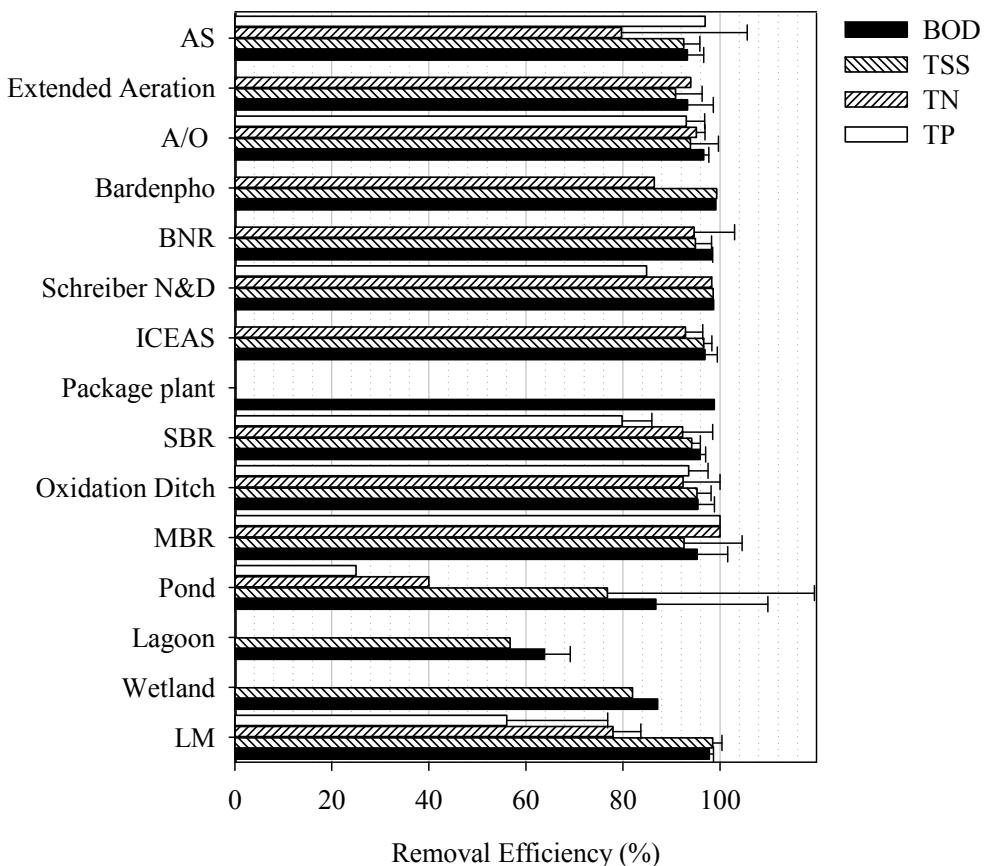


Figure 4.40. Detailed comparison of removal efficiency of each subcategory.
Error bars stand for 95% confidence intervals.

CHAPTER 5

THE WAWTTAR MODEL

The information on treatment processes and cost information results have been incorporated into the WAWTTAR model. The WAWTTAR model can be found at <http://firehole.humboldt.edu/wawttar/>. This website also contains a detailed user manual, some of which is repeated here.

5.1. INTRODUCTION TO WAWTTAR

WAWTTAR is a tool to assist in the planning and implementation of water and wastewater treatment systems, including treatment systems incorporating water reuse. The program was designed to be used at the pre-feasibility step in facility planning and/or infrastructure investment. The initial development goal was to develop a planning tool that could be used by both donors and beneficiaries of waste/wastewater infrastructure investments to maximize cultural acceptance of the facility and thereby minimize the risk of financial and technological failure. The program has an extensive database of water and wastewater treatment processes (over 200, all user expandable), on-site/decentralized waste and wastewater treatment processes, and a range of collection systems. The process database includes removal efficiencies, resource requirements, bases for design, color photographs, line drawings, and referenced text files. The process can be used to formulate a wide range of treatment systems (treatment trains).

WAWTTAR is a predictive model intended to assist planners in selecting suitable water and wastewater treatment options appropriate to the material and manpower resources available to particular communities throughout the world. The localized performance and cost of a large number of possible systems can be estimated with WAWTTAR for locations and conditions for which basic information on the problem to be solved is available. For example, decentralized on-site systems can be compared with centralized collection and treatment systems. WAWTTAR is designed to assist in alleviating the problem of overlooking good processes for water and wastewater treatment and also to help screen out treatment technologies which are inappropriate for given locales and situations. The selection of inappropriate technologies often results in facilities that perform poorly and fall into disrepair due to a lack of basic resources such as spare parts, O&M personnel, and technical expertise. It is hoped that design errors of this kind can be significantly reduced or eliminated via the use of WAWTTAR. WAWTTAR is designed to be used by those with some technical background in water and wastewater treatment.

WAWTTAR's main use is to screen and research possible water and wastewater treatment options, with emphasis placed on options that incorporate water reuse. (WAWTTAR does not exclude more conventional options and is of equal usefulness in the screening and research of such options.) It is intended to assist planners to improve their strategies for water and wastewater treatment in most locations and under local conditions. It will not choose the "best" possible option for a given situation, which can be done only by using solid engineering judgment. It can, however, be used to evaluate many more systems than would ordinarily be possible on the basis of performance and cost-effectiveness and therefore facilitate the selection of sensible options. WAWTTAR is not a dynamic program and does

not analyze the response of a given system to changing influent conditions. Such issues must be explored by multiple trials of treatment systems with different influent quality.

5.2. WAWTTAR COMPONENTS

The program consists of four databases, an editor to create treatment trains, an editor to describe a community, and a calculator to sort the treatment processes through the community descriptors, receiving water standards, and reuse standards. The four databases are wastewater (including on-site) processes, water treatment processes, collection systems, and water quality standards. All databases can be edited to update and/or to add or delete information.

The water quality standard database contains a collection of U.S. and international potable and wastewater discharge and reuse standards. Each standard can specify a minimum and/or maximum concentration for any of nearly 100 water quality constituents. The user can enter new or modified standards in just a few moments if no existing standard in the database is appropriate for the problem under consideration.

The collection system database contains a number of conventional and alternative wastewater collection systems. Each collection system is characterized by text information describing the technology, pictures and line drawings of components of the collection system, and cost curves that relate the cost per capita to the population density of the community.

The water and wastewater treatment databases share a common structure. The main purpose of the process database is to provide information on the capabilities, physical and cultural limitations, costs, resource requirements, and possible environmental impacts of water and wastewater treatment and reuse processes. Cultural limitations and environmental impacts are also of prime importance and, unlike many facility planning efforts, are given attention equal to that of economic and performance factors. Cultural limitations are significant for the reasons discussed previously—a treatment technology which is in conflict with cultural norms of a given location is of little use. Environmental impacts are important since water and wastewater treatment systems have by-products and influence local conditions. It is important to avoid substituting one set of environmental problems for another, such as a wastewater treatment process that negatively impacts groundwater wells because of by-products and hydrological conditions. Alternatively, some processes such as constructed wetlands can have beneficial environmental impacts, and scenarios exist where such possible benefits should be taken into account in a positive sense.

While the editor for the process database is easy to use, detailed knowledge of a treatment process is required to enter a new process or edit an existing one. WAWTTAR uses a curve fit of land requirements, construction costs, and O&M costs and performance vs. process loading (hydraulic, organic, or solids) to perform calculations. Cost breakdowns are to localize construction and O&M costs for a particular community. The construction cost for each process is divided into categories of labor, earthwork, manufactured equipment, structures, concrete, steel, and pipes/valves/instruments. O&M cost categories are labor, chemicals, materials, and energy and land requirements. These must be included in any treatment process data file. Information on treatment processes can come from USEPA documents, technical reports, manufacturers, and practical experience as developed or reported by private and public agencies. In addition to the technical data described above,

sufficient reference material (text, photos, and line drawings) is provided for each process so that WAWTTAR can serve as an educational tool for engineers and community planners.

The treatment processes are joined together into treatment trains representing logical assemblies of processes to treat water or wastewater. While a number of treatment trains are preassembled, a train editor is provided so that the user can easily construct new trains or modify existing trains that might be worthy of consideration for the problem under study. The treatment trains are assembled in a “point and click” fashion from the list of processes in the treatment process database.

An editor is also provided to enter the community under consideration into the community database. The community database contains previously analyzed problems and a comprehensive list of questions intended to describe the relevant characteristics of the community in question. These questions include water demand, wastewater production, resource cost and availability, the presence or absence of institutional support, population characteristics, and various cultural factors which could affect the handling of waste.

The availability and cost of resources can dramatically affect the feasibility of treatment and reuse options from construction to everyday O&M. Resources in this case include the type and reliability of power supply, manpower ranging from simple unskilled labor to technical and professional personnel, a list of treatment chemicals that are readily available, and any other type of human or physical capital that might be necessary.

5.3. WAWTTAR OPERATION

The basic operation of WAWTTAR is as follows: problem parameters such as performance standards, material costs, raw water or wastewater quality, community needs and capabilities, and planning horizon are entered by the user into the community database. The user can then proceed using the existing list of treatment trains, or the user can construct several additional treatment trains from a supplied, comprehensive list of available treatment processes. The user also specifies whether the calculation of treatment process performance should be based on the maximum efficiency, the minimum efficiency, or the mean efficiency. The user then instructs WAWTTAR to find feasible and infeasible treatment trains from the list of potential trains.

WAWTTAR first screens these potential trains based on community resource availability, followed by social and cultural considerations, treatment process limitations, reuse quality limitations (if reuse has been specified), and finally effluent disposal quality (water quality standards). This screening process for selecting feasible treatment trains is illustrated in Figure 5.1. Treatment trains that fail any of the screening criteria are classified as infeasible treatment trains and are eliminated from further consideration. WAWTTAR then calculates the performance, construction costs, and O&M costs of the remaining feasible treatment systems based on simple mathematical models of each of the treatment processes. Feasible treatment trains are sorted based on a user-specified criterion of minimum capital cost, minimum O&M cost, or minimum total cost.

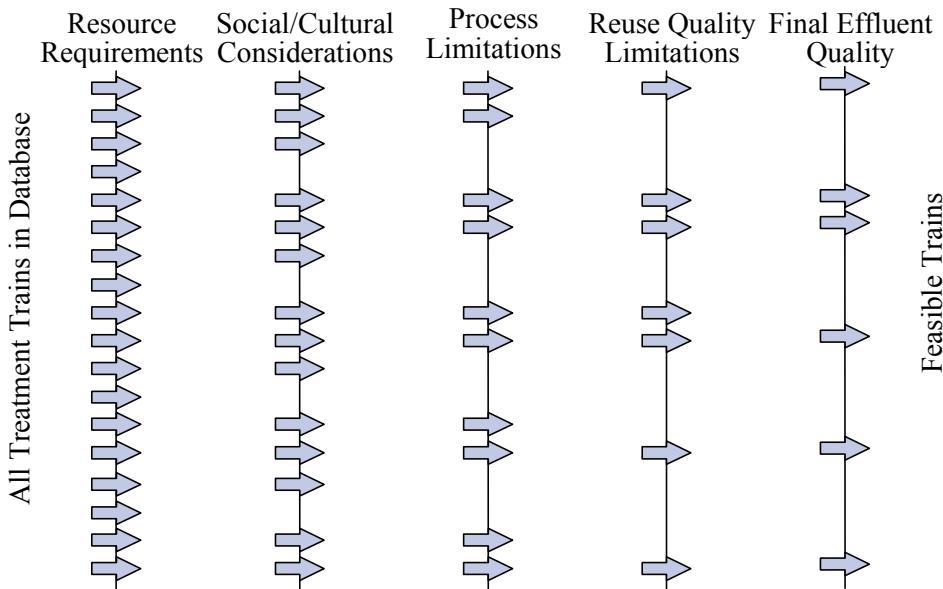


Figure 5.1. Screening process used to identify feasible treatment trains in WAWTTAR.

5.4. WAWTTAR OUTPUT

Any treatment train that fails the screening criteria established by the user is classified as infeasible, and entries are made in the “Infeasible Solution File.” The Infeasible Solution File is an output text file that contains general design criteria for the community (planning period, design population, design flow, and effluent standard) and information on what screening criterion was not met by the treatment train. Frequently, review of why a train was classified as infeasible yields important insight into the current problem and design process. Therefore, the user is encouraged to examine and potentially re-evaluate problem specifications after consideration of the material available in the Infeasible Solution File.

Information detailing the cost and performance of feasible treatment trains is output to the Feasible Solution File. This text file again contains the general design criteria for the problem, followed by a detailed accounting of capital cost, O&M cost, land requirements, and land cost for each process in each feasible train. The total cost for the train, total per capita cost, and total cost per dwelling for each treatment train also are supplied. All costs are reported based on a user-specified choice of annual or total project costs. An adaptability index, ranging from 0 to 3, which rates the adaptability of each train to upgrading and which provides for variation in hydraulic loading and changes in influent quality, is also reported. Final effluent quality for each of up to 10 user-specified water quality constituents is reported for each train. Finally, potential social and environmental impacts for each feasible treatment train are reported as code numbers that are explained at the end of the file. After the listing of information on each feasible treatment train, the trains are presented in a table in ranked order. As noted earlier, the user can specify rank criteria of minimum capital cost, minimum O&M cost, or minimum total project cost.

5.5. WAWTTAR APPLICATION

WAWTTAR has been used in a wide range of communities including Jamaica (semirural setting), Bulgaria (municipal/industrial setting), the West Bank and Gaza (municipal and periurban setting), Koror (Palau), Brazil, two small communities in Hawaii, and a number of small to medium-sized communities in California, Oregon, Washington, Idaho, and Arizona. Validation exercises to date have shown that the program is sensitive to the range of environmental, economic, and social conditions considered in the program design. All applications have found WAWTTAR to be a useful tool for the pre-feasibility stage of the wastewater facility planning process. The program is also being used in a number of universities in the United States as part of the curriculum in water and wastewater engineering. WAWTTAR and associated documentation can be freely downloaded from the WAWTTAR website at <http://firehole.humboldt.edu/wawttar>.

5.6. INCORPORATING NEW TREATMENT PROCESS COST DATA INTO WAWTTAR

The building blocks of the treatment trains compared by WAWTTAR are individual treatment processes. Realistic construction and O&M costs for commonly used treatment processes are needed to allow a meaningful evaluation of the appropriateness and cost-effectiveness of a treatment train. The majority of cost data currently provided in WAWTTAR are from USEPA sources and generally are for facilities with a design flow rate greater than 1 mgd. In addition, many of the data are over 15 years old and do not include some of the new technologies in common use today. Cost information collected as part of this research activity fills a big gap in the existing database by providing a source of contemporary data for small treatment facilities. Data on the cost of individual treatment processes collected during this project have been evaluated for inclusion into the WAWTTAR construction and O&M cost curves. In some cases, the new data have filled in a missing region on an existing cost curve. In other cases, the new data have been averaged along with existing data to improve the reliability of the existing cost curve. In a couple of cases, the new data have completely replaced existing cost information since they were judged to be more representative of existing construction practices. While the process of incorporating new data into WAWTTAR is ongoing as new cost information continues to trickle in, a new version of the WAWTTAR database will be made available soon for download from the WAWTTAR website (<http://firehole.humboldt.edu/wawttar/>). The new version of the database will contain not only the new cost data collected as part of this project but also a number of treatment trains containing treatment processes appropriate for small communities which plan on reusing the effluent.

CHAPTER 6

CONCLUSIONS

The treatment trains reviewed for this project include a range of conventional, advanced, and alternative treatment plants and systems. The costs span a range of flows, allowing for water reuse treatment costs to be quickly estimated.

The primary value of this work is the extensive cost database, where the cost and operation data from existing small-scale wastewater treatment and water reuse facilities have been gathered and synthesized.

The selection of small-scale reclamation systems will depend on many factors, such as the type of reuse application, regulations, availability of land, the budget, and staffs. Based on the results of this project, natural systems may be the most cost-effective solution for small communities if inexpensive land is available and effluent water can fulfill the local regulations. If high water quality is desired and a budget is available, conventional customized systems can be used. Membrane customized systems can be used if even higher water quality is needed. For example, membrane systems can provide increased removal of trace organics (microconstituents) and provide a pathogen barrier that nonmembrane systems cannot attain.

The data within this project can be mined for specifically relevant applications, based upon the type of recycled water use and the guiding regulations at the point of use. For example, treatment plants not needing filtration and high levels of disinfection would reduce costs compared to the values shown here.

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APPENDIX A

SUMMARIZED STATE GUIDELINES AND REGULATIONS FOR RECLAIMED WATER

Table A. Summarized Guidelines and Regulations for Reclaimed Water

State	Treatment Standards nitrogen < 10 mg/L. Disinfection Standards coliform bacteria < 1/100 mL (maximum).	Treatment Standards, Disinfection Standards, and Design Requirements
Alabama		Treatment Standards from source other than stabilization pond: TSS: arithmetic mean < 30 mg/L (30 days), < 45 mg/L (7 days), < 60 mg/L (1 day); from source at a stabilization pond: < 70 mg/L (30 days); Disinfection Standards from source other than stabilization pond: BOD: arithmetic mean < 30 mg/L (30 days), < 45 mg/L (7 days), < 60 mg/L (1 day); from source at a stabilization pond: < 45 mg/L (30 days) and > 65% removal by weight, < 65 mg/L (7 days); pH 6–9.
Alaska		Treatment Standards Class A+: turbidity: <= 2 NTU (24-h average), <= 5 NTU (maximum), nitrogen < 10 mg/L (5-sample geometric mean); Class A: turbidity: <= 2 NTU (24-h average), <= 5 NTU (maximum); Class B+: nitrogen < 10 mg/L (5-sample geometric mean); Class C: total retention time in wastewater stabilization ponds > 20 days. Disinfection Standards Class A+, Class A: fecal coliform not detectable in 4 of the last 7 samples (average), < 23/100 mL (maximum); if alternative treatment processes or alternative turbidity criteria are used or if reclaimed water is blended with other water, there is no detectable enteric virus in 4 of the last 7 monthly reclaimed water samples; Class B+, Class B: fecal coliform < 200/100 mL in 4 of the last 7 samples (average), < 800/100 mL (maximum); Class C: fecal coliform < 1000/100 mL in 4 of the last 7 samples (average), < 4000/100 mL (maximum).
Arizona		Design Requirements The minimum chlorine contact time is 15 min for wastewater at 70 °F and 30 min for wastewater at 50 °F, based on a flow equal to four times the daily design flow; required concentration of chlorine (TSS < 30 mg/L and BOD ₅ < 30 mg/L): 15–30 (pH 6), 20–35 (pH 7), 30–45 (pH 8); required concentration of chlorine (TSS < 20 mg/L and BOD ₅ < 20 mg/L): 6–10 (pH 6), 10–20 (pH 7), 20–35 (pH 8).

Table A. Summarized Guidelines and Regulations for Reclaimed Water

State	Treatment Standards, Disinfection Standards, and Design Requirements	
	Treatment Standards turbidity: <= 2 NTU (24-h average), <= 5 NTU (5% in 24 h), < 10 NTU (maximum) (coagulated and passed through natural undisturbed soils or a bed of filter media); or < 0.2 NTU (5% of 24 h) and < 0.5 NTU (maximum) (MF, UF, NF, or RO membrane).	
	Disinfection Standards	
California	Disinfected Tertiary Recycled Water: total coliform < 2.2 MPN/100 mL in 7 days (median), only one sample > 23 MPN/100 mL in 30 days, none > 240 MPN/100 mL in 30 days; Disinfected Secondary-2.2 Recycled Water: total coliform < 2.2 MPN/100 mL in 7 days (median), only one sample > 23 MPN/100 mL in 30 days; Disinfected Secondary-23 Recycled Water: total coliform < 23 MPN/100 mL in 7 days (median), only one sample > 240 MPN/100 mL in 30 days.	
	Design Requirements	
	Disinfected Tertiary Recycled Water: (1) A chlorine disinfection process following filtration that provides a CT value >= 450 mg-min/L at all times with a modal contact time of at least 90 min, based on peak dry weather design flow; or (2) a disinfection process that, when combined with the filtration process, has been demonstrated to inactivate and/or remove 99.999% of the PFU of F-specific bacteriophage MS2 or poliovirus in the wastewater. A virus that is at least as resistant to disinfection as poliovirus is may be used for purposes of demonstration.	
	Treatment Standards	
	Category 1: TSS < 30 mg/L (daily maximum); Category 2, Category 3: turbidity: <= 3 NTU (monthly average), <= 5 NTU in more than 5% of the individual analytical results during any calendar month.	
	Disinfection Standards	
Colorado	Category 1, Category 2: <i>E. coli</i> < 126/100 mL (monthly geometric mean), < 235/100 mL (maximum); Category 3: <i>E. coli</i> below detection limit in at least 75% of samples in a calendar month, < 126/100 mL (maximum).	
	Design Requirements	
	Section 5.16.0 (Disinfection), 5.16.1 (Chlorination and Dechlorination), 5.16.2 (UV Disinfection), 5.16.3 (Ozone Disinfection) of Policy 96-1 - Design Criteria Considered in the Review of Wastewater Treatment Facilities.	
	Treatment Standards	
	Restricted Public Access Sites: TSS < 50 mg/L (mechanical systems), < 90 mg/L (ponds), BOD < 50 mg/L (average), < 75 mg/L under peak loads;	
	Limited Public Access Sites: TSS < 30 mg/L, BOD < 30 mg/L;	
	Unlimited Public Access Sites: turbidity < 5 NTU, TSS < 10 mg/L, BOD < 10 mg/L.	
	Disinfection Standards	
Delaware	Restricted Public Access Sites: fecal coliform < 200/100 mL (maximum), disinfection requirements may be waived when wastewater is irrigated in remote or restricted-use sites such as forests;	
	Limited Public Access Sites: fecal coliform < 200/100 mL (maximum);	
	Unlimited Public Access Sites: fecal coliform < 20/100 mL (maximum).	

Table A. Summarized Guidelines and Regulations for Reclaimed Water Treatment Standards, Disinfection Standards, and Design Requirements

State	Treatment Standards	Disinfection Standards	Design Requirements
Florida	<p>Basic disinfection: TSS < 10 mg/L, BOD < 20 mg/L (annual arithmetic mean), <30 mg /L (4 samples in a month), <45 mg /L (7 samples in a month), < 60 mg /L (maximum);</p> <p>High-level disinfection: TSS < 5 mg/L, BOD < 20 mg/L (annual arithmetic mean), < 30 mg /L (4 samples in a month), <45 mg /L (7 samples in a month), < 60 mg /L (maximum);</p> <p>High-level disinfection (principal or full treatment and disinfection): nitrogen < 10 mg/L (annual average), TSS < 5 mg/L, BOD < 20 mg/L (annual arithmetic mean), < 30 mg /L (4 samples in a month), < 45 mg /L (7 samples in a month), < 60 mg /L (maximum);</p> <p>Intermediate-level disinfection: nitrogen < 12 mg/L (annual average), TSS < 10 mg/L, BOD < 20 mg/L (annual arithmetic mean), < 30 mg /L (4 samples in a month), < 45 mg /L (7 samples in a month), < 60 mg /L (maximum);</p> <p>Low-level disinfection: TSS < 40–60 mg/L, BOD < 40–60 mg/L;</p> <p>Industrial use: TSS < 10 mg/L.</p>	<p>Basic disinfection: pH 6–8.5, fecal coliform < 200/100 mL (annual arithmetic mean of monthly values and geometric mean of 10 separate samples in a month), and < 400/100 mL in 10% of the samples in a month, < 800/100 mL (maximum), chlorine (if used) residual > 0.5 mg/L for more than 15 min of contact time at the peak hourly flow;</p> <p>High-level disinfection: pH 6–8.5, fecal coliform < detection limits, a domestic wastewater facility: < detection limits in 75% of the samples, < 25/100 mL in 25% of the samples (maximum), chlorine (if used) residual > 1 mg/L for more than 15 min of contact time at the peak hourly flow. For new and expanded treatment facilities after 07/01/1991: > 25 mg/L (fecal coliforms < 1000/100 mL), > 40 mg/L (1000/100 mL < fecal coliforms < 10,000/100 mL), > 120 mg/L (fecal coliforms > 10,000/100 mL);</p> <p>High-level disinfection (principal or full treatment and disinfection): pH 6–8.5, total organic carbon: < 3 mg/L (monthly average), < 5 mg/L (maximum) (full), total organic halide: < 0.2 mg/L (monthly average), < 0.3 mg/L (maximum) (full), fecal coliform < detection limits, a domestic wastewater facility: < detection limits in 75% of the samples, < 25/100 mL in 25% of the samples (maximum), chlorine (if used) residual > 1 mg/L for more than 15 min of contact time at the peak hourly flow. For new and expanded treatment facilities after 07/01/1991, > 25 mg/L (fecal coliforms < 1000/100 mL), > 40 mg/L (1000/100 mL), > 120 mg/L (fecal coliforms > 10,000/100 mL);</p> <p>Intermediate-level disinfection: pH: 6–8.5, fecal coliform < 14/100 mL (annual arithmetic mean of monthly values and median of 10 separate samples in a month), and < 43/100 mL in 10% of the samples in a month, < 86/100 mL (maximum; chlorine [if used] residual > 1 mg/L for more than 15 min of contact time at the peak hourly flow);</p> <p>Low-level disinfection: pH: 6–8.5, fecal coliform < 2400/100 mL;</p> <p>Industrial use: pH: 6–8.5, case by case under A.A.C. chapter 9, article 7.</p>	<p>Basic disinfection: The Department shall approve alternatives to the specified TSS limitation if the applicant provides reasonable assurances in the engineering report that the alternative control measures will ensure nonlogging of the system;</p> <p>High-level disinfection: Filtration shall be provided for TSS control. Chemical feed facilities for coagulant, coagulant aids, or polyelectrolytes shall</p>

Table A. Summarized Guidelines and Regulations for Reclaimed Water

State	Treatment Standards, Disinfection Standards, and Design Requirements				
	be provided. Such chemical feed facilities may be idle if the TSS limitation is being achieved without chemical addition. A pretreatment program shall be prepared and implemented;				
	High-level disinfection (principal or full treatment and disinfection): Discharges to surface waters shall meet reclaimed water or effluent limits established by procedures contained in Chapter 62-650, F.A.C., and the requirements of the antidegradation policy contained in Rules 62-4.242 and 62-302.300, F.A.C. No mixing zones shall be allowed; control measures will ensure nonclogging of the system;				
	Intermediate-level disinfection: Alternatives to the specified TSS limitation shall be approved by the Department if the applicant provides an affirmative demonstration that the alternative control measure will ensure nonclogging of the system.				
Georgia	Treatment Standards turbidity <= 3 NTU, TSS < 5 mg/L, BOD < 5 mg/L, pH: 6-9.				
	Disinfection Standards fecal coliform < 23/100 (monthly geometric mean), < 100/100 mL (maximum), detectable disinfectant residual at the delivery point (strongly recommended).				
Hawaii	Disinfection Standards R-1 (Significant reduction in viral and bacterial pathogens): fecal coliform < 2.2/100 mL in 7 days (median), < 23/100 mL in more than one sample in any 30 days, < 200/100 mL (maximum), a disinfection process that, when combined with the filtration process, has been demonstrated to inactivate and/or remove 99.999% of the PFU of F-specific bacteriophage MS2 or poliovirus in the wastewater. A virus that is at least as resistant to disinfection as poliovirus is may be used for purposes of demonstration, a disinfection process that, when combined with the filtration process, has been demonstrated to inactivate and/or remove 99.999% of the PFU of F-specific bacteriophage MS2 or poliovirus in the wastewater. A virus that is at least as resistant to disinfection as poliovirus is may be used for purposes of demonstration;				
	R-2 (Disinfected Secondary-23 Recycled Water): fecal coliform < 23/100 in 7 days (median), < 200/100 mL in more than one sample in any 30 days;				
Idaho	R-2 (Undisinfected Secondary Recycled Water): none.				
	Disinfection Standards A: total coliform < 2.2/100 mL (average); B: total coliform < 2.2/100 mL (average); C: total coliform < 23/100 mL (average); D: total coliform < 230/100 mL (maximum); E: up to "too numerous to count".				
Indiana	Treatment Standards Pollutant-bearing water application on land with a high potential for public exposure: TSS < 5 mg/L, BOD < 10 mg/L, pH 6-9; Domestic wastewater application on land with a low potential for public exposure: TSS < 30 mg/L, BOD < 30 mg/L, pH 6-9. Disinfection Standards Pollutant-bearing water application on land with a high potential for public exposure: fecal coliform not detectable (mean), < 14/100 mL				

Table A. Summarized Guidelines and Regulations for Reclaimed Water

State	Treatment Standards, Disinfection Standards, and Design Requirements
	(maximum), chlorine (if used) residual > 1 mg/L after 30-min contact time;
	Domestic wastewater application on land with a low potential for public exposure: fecal coliform <= 200/100 mL (average), <= 800/100 mL (maximum).
Iowa	
	Disinfection Standards
	0.5 mg of chlorine/L for 15 min.
	Treatment Standards
	Slow Rate Class I: TSS < 90 mg/L, BOD < 70 mg/L;
	Slow Rate Class II: TSS < 10 mg/L, BOD < 10 mg/L;
	Overland Flow: TSS < 90 mg/L, BOD < 70 mg/L;
	Rapid Infiltration: TSS and BOD: case by case.
Maryland	
	Disinfection Standards
	Slow Rate Class I: fecal coliform < 200/100 mL (maximum), < 3/100 mL in golf courses (maximum);
	Slow Rate Class II: fecal coliform < 3/100 mL (maximum);
	Overland Flow: fecal coliform < 200/100 mL (maximum);
	Rapid Infiltration: case by case.
	Treatment Standards
	Urban Reuse - Spray irrigation of golf courses and landscaping projects: turbidity <= 2 NTU, nitrogen < 10 mg/L, TSS < 5 mg/L, BOD <= 10 mg/L, pH 6-9;
	Urban Reuse - Toilet flushing: turbidity <= 5 NTU, nitrogen < 10 mg/L, TSS < 10 mg/L, BOD <= 30 mg/L, pH 6-9;
	Indirect Aquifer Recharge: turbidity <= 2 or 5 NTU, nitrogen < 10 mg/L, TSS < 5 or 10 mg/L, BOD <= 10 or 30 mg/L, pH 6-9.
Massachusetts	
	Disinfection Standards
	Urban Reuse - Spray irrigation of golf courses and landscaping projects: fecal coliform none detectable/100 mL in 7 days (mean), < 14/100 mL (maximum);
	Urban Reuse - Toilet flushing: fecal coliform < 100/100 mL (maximum);
	Indirect Aquifer Recharge: fecal coliform none detectable/100 mL in 7 days (mean), < 14/100 mL or 100/100 mL (maximum).
Missouri	
	Disinfection Standards
	fecal coliform < 200/100 mL (maximum), total residual chlorine of 0.5 mg/L after 15 min of contact time at peak flow.
	Treatment Standards
	Spray Irrigation of Food Crops: TSS < 10 mg/L, BOD < 10 mg/L.
	Disinfection Standards
Montana	
	Spray Irrigation of Food Crops: fecal coliform < 23/100 mL in 30 days;
	Spray Irrigation of Fodder, Fiber, and Seed Crops: fecal coliform < 23/100 mL in 7 days;
	Landscape Irrigation: fecal coliform < 200/100 mL in 7 days and < 400/100 mL in any 2 consecutive samples, or median < 2.2/100 mL and <

Table A. Summarized Guidelines and Regulations for Reclaimed Water

Treatment Standards, Disinfection Standards, and Design Requirements	
State	23/100 mL for irrigation of parks, playgrounds, schoolyards, unrestricted golf courses, and other areas where the public has similar access or exposure.
Disinfection Standards	fecal coliform: maximum < 200 CFU/100 mL for a 30-day average, no more than 10% of the samples > 400 CFU/100 mL.
Treatment Standards	A: dissolved oxygen ≥ 6.0 mg/L. <u>Disinfection Standards</u> A, B: total coliform < 2.2/100 mL in 30 days (geometric mean), < 23/100 mL (maximum daily); C: fecal coliform < 23/100 mL in 30 days (geometric mean), < 240/100 mL (maximum daily); D: fecal coliform < 200/100 mL in 30 days (geometric mean), < 400/100 mL (maximum daily); E: none.
Nevada	<u>Treatment Standards</u> Type I RWBR - Public Access System, Type II RWBR - Restricted-access and Nonedible Crop Systems, Type IV RWBR - Industrial Systems, Maintenance Operations and Construction Type I RWBR - Public Access System, Type II RWBR - Restricted-access and Nonedible Crop Systems: fecal coliform < 2.2/100 mL in 7 days (mean), < 14/100 mL (maximum), 1-mg/L chlorine for 15 min, or Design UV dose of 100 mJ/cm ² under maximum daily flow; Type III RWBR - Agricultural Edible Crop Systems, Type IV RWBR - Industrial Systems, Maintenance Operations and Construction: fecal coliform < 200/100 mL (monthly geometric mean), < 400/100 mL (weekly geometric mean); Type III water: > 1 mg of chlorine/L for 15 min, or Design UV dose of 75 mJ/cm ² under maximum daily flow.
New Jersey	<u>Treatment Standards</u> Type I RWBR - Public Access System, Type II RWBR - Restricted-access and Nonedible Crop Systems, Type IV RWBR - Industrial Systems, Maintenance Operations and Construction Type I RWBR - Public Access System, Type II RWBR - Restricted-access and Nonedible Crop Systems: fecal coliform < 2.2/100 mL in 7 days (mean), < 14/100 mL (maximum), 1-mg/L chlorine for 15 min, or Design UV dose of 100 mJ/cm ² under maximum daily flow; Type III RWBR - Agricultural Edible Crop Systems, Type IV RWBR - Industrial Systems, Maintenance Operations and Construction: fecal coliform < 200/100 mL (monthly geometric mean), < 400/100 mL (weekly geometric mean); Type III water: > 1 mg of chlorine/L for 15 min, or Design UV dose of 75 mJ/cm ² under maximum daily flow.
New Mexico	<u>Treatment Standards</u> Class 1A: turbidity < 3 NTU (30-day average), < 5 NTU (maximum), BOD < 10 mg/L (30-day average), < 15 mg/L (maximum); Class 1B: TSS < 30 mg/L (30-day average), < 45 mg/L (maximum), BOD < 30 mg/L (30-day average), < 45 mg/L (maximum); Class 2: TSS < 30 mg/L (30-day average), < 45 mg/L (maximum), BOD < 30 mg/L (30-day average), < 45 mg/L (maximum); Class 3: TSS < 75 mg/L (30-day average), < 90 mg/L (maximum), BOD < 30 mg/L (30-day average), < 45 mg/L (maximum). <u>Disinfection Standards</u> Class 1A: fecal coliform < 5/100 mL (30-day average), < 23/100 mL (maximum); Class 1B: fecal coliform < 100/100 mL (30-day average), < 200/100 mL (maximum); Class 2: fecal coliform < 200/100 mL (30-day average), < 400/100 mL (maximum); Class 3: fecal coliform < 1000/100 mL (30-day average), < 5000/100 mL (maximum).
North Carolina	<u>Treatment Standards</u> turbidity < 10 NTU, nitrogen < 4 mg/L (monthly), 6 mg/L (daily), TSS < 5 mg/L (monthly), 10 mg/L (daily), BOD < 10 mg/L (monthly), 15

Table A. Summarized Guidelines and Regulations for Reclaimed Water		Treatment Standards, Disinfection Standards, and Design Requirements	
State			
North Dakota	mg/L (daily).	Disinfection Standards fecal coliform <= 14/100 mL (monthly geometric mean), <= 25/100 mL (daily maximum).	
	Treatment Standards	TSS < 30 mg/L, BOD < 25 mg/L.	
	Disinfection Standards	maximum fecal coliform < 200/100 mL (30-day consecutive period), and < 400/100 mL in 10% of samples during any 30-consecutive-day period.	
Ohio	Disinfection Standards	Unrestricted-access sites: fecal coliform < 23/100 mL (30-day average); Restricted-access sites: fecal coliform of 30-day average < 23/100 mL (<100 ft), < 200/100 mL (100–200 ft), < 1000/100 mL (> 200 ft); Agricultural sites: fecal coliform of 30-day average < 23/100 mL (<100 ft), < 1000/100 mL (100–200 ft).	
	Treatment Standards	IV: 24-h mean < 2 NTU, 5% time during 24 h < 5 NTU.	
Oregon	Disinfection Standards	I: none; II: total coliform < 23 (7-day median), < 240/100 mL in 2 consecutive samples (maximum); III: total coliform < 2.2 (7-day median), < 23/100 mL (maximum); IV: total coliform < 2.2 (7-day median), < 23/100 mL (maximum).	
	Disinfection Standards	fecal coliform < 200/100 mL (monthly average), < 400/100 mL (daily maximum) reclaimed water systems with application in areas with a high potential for contact.	
South Carolina	Disinfection Standards	total coliform < 200/100 mL (geometric mean).	
South Dakota	Treatment Standards	Sites Open to Public Access: <= 30 mg/L.	
	Disinfection Standards	Sites Closed to Public Access: All wastewater must be treated to a level afforded by lagoons. Disinfection is generally not required for restricted-access land treatment sites. The TDHE may, however, require disinfection when deemed necessary;	
	Sites Open to Public Access:	fecal coliform < 200/100 mL (average).	
Tennessee	Treatment Standards	Type I: turbidity < 3 NTU, BOD < 5 mg/L; Type II: BOD: system other than pond: < 20 mg/L, or < 15 mg/L (CBOD ₅); pond system: < 30 mg/L.	
	Disinfection Standards		
Texas			

Table A. Summarized Guidelines and Regulations for Reclaimed Water

State	Treatment Standards, Disinfection Standards, and Design Requirements	
	Type I: fecal coliform < 20 CFU/100 mL (average), < 75 CFU/100 mL (maximum); Type II: fecal coliform < 200 CFU/100 mL (average), < 800 CFU/100 mL (maximum).	
Utah	<p>Treatment Standards</p> <p>Type I Treated Domestic Wastewater Effluent Where Human Exposure is Likely: turbidity: daily mean < 2 NTU, maximum < 5 NTU, TSS < 5 mg/L, BOD < 10 mg/L, pH 6–9;</p> <p>Type II Treated Domestic Wastewater Effluent Where Human Exposure is Unlikely: TSS: monthly arithmetic mean < 25 mg/L, weekly mean < 35 mg/L, BOD < 25 mg/L, pH 6–9.</p> <p>Disinfection Standards</p> <p>Type I Treated Domestic Wastewater Effluent Where Human Exposure Is Likely: <i>E. coli</i>: none detected, < 9/100 mL (maximum), chlorine > 1.0 mg/L after 30-min contact time at peak flow;</p> <p>Type II Treated Domestic Wastewater Effluent Where Human Exposure Is Unlikely: <i>E. coli</i> < 126/100 mL (weekly median), < 500/100 mL (maximum).</p>	
Vermont	<p>Treatment Standards</p> <p>turbidity < 2 NTU (monthly average), < 5 NTU (single sample), total nitrogen < 5 mg/L, ammonia nitrogen < 1 mg/L, TSS < 5 mg/L, BOD < 10 mg/L.</p> <p>Disinfection Standards</p> <p><i>E. coli</i> < 2.2/100 mL (geometric mean of 5 samples), < 25/100 mL (maximum), residual chlorine > 1 mg/L.</p> <p>Treatment Standards</p>	
Virginia	<p>Level 1: fecal coliform: monthly geometric mean <= 14/100 mL, corrective action threshold (CAT) at > 49/100 mL, or <i>E. coli</i>: monthly geometric mean <= 11/100 mL, CAT > 35/100 mL, or enterococci: monthly geometric mean <= to 11/100 mL, CAT > 24/100 mL, total residual chlorine: CAT < 1.0 mg/L after a minimum contact time of 30 min at average flow or 20 min at peak flow, pH 6.0–9.0, 5-day BOD: monthly average <= to 10 mg/L, or CBOD: monthly average <= to 8 mg/L, turbidity: daily average of discrete measurements recorded over a 24-h period <= 2 NTU, CAT > 5 NTU.</p> <p>Level 2: fecal coliform: monthly geometric mean <= to 200/100 mL, CAT > 800/100 mL, or <i>E. coli</i>: monthly geometric mean <= 126/100 mL, CAT > 235/100 mL, or enterococci: monthly geometric mean <= to 35/100 mL, CAT > 104/100 mL, total residual chlorine: CAT < 1.0 mg/L after a minimum contact time of 30 min at average flow or 20 min at peak flow, pH 6.0–9.0, BOD: monthly average <= 30 mg/L, maximum weekly average 45 mg/L, or CBOD: monthly average <= 25 mg/L, maximum weekly average 40 mg/L, TSS: monthly average <= 30 mg/L, maximum weekly average = 45 mg/L.</p> <p>Treatment Standards</p> <p>turbidity <= 2 NTU (average), <= 5 NTU (maximum), TSS < 30 mg/L (monthly arithmetic mean of 24-h composite, collected daily), BOD < 30 mg/L (monthly arithmetic mean of 24-h composite, collected weekly), dissolved oxygen > 0.</p> <p>Disinfection Standards</p> <p>A, B: total coliform < 2.2/100 mL in last 7 days (median), < 23/100 mL (maximum); C: total coliform < 23/100 mL in last 7 days (median), < 240/100 mL (maximum);</p>	
Washington		

Table A. Summarized Guidelines and Regulations for Reclaimed Water

State	Treatment Standards, Disinfection Standards, and Design Requirements
	D: total coliform < 240/100 mL in last 7 days (median).
Design Requirements	Concentration of chlorine > 1 mg/L for 30 min where chlorine is used, and chlorine residue of 0.5 mg/L should be maintained unless reclaimed water is used for impoundments and storage ponds and approved by Department of Health and Ecology.
	Treatment Standards
	Absorption Pond: nitrogen < 10 mg/L (after 1/1/90), < 20 (between 1/1/90 and 1/1/85), none (before 1/1/85), BOD < 50 mg/L (monthly average), TDS < 500 mg/L, Cl < 250 mg/L;
Wisconsin	Spray Irrigation: BOD < 50 mg/L (monthly average);
	Ridge and Furrow: BOD < 50 mg/L (monthly average);
	Overland Flow: case by case;
	Other: case by case.
	Disinfection Standards
Wyoming	A: fecal coliform < 2.2/100 mL (maximum); B: fecal coliform > 2.2, and < 200/100 mL (maximum); C: fecal coliform > 200, and < 1000/100 mL (maximum).

APPENDIX B

WEBSITES OF STATE GUIDELINES AND REGULATIONS FOR RECLAIMED WATER

Table B. Websites of State Guidelines and Regulations for Reclaimed Water

State	Titles	Websites
Alabama	Groundwater Maximum Contaminant Levels Applicable to Groundwater Affected by Land Treatment Sites; Based on regulations developed after P.L. 92-523 (The Safe Drinking Water Act), Title 40, Parts 141 and 143	http://www.adem.state.al.us/WaterDivision/Industrial/Guidance.htm
Alaska	Alaska Administrative Code, Title 18 - Environmental Conservation, Chapter 72, Article 2	http://www.dec.state.ak.us/regulations/index.htm
Arizona	Arizona Administrative Code Title 18 Environmental Quality, Chapter 9 Water Pollution Control, Title 18, Chapter 11 Water Quality Standards	http://www.azsos.gov/public_services/Table_of_Contents.htm
Arkansas	“The Purple Book” Excerpts from the Health and Safety Code, Water Code, and Titles 22 and 17 of the California Code of Regulations	http://www.adec.state.ar.us/regs/default.htm
California	“The Purple Book” Excerpts from the Health and Safety Code, Water Code, and Titles 22 and 17 of the California Code of Regulations	http://www.cdphe.state.co.us/op/wqcc/GeneralInfo/StatutesRegulationsPolicies/Policies/96-1_07.pdf
Colorado	Colorado Department of Public Health and Environment, Policy 96-1 - Design Criteria Considered in the Review of Wastewater Treatment Facilities; Regulation 84 - Reclaimed Water Control Regulation; Regulation 62 - Regulations for Effluent Limitations	http://www.cdphe.state.co.us/regulations/wqcrcregs/100284wqccreclaimedwater2007.pdf
Connecticut	Guidance and Regulations Governing Land Treatment of Wastes	http://www.ct.gov/dep/site/default.asp
Delaware	Guidance and Regulations Governing the Land Treatment Of Wastes	http://www.dnrec.state.de.us/dnrec2000/;http://www.dnrec.state.de.us/water2000/Sections/GroundWat/GWDSRegulations.htm
Florida	Chapter 62-610 Reuse of Reclaimed Water and Land Application	http://www.dep.state.fl.us/legal/Rules/wastewater/62-610.pdf ; http://www.dep.state.fl.us/legal/Rules/wastewater/62-600.pdf ; http://www.dep.state.fl.us/water/reuse/apprules.htm
Georgia	Guidelines for Water Reclamation and Urban Water Reuse	http://www.gaepl.org/Files_techguide/wph/reuse.pdf
Hawaii	Guidelines for the Treatment and Use of Recycled Water	http://hawaii.gov/health/environmental/water/wastewater/forms.html

Table B. Websites of State Guidelines and Regulations for Reclaimed Water

State	Titles	Websites
Idaho	58.01.17, Rules for the Reclamation and Reuse of Municipal and Industrial Wastewater	http://adm.idaho.gov/adminrules/rules/idapa58/58index.htm
Illinois	Title 35 of the Illinois Administrative Code Subtitle C Chapter II: Part 372, Illinois Design Standards for Slow Rate Land Application of Treated Wastewater Article 6.1 Land Application of Biosolid, Industrial Waste Product, and Pollutant Water	http://www.jpcb.state.il.us/SLR/IPCBandIEPAEnvironmentalRegulations-Title35.asp
Indiana		http://www.in.gov/legislative/lac/title327.html
Iowa	Iowa Wastewater Facilities Design Standards Chapter 21: Land Application of Wastewater	http://www.iowadnr.com/water/wastewater/downloads.html
Kansas	Administrative Rules and Regulations, 28-16. Water Pollution Control	http://www.kdheks.gov/pdf/regs/28-16.pdf
Kentucky		http://kentucky.gov/Default.html
Louisiana		http://www.state.la.us/
Maine		http://www.state.me.us/
Maryland	Guidelines for Land Treatment of Municipal Wastewaters	http://www.mde.state.md.us/assets/document/MDE-WMA-001%20(Land-Treatment%20Guidelines).pdf
Massachusetts	Reclaimed Water Use - Interim Guidelines (Wastewater Reuse)	http://www.mass.gov/dep/water/laws/policies.htm
Michigan		http://www.michigan.gov/deq/0,1607,7-135-3313_3682-14902--,00.html
Minnesota		http://www.state.mn.us/cgi-bin/portal/mn/jsp/home.do?agency=NorthStar
Mississippi		http://www.mississippi.gov/
Missouri	Division 20 - Clean Water Commission, Chapter 8 - Design Guides	http://www.sos.mo.gov/adrules/esr/current/10csr/10csr.asp
Montana	Design Standards for Wastewater Facilities	http://www.deq.state.mt.us/wqinfo/Circulars/DEQ2.PDF
Nebraska	NEBRASKA Administrative Code, Title 119 – Nebraska Department of Environmental Quality	http://www.deq.state.ne.us/
Nevada	NAC 445A.276 Reuse Categories: Requirements for Bacteriological Quality of Effluent	http://www.leg.state.nv.us/NAC/NAC-445A.html
New Hampshire		http://www.state.nh.us/
New Jersey	Technical Manual for Reclaimed Water for Beneficial Reuse	http://www.state.nj.us/dep/dwq/techman.htm
New Mexico		http://www.nmenv.state.nm.us/gwb/New_Pages/docs_policy/NMED_REUSE_1-24-07.pdf

Table B. Websites of State Guidelines and Regulations for Reclaimed Water

State	Titles	Websites
New York		http://www.dec.state.ny.us
North Carolina	Administrative Rules, Title 15A, Chapter 02, Subchapter T, Waste Not Discharged to Surface Waters, 15A NCAC 02T .0906 Reclaimed Water Effluent Standards	http://reports.oah.state.nc.us/ncac.asp
North Dakota	Division of Water Quality Criteria for Irrigation with Treated Wastewater Recommended Criteria for Land Disposal of Effluent	http://www.health.state.nd.us/wq/
Ohio	The Ohio State University Extension Bulletin 860 Reuse of Reclaimed Wastewater through Irrigation	http://ohioline.osu.edu/b860/
Oklahoma	252:621 Non-Industrial Impoundments and Land Application, 252:656 Water Pollution Control Facility Construction	http://www.deq.state.ok.us/mainlinks/deqrules.htm
Oregon	Division 55 340-055 Treatment and Monitoring Requirements for Use of Reclaimed Water	http://arcweb.sos.state.or.us/rules/OARs_300/OAR_340/340_055.html
Pennsylvania		http://www.dep.state.pa.us/dep/deputate/watermgmt/Wqp/WQP_WM/WM_Sewage.htm
Rhode Island		http://www.state.ri.us/
South Carolina	Chapter XII Recommended Design Criteria for Disposal of Effluent by Irrigation Chapter XIII Recommended Design Criteria for Groundwater Monitoring Wells Chapter XVI Recommended Design Criteria for Artificial Wetland Systems	http://www.state.sc.us/denr/DES/P&S/designcriteria/designT.html
Tennessee	Design Criteria for Sewage Works	http://www.state.tn.us/environment/wpc/publications/dcChapter1_1_6.pdf
Texas	Water Reclamation and Reuse Regulation (9VAC25-740)	http://info.sos.state.tx.us/pub/plsql/readtac\$ext.viewtac
Utah	Utah Administrative Code, Environmental Quality, R-317-1-4	http://www.rules.utah.gov/publicat/code.htm
Vermont	Adopted Indirect Discharge Rules, Subchapter 5 – Technical Standards for Wastewater Disposal Systems and Potable Water Supplies	http://www.anr.state.vt.us/dec/ww/indirect.htm#IDRs
Virginia	Water Reclamation and Reuse Regulation (9VAC25-740)	http://www.ecy.wa.gov/programs/wq/reclaim/standards.pdf
Washington	Water Reclamation and Reuse Standards; standards for wetlands and direct aquifer recharge are also included in section 2 and section 3.	http://www.ecy.wa.gov/biblio/97023.html
West Virginia	Title 64 Series 47 Chapter 16-1 Sewage Treatment and Collection System Design Standards	http://www.wvsos.com/csr/verify.asp?TitleSeries=64-47
Wisconsin	NR 206 Land Disposal of Municipal and Domestic Wastewaters	http://www.legis.state.wi.us/rsb/code/nr/nr200.html
Wyoming	Wyoming Water Quality Regulations Chapter 21-Reuse of Treated Wastewater	http://soswy.state.wy.us/RULES/2804.pdf

APPENDIX C

USES OF RECLAIMED WATER IN SELECTED STATES

Table C.1. Uses of Reclaimed Water in Arizona

Type of Reuse	Category		
	Class A	Class B	Class C
Irrigation of food crops	Allowed	Allowed	
Recreational impoundments	Allowed	Allowed	
Residential landscape irrigation	Allowed	Allowed	
School ground landscape irrigation	Allowed	Allowed	
Open-access landscape irrigation	Allowed	Allowed	
Toilet and urinal flushing	Allowed	Allowed	
Fire protection systems	Allowed	Allowed	
Spray irrigation of an orchard or vineyard	Allowed	Allowed	
Commercial closed loop air-conditioning systems	Allowed	Allowed	
Vehicle and equipment washing (does not include self-service vehicle washes)	Allowed	Allowed	
Snow-making	Allowed	Allowed	
Surface irrigation of an orchard or vineyard	Allowed	Allowed	
Golf course irrigation	Allowed	Allowed	
Restricted-access landscape irrigation	Allowed	Allowed	
Landscape impoundment	Allowed	Allowed	
Dust control	Allowed	Allowed	
Soil compaction and similar construction activities	Allowed	Allowed	
Pasture for milking animals	Allowed	Allowed	
Livestock watering (dairy animals)	Allowed	Allowed	
Concrete and cement mixing	Allowed	Allowed	
Material washing and sieving	Allowed	Allowed	
Street cleaning	Allowed	Allowed	
Pasture for nondairy animals	Allowed	Allowed	
Livestock watering (nondairy animals)	Allowed	Allowed	
Irrigation of sod farms	Allowed	Allowed	

Table C.1. Uses of Reclaimed Water in Arizona

Type of Reuse ¹	Category
Irrigation of fiber, seed, forage, and similar crops	Allowed
Silviculture	Allowed

Table C.2. Uses of Reclaimed Water in California

Type of Reuse ¹	Category
Irrigation²	
Food crops, including all edible root crops, where the recycled water comes into contact with the edible portion of the crop	Allowed
Parks and playgrounds	Allowed
Schoolyards	Allowed
Residential landscaping	Allowed
Unrestricted-access golf courses	Allowed
Any other irrigation use not specified and not prohibited by other sections of the California Code of Regulations	Allowed
Food crops where edible portion is produced above ground and not contacted by recycled water	Allowed
Cemeteries	Allowed
Freeway landscaping	Allowed
Restricted-access golf courses	Allowed
Ornamental nursery stock and sod farms where access by the general public is not restricted	Allowed
Pasture for animals producing milk for human consumption	Allowed
Any nonedible vegetation where access is controlled so that the irrigated area cannot be used as if it were part of a park, playground, or school yard	Allowed
Orchards where the recycled water does not come into contact with the edible portion of the crop	Allowed

Table C.2. Uses of Reclaimed Water in California

Type of Reuse	Category
Vineyards where the recycled water does not come into contact with the edible portion of the crop	Allowed
Non food-bearing trees (Christmas tree farms are included in this category, provided no irrigation with recycled water occurs for a period of 14 days prior to harvest or access by the general public)	Allowed
Fodder and fiber crops and pasture for animals not producing milk for human consumption	Allowed
Seed crops not eaten by humans	Allowed
Food crops that must undergo commercial pathogen-destroying processing before being consumed by humans	Allowed
Ornamental nursery stock and sod farms, provided no irrigation with recycled water occurs for a period of 14 days prior to harvesting, retail sale, or access by the general public	Allowed
Supply for Impoundment	
Nonrestricted recreational impoundments with supplemental monitoring for pathogenic organisms	Allowed ³
Restricted recreational impoundments and publicly accessible fish hatcheries	Allowed
Landscape impoundments without decorative fountains	Allowed
Supply for Cooling or Air Conditioning	
Industrial or commercial cooling or air conditioning involving cooling tower, evaporative condenser, or spraying that creates a mist	Allowed ⁴
Industrial or commercial cooling or air conditioning not involving a cooling tower, evaporative condenser, or spraying that creates a mist	Allowed
Other Uses⁵	
Flushing toilets and urinals	Allowed
Priming drain traps	Allowed
Industrial process water that may contact workers	Allowed
Structural firefighting	Allowed
Decorative fountains	Allowed
Commercial laundries	Allowed
Consolidation of backfill material around potable water pipelines	Allowed
Artificial snow-making for commercial outdoor uses	Allowed

Table C.2. Uses of Reclaimed Water in California

Type of Reuse	Category
Commercial car washes, including hand washes if the recycled water is not heated, where the general public is excluded from the washing process	Allowed
Industrial boiler feed	Allowed
Nonstructural firefighting	Allowed
Backfill consolidation around nonpotable piping	Allowed
Soil compaction	Allowed
Mixing of concrete	Allowed
Dust control on roads and streets	Allowed
Cleaning of roads, sidewalks, and outdoor work areas	Allowed
Industrial process water that will not come into contact with workers	Allowed
Flushing of sanitary sewers	Allowed

Notes:

1. Exceptions: The requirements set forth in this chapter shall not apply to the use of recycled water on-site at a water recycling plant or wastewater treatment plant, provided that access by the public to the area of on-site recycled water use is restricted.
2. Exceptions: For filtration pursuant to Section 60301.320(a) coagulation need not be used as part of the treatment process, provided that the filter effluent turbidity does not exceed 2 NTU, the turbidity of the influent to the filters is continuously measured, the influent turbidity does not exceed 5 NTU for more than 15 min and never exceeds 10 NTU, and the capability to automatically activate chemical addition or divert the wastewater should the filter influent turbidity exceed 5 NTU for more than 15 min exists.
3. Exceptions: Disinfected tertiary recycled water that has not received conventional treatment may be used for nonrestricted recreational impoundments, provided the recycled water is monitored for the presence of pathogenic organisms in accordance with the following: (1) During the first 12 months of operation and use, the recycled water shall be sampled and analyzed monthly for *Giardia*, enteric viruses, and *Cryptosporidium*. Following the first 12 months of use, the recycled water shall be sampled and analyzed quarterly for *Giardia*, enteric viruses, and *Cryptosporidium*. The ongoing monitoring may be discontinued after the first 2 years of operation with the approval of the department. This monitoring shall be in addition to the monitoring set forth in Section 60321. (2) The samples shall be taken at a point following disinfection and prior to the point where the recycled water enters the use impoundment. The samples shall be analyzed by an approved laboratory.
4. Whenever a cooling system, using recycled water in conjunction with an air-conditioning facility, utilizes a cooling tower or otherwise creates a mist that could come into contact with employees or members of the public, the cooling system shall comply with the following: (1) A drift eliminator shall be used whenever the cooling system is in operation. (2) A chlorine or other biocide shall be used to treat the cooling system recirculating water to minimize the growth of *Legionella* and other microorganisms.
5. Recycled water used for the following shall be disinfected tertiary recycled water, except that for filtration being provided pursuant to Section 60301.320(a) coagulation need not be used as part of the treatment process, provided that the filter effluent turbidity does not exceed 2 NTU, the turbidity of the influent to the filters is continuously measured, the influent turbidity does not exceed 5 NTU for more than 15 min and never exceeds 10 NTU, and the capability to automatically activate chemical addition or divert the wastewater should the filter influent turbidity exceed 5 NTU for more than 15 min exists.

Table C.3. Uses of Reclaimed Water in Colorado

Type of Reuse	Category			Additional Conditions Required 84.8(A)
	Category 1	Category 2	Category 3	
Industrial				
Cooling tower	Allowed	Allowed	Allowed	1
Concrete mixing and washout	Allowed	Allowed	Allowed	2
Dust control	Allowed	Allowed	Allowed	3
Soil compaction	Allowed	Allowed	Allowed	3
Closed loop cooling system	Allowed	Allowed	Allowed	3
Landscape Irrigation				
Restricted access	Allowed	Allowed	Allowed	
Unrestricted access	Allowed	Allowed	Allowed	4
Resident controlled			Allowed	4,5
Commercial				
Mechanized street cleaning	Allowed	Allowed	Allowed	3
Zoo operations	Allowed	Allowed	Allowed	
Fire Protection				
Nonresidential fire protection		Allowed	Allowed	6
Residential fire protection			Allowed	6

Notes:

1. If there is a significant likelihood for aerosols to drift to public or worker areas, adequate signage is required. Consider supplemental disinfection and chlorine residual and/or public access restrictions.
2. Category 1 water is allowed in the mixing process only; using it to wash off trucks and to supply trucks is prohibited. Category 2 water may be used for mixing or washing or as truck supply water as long as the user complies with the requirements set forth in Section 84.9 of this regulation. Mixing and washing activities must be contained (e.g., flow to lined pit or to approved concrete washout area or within enclosed equipment), as to prevent any off-site runoff or discharge to groundwater. Truck drivers and workers shall be trained in the proper use and washout procedures when using reclaimed water.
3. Application rates shall minimize ponding on or runoff from the area approved for application or use.
4. No reclaimed water piping shall be extended to or supported from any residential structure, and there shall be no accessible above-grade outlets from the reclaimed water system at any residential structure. At least one exterior hose bib, supplied with potable water, shall be provided at each residential structure.
5. The treater shall develop and implement a public education program to inform residents and plumbing contractors and inspectors who deal with the resident-controlled landscape irrigation systems about the need to (a) strictly prohibit cross-connections between the reclaimed water and potable water systems; (b) clearly and distinctively identify the potable service lines and plumbing from the reclaimed water service lines and plumbing; and (c) avoid contact with and strictly minimize ponding or runoff of the reclaimed water. The treater shall implement a cross-connection inspection program and shall have the authority to discontinue reclaimed water service to any resident who flagrantly or repeatedly misuses reclaimed water in a manner inconsistent with this regulation. The treater shall maintain a map indicating all areas where reclaimed water is provided for resident-controlled landscape irrigation.

Table C.3. Uses of Reclaimed Water in Colorado

Type of Reuse	Category
6. The user shall develop and implement a program, including notices in fire department newsletters and fire department preplans, to educate the public and firefighters that reclaimed water is used for fire protection. The user shall develop a program to educate plumbing and fire protection system contractors and inspectors expected to access the fire protection system about the need to confirm that cross-connections between the reclaimed water and potable water systems do not exist and about the requirement to clearly identify the potable and reclaimed water systems throughout the building. All personnel authorized to use the reclaimed water for fire protection shall be educated to avoid contact with and strictly minimize ponding or runoff of the reclaimed water during nonemergency testing or training. An annual cross-connection inspection shall be made at each structure to which reclaimed water piping is extended for fire protection to ensure that no cross-connection exists. The person treating shall maintain a map indicating the location of all fire hydrants, sprinkler systems, and standpipe systems provided with reclaimed water.	

Table C.4. Uses of Reclaimed Water in Florida

Type of Reuse	Category					
	Slow Land Application Systems; Restricted Public Access	Slow Land Application Systems; Public Access Areas, Residential Irrigation, and Edible Crops	High-Rate Land Application Systems	Groundwater Recharge and Indirect Potable Reuse	Overland Flow Systems	Industrial Use
Slow land application systems	Allowed	Allowed	Allowed	Allowed		
Applied to vegetative land surfaces, cattle-grazing areas	Allowed	Allowed	Allowed	Allowed		
Restricted public access areas	Allowed					
Public access areas			Allowed			
Residential irrigation			Allowed			
Golf courses			Allowed			
Cemeteries			Allowed			
Parks			Allowed			
Landscape areas			Allowed			
Highway medians			Allowed			
Fire protection			Allowed			
Aesthetic purposes (decorative ponds or fountains)			Allowed			
Irrigation of edible crops			Allowed			
Dust control on construction sites			Allowed			
Toilet flushing			Allowed			
Additional uses			Allowed			

Table C.4. Uses of Reclaimed Water in Florida

Type of Reuse	Category				
	Slow Land Application Systems; Restricted Public Access	Slow Land Application Systems; Public Access Areas, Residential Irrigation, and Edible Crops	High-Rate Land Application Systems	Groundwater Recharge and Indirect Potable Reuse	Overland Flow Systems
Water supply for commercial laundries		Allowed			
Vehicle washing		Allowed			
Flushing of sanitary sewers and reclaimed water lines		Allowed			
Mixing of concrete		Allowed			
Manufacture of ice for ice rinks		Allowed			
Cleaning of roads, sidewalks, and outdoor work areas		Allowed			
High-rate land application systems		Allowed			
Injection to groundwaters		Allowed			
Salinity control		Allowed			
Discharge to surface waters		Allowed			
Indirect potable reuse		Allowed			
Overland flow systems (sprinkling or flooding upper reaches of terraced, sloped, vegetated surfaces [sod farms, forests, fodder crops, pastures, etc.])					Allowed
Industrial use (cooling water, wash water, process water in industrial facilities)					Allowed
Treated industrial wastewater for land application					Allowed

Table C.5. Uses of Reclaimed Water in Hawaii

Type of Reuse	Category		
	R-1	R-2	R-3
Irrigation: (S)pray, (D)rip & Surface, (U)surface, (A)LL=SD & U, Spray with (B)uffer, (N)oT Allowed, /=or			
Golf course landscapes	A	U/B	N
Freeway and cemetery landscapes	A	A	N
Food crops where recycled water contacts the edible portion of the crop, including all root crops	A ¹	N	N

Table C.5. Uses of Reclaimed Water in Hawaii

Type of Reuse		Category		
		R-1	R-2	R-3
Parks, elementary school yards, athletic fields, and landscapes around some residential property		A	U	N
Roadside and median landscapes		A	U/B	N
Inedible vegetation in areas with limited public exposure		A	AB	U
Sod farms		A	AB	N
Ornamental plants for commercial use		A	AB	N
Food crops above ground and not contacted by irrigation		A	U	N
Pastures for milking and other animals		A	U	N
Fodder, fiber, and seed crops not eaten by humans		A	AB	DU
Orchards and vineyards bearing food crops		A	D/U	DU
Orchards and vineyards not bearing food crops during irrigation		A	AB	DU
Timber and trees not bearing food crops		A	AB	DU
Food crops undergoing commercial pathogen-destroying process before consumption		A	AB	DU
Supply to Impoundments				
Restricted recreational impoundments		A	N	N
Basins at fish hatcheries		A	N	N
Landscape impoundments without decorative fountain		A	A	N
Landscape impoundments with decorative fountain		A	N	N
Supply to Other Uses				
Flushing of toilets and urinals		A	N	N
Structural firefighting		A	A	N
Nonstructural firefighting		A	A	N
Commercial and public laundries		A	N	N
Cooling of saws while cutting pavement		A	N	N
Decorative fountains		A	N	N
Washing of yards, lots, and sidewalks		A	N	N
Flushing of sanitary sewers		A	A	N
High-pressure water blasting to clean surfaces		A	N	N
Industrial process without exposure of workers		A	A	N
Industrial process with exposure of workers		A	N	N
Cooling or air-conditioning system without tower, evaporative condenser, spraying, or other features that emit vapor or droplets		A	A	N
Cooling or air-conditioning system with tower, evaporative condenser, spraying, or other features that emit vapor or droplets		A	N	N

Table C.5. Uses of Reclaimed Water in Hawaii

Type of Reuse	Category	R-1	R-2	R-3
Industrial boiler feed		A	A	N
Water jetting for consolidation of backfill material around piping during water shortages		A	N	N
Water jetting for consolidation of backfill material around piping for recycled water, sewage, storm drainage, and gas, as well as electrical conduits		A	A	N
Washing aggregate and making concrete		A	A	N
Dampening roads and other surfaces for dust control		A	A	N
Dampening brushes and street surfaces in street sweeping		A	A	N
Note:				
1. Allowed under the following conditions: The turbidity of the influent to the filters is continuously measured, the influent turbidity does not exceed 5 NTU for more than 15 min and never exceeds 10 NTU, and the capability to automatically activate chemical addition or divert the wastewater should the filter influent turbidity exceed 5 NTU for more than 15 min exists. The UV disinfection unit must conform to Appendix K: UV Disinfection Guidelines for R-1 Water.				

Table C.6. Uses of Reclaimed Water in Idaho

Type of Reuse	Category	A	B	C	D	E
Residential irrigation at individual homes	Allowed					
Groundwater recharge using surface spreading, seepage ponds, or other unlined surface water features	Allowed					
Groundwater recharge using subsurface distribution	Allowed					
Fire suppression from dedicated, marked hydrants	Allowed					
Dust suppression at construction sites	Allowed					
Contact with any edible portion of raw food crops	Allowed	Allowed				
Irrigation of golf courses, parks, playgrounds, school yards	Allowed	Allowed				
Irrigation of orchards and vineyards during the fruiting season, if no fruit harvested for raw use comes in contact with the irrigation water or ground or if the water contacts only the inedible portion of raw food crops	Allowed	Allowed	Allowed	Allowed		
Irrigation of cemeteries or roadside vegetation	Allowed	Allowed	Allowed			
Toilet flushing at industrial and commercial sites	Allowed	Allowed	Allowed			
Irrigation of fodder, seed, or processed food crops	Allowed	Allowed	Allowed	Allowed		
Irrigation of forested sites	Allowed	Allowed	Allowed	Allowed	Allowed	

Table C.7. Uses of Reclaimed Water in Nevada

Type of Reuse	Category				
	Class A	Class B	Class C	Class D	Class E
Spray irrigation of land used as a cemetery, commercial lawn, golf course, greenbelt, or park even if: (1) Public access to the area of use is not controlled; and (2) Human contact with the treated effluent can reasonably be expected to occur	Allowed				
An impoundment in which swimming is prohibited even if: (1) Public access to the impoundment is not controlled; and (2) Human contact with the treated effluent can reasonably be expected to occur	Allowed				
Any other use that is approved by the Division	Allowed				
Spray irrigation of land used as a cemetery, commercial lawn, golf course, greenbelt or park if: (1) Public access to the area of use is controlled; and (2) Human contact with the treated effluent cannot reasonably be expected to occur	Allowed	Allowed	Allowed	Allowed	
Subsurface irrigation of land used as a commercial lawn, greenbelt, or park	Allowed	Allowed	Allowed	Allowed	
Cooling water in an industrial process	Allowed	Allowed	Allowed	Allowed	
Firefighting operations in an urban area if approved by the fire department, fire protection district, or other firefighting agency in whose district the fire occurs	Allowed	Allowed	Allowed	Allowed	
Any other use that is approved by the Division	Allowed	Allowed	Allowed	Allowed	
Spray irrigation of land used as a cemetery, golf course, or greenbelt if: (1) Public access to the area of use is controlled; (2) Human contact with the treated effluent does not occur; and (3) A buffer zone of not less than 100 ft is maintained	Allowed	Allowed	Allowed	Allowed	Allowed
Watering of nursery stock if public access to the area of use is controlled	Allowed	Allowed	Allowed	Allowed	
Establishment, restoration, or maintenance of a wetland if public access to the wetland is controlled	Allowed	Allowed	Allowed	Allowed	
Washing of gravel used in concrete mixing	Allowed	Allowed	Allowed	Allowed	
Feed water for a boiler	Allowed	Allowed	Allowed	Allowed	
An impoundment if: (1) Public access to the impoundment is controlled; and (2) Human contact with the treated effluent cannot reasonably be expected to occur	Allowed	Allowed	Allowed	Allowed	
Firefighting of forest or other wilderness fires if approved by the fire department, fire protection district, or other firefighting agency in whose district the fire occurs	Allowed	Allowed	Allowed	Allowed	
Spray irrigation of land used for agricultural purposes if: (1) Public access to the area of use is prohibited; and (2) A buffer zone of not less than 400 ft is maintained	Allowed	Allowed	Allowed	Allowed	Allowed
Surface irrigation of land used: (1) As greenbelt if: (I) Public access to the area of use is prohibited; and (II) Human contact with the treated effluent does not occur. (2) For agricultural purposes; and (3) For the cultivation of fruit-bearing trees or nut-bearing trees	Allowed	Allowed	Allowed	Allowed	

Table C.7. Uses of Reclaimed Water in Nevada

Type of Reuse	Category	Class A	Class B	Class C	Class D	Class E
Subsurface irrigation of land used for agricultural purposes if public access is controlled		Allowed	Allowed	Allowed	Allowed	
Dust control		Allowed	Allowed	Allowed	Allowed	
Soil compaction		Allowed	Allowed	Allowed	Allowed	
Flushing sewer lines		Allowed	Allowed	Allowed	Allowed	
An impoundment if: (1) Public access to the impoundment is prohibited; (2) All human activities involving contact with the treated effluent are prohibited; and (3) Human contact with the treated effluent does not occur		Allowed	Allowed	Allowed	Allowed	
Spray irrigation of land used for agricultural purposes if: (1) Public access to the area of use is prohibited; and (2) A buffer zone of not less than 800 ft is maintained		Allowed	Allowed	Allowed	Allowed	

Table C.8. Uses of Reclaimed Water in New Mexico

Type of Reuse	Category	Class 1A	Class 1B	Class 2	Class 3
All Class 1 uses. No setback limit to dwelling unit or occupied establishment		Allowed			
Backfill around potable water pipes		Allowed			
Irrigation of food crops ¹		Allowed			
Impoundments (recreational or ornamental)		Allowed			
Irrigation of parks, school yards, golf courses		Allowed			
Irrigation of urban landscaping		Allowed			
Snow-making		Allowed			
Street cleaning		Allowed			
Toilet flushing		Allowed			
Backfill around nonpotable piping		Allowed			
Concrete mixing		Allowed			
Dust control		Allowed			
Irrigation of fodder, fiber, and seed crops for milk-producing animals		Allowed			
Irrigation of roadway median landscapes		Allowed			
Irrigation of sod farms		Allowed			
Livestock watering		Allowed			
Soil compaction		Allowed			

Table C.8. Uses of Reclaimed Water in New Mexico

Type of Reuse	Category
Irrigation of fodder, fiber, and seed crops for non-milk-producing animals	Allowed Allowed
Irrigation of forest trees (silviculture)	Allowed Allowed
Note:	
1. Irrigation of food crops should be allowed for food crops when there is no contact between the edible portion of the crop and the wastewater. Spray irrigation is prohibited for food crops.	

Table C.9. Uses of Reclaimed Water in Oregon

Type of Reuse	Category		
	Level I	Level II	Level III
Buffers for irrigation:	Surface: 10 ft Spray: site-specific	Surface 10 ft Spray: 70 ft	10 ft
Agricultural food crops	N/A	N/A	N/A
Processed food crops	N/A	1	1
Orchards and vineyards	N/A	2	2
Fodder, fiber, and seed crops not for human ingestion	3	1	1
Pasture for animals	N/A	4	4
Sod	N/A	1	1
Ornamental nursery stock	N/A	1	1
Christmas trees	N/A	1	1
Firewood	N/A	1	1
Commercial timber	3	1	1
Parks, playgrounds, school yards, golf courses with contiguous residences	N/A	N/A	N/A
Golf courses without contiguous residences	N/A	5,7	5,7
Cemeteries, highway medians, landscapes without frequent public access	N/A	5,7	5,7
Industrial or commercial use	N/A	9,10,11,12	9,10,11,12
Construction use	N/A	9,10,11,12,13	9,10,11,12,13
Impoundments: unrestricted	N/A	N/A	N/A
Restricted	N/A	N/A	N/A
Landscape impoundments	N/A	8,10,14	8,10,14

Notes:

1. Advisory Notice Only: The Oregon State Health Division recommends that there should be no irrigation of effluent for 3 days prior to harvesting.

Table C.9. Uses of Reclaimed Water in Oregon

Type of Reuse	Category
2. Surface irrigation where edible portion of crop does not contact the ground and where fruit or nuts shall not be harvested off the ground.	
3. The Department may permit spraying if it can be demonstrated that public health and the environment will be adequately protected from aerosols. Advisory Notice Only:	
4. Surface or spray irrigation: no animals shall be on the pasture during irrigation.	
5. Signs shall be posted around the perimeter of the facility's perimeter and other locations indicating that reclaimed water is used for irrigation and is not safe for drinking, and in the case of effluent quality Levels II and III for body contact (e.g., for Level IV, ATTENTION: RECLAIMED WATER USED FOR IRRIGATION DO NOT DRINK × ATENCION: RECLAMADO DESPERDICIO DE AGUA USADO PARA LA IRRIGACION × ATENCION: RECLAMADO DESPERDICIO DE AGUA USADO PARA LA IRRIGACION WATER USED FOR IRRIGATION AVOID CONTACT DO NOT DRINK × ATENCION: RECLAMADO DESPERDICIO DE AGUA USADO PARA LA IRRIGACION).	
6. Reclaimed water shall be applied in a manner so that it is not sprayed onto areas where food is prepared or served or onto drinking fountains.	
7. Reclaimed water shall be applied in a manner so that it is not sprayed within 100 ft from areas where food is prepared or served or where drinking fountains are located.	
8. Signs shall be posted around the perimeter and other locations indicating that reclaimed water is used and is not safe for drinking and in the case of effluent quality Levels II and III for body contact (e.g., for Level IV, ATTENTION: RECLAMADO DESPERDICIO DE AGUA NO BEBA EL AGUA; for Levels II and III, ATTENCION: RECLAMADO DESPERDICIO DE AGUA EVITE EL CONTACTO NO BEBA EL AGUA).	
9. The Department may impose more-stringent limits on the use of reclaimed water if it believes they are necessary to protect public health and the environment.	
10. There shall be no disposal of reclaimed waters into surface or groundwaters without authorization by an NPDES or Water Pollution Control Facility (WPCF) permit.	
11. Use of reclaimed water in evaporative cooling systems shall be approved only if the user can demonstrate that aerosols will not present a hazard to public health.	
12. Members of the public and employed personnel at the site of the use of reclaimed water shall be notified that the water is reclaimed water. Stipulations for how this notification will be provided shall be specified in the reclaimed water use plan.	
13. Unless decontaminated in a manner approved in writing by the Oregon Health Division, tanker trucks or trailers that transport and/or use reclaimed water may not transport potable water intended for use as domestic water. A tanker truck or trailer that transports and/or uses reclaimed water shall have the words "NONPOTABLE WATER" written in 6-in.-high letters on each side and the rear of the truck. The words "NONPOTABLE WATER" shall not be removed until decontamination as approved by the Health Division has occurred.	
14. Aerators or decorative fixtures that may generate aerosols shall not be used unless approved in writing by the Department. Approval will be considered if it can be demonstrated that aerosols will be confined to the area of the impoundment or a restricted area around the impoundment.	

Table C.10. Uses of Reclaimed Water in Virginia

Type of Reuse	Category ^a	
	Level 1	Level 2
Urban - Unrestricted access		
All types of landscape irrigation in public access areas (i.e., golf courses, cemeteries, public parks, school yards, and athletic fields)	Allowed	
Toilet flushing – nonresidential		
Firefighting or fire protection and fire suppression in nonresidential buildings		

Table C.10. Uses of Reclaimed Water in Virginia

Type of Reuse	Category ^a	Level 1	Level 2
Outdoor domestic or residential reuse (i.e., lawn watering and noncommercial car washing)			
Commercial car washes			
Commercial air-conditioning systems			
Irrigation – Unrestricted access^b		Allowed	
Irrigation for any food crops not commercially processed, including crops eaten raw			
Irrigation – Restricted access^{b,c}			
Irrigation for any food crops commercially processed		Allowed	
Irrigation for nonfood crops and turf, including fodder, fiber and seed crops; pasture for foraging livestock; sod farms; ornamental nurseries; and silviculture			
Landscape Impoundments^d			
Potential for public access or contact		Allowed	
Landscape Impoundments^d			
No potential for public access or contact		Allowed	
Construction^e			
Soil compaction		Allowed	
Dust control			
Washing of aggregate			
Manufacture of concrete			
Industrial^e			
Commercial laundries		Allowed	
Industrial^e			
Livestock watering ^f			
Aquaculture ^g			
Stack scrubbing			
Street washing			
Boiler feed			
Ship ballast			
Once-through cooling ^h			
Recirculating cooling towers ^h			

Notes:

a For reclaimed industrial wastewater, minimum standards required shall be determined on a case-by-case basis relative to the proposed reuse or reuses.

b Reclaimed water treated to Level 1 or 2 may be used for surface irrigation, including spray irrigation. Reclaimed water treated to Level 2 may be used for spray irrigation if

Table C.10. Uses of Reclaimed Water in Virginia

Type of Reuse	Category ^a	
	Level 1	Level 2
the area to be irrigated has restricted public access and has appropriate setbacks in accordance with 9VAC25-740-170. Reclaimed water treated to Level 1 or 2 may be used for irrigation of food crops eaten raw, excluding root crops, only when there will be no direct contact (or indirect contact via aerosol carry) between the reclaimed water and edible portions of the crop.		
c For irrigation with reclaimed water treated to Level 2, the following shall be prohibited unless Level 1 disinfection is provided:		
1. Grazing by milking animals on the irrigation reuse site for 15 days after irrigation with reclaimed water ceases, and		
2. Harvesting, retail sale, or access by the general public to ornamental nursery stock or sod farms for 14 days after irrigation with reclaimed water ceases.		
d Landscape impoundments may also be used to store reclaimed water for other subsequent reuses of that reclaimed water, such as irrigation, if included in an inventory of reclaimed water storage facilities submitted to the board pursuant to 9VAC25-740-110 C 15.		
e Worker contact with reclaimed water treated to Level 2 shall be minimized. Level 1 disinfection shall be provided when worker contact with reclaimed water is likely.		
f Level 1 disinfection shall be provided when the reclaimed water is consumed by milking livestock.		
g Level 1 disinfection shall be provided for aquaculture production of fish to be consumed raw, such as for sushi.		
h Windblown spray generated by once-through cooling or recirculating cooling towers using reclaimed water treated to Level 2 shall not reach areas accessible to workers or the public unless Level 1 disinfection is provided. See also setback requirements in 9VAC25-740-170 for open cooling towers.		

Table C.11. Uses of Reclaimed Water in Washington

Type of Reuse	Category			
	Class A	Class B	Class C	Class D
Irrigation of Nonfood Crops				
Trees and fodder, fiber, and seed crops	Allowed	Allowed	Allowed	Allowed
Sod ornamental plants for commercial use and pasture to which milking cows or goats have access	Allowed	Allowed	Allowed	Allowed
Irrigation of Food Crops				
Spray irrigation				
All food crops	Allowed	Allowed	Allowed	Allowed
Food crops which undergo physical or chemical processing sufficient to destroy all pathogenic agents	Allowed	Allowed	Allowed	Allowed
Surface irrigation				
Food crops where there is no reclaimed water contact with edible portion of crop	Allowed	Allowed		
Root crops	Allowed	Allowed	Allowed	Allowed
Orchards and vineyards	Allowed	Allowed	Allowed	Allowed
Food crops which undergo physical or chemical processing sufficient to destroy all pathogenic agents	Allowed	Allowed	Allowed	Allowed
Landscape Irrigation				
Restricted-access areas (e.g., cemeteries and freeway landscapes)	Allowed	Allowed	Allowed	
Open-access areas (e.g., golf courses, parks, playgrounds, school yards, and residential landscapes)	Allowed	Allowed		

Table C.11. Uses of Reclaimed Water in Washington

Type of Reuse	Category			
	Class A	Class B	Class C	Class D
Impoundments				
Landscape impoundments	Allowed	Allowed	Allowed	Allowed
Restricted recreational impoundments	Allowed	Allowed	Allowed	Allowed
Nonrestricted recreational impoundments	Allowed	Allowed	Allowed	Allowed
Fish Hatchery Basins				
Decorative Fountains				
Flushing of Sanitary Sewers				
Street Cleaning	Allowed	Allowed	Allowed	Allowed
Street sweeping, brush dampening	Allowed	Allowed	Allowed	Allowed
Street washing, spray	Allowed	Allowed	Allowed	Allowed
Washing of Corporation Yards, Lots, and Sidewalks				
Dust Control (Dampening of Unpaved Roads and Other Surfaces)				
Dampening of Soil for Compaction (at Construction Sites, Landfills, etc.)				
Water Jetting for Consolidation of Backfill around Pipelines				
Pipelines for reclaimed water, sewage, storm drainage, and gas and conduits for electricity	Allowed	Allowed	Allowed	Allowed
Firefighting and Protection				
Dumping from aircraft	Allowed	Allowed	Allowed	Allowed
Hydrants or sprinkler systems in buildings	Allowed	Allowed	Allowed	Allowed
Toilet and Urinal Flushing				
Ship Ballast				
Washing of Aggregate and Making of Concrete				
Industrial Boiler Feed				
Industrial Cooling				
Aerosols or other mist not created	Allowed	Allowed	Allowed	Allowed
Aerosols or other mist created (e.g., use in cooling towers, forced-air evaporation, or spraying)	Allowed	Allowed	Allowed	Allowed
Industrial Process				
Without exposure of workers	Allowed	Allowed	Allowed	Allowed
With exposure of workers	Allowed	Allowed	Allowed	Allowed

Table C.12. Uses of Reclaimed Water in Wyoming

Type of Reuse	Category		
	A	B	C
Irrigation			
Land with a high potential for public exposure	Allowed		
Land with a moderate potential for public exposure	Allowed	Allowed	
Land with a low potential for public exposure	Allowed	Allowed	Allowed
Direct-human-consumption food crops	Allowed	Allowed	
Indirect-human-consumption food crops	Allowed	Allowed	Allowed

APPENDIX D

SUGGESTED GUIDELINES FOR WATER REUSE BY USEPA AND USAID¹

Table D. Suggested Guidelines for Water Reuse by USEPA and USAID

Types of Reuse	Treatment	Reclaimed Water Quality ²	Reclaimed Water Monitoring	Setback Distances ³	Comments
Urban Reuse All types of landscape irrigation, (e.g., golf courses, parks, cemeteries) – also vehicle washing, toilet flushing, use in fire protection systems and commercial air conditioners, and other uses with similar access or exposure to the water	Secondary ⁴ Filtration, ⁵ Disinfection ⁶	pH = 6–9; < 10-mg/L BOD, ⁷ < 2 NTU, ⁸ No detectable fecal coliform/100 mL, ^{9,10} 1-mg/L Cl ₂ residual (minimum) ¹¹	pH - weekly; BOD - weekly; Turbidity continuous; Coliform - daily; Cl ₂ residual continuous	50 ft (15 m) to potable water supply wells	See Appendix E. At controlled-access irrigation sites where design and operational measures significantly reduce the potential of public contact with reclaimed water, a lower level of treatment, e.g., secondary treatment and disinfection to achieve < 14 fecal coliform/100 mL, may be appropriate. Chemical (coagulant and/or polymer) addition prior to filtration may be necessary to meet water quality recommendations. The reclaimed water should not contain measurable levels of viable pathogens. Reclaimed water should be clear and odorless. A higher chlorine residual and/or a longer contact time may be necessary to ensure that viruses and parasites are inactivated or destroyed. A chlorine residual of 0.5 mg/L or greater in the distribution system is recommended to reduce odors, slime, and bacterial regrowth.
Restricted-access Area Irrigation Sod farms, silviculture sites, and other areas where public access is prohibited, restricted, or infrequent	Secondary ⁴ Disinfection ⁶	pH = 6–9; < 30-mg/L BOD, ⁷ < 30-mg/L TSS, ⁸ < 200 fecal coliform/100 mL, ^{9,13,14} 1-mg/L Cl ₂ residual (minimum) ¹¹	pH - weekly; BOD - weekly; TSS - daily; Coliform - daily; Cl ₂ residual continuous	300 ft (90 m) to potable water supply wells; 100 ft (30 m) to areas accessible to the public (if spray irrigation)	See Appendix E. If spray irrigation, TSS less than 30 mg/L may be necessary to avoid clogging of sprinkler heads.
Agricultural Reuse – Food Crops Not	Secondary ⁴ Filtration, ⁵	pH = 6–9; < 10-mg/L BOD, ⁷	pH - weekly; BOD - weekly;	50 ft (15 m) to potable water	See Appendix E. Chemical (coagulant and/or polymer) addition prior to

Table D. Suggested Guidelines for Water Reuse by USEPA and USAID

Types of Reuse	Treatment	Reclaimed Water Quality ²	Reclaimed Water Monitoring	Setback Distances ³	Comments
Commercially Processed¹⁵ Surface or spray irrigation of any food crop, including crops eaten raw	Disinfection ⁶	< 2 NTU ⁸ No detectable fecal coliform/100 mL, ^{9,10} 1-mg/L Cl ₂ residual (minimum) ¹¹	Turbidity continuous Coliform - daily; Cl ₂ residual continuous	Supply wells	Filtration may be necessary to meet water quality recommendations. The reclaimed water should not contain measurable levels of viable pathogens. ¹² A higher chlorine residual and/or a longer contact time may be necessary to ensure that viruses and parasites are inactivated or destroyed. High nutrient levels may adversely affect some crops during certain growth stages.
Agricultural Reuse – Food Crops Commercially Processed¹⁵ Surface irrigation of orchards and vineyards	Secondary⁴ Disinfection ⁶	pH = 6–9; < 30-mg/L BOD, ⁷ < 30-mg/L TSS; < 200 fecal coliform/100 mL, ^{9,13,14} 1-mg/L Cl ₂ residual (minimum) ¹¹	pH - weekly; BOD - weekly; TSS - daily; Coliform - daily; Cl ₂ residual continuous	300 ft (90 m) to potable water supply wells; 100 ft (30 m) to areas accessible to the public (if spray irrigation)	See Appendix E. If spray irrigation, TSS less than 30 mg/L may be necessary to avoid clogging of sprinkler heads. High nutrient levels may adversely affect some crops during certain growth stages.
Agricultural Reuse – Nonfood Crops Pasture for milking animals; fodder, fiber, and seed crops	Secondary⁴ Disinfection ⁶	pH = 6–9; < 30-mg/L BOD, ⁷ < 30-mg/L TSS; < 200 fecal coliform/100 mL, ^{9,13,14} 1-mg/L Cl ₂ residual (minimum) ¹¹	pH - weekly; BOD - weekly; TSS - daily; Coliform - daily; Cl ₂ residual continuous	300 ft (90 m) to potable water supply wells; 100 ft (30 m) to areas accessible to the public (if spray irrigation)	See Appendix E. If spray irrigation, TSS less than 30 mg/L may be necessary to avoid clogging of sprinkler heads. High nutrient levels may adversely affect some crops during certain growth stages. Milking animals should be prohibited from grazing for 15 days after irrigation ceases. A higher level of disinfection, e.g., to achieve < 14 fecal coliform/100 mL, should be provided if this waiting period is not observed.
Recreational Impoundments Incidental contact (e.g., fishing and boating) and full-body contact with reclaimed water allowed	Secondary⁴ Filtration, ⁵ Disinfection ⁶	pH = 6–9; < 10-mg/L BOD, ⁷ < 2 NTU, ⁸ No detectable fecal coliform/100 mL, ^{9,10} 1-mg/L Cl ₂ residual (minimum) ¹¹	pH - weekly; BOD - weekly; Turbidity continuous; Coliform - daily; Cl ₂ residual continuous	500 ft (150 m) to potable water supply wells (minimum) if bottom not sealed	Dechlorination may be necessary to protect aquatic species of flora and fauna. Reclaimed water should be unirritating to skin and eyes. Reclaimed water should be clear and odorless. Nutrient removal may be necessary to avoid algal growth in impoundments. Chemical (coagulant and/or polymer) addition prior to filtration may be necessary to meet water quality recommendations. The reclaimed water should not contain measurable levels of viable pathogens. ¹² A higher chlorine residual and/or a longer contact time may be necessary to

Table D. Suggested Guidelines for Water Reuse by USEPA and USAID

Types of Reuse	Treatment	Reclaimed Water Quality ²	Reclaimed Water Monitoring	Setback Distances ³	Comments
Landscape Impoundments Aesthetic impoundment where public contact with reclaimed water is not allowed	Secondary, ⁴ Disinfection ⁶	< 30-mg/L BOD, ⁷ < 30-mg/L TSS; < 200 fecal coli/100 mL, ^{9, 13, 14} 1-mg/L Cl ₂ residual (minimum) ¹¹	pH - weekly; TSS - daily; Coliform - daily; Cl ₂ residual continuous	500 ft (150 m) to potable water supply wells (minimum) if bottom not sealed	ensure that viruses and parasites are inactivated or destroyed. Fish caught in impoundments can be consumed.
Construction Use Soil compaction, dust control, washing aggregate, making concrete	Secondary, ⁴ Disinfection ⁶	< 30-mg/L BOD, ⁷ < 30-mg/L TSS; < 200 fecal coli/100 mL, ^{9, 13, 14} 1-mg/L Cl ₂ residual (minimum) ¹¹	BOD - weekly; TSS - daily; Coliform - daily; Cl ₂ residual continuous		Worker contact with reclaimed water should be minimized. A higher level of disinfection, e.g., to achieve < 14 fecal coli/100 mL, should be provided when frequent work contact with reclaimed water is likely.
Industrial Reuse Once-through cooling	Secondary, ⁴ Disinfection ⁶	pH = 6-9; < 30-mg/L BOD, ⁷ < 30-mg/L TSS; < 200 fecal coli/100 mL, ^{9, 13, 14} 1-mg/L Cl ₂ residual (minimum) ¹¹	pH - weekly; BOD - weekly; TSS - daily; Coliform - daily; Cl ₂ residual continuous	300 ft (90 m) to areas accessible to the public	Windblown spray should not reach areas accessible to workers or the public.
Recirculating cooling towers	Secondary, ⁴ Disinfection ⁶ (chemical coagulation and filtration 5 may be needed)	Variable depends on recirculation ratio: pH = 6-9; < 30-mg/L BOD, ⁷ < 30-mg/L TSS; < 200 fecal coli/100 mL, ^{9, 13, 14} 1-mg/L Cl ₂ residual (minimum) ¹¹	pH - weekly; BOD - weekly; TSS - daily; Coliform - daily; Cl ₂ residual continuous	300 ft (90 m) to areas accessible to the public; may be reduced or eliminated if high level of disinfection is provided.	Windblown spray should not reach areas accessible to workers or the public. Additional treatment by user is usually provided to prevent scaling, corrosion, biological growth, fouling, and foaming.

Table D. Suggested Guidelines for Water Reuse by USEPA and USAID

Types of Reuse	Treatment	Reclaimed Water Quality ²	Reclaimed Water Monitoring	Setback Distances ³	Comments
Other Industrial Uses				Depends on site-specific uses	
Environmental Reuse Wetlands, marshes, wildlife habitat, stream augmentation	Variable; Secondary ⁴ ; Disinfection ⁶ (minimum)	Variable, but not to exceed: < 30-mg/L BOD; < 30-mg/L TSS; < 200 fecal colif/100 mL ^{9,13,14}	BOD - weekly; TSS - daily; Coliform - daily; Cl ₂ residual continuous		Dechlorination may be necessary to protect aquatic species of flora and fauna. Possible effects on groundwater should be evaluated. Receiving water quality requirements may necessitate additional treatment. The temperature of the reclaimed water should not adversely affect ecosystem.
Groundwater Recharge Spreading or injection into aquifers not used for public water supply	Site-specific and use-dependent; Primary (minimum) for spreading; Secondary ⁴ (minimum) for injection	Site-specific and use dependent	Depends on treatment and use		Facility should be designed to ensure that no reclaimed water reaches potable water supply aquifers. For spreading projects, secondary treatment may be needed to prevent clogging. For injection projects, filtration and disinfection may be needed to prevent clogging.
Indirect Potable Reuse Groundwater recharge by spreading into potable aquifers	Secondary ⁴ ; Disinfection ⁶ May also need filtration ⁵ and/or advanced wastewater treatment ¹⁶	Secondary ⁴ ; Disinfection ⁶ Meet drinking water standards after percolation through vadose zone	Includes, but not limited to, the following: pH - daily; Coliform daily; Cl ₂ residual continuous; Drinking water standards quarterly; Other ¹⁷ - depends on constituent. BOD - weekly; turbidity continuous	500 ft (150 m) to extraction wells; May vary depending on treatment provided and site-specific conditions	The depth to groundwater (i.e., thickness to the vadose zone) should be at least 6 ft (2 m) at the maximum groundwater mounding point. The reclaimed water should be retained underground for at least 6 months prior to withdrawal. Recommended treatment is site-specific and depends on factors such as type of soil, percolation rate, thickness of vadose zone, native groundwater quality, and dilution. Monitoring wells are necessary to detect the influence of the recharge operation on the groundwater. The reclaimed water should not contain measurable levels of viable pathogens after percolation through the vadose zone. ¹²

Table D. Suggested Guidelines for Water Reuse by USEPA and USAID

Types of Reuse	Treatment	Reclaimed Water Quality ²	Reclaimed Water Monitoring	Setback Distances ³	Comments
Indirect Potable Reuse Groundwater recharge by injection into potable aquifers	Secondary ⁴ ; Filtration ⁵ ; Disinfection ⁶ ; Advanced wastewater treatment ¹⁶	Includes, but not limited to, the following: pH = 6.5–8.5; < 2 NTU; No detectable total coliform/100 mL ^{9,10} 1-mg/L Cl ₂ residual (minimum), ¹¹ < 3-mg/L TOC; < 0.2-mg/L TOX; Meet drinking water standards	Includes, but not limited to, the following: pH - daily; Turbidity continuous; Total coliform daily; Cl ₂ residual continuous; Drinking water standards quarterly; Other ¹⁷ - depends on constituent	2000 ft (600 m) to extraction wells; May vary depending on site-specific conditions	The reclaimed water should be retained underground for at least 9 months prior to withdrawal. Monitoring wells are necessary to detect the influence of the recharge operation on the groundwater. Recommended quality limits should be met at the point of injection. The reclaimed water should not contain measurable levels of viable pathogens after percolation through the vadose zone. ¹² A higher chlorine residual and/or a longer contact time may be necessary to ensure virus and protozoan inactivation.
Indirect Potable Reuse Augmentation of surface supplies	Secondary ⁴ ; Filtration ⁵ ; Disinfection ⁶ ; Advanced wastewater treatment ¹⁶	Includes, but not limited to, the following: pH = 6.5–8.5; < 2 NTU; No detectable total coliform/100 mL ^{9,10} 1-mg/L Cl ₂ residual (minimum), ¹¹ < 3-mg/L TOC; Meet drinking water standards	Includes, but not limited to, the following: pH - daily; Turbidity continuous; Total coliform daily; Cl ₂ residual continuous; Drinking water standards quarterly; Other ¹⁷ - depends on constituent	Site-specific	Recommended level of treatment is site-specific and depends on factors such as receiving water quality, time and distance to point of withdrawal, and dilution and subsequent treatment prior to distribution for potable uses. The reclaimed water should not contain measurable levels of viable pathogens. ¹² A higher chlorine residual and/or a longer contact time may be necessary to ensure virus and protozoan inactivation.

Notes:

1. These guidelines are based on water reclamation and reuse practices in the United States, and they are especially directed at states that have not developed their own regulations or guidelines. While the guidelines should be useful in many areas outside the United States, local conditions may limit the applicability of the guidelines in some countries. It is explicitly stated that the direct application of these suggested guidelines will not be used by USAID as strict criteria for funding.
2. Unless otherwise noted, recommended quality limits apply to the reclaimed water at the point of discharge from the treatment facility.
3. Setback distances are recommended to protect potable water supply sources from contamination and to protect humans from unreasonable health risks due to exposure to reclaimed water.

Table D. Suggested Guidelines for Water Reuse by USEPA and USAID

Types of Reuse	Treatment	Reclaimed Water Quality ²	Reclaimed Water Monitoring	Setback Distances ³	Comments
4. Secondary treatment processes include activated sludge processes, trickling filters, and RBCs and may include stabilization pond systems. Secondary treatment should produce effluent in which both the BOD and TSS do not exceed 30 mg/L.					
5. Filtration means the passing of wastewater through natural undisturbed soils or filter media such as sand and/or anthracite or filter cloth or the passing of wastewater through microfilters or other membrane processes.					
6. Disinfection means the destruction, inactivation, or removal of pathogenic microorganisms by chemical, physical, or biological means. Disinfection may be accomplished by chlorination, UV radiation, ozonation, other chemical disinfectants, membrane processes, or other processes. The use of chlorine as defining the level of disinfection does not preclude the use of other disinfection processes as an acceptable means of providing disinfection for reclaimed water.					
7. As determined from the BOD ₅ .					
8. The recommended turbidity limit should be met prior to disinfection. The average turbidity should be based on a 24-h time period. The turbidity should not exceed 5 NTU at any time. If TSS is used in lieu of turbidity, the TSS should not exceed 5 mg/L.					
9. Unless otherwise noted, recommended coliform limits are median values determined from the bacteriological results of the last 7 days for which analyses have been completed. Either the membrane filter or fermentation-tube technique may be used.					
10. The number of fecal coliform organisms should not exceed 14/100 mL in any sample.					
11. Total chlorine residual should be met after a minimum contact time of 30 min.					
12. It is advisable to fully characterize the microbiological quality of the reclaimed water prior to implementation of a reuse program.					
13. The number of fecal coliform organisms should not exceed 800/100 mL in any sample.					
14. Some stabilization pond systems may be able to meet this coliform limit without disinfection.					
15. Commercially processed food crops are those that, prior to sale to the public or others, have undergone chemical or physical processing sufficient to destroy pathogens.					
16. Advanced wastewater treatment processes include chemical clarification, carbon adsorption, RO and other membrane processes, air stripping, UF, and ion exchange.					
17. Monitoring should include inorganic and organic compounds, or classes of compounds, that are known or suspected to be toxic, carcinogenic, teratogenic, or mutagenic and are not included in the drinking water standards.					

APPENDIX E
RECOMMENDED LIMITS FOR CONSTITUENTS IN RECLAIMED WATER FOR IRRIGATION BY USEPA AND USAID

Table E. Recommended Limits for Constituents in Reclaimed Water for Irrigation by USEPA and USAID

Constituent	Long-Term Use (mg/L)	Short-Term Use (mg/L)	Remarks
Aluminum	5	20	Can cause a loss of productivity in acid soils, but soils at pH 5.5 to 8.0 will precipitate the ion and eliminate toxicity.
Arsenic	0.1	2	Toxicity to plants varies widely, ranging from 12 mg/L for Sudan grass to less than 0.05 mg/L for rice.
Beryllium	0.1	0.5	Toxicity to plants varies widely, ranging from 5 mg/L for kale to 0.5 mg/L for bush beans.
Boron	0.75	2	Essential to plant growth, with optimum yields for many obtained at a few tenths of a milligram per liter in nutrient solutions. Toxic to many sensitive plants (e.g., citrus) at 1 mg/L. Usually sufficient quantities in reclaimed water to correct soil deficiencies. Most grasses are relatively tolerant at 2.0 to 10 mg/L.
Cadmium	0.01	0.05	Toxic to beans, beets, and turnips at concentrations as low as 0.1 mg/L in nutrient solution. Conservative limits recommended.
Chromium	0.1	1	Not generally recognized as an essential growth element. Conservative limits recommended because of lack of knowledge on toxicity to plants.
Cobalt	0.05	5	Toxic to tomato plants at 0.1 mg/L in nutrient solution. Tends to be inactivated by neutral and alkaline soils.
Copper	0.2	5	Toxic to a number of plants at 0.1 to 1.0 mg/L in nutrient solution.
Fluoride	1	15	Inactivated by neutral and alkaline soils.
Iron	5	20	Not toxic to plants in aerated soils but can contribute to soil acidification and loss of essential phosphorus and molybdenum.
Lead	5	10	Can inhibit plant cell growth at very high concentrations.
Lithium	2.5	2.5	Tolerated by most crops at concentrations up to 5 mg/L; mobile in soil. Toxic to citrus at low doses—recommended limit is 0.075 mg/L.
Manganese	0.2	10	Toxic to a number of crops at a few tenths of a milligram to a few milligrams per liter in acidic soils.
Molybdenum	0.01	0.05	Nontoxic to plants at normal concentrations in soil and water. Can be toxic to livestock if forage is grown in soils with high levels of available molybdenum.

Table E. Recommended Limits for Constituents in Reclaimed Water for Irrigation by USEPA and USAID

Constituent	Long-Term Use (mg/L)	Short-Term Use (mg/L)	Remarks
Nickel	0.2	2	Toxic to a number of plants at 0.5 to 1.0 mg/L; reduced toxicity at neutral or alkaline pH.
Selenium	0.02	0.02	Toxic to plants at low concentrations and to livestock if forage is grown in soils with low levels of selenium.
Tin, tungsten, and titanium	—	—	Effectively excluded by plants; specific tolerance levels unknown.
Vanadium	0.1	1	Toxic to many plants at relatively low concentrations.
Zinc	2	10	Toxic to many plants at widely varied concentrations; reduced toxicity at increased pH (6 or above) and in fine-textured or organic soils.
Constituent	Recommended Limit		Remarks
pH	6		Most effects of pH on plant growth are indirect (e.g., pH effects on heavy metals' toxicity described above).
TDS	500 to 2000 mg/L		Below 500 mg/L, no detrimental effects are usually noticed. Between 500 and 1000 mg/L, TDS in irrigation water can affect sensitive plants. At 1000 to 2000 mg/L, TDS levels can affect many crops and careful management practices should be followed. Above 2000 mg/L, water can be used regularly only for tolerant plants on permeable soils.
Free chlorine residual	<1 mg/L		Concentrations greater than 5 mg/L cause severe damage to most plants. Some sensitive plants may be damaged at levels as low as 0.05 mg/L.

APPENDIX F

RECOMMENDED MINIMUM VERIFICATION MONITORING OF MICROBIAL PERFORMANCE TARGETS FOR WASTEWATER AND EXCRETA USE IN AGRICULTURE AND AQUACULTURE BY THE WHO

Table F. Recommended Minimum Verification Monitoring of Microbial Performance Targets for Wastewater and Excreta Use in Agriculture and Aquaculture by WHO

Activity/Exposure	Water Quality Monitoring ^a Parameters	
Agriculture	<i>E. coli</i> per 100 mL ^b (arithmetic mean)	Helminth eggs per liter ^b (arithmetic mean)
Unrestricted irrigation		
Root crops	$\leq 0.10^3$	≤ 0.1
Leaf crops	$\leq 0.10^4$	
Drip irrigation, high-growing crops	$\leq 0.10^5$	
Restricted irrigation		
Labor-intensive, high-contact agriculture	$\leq 0.10^4$	≤ 0.1
Highly mechanized agriculture	$\leq 0.10^5$	
Septic tank	$\leq 0.10^6$	
Aquaculture	<i>E. coli</i> per 100 mL ^b (arithmetic mean)	Viable trematode eggs per liter ^b
Produce consumers		
Pond	$\leq 0.10^4$	Not detected
Wastewater	$\leq 0.10^5$	Not detected
Excreta	$\leq 0.10^6$	Not detected
Workers, local communities		
Pond	$\leq 0.10^3$	No viable trematode eggs
Wastewater	$\leq 0.10^4$	No viable trematode eggs
Excreta	$\leq 0.10^5$	No viable trematode eggs

Notes:

^aMonitoring should be conducted at the point of use or the point of effluent discharge. Frequency of monitoring is as follows:

- Urban areas: one sample every 2 weeks for *E. coli* and one sample per month for helminth eggs.
- Rural areas: one sample every month for *E. coli* and one sample every 1–2 months for helminth eggs.

Five-liter composite samples are required for helminth eggs prepared from grab samples taken six times per day. Monitoring for trematode eggs is difficult because of a lack of standardized procedures. The inactivation of trematode eggs should be evaluated as part of the validation of the system.

^bFor excreta, weights may be used instead of volumes, depending on the type of excreta: 100 mL of wastewater is equivalent to 1–4 g of total solids; 1 L = 10–40 g of total solids. The required *E. coli* or helminth numbers would be the same per unit of weight.

APPENDIX G

REGULATIONS FOR OPERATOR CERTIFICATION IN CALIFORNIA

Title 23. Waters

Division 3. State Water Resources Control Board and Regional Water Quality Control Boards

Chapter 26. Classification of Wastewater Treatment Plants and Operator Certification Article 1. General Provisions

§ 3670. Purpose.

The primary purpose of the Wastewater Treatment Plant Classification, Operator Certification, and Contract Operator Registration Program is to protect public health and the environment by providing for the effective operation of wastewater and water recycling treatment plants through the certification of wastewater treatment plant operators.

§ 3670.1. Certification Requirements for Operation of Wastewater Treatment Plants.

No person shall operate a wastewater treatment plant within the meaning of these regulations unless that person has been certified by the division as a wastewater treatment plant operator or operator-in-training at a grade appropriate for the class of plant being operated.

§ 3670.2. Certification Requirement for Operation of Water Recycling Treatment Plants.

- (a) Except as provided in subsection (b) below, no person shall operate a water recycling treatment plant unless that person has been certified by the division as a wastewater treatment plant operator or operator-in-training at a grade appropriate for the class of plant being operated.
- (b) A person certified by the Department of Health Services as a water treatment plant operator may operate a water recycling treatment plant at a grade appropriate for the class of plant operated.
- (c) The State Board may refuse to approve use of a certificate issued by the Department of Health Services or suspend or revoke its approval of the use of the certificate if the operator commits any of the prohibited acts described in Article 7 (commencing with section 3710) of Chapter 26 of Division 3 of the California Code of Regulations.

§ 3671. Definitions.

The following definitions shall apply to this chapter:

- (a) “Activated sludge treatment” means a wastewater treatment process in which predominantly biodegradable pollutants in wastewater are adsorbed and/or absorbed by a suspended mass of living aerobic organisms called “activated sludge”. The suspended mass is subsequently separated from the treated wastewater by a sedimentation process either for further use in the process or for disposal.
- (b) “Agency” or “municipality” means any government agency created by federal law or any city, town, county, district, or other government created by or pursuant to state law which owns or operates a wastewater treatment plant. “Agency” also includes any privately-owned organization which owns or operates a wastewater treatment plant regulated by the Public Utilities Commission pursuant to Sections 216 and 230.6 of, and Chapter 4 (commencing with Section 701) of Part 1 of division 1 of the Public Utilities Code.
- (c) “Appellant” means a person who appeals a decision made by the Office of Operator Certification or division Chief regarding denial of an application, the results of an examination, or disciplinary action taken.
- (d) “Applicant” means a person who files an application for an examination, certification, renewal, or reinstatement as a wastewater treatment plant operator or operator-in-training.
- (e) “Basic science courses” means college-level courses in the combined fields of mathematics, physics, chemistry, and biology.
- (f) “Biological filtration treatment” (biofiltration) means a wastewater treatment process in which predominantly biodegradable pollutants in wastewater are adsorbed and/or absorbed by

masses of living aerobic organisms and which are attached to stationary support media as the wastewater is caused to trickle over the media. Settleable material that may have sloughed from the medium surfaces is subsequently separated from the treated wastewater by a sedimentation process for disposal.

- (g) "Board" or "State Water Board" as used in this chapter means the five members of the State Water Resources Control Board.
- (h) "Chief Plant Operator" means a supervisor who is certified as an operator and who is responsible for the overall operation of a wastewater treatment plant.
- (i) "Contract operator" means any person or entity who enters a promissory agreement to operate a wastewater treatment plant.
- (j) "Direct supervision" means the oversight and inspection of the work performance of an operator-in-training by the supervisor, without an intervening person, to ensure the safe and proper execution of the duties of the operator-in-training.
- (k) "Division" means that unit of the division of the board in which the Office of Operator Certification is located.
- (l) "Extended aeration treatment" means a modification of the activated sludge treatment process which utilizes long aeration periods to promote aerobic digestion of the biomass.
- (m) "Maintenance" means those activities which will be credited toward operator experience under the certification program. Those activities are limited to the day-to-day servicing, adjustment or regulation of equipment which are performed by an operator and are necessary to maintain reliable operation of major treatment processes.
- (n) "Office of Operator Certification" means that unit of the division which administers the Wastewater Treatment Plant Classification and Operator Certification Program.
- (o) "Operates" means the performance of day-to-day activities primarily consisting of the control of any process which may affect the quality of the discharge of a wastewater treatment plant. "Operates" may include performance of day-to-day maintenance work so long as the primary function of the operator is control of the process. "Operates" does not include maintenance functions which are not necessary for the reliable operation of major treatment processes.
- (p) "Operator" means any person operating a wastewater treatment plant and who occupies a position and performs duties for which the Office of Operator Certification requires an operator certificate.
- (q) "Operator-in-training" means any person who operates a wastewater treatment plant under the direct supervision of a certified operator while gaining experience to qualify for an operator certificate.
- (r) "Pond treatment" means processing in a pond in which biological oxidation of organic matter is effected by natural or artificially accelerated transfer of oxygen to the water.
- (s) "Preliminary treatment" means a process or processes to remove or reduce in size solids which could damage equipment or reduce effectiveness of other treatment processes.
- (t) "Primary treatment" means a wastewater treatment process that allows those substances in wastewater that readily settle or float to be separated from the water being treated.
- (u) "Secondary treatment" means treatment beyond primary treatment to remove colloidal and dissolved organic matter and further remove suspended matter, usually by biological processes such as activated sludge and biological filtration treatment.
- (v) "Shift supervisor" means a certified operator who oversees and directs the operation or a phase of operation of a wastewater treatment plant during a specific work period and who reports to a supervisor or a chief plant operator.
- (w) "Supervisor" means a certified operator who oversees and directs the operation of a wastewater treatment plant, who inspects the performance of other operators of a wastewater treatment plant, and who reports to the chief plant operator.
- (x) "Tertiary treatment" (advanced waste treatment) means treatment beyond secondary treatment, which may include filtration, coagulation and nutrient removal, but excluding disinfection.
- (y) "Wastewater treatment plant" means either of the following:
 - (1) Any facility owned by a state, local, or federal agency and used in the treatment or reclamation of sewage and industrial wastes.
 - (2) Any privately owned facility used in the treatment or reclamation of sewage and industrial wastes, and regulated by the Public Utilities Commission pursuant to Sections 216 and

230.6 of, and Chapter 4 (commencing with Section 701) of Part 1 of Division 1, of the Public Utilities Code.

- (z) "Water recycling treatment plant" means a treatment plant that receives and further treats secondary and/or tertiary effluent from a wastewater treatment plant.

Article 2. Classification of Wastewater Treatment Plants and Agency Reporting Requirements

§ 3675. Classification of Wastewater and Water Recycling Treatment Plants.

- (a) The division shall classify all wastewater treatment plants, including water recycling treatment plants, according to the following criteria:

Class	Treatment Process	Design Flow (in millions of gallons per day)
I	Pond	All
	Primary	1.0 or less
II	Primary	Greater than 1.0 through 5.0
	Biofiltration	1.0 or less
	Extended Aeration	All
III	Primary	Greater than 5.0 through 20.0
	Biofiltration	Greater than 1.0 through 10.0
	Activated Sludge	5.0 or less
	Tertiary	1.0 or less
IV	Primary	Greater than 20.0
	Biofiltration	Greater than 10.0 through 30.0
	Activated Sludge	Greater than 5.0 through 20.0
	Tertiary	Greater than 1.0 through 10.0
V	Biofiltration	Greater than 30.0
	Activated Sludge	Greater than 20.0
	Tertiary	Greater than 10.0

- (b) Plants may be classified in a group different than indicated in this section if:

- (1) they have characteristics which make operation more difficult than the operation of other similar plants of the same flow range; or,
- (2) the conditions of flow or the use of the receiving waters require an unusually high degree of plant operational control; or,
- (3) they use an approved method of wastewater treatment which is not included in this section.

§ 3676. Reporting Requirements by Agencies to the Division.

- (a) Within 30 calendar days after a plant begins operating, each agency shall submit to the division a description of the plant's treatment processes, a design flow of the plant, an organization chart, and job descriptions and duty rosters for plant personnel.
- (b) Each agency shall notify the division in writing within 30 calendar days of a change in the employment of the person designated as chief plant operator and any change in the reportable items in subsection (a) above which may affect the classification of the wastewater treatment plant.
- (c) Each agency shall notify the division in writing within 30 calendar days of any final disciplinary action resulting in suspension, demotion, or discharge of a certified operator or operator-in-training if the disciplinary action is the result of the operator's commission of any of the acts which are grounds for discipline listed in Section 3710. The notice shall identify the name of the operator or operator-in-training, the specific violations and the disciplinary action taken.
- (d) Reports regarding final disciplinary action received from agencies shall be retained in state board files for a period of three years unless the state board takes disciplinary action. If the state board takes disciplinary action, reports submitted by agencies shall remain in state board files for ten years.

Article 3. Grades of Operator Certification for the Operation of Wastewater Treatment Plants

§ 3680. Grades of Operator Certification.

- (a) Chief Plant Operators - For all plant classes, each chief plant operator shall possess a valid operator certificate of a grade at least equivalent to the class of plant operated.
- (b) Supervisors and Shift Supervisors
 - (1) In Class II, III, and IV plants, supervisors and shift supervisors shall possess valid operator certificates no more than one grade lower than the class of plant operated.
 - (2) In Class V plants, shift supervisors shall possess at least valid Grade III certificates and supervisors shall possess at least Grade IV certificates.
- (c) Operators - Each operator shall possess at least a valid Grade I certificate or a valid operator-in-training certificate. In Class IV and V plants. 50 percent of the operators shall possess at least valid Grade II certificates or valid operator-in-training certificates at the Grade II or higher level.

Article 4. Minimum Qualifications

§ 3683. Education and Experience Requirements.

- (a) No person shall be issued a certificate unless that person passes a written examination specified by these regulations and meets the education and experience requirements prescribed by this article.
- (b) Persons may apply to take an operator certification examination if:
 - (1) they have completed the education necessary for the certificate prior to the final filing date for the examination, in accordance with the provisions of subsection (c) of this section; and,
 - (2) there is sufficient time to gain the experience necessary to qualify for the certificate for which they are applying within four years of June 30 or December 31 (whichever is sooner) following an examination for Grades II, III, IV, and V and within 2 years of June 30 or December 31 (whichever is sooner) following an examination for Grade I.
- (c) Eligibility for certification shall be based on the following qualifications for each grade of wastewater treatment plant operator. Educational points shall be credited pursuant to the provisions of Section 3685.
 - (1) Grade I:
 - Education: Six educational points; AND,
 - Experience: One year of experience performing the functions of a wastewater treatment plant operator
 - (2) Grade II:
 - (A) Education: Graduation from high school or equivalent as specified in Section 3686 and six educational points; AND,
 - Experience: Two years of experience performing the functions of a wastewater treatment plant operator; OR,
 - (B) Experience: One and one-half years of experience performing the functions of a wastewater treatment plant operator while certified as a Grade I operator.
 - (3) Grade III:
 - (A) Education: An associate degree or completion of 60 semester units at a college or university, either of which includes 15 semester units of basic science courses; AND,
 - Experience: Two years of experience performing the functions of a wastewater treatment plant operator; OR,
 - (B) Education: Graduation from high school or equivalent as specified in Section 3686 and 16 educational points; AND,
 - Experience: Fours years of experience performing the functions of a wastewater treatment plant operator; OR,
 - (C) Experience: Three years of experience performing the functions of a wastewater treatment plant operator while certified as a Grade II operator.
 - (4) Grade IV:
 - (A) Education: A bachelor's degree with a major related to wastewater treatment and which includes a minimum of 30 semester units of basic science courses; AND,

- Experience: Two years of experience performing the functions of a wastewater treatment plant operator; OR,
- (B) Education: An associate degree or completion of 60 semester units at a college or university, either of which includes 15 semester units of basic science courses; AND,
Experience: Four years of experience performing the functions of a wastewater treatment plant operator; OR,
- (C) Education: Graduation from high school or equivalent as specified in Section 3686 and 32 educational points; AND,
Experience: Six years of experience performing the functions of a wastewater treatment plant operator; OR,
- (D) Experience: Four years of experience performing the functions of a wastewater treatment plant operator while certified as a Grade III operator.
- (5) Grade V:
- (A) Credential: A valid license as a civil or chemical engineer issued by the California Department of Consumer Affairs, Board of Registration for Professional Engineers and Land Surveyors; AND,
Experience: Four years of experience performing the functions of a wastewater treatment plant operator; OR,
- (B) Education: A bachelor's degree with a major related to wastewater treatment and which includes a minimum of 30 semester units of basic science courses; AND,
Experience: Five years of experience performing the functions of a wastewater treatment plant operator; OR,
- (C) Education: An associate degree or completion of 60 semester units at a college or university, either of which includes 15 semester units of basic science courses; AND,
Experience: Six years of experience performing the functions of a wastewater treatment plant operator; OR,
- (D) Education: Graduation from high school or equivalent as specified in Section 3686 and 48 educational points; AND,
Experience: Ten years of experience performing the functions of a wastewater treatment plant operator; OR,
- (E) Experience: Six years of experience performing the functions of a wastewater treatment plant operator while certified as a Grade IV operator.

§ 3684. Experience Credits.

- (a) Applicants may be credited with one year of experience if they have had two or more years of full-time experience in the operation of a water treatment plant regulated by the California Department of Health Services or by a government agency in another state and while in possession of a valid water treatment plant operator certificate, if:
- (1) the water treatment plant where the experience was gained uses two or more of the following processes: coagulation, sedimentation, aeration, filtration, oxidation, or disinfection; and,
- (2) at the time of their application for certification, they have had one year of full-time experience in the operation of a wastewater treatment plant.
- (b) Applicants, who have one year of experience in the operation of a wastewater treatment plant may substitute 16 educational points for one year of experience. Those educational points used to substitute for experience at one grade may not be used again to substitute for experience at another grade. The substitution may not be made by applicants qualifying under the provisions of Sections 3683 (c) (1) and 3683 (c) (4) (A).

§ 3685. Educational Points.

- (a) Pursuant to the provisions of this article, applicants may be required to obtain educational points to qualify for certification. Educational points may be earned as follows:
- (1) One completed three-unit semester course which is directly related to wastewater treatment and which is part of the curriculum of an accredited college or university is equal to eight educational points. Completed courses which result in more or less than

three units or which are quarter units rather than semester units will be credited with educational points on a proportional basis.

- (2) All other courses will be assigned educational points at the rate of one educational point per 10 hours of completed classroom instruction. Subjects which are directly related to wastewater treatment shall be assigned full credit for educational points. Subjects which are indirectly related shall be given one half credit.
- (3) One Continuing Education Unit which is directly related to wastewater treatment is equal to one educational point.

(b) Applicants may not substitute experience for educational points.

§ 3686. High School Equivalence.

High school equivalence may be obtained by substituting six educational points for each uncompleted year of high school through grade 12 or by passing an approved General Educational Development test, or by obtaining a Certificate of Proficiency issued by the State Board of Education in accordance with Section 48412 of the Education Code.

Article 5. Examination and Certification of Wastewater Treatment Plant Operators

§ 3700. Application for Examination.

- (a) Content - An application for examination shall contain but not be limited to the following information:
 - (1) the applicant's full name, mailing address, work telephone number, and date of birth;
 - (2) information regarding former employment, current operator status, other operator certificates held in California or other states, engineering registrations held, and education and experience gained;
 - (3) if employed as an operator, the original signature of the chief plant operator, verifying the applicant's experience as an operator;
 - (4) the applicant's original signature;
 - (5) copies of college transcripts, grade cards, or certificates of completion for courses related to wastewater treatment to verify completion of education requirements;
 - (6) any additional information, evidence, statements, or documents to support the application for examination as requested by the division; and,
 - (7) the application fee and examination fee as prescribed by Article 8.
- (b) Submittal - Applications for examination shall be postmarked by the final filing date as specified in this subsection. Applications postmarked after the final filing date shall be held over and processed for the next scheduled examination.

Date of Examination	Final Filing Date
April 10, 1999	February 1, 1999
October 2, 1999	August 1, 1999
April 1, 2000	February 1, 2000
October 7, 2000	August 1, 2000
April 7, 2001	February 1, 2001
October 6, 2001	August 1, 2001
April 6, 2002	February 1, 2002
October 5, 2002	August 1, 2002
April 5, 2003	February 1, 2003
October 4, 2003	August 1, 2003
April 3, 2004	February 1, 2004
October 2, 2004	August 1, 2004

- (c) Division review - The division shall review applications and supporting documents to determine eligibility for examination.

Unless otherwise specified by this chapter, division evaluation of experience gained in California will be based on work performed while employed in a position which requires operator certification in California. Evaluation of experience gained outside California will be based on work performed while employed in a position comparable to one which requires operator certification in California. Division evaluation of experience will be based on the

actual work performed by the applicant without respect to job titles assigned by the employing agencies.

- (d) Notice - The division shall notify applicants in writing within 30 calendar days of receipt of an application whether it is complete or deficient. If there is a deficiency, the division shall identify the deficiency and inform the applicant in writing of the specific information required.
- (e) Deficient applications - Applications which do not contain proof of completion of education requirements and the correct application and examination fees shall be considered deficient applications. Deficient applications shall not be processed for the current examination. The applicant shall be required to reapply to take a subsequent examination.
- (f) Processing times - the division's median, minimum, and maximum processing times for applications for examination between September 1989 and September 1991 were:
 - Median - 30 days
 - Minimum - 3 days
 - Maximum - 112 days

§ 3701. Examinations.

- (a) Written examinations for each wastewater treatment plant operator grade shall contain questions to determine applicants' knowledge of wastewater treatment plant operation. Mathematical problems related to process control and evaluation will be included. Each higher grade examination will require progressively more detailed knowledge of the subject matter.
- (b) Content by grade
 - (1) Grade I examinations shall contain questions regarding knowledge of basic safety practices and hazards related to the operation of wastewater treatment plants; wastewater constituents including simple and routine sampling and analysis procedures; procedures involved in operating and maintaining preliminary and primary treatment facilities including sludge digestion and disinfection; specifics regarding the operation of stabilization ponds; and state regulations regarding the classification of wastewater treatment plants and operator certification.
 - (2) Grade II examinations shall contain questions regarding knowledge of those components of the Grade I examination as prescribed in (1) above; commonly used processes for preliminary, primary, and secondary treatment including disinfection, sludge handling, and digestion; routine sampling and analysis procedures for evaluation of process and overall plant performance; and basic supervision responsibilities.
 - (3) Grade III examinations shall contain questions regarding knowledge of those components of the Grade I and II examinations as prescribed in (1) and (2) above; limitations, controls, and performance calculations for primary and secondary treatment and sludge-handling processes; basic principles of tertiary treatment processes; state regulations regarding water recycling; and public health issues.
 - (4) Grade IV examinations shall contain questions regarding knowledge of those components of the Grade I, II, and III examinations as prescribed in (1), (2), and (3) above; limitations, controls, and performance calculations for tertiary treatment processes; wastewater treatment requirements and practices for water reclamation and reuse; supervision and management responsibilities including energy management, safety program development and control, and operator training and budget development and control.
 - (5) Grade V examinations shall contain questions regarding knowledge of those components of the Grades I, II, III, and IV examinations as prescribed in (1), (2), (3), and (4) above.
- (c) Frequency - A minimum of two examinations shall be given each year.
- (d) Dishonest conduct - An applicant who engages in dishonest conduct during an examination shall have his or her examination materials confiscated, shall not have the examination graded, and shall be denied the opportunity to take the next scheduled examination. The application and examination fees paid by the applicant shall not be refunded. The applicant also may be subject to administrative sanctions pursuant to Article 7 and Section 13627 of the Water Code.

- (e) Confidentiality of examination questions - Examination questions are confidential. Any person who copies questions or removes all or part of any examination from the examination room or who conveys or exposes all or part of any examination for an unauthorized use may be denied certification pursuant to the provisions of Article 7. The applicant also may be subject to administrative sanctions pursuant to Article 7 and Section 13627 of the Water Code.
- (f) Notification of results - Within 90 calendar days after an examination, the division shall notify applicants in writing whether they have passed or failed the examination.
 - (1) If an applicant fails the examination, he or she may be eligible to take a subsequent examination upon request and upon submitting an application and examination fee prescribed by Article 8. The request for re-examination must be postmarked by the final filing date set forth in Section 3700.
 - (2) An applicant who passes the examination and who had completed the education and experience requirements before taking the examination shall be instructed in the notice of examination results to remit the applicable certification fee. Within 30 calendar days of receiving the certification fee, the division shall issue the operator certificate.
 - (3) An applicant who passes the examination before completing the experience requirements shall apply for certification upon completing the requirements in accordance with the provisions of Section 3702.
- (g) Expiration of examination results - Examination results are valid for four years from June 30 or December 31 following the examination (whichever date is sooner).

§ 3702. Application for Certification.

- (a) If an applicant is qualified for certification at the time of the examination, and has documented such qualification in the application for examination, no application for certification is required. However, if an applicant must gain experience after the final filing date for the examination before being eligible for certification, an application for certification is required in accordance with the provisions of this section.
- (b) An application for certification shall include but not be limited to:
 - (1) the applicant's full name, mailing address, work telephone number, and date of birth;
 - (2) all employment, education, and experience information not reported on the application for examination, including current employment and current operator status;
 - (3) the date when the applicant passed the examination;
 - (4) information regarding current employment and current operator status;
 - (5) the applicant's original signature;
 - (6) if employed at a wastewater treatment plant, the chief plant operator's original signature;
AND,
 - (7) the certification fee prescribed by Article 8.

§ 3702.1. Issuance of Certificates.

- (a) Operator certificates issued by the division shall contain but not be limited to the following:
 - (1) The operator's name and grade;
 - (2) The certificate number;
 - (3) The issue date of the certificate;
 - (4) The State Water Board seal;
 - (5) The name, "State Water Resources Control Board"; AND,
 - (6) The signature of a board member or board member designee.
- (b) Upon successful completion of the application and examination process and within 30 calendar days of payment of the certification fee prescribed by Article 8, the board shall issue an operator certificate or operator-in-training certificate.
- (c) The issue date of a certificate shall be the date of receipt of an application for examination and certification which meets the requirements of these regulations.
- (d) The division may refuse to issue a certificate if it has determined that the applicant has committed any act which is grounds for disciplinary action as specified in section 3710.

§ 3702.2. Application for Certificate Renewal.

- (a) Renewal dates - Except as specified in Subsection 3709 (d), operator certificates are renewable every two years. Certificates issued for applications with a postmark between May 1 and October 31 shall have a renewal date of June 30. Certificates issued for applications with a postmark between November 1 and April 30 shall have a renewal date of December 31.

- (b) Division notice - At least 60 calendar days prior to expiration of an operator certificate, the division shall provide written notification of the expiration date to the certificate holder at his or her address of record. Failure to receive a notice of renewal does not relieve the certificate holder from the responsibility of renewing a certificate on or before the expiration date.
- (c) Content - An application for renewal shall include but not be limited to:
 - (1) the applicant's name, mailing address, grade, certificate number, and classification or title;
 - (2) if employed by a wastewater treatment plant as an operator, the name, telephone number, and mailing address of the wastewater treatment plant where employed and the name of the supervisor;
 - (3) the renewal fee prescribed by Article 8.
- (d) Submittal - A certificate holder who wishes to renew a certificate shall submit to the division a completed application as specified in subsection (c) of this section. The application shall be postmarked no later than the expiration date on the certificate.
- (e) Division review - Within 15 calendar days of receipt of an application for renewal, the division shall notify the certificate holder if the application is deficient. If there is a deficiency, the division shall inform the certificate holder by telephone or letter of the specific information necessary to complete the application for renewal. Deficiencies will not prevent the Office of Operator Certification from issuing a new certificate if the application and fee are postmarked by the expiration date of the certificate.

§ 3702.3. Issuance of Renewal Certificate.

An operator certificate shall indicate the first expiration date of the certificate. Thereafter, a renewal certificate shall be issued in accordance with the provisions of Section 3702.2 and this section.

- (a) Within 30 calendar days of receipt of a completed application for renewal, the division shall issue a renewal certificate or inform the applicant of the reason the certificate will not be issued.
- (b) The renewal certificate shall not be issued until any unpaid fees have been paid.
- (c) The division may refuse to renew a certificate if it has determined that the applicant has operated a wastewater treatment plant while the operator certificate was expired or at a grade for which the applicant was not certified or that the applicant has committed any act which is grounds for disciplinary action.
- (d) A renewal certificate shall contain but not be limited to the following:
 - (1) The certificate holder's name and address;
 - (2) The certificate number and grade;
 - (3) The expiration date of the certificate.

§ 3702.4. Reinstate.

- (a) An expired operator certificate may be reinstated within one year following the expiration of the certificate, provided the holder of the expired certificate applies for renewal and reinstatement as prescribed by Subsection (b) of this section. A certificate which has been expired for more than one year shall not be reinstated. If the applicant wishes to become certified again, he or she must meet all requirements for an initial operator certificate.
- (b) The application for reinstatement shall be considered complete when it includes the renewal and reinstatement fees prescribed by Article 8 and all the information required to renew the certificate as prescribed by Section 3702.2.
- (c) The division may refuse to reinstate a certificate if it has determined that the applicant has operated a wastewater treatment plant while his or her certificate was expired or at a grade for which he or she was not certified or has committed any act which is grounds for disciplinary action.
- (d) The expiration date of a reinstated certificate shall remain the same as if the certificate had not expired.

§ 3702.5. Replacement.

A certificate which has been lost, stolen, or destroyed may be replaced by the division, provided the operator or operator-in-training submits a signed statement explaining the circumstances of the loss, theft or destruction of the certificate. A replacement fee prescribed by Article 8 must be submitted with the signed statement.

§ 3703. Posting Certificates.

Certified operators and operators-in-training shall display their valid certificates at the wastewater treatment plant where employed.

§ 3704. Reciprocity with Other States.

- (a) The division may issue Grades I and II operator certificates by reciprocity in accordance with the procedures set forth in Article 5. No examination or examination fee will be required of persons who hold comparable certifications in other states, provided:
- (1) the experience and education requirements of that state are comparable to the division's requirements;
 - (2) the applicant has passed a written examination within the preceding four years in another state that is comparable to the examination given by the division;
 - (3) reciprocal privileges are granted by the other state to operators certified by the division;
 - (4) the applicant completes an application for operator certification and meets the minimum qualifications for certification in California; AND,
 - (5) the applicant pays the application, certification, and reciprocity fees prescribed by Article 8.
- (b) The division may refuse to issue an operator's certificate by reciprocity if it has determined that the applicant's certificate to operate a wastewater treatment plant has been revoked or suspended in another state, or if the applicant has been otherwise disciplined in another state for any of the violations set forth in Section 3710.

§ 3707. Employment of an Operator-in-Training.

An agency may employ a person to act in the capacity of any grade of certified operator, provided the person is certified as an operator-in-training, is under the direct supervision of a certified operator of the same or higher grade, and is performing the duties of the grade of operator for which the certificate was issued.

§ 3708. Application for Operator-in-Training Examination and Certification.

- (a) Persons may apply for examination and operator-in-training certification in accordance with the procedures set forth in Article 5.
- (b) Applicants for Grade I operator-in-training certification may, but are not required to, pass the Grade I examination prior to issuance of the Grade I operator-in-training certificate.
- (c) Persons may apply for operator-in-training certification at the Grades II, III, IV, and V levels if they:
- (1) meet the minimum education requirements and could meet the minimum experience requirements for the grade for which they are applying as prescribed in Article 4 within four years of June 1 or December 1 following the examination (whichever date is sooner); and,
 - (2) pass the examination at the grade for which they are applying; and,
 - (3) make application for examination and operator-in-training certification in accordance with the procedures set forth in Sections 3700, 3701, and 3702 of Article 5; and,
 - (4) supply the name and telephone number of the supervising operator.
- (d) Applications for operator-in-training certification at any grade must be signed by the chief plant operator of the plant where the operator-in-training is to be employed.

Article 6. Operators-in-Training

§ 3709. Issuance, Renewal, and Replacement of Operator-in-Training Certificates.

- (a) Operator-in-training certificates shall be issued in the name of the applicant to the mailing address of the employing wastewater treatment plant. Operator-in-training certificates are valid only while the operator is employed at the plant for which the certificate was issued. The expiration date of the operator-in-training certificate shall not exceed the expiration date of the applicant's examination results.
- (b) Operator-in-training certificates issued by the division shall contain but not be limited to the following:
- (1) The name and grade of the operator-in-training;
 - (2) The issue date of the certificate; and,
 - (3) The name of the wastewater treatment plant at which the operator-in-training is to be employed.

- (c) Operator-in-training certificates shall be issued, renewed, reinstated, and replaced in accordance with the provisions of Article 5 unless otherwise specified in this article.
- (d) Operator-in-training certificates at the Grade I level are valid for up to two years. If the Grade I operator passes the Grade I examination before the expiration of the Grade I operator-in-training certificate, that certificate may be renewed one time for two years. If the Grade I operator-in-training does not pass the Grade I examination before the expiration of the Grade I operator-in-training certificate, the Grade I operator-in-training certificate shall not be renewed. Operator-in-training certificates at the Grades II, III, IV, and V levels are valid for up to two years and may be renewed once pursuant to the provisions of Section 3702.2.
- (e) A person certified as an operator-in-training at any grade must complete the education and experience requirements and obtain an operator certificate at that grade or higher before being eligible to apply for an operator-in-training certificate at a higher grade.

Article 7. Prohibited Acts, Disciplinary Action, and Appeal Process

§ 3710. Grounds for Discipline.

- (a) A certified operator or operator-in-training may be subject to administrative sanctions including reprimand or denial, suspension, probation, or revocation of a certificate pursuant to Section 13627 of the Water Code for performing, or allowing or causing another to perform, any of the following acts:
 - (1) willfully or negligently violating, causing, or allowing violation of these regulations;
 - (2) without regard to intent or negligence, operating or allowing the operation of a wastewater treatment plant by a person who is not certified at the grade necessary for the position or whose certificate has expired;
 - (3) submitting false or misleading information on any document provided to the division including applications for examination, certification, or renewal;
 - (4) engaging in dishonest conduct during an examination, or violating confidentiality of examination questions;
 - (5) using fraud or deception in the course of employment as an operator;
 - (6) failing to use care or good judgment in the course of employment as an operator or failing to apply knowledge or ability in the performance of duties;
 - (7) willfully or negligently causing or violating or allowing the violation of appropriate waste discharge requirements as prescribed by Article 4 of Chapter 4 of Division 7 of the Water Code, or the violation of Section 402 of the Clean Water Act which contains the provisions of the National Pollutant Discharge Elimination System permit.
- (b) A chief plant operator may be subject to disciplinary actions specified in subsection (a) for willfully or negligently failing to ensure that an operator-in-training is directly supervised as required by section 3707.

§ 3711. Appeals.

Applicants or certificate holders may appeal discretionary decisions made by the Office of Operator Certification regarding denial of an application, the results of an examination, or disciplinary action taken. Appeals must be in writing and postmarked within 30 calendar days of receipt of the Office of Operator Certification decision. Appellants must include with their requests, all documents and evidence to be considered by division staff in its review of the appeal.

§ 3712. Action by Division.

After consideration of an appeal and within 30 calendar days of receipt of the appeal, division staff shall make a recommendation to the division chief. The division chief shall review the evidence and the division recommendation and shall make a determination within 30 calendar days of receipt of the recommendation. The determination shall be in writing, labeled as the division chief's determination, and shall inform the appellant that the determination is final and conclusive unless the appellant petitions the board for review in accordance with the provisions of Section 3713.

§ 3713. Petition for Review by Board.

- (a) An appellant who wishes to appeal the division chief's determination may petition the board for a review. The petition must be in writing and postmarked no later than 30 calendar days after the date of receipt of the determination by the appellant.
- (b) A petition for review by the board shall contain:
 - (1) the name and address of the appellant;

- (2) the appellant's argument against the Office of Operator Certification decision and the division chief's determination;
 - (3) the specific action which the appellant seeks from the board.
- (c) The appellant may make a written request for a hearing for the purpose of presenting evidence not considered by the division or for presenting oral arguments or both. Any request to present evidence not provided to the division must include a statement as to why the evidence was not presented to the division.

§ 3714. Defective Petitions.

Within 30 calendar days of receipt by the board of a petition which does not comply with the provisions of Section 3713, the board shall notify the appellant in writing in what respect the petition is defective and that an amended petition must be postmarked within 30 calendar days of receipt of notice of the deficiency. If a properly amended petition is not postmarked within 30 calendar days, the petition shall be dismissed unless the appellant can show good cause for an extension of time.

§ 3715. Action by Board.

- (a) After consideration of the appellant's petition and the division chief's determination, the board shall:
 - (1) refuse to consider the petition if it does not meet the requirements of Sections 3713 and 3714; or,
 - (2) deny the appellant's petition upon a finding that the division chief's determination was proper; or,
 - (3) set aside or modify the division chief's determination; or,
 - (4) direct the division to take other appropriate action.
- (b) Before taking final action, the board may, in its discretion, hold a hearing for the purpose of oral argument or receipt of additional evidence or both, or the board may provide for an informal meeting between the appellant, division staff, and one or more members of the board and other persons as the board deems suitable for the purpose of attempting to resolve the dispute between the appellant and the division.
- (c) If a hearing is scheduled, the board shall mail a notice to the appellant indicating the date, time, and place of the hearing and of the issues to be considered. The hearing shall be conducted in a manner deemed most suitable for securing all relevant evidence without unnecessary delay.

§ 3716. Appeal of Division Processing Times.

- (a) The Office of Operator Certification shall process applications for examination and certification within the time limits prescribed by this chapter. Persons whose applications for examination or certification have not been processed within the time limits prescribed by these regulations, may appeal to the board for a refund of fees in accordance with the provisions of Section 3711. If the board finds that the time limits have not been met, and the Office of Operator Certification has not shown good cause why the time limits have not been met, the board shall direct the Office of Operator Certification to reimburse all fees paid by the appellant in connection with the pending application for examination or certification.
- (b) The Office of Operator Certification shall have good cause for exceeding the time limits when:
 - (1) the number of applications to be processed exceeds by 15 percent the number processed in the same calendar quarter of the preceding year.
 - (2) the Office of Operator Certification must rely on another public or private entity for all or part of the processing and delay is caused by the other entity.
 - (3) the delay is caused by a delay or omission of the applicant.

Article 8. Fees

§ 3717. Operator and Operator-In-Training Fees.

Except as provided by Section 3716, application fees are nonrefundable.

- (a) Application fee for certification as an operator-in-training:

Grade I: \$ 95
Grade II: \$130
Grade III: \$170
Grade IV: \$190
Grade V: \$190

- (b) Application fee for an examination:

Grade I: \$40
Grade II: \$50
Grade III: \$70
Grade IV: \$80
Grade V: \$80

(c) Examination fees are:

Grade I: \$ 40
Grade II: \$ 50
Grade III: \$125
Grade IV: \$170
Grade V: \$170

(d) Operator certification fees are:

Grade I: \$ 95
Grade II: \$130
Grade III: \$170
Grade IV: \$190
Grade V: \$190

(e) Operator and operator-in-training certification renewal fees are:

Grade I: \$ 95
Grade II: \$130
Grade III: \$170
Grade IV: \$190
Grade V: \$190

(f) Reinstatement fee - The reinstatement fee for all grades is \$50.

(g) Replacement fee - The fee for replacing a lost, damaged or destroyed certificate is \$20.

(h) Reciprocal fee - In addition to the application and certification fees, applicants for reciprocal certification shall pay a fee of \$50 to cover the cost of verifying and evaluating out-of-state experience and reviewing out-of-state examinations.

Article 9. Advisory Committee

§ 3718. Advisory Committee Membership and Responsibilities.

- (a) The advisory committee appointed pursuant to Section 13631 of the Water Code shall consist of nine members. The members of the committee in office on January 1, 1992, shall continue as members of the advisory committee, and their terms shall expire as follows:
- (1) On June 30, 1992, one representative from a statewide organization representing local sanitation agencies; one representative from a statewide organization representing wastewater treatment plant operators and supervisors; one representative from a university or state college; and, one representative from an organized labor union which represents wastewater treatment plant operators.
 - (2) On June 30, 1994, the remaining five members whose terms are scheduled to expire on June 30, 1993.
- (b) Thereafter, all members shall serve for a period of four years at which time they shall be eligible for reappointment.
- (c) The committee shall meet when necessary to review all proposed regulations and make recommendations to the board prior to adoption of any regulations or changes therein and approve any course for operator training.

Article 10. Wastewater Treatment Plant Contract Operators

§ 3719. Registration Requirement.

No person or entity shall enter a contract to operate a wastewater treatment plant unless that person or entity has been registered by the division as a contract operator. The registration authorizes the contract operator to operate one or more wastewater treatment plants. All wastewater treatment plant operators employed by the contract operator must be certified according to the provisions of this chapter.

§ 3719.10. Term of Registration.

Contract operator registrations shall be valid for a period of one year from the date of issue.

§ 3719.11. Application for Registration.

- (a) Application Content - An application for registration as a contract operator shall include but not be limited to:
 - (1) the name, street address, and telephone number of the person or entity contracting to operate the wastewater treatment plant(s);
 - (2) the name, address, and telephone number, if known, of the wastewater treatment plant(s) to be operated and the duration of each contract;
 - (3) the name and grade of each wastewater treatment plant operator employed at the plant(s);
 - (4) the name and grade of the chief plant operator for each wastewater treatment plant to be operated;
 - (5) the original signature of the person authorized by the contract operator to enter the contract;
 - (6) the registration fee as prescribed by section 3719.19.
- (b) Application submittal - For persons operating wastewater treatment plants on or before the effective date of these regulations, applications for registration shall be postmarked within 60 calendar days after the effective date of the regulations. If a contract to operate a wastewater treatment plant is entered into after the effective date of these regulations and the contract operator is not already registered, the application for registration shall be submitted and the registration issued before contract operations begin.
- (c) Division review of application and notice to applicant - The division shall review applications for registration and shall notify applicants in writing within 30 calendar days of receipt whether the application is deficient. If there is a deficiency, the division shall inform the applicant by telephone or letter of the specific information required to complete the application.

§ 3719.12. Issuance/content of Certificate of Registration.

- (a) Content of certificate of registration - The certificate of registration issued by the division shall be in the form of a wall certificate and shall contain but not be limited to:
 - (1) the applicant's name, business address, and registration number;
 - (2) the issue and expiration date of the registration;
 - (3) the State Water Board seal; AND,
 - (4) the signature of a State Water Board member or member designee.
- (b) Issuance of certificate of registration - Unless otherwise specified in subsection (c), within 30 calendar days of receipt of a complete and approved application for registration, the division shall issue a contract operator certificate of registration. The division shall also issue one wall certificate to the contract operator for each wastewater treatment plant operated. The certificate shall include the name of the wastewater treatment plant to be operated in addition to the items in subsection (a) (1) through (4) above. Certificates are not transferable.
- (c) Refusal to issue a certificate of registration - The division may refuse to issue a certificate of registration if it has determined that the applicant has committed any act which is grounds for disciplinary action as specified in section 3710 of Article 7 or section 3719.17 of this article.

§ 3719.13. Renewal of Registration.

- (a) Division notice of renewal date - At least 60 calendar days prior to the expiration of a contract operator registration, the division shall provide written notification of the expiration date to the registration holder at his or her address of record. Failure to receive a notice of renewal does not relieve the registration holder from the responsibility of renewing a registration on or before the expiration date.
- (b) Content of renewal application - An application for renewal of a contract operator registration shall include but not be limited to:
 - (1) the name, business address, telephone number, and registration number of the person or entity contracting to operate the wastewater treatment plant(s);
 - (2) the name, address, and telephone number of all wastewater treatment plants operated and the duration of each contract;
 - (3) the name and grade of each wastewater treatment plant operator employed at the plant(s);
 - (4) the name and grade of the chief plant operator for each wastewater treatment plant to be operated;
 - (5) the original signature of the person authorized by the contract operator to enter the contract; AND,

- (6) the renewal fee as prescribed by section 3719.19.
- (c) Renewal application submittal - A registration holder who wishes to renew a registration shall submit to the division a completed application as specified in subsection (b). The application for renewal shall be postmarked no later than 30 calendar days before the expiration of the registration. If the application for renewal is postmarked later than 30 calendar days before expiration, the registration holder shall pay a late fee in an amount prescribed by section 3719.19.
- (d) Division review of renewal application and notice to applicant - The division shall review the renewal application and shall notify the registration holder within 30 calendar days whether the application is deficient. If there is a deficiency, the division shall inform the registration holder by telephone or letter of the specific information necessary to complete the application for renewal.

§ 3719.14. Issuance/Content of Renewed Certification of Registration.

- (a) Content of renewed certificate of registration - A renewed contract operator registration shall be in the form of a wall certificate and shall contain but not be limited to:
- (1) the registration holder's name, business address, and registration number;
 - (2) the original issue date and next expiration date of the registration;
 - (3) the State Water Board seal; AND,
 - (4) the signature of a State Water Board member or member designee.
- (b) Issuance of renewed certificate of registration - Within 30 calendar days of the receipt of a complete and approved renewal application, the division shall issue a certificate of registration or inform the applicant of the reason the certificate will not be issued. The division shall also issue one wall certificate to the contract operator for each wastewater treatment plant operated. The certificate shall include the name of the wastewater treatment plant operated in addition to the items in subsection (a) (1) through (4) above.
- (c) Refusal to renew registration - The registration shall not be renewed until any unpaid fees or fines have been paid. The division may refuse to renew a registration if it has determined that the applicant has operated a wastewater treatment plant while the registration was expired or has committed any act which is grounds for disciplinary action pursuant to section 3710 of Article 7 or section 3719.17 of this article.

§ 3719.15. Replacement of Certificate of Registration.

A certificate of registration which has been lost, stolen, or destroyed may be replaced by the division. The replacement fee as prescribed by section 3719.19 must be submitted with a request for replacement.

§ 3719.16. Posting the Certificate of Registration.

A valid, unexpired certificate of registration shall be displayed and clearly visible at each wastewater treatment plant where the registration holder has a contract to provide services.

§ 3719.17. Prohibited Acts and Disciplinary Action.

Grounds for discipline - The State Water Board may refuse to grant, or may suspend or revoke, any registration for good cause, including but not limited to any of the following reasons:

- (a) willfully or negligently violating, causing, or allowing the violation of Articles 1 through 10 of Chapter 26;
- (b) without regard to intent or negligence, operating or allowing the operation of a wastewater treatment plant by a person who is not certified at the grade necessary for the position or whose certificate has expired;
- (c) operating a wastewater treatment plant without a valid and current registration;
- (d) submitting false or misleading information on any document provided to the division including applications for registration or registration renewal;
- (e) using fraud or deception in the course of contracting to operate a wastewater treatment plant including, but not limited to, submitting false or misleading documents to the owner(s) of the wastewater treatment plant under contract;
- (f) failing to use care or good judgment while operating a wastewater treatment plant;
- (g) willfully or negligently causing or violating or allowing the violation of appropriate waste discharge requirements as prescribed by Article 4 of Chapter 4 of Division 7 of the Water Code, or the violation of Section 402 of the Clean Water Act which contains the provisions of the National Pollutant Discharge Elimination System permit.

§ 3719.18. Appeals.

Applicants or registration holders may appeal discretionary decisions made by the division regarding denial of an application for registration, registration renewal, or disciplinary action taken.

Appeals shall be processed in accordance with the provisions of sections 3712 through 3716 of Article 7.

§ 3719.19. Wastewater Treatment Plant Contract Operator Registration Fees.

Contract operator fees are as follows:

- (a) Initial Registration Fee - The initial contract operator registration fee is \$100. For each operator employed by the contract operator in California, a fee of \$25 shall also be paid by the contract operator up to a maximum of \$500 in combined contract operator registration fees and employee registration fees.
- (b) Renewal Fee - The annual renewal fee is \$100 plus \$25 for each person employed by the contract operator in California up to a maximum of \$500 in combined contract operator fees and employee registration fees.
- (c) Late fee - Each contract operator who fails to have a renewal application postmarked at least 30 days before expiration shall pay a late fee of \$50 in addition to the renewal fee.
- (d) Replacement Fee - The fee for replacing lost, damaged, or destroyed certificates is \$30.

APPENDIX H

ADDITIONAL ALTERNATIVE TREATMENT SYSTEMS

Two alternative treatment systems are discussed in this appendix. Although these two systems have not been as widely installed as other treatment trains mentioned earlier in this report, they show many potential benefits for cost-effective small-scale water reclamation.

H.1. PONWRS

The point-of-need water recycling system (PONWRS) was developed by Great Circle Water. The general concept of the PONWRS is to remove pathogens without removing nutrients. This system mines the sewer for nutrients, leaving the solids. The PONWRS is a nonbiological treatment system and is relatively easy to start up and maintain. As there are no open reactors in the PONWRS, potential odor is reduced. The design does not include a way to handle solids.

The flow diagram of a PONWRS is shown in Figure H.1. The PONWRS consists of the following subprocesses: vortex separation, filtration, gas flotation, and UV disinfection. Raw wastewater is removed from a sewer trunk line, pumped via a chopper pump into the vortex separation unit, and then sent through the remaining PONWRS process. The PONWRS is currently installed only as a pilot unit at the Dublin San Ramon Services District in Pleasanton, CA.

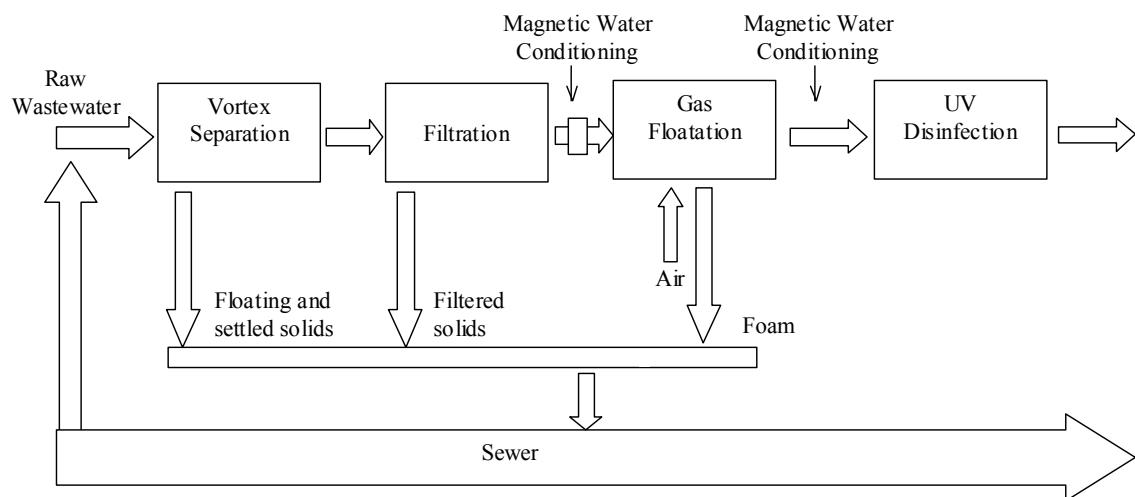


Figure H.1. Flow chart of the Great Circle Water PONWRS.

H.2. IMANS®

The Integrated Membrane System (IMANS®), like the PONWRS, utilizes nonbiological processes to remove pathogens. The nonbiological process allows for rapidly starting and stopping the processing of water on demand. Unlike the PONWRS, the IMANS® can be designed to handle solids. The flow diagram of an IMANS® is shown in Figure H.2.

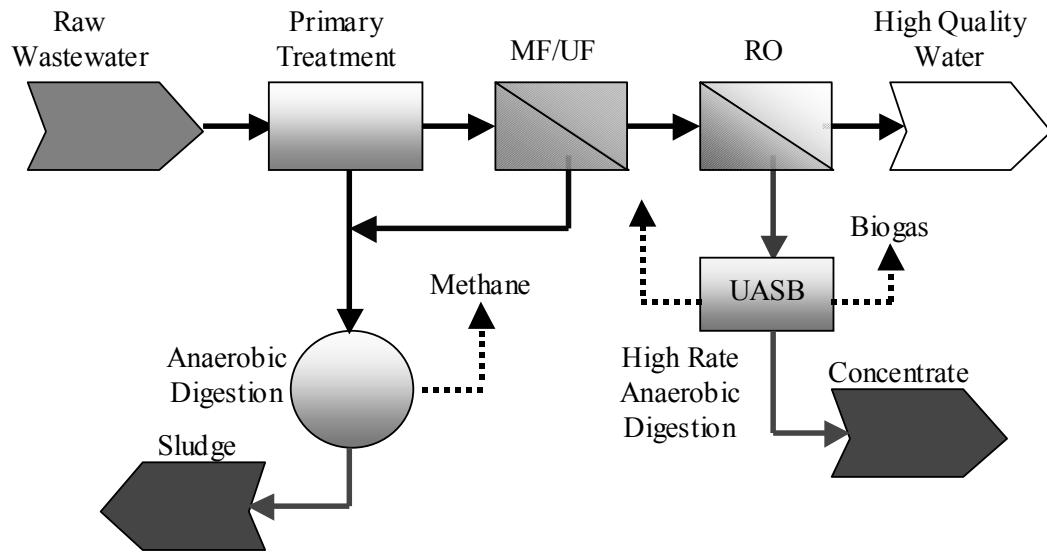


Figure H.2. Flow chart of IMANS®.

The IMANS[®] approach involves conventional primary settling of the wastewater, followed by microfiltration (MF) or ultrafiltration (UF). Solid material removed by the MF membranes may be returned to the anaerobic digesters with the solids from primary clarification. The MF product stream containing soluble organic material is treated in a reverse osmosis (RO) or nanofiltration (NF) process. The RO permeate is a high-quality water ready for final disinfection and use, while the RO brine contains rejected salts and concentrated soluble organic material yet is free of suspended material. This organic-rich concentrate is then stabilized in an anaerobic digestion process. The system eliminates the need for conventional secondary activated sludge treatment.

The advantages of IMANS[®] are the low construction costs and small carbon footprint due to the absence of secondary activated sludge treatment and the energy saving from biogas produced through anaerobic digestion. The system also can be tailored to meet discharge needs, and there is less odor as no open reactors are used. A 0.2-mgd IMANS[®] has been built and tested at the Orange County Sanitation District in California.

APPENDIX I

UTILITY SURVEY

I. Utility and Contact Information

Utility name _____
Utility location _____
Utility website _____
Your name _____
Your title _____
Your mailing address _____
Your phone and fax _____
Your e-mail _____
Other contact _____

II. Utility Process Description – Flow

	Influent	Effluent
BOD		
TSS		
Are there water quality components that require special treatment?		
<i>Example: Arsenic</i>		
<hr/>		
Design flow		
Daily average flow		
Dry flow		
Wet flow		

Please provide a description of your current treatment system in the format and space provided:

primary – secondary – tertiary – disinfection – reuse

III. Utility Construction and Upgrades: Please provide the dollar amount, year of each cost, and source of funding.

Please circle the corresponding process and provide a description of the components in the space provided below:

Construction Cost & Year	\$	year:	source:
		primary – secondary – tertiary – disinfection – reuse	
Upgrade Cost & Year	\$	year:	source:
		upgrade components:	
Upgrade Cost & Year	\$	year:	source:
		upgrade components:	
Expected Future Upgrade Cost & Year	\$	year:	source:
		upgrade components:	

IV. Operations and Maintenance

Current Annual Operations & Maintenance	\$	
Electricity Costs	\$	
Chemical (Disinfection) Costs	\$	
Testing Costs	\$	
Estimated Time and/or Costs Dealing with Regulatory Actions (permitting, fines, etc.)	\$	time:

Staff Costs	# staff	h/wk	training level	grade level	pay (\$/mo.)	mandatory certification requirement
Operations director						
Lead person						
Utility person II						
Utility person I						
Utility maintenance						
Seasonal laborer						
Other information						

V. Utility Process Description – Equipment: MAKE COPIES AS NEEDED

Process:

Equipment:

Automated: Y N

of units:

Capacity:

Land requirement (acres, square feet, etc.):

Maintenance requirement (h/wk): 0–5 5–10 10–15 15+

Operator level required to operate/maintain: I II III IV V

Notes:

Process:

Equipment:

Automated: Y N

of units:

Capacity:

Land requirement (acres, square feet, etc.):

Maintenance requirement (h/wk): 0–5 5–10 10–15 15+

Operator level required to operate/maintain: I II III IV V

Notes:

VI. Influent Water Quality

Nitrogen

Phosphorus

Fecal coliform (average)

Fecal coliform (maximum)

E. coli

Giardia

Cryptosporidium

Enterovirus

Settleable solids

Total suspended solids (TSS)

Total dissolved solids (TDS)

Biological oxygen demand (BOD_5)

Chemical oxygen demand (COD)

Total organic carbon (TOC)

pH

Minimum winter water temperature

Other

VII. Treatment Requirement

	Required? (Yes or No)	Regulated Level
Secondary treatment (BOD removal)		
Ammonia removal (nitrification)		
Nitrogen removal (denitrification)		
Phosphorus removal		
Filtration (turbidity/TSS reduction)		
Disinfection		
Fecal coliform (average)		
Fecal coliform (maximum)		
<i>E. coli</i>		
Chlorine residual		
Contact time		
CT value		
Total suspended solids (TSS)		
Turbidity (NTU)		
Chemical oxygen demand (COD)		
Total organic carbon (TOC)		
Total organic halogen (TOX)		
Dissolved oxygen (DO)		
Hydrogen sulfide (H ₂ S)		
pH		
Disinfection by-products (THMs, HAAs, nitrosoamines)		
Metals		
Toxicity		
Other		

VIII. Anecdotal Information and Potential Process Options: Please circle Yes or No, estimate how much time is spent (if appropriate), and provide a brief explanation in the space provided.

Please provide any information regarding the decision to install or not install a reuse system.

Are there issues associated with the treatment process such as permitting, community acceptance, and negative responses from environmental groups?

Treatment:

Y/N

time:

Reuse:

Y/N

time:

Are there issues with odors, aesthetics, vectors, or attractive nuisances?

Treatment:

Y/N

time:

Reuse:

Y/N

time:

Does the treatment facility produce ancillary (additional) benefits?

Treatment:

Y/N

Reuse:

Y/N

If you could redesign the system, would you and why?

Treatment:

Y/N

Reuse:

Y/N

Does the treatment address any nonregulated treatment objectives?

Y/N

Other requirements and questions?

Thank you for your participation!

APPENDIX J DATA

Table J.1. Facility Details and Costs

Process #	Ammonia Removal (Nitrification)	Nitrogen Removal (Denitrification)	Phosphorus Removal	Filtration	Disinfection	Flow (mgd)	Worth Cost (\$M)	Present Cost (\$M/mgd)	Adjusted Construction Cost (\$M)	Unit Construction Cost (\$M/mgd)	Annual O&M Cost (\$M)	Adjusted Annual O&M Cost (\$/1000 gal)	
1 Yes	Yes	Yes	Yes	Yes	Yes	1,500	\$49.34	\$32.90	\$13.99	\$9.33	\$1.70	\$3.11	
2 Yes	Yes	Yes	Yes	Yes	Yes	0,149	\$2.79	\$18.71	\$1.86	\$12.49	\$0.04	\$0.82	
3						1,500			\$4.71	\$3.14			
4 Yes	Yes	Yes	Yes	Yes	Yes	3,160	\$61.88	\$19.58	\$29.43	\$9.31	\$1.56	\$1.35	
5						3,690	\$169.50	\$45.94	\$41.06	\$11.13	\$1.18	\$4.59	
6 Yes	Yes	Yes	Yes	Yes	Yes	0,900	\$36.12	\$40.14	\$4.87	\$5.41	\$1.50	\$4.58	
7 Yes	Yes	Yes	Yes	Yes	Yes	2,500			\$7.61	\$3.04			
8						0,220			\$0.84	\$3.84			
9 Yes	Yes	Yes	Yes	Yes	Yes	2,345	\$27.71	\$11.82	\$20.10	\$8.57	\$0.37	\$0.43	
10 Yes	Yes	Yes	Yes	Yes	Yes	2,307	\$34.12	\$14.79	\$23.28	\$10.09	\$0.52	\$0.62	
11						4,000			\$2.29	\$0.57			
12						0,350	\$22.70	\$64.87	\$8.65	\$24.72	\$0.68	\$5.30	
13						0,733	\$17.93	\$24.46	\$4.30	\$5.87	\$0.66	\$2.45	
14 Yes	Yes	Yes	Yes	Yes	Yes	1,804	\$19.11	\$10.59	\$6.40	\$3.55	\$0.61	\$0.93	
15 Yes	Yes	Yes	Yes	Yes	Yes	1,500			\$5.03	\$3.35			
16						Y	1,000	\$27.14	\$4.08	\$4.08	\$1.11	\$3.04	
17						Yes	0,250	\$8.04	\$32.16	\$3.93	\$15.74	\$0.20	\$2.17
18						Yes	0,700	\$8.15	\$11.64	\$1.65	\$2.36	\$0.31	\$1.22
19						Yes	0,700	\$6.89	\$9.85	\$0.75	\$1.08	\$0.30	\$1.16
20							2,000	\$28.03	\$14.02	\$6.08	\$3.04	\$1.06	\$1.45
21							0,300	\$5.05	\$16.82	\$1.80	\$6.00	\$0.16	\$1.43
22						Yes	0,600	\$14.56	\$24.27	\$1.81	\$3.01	\$0.61	\$2.80
23							0,150	\$5.71	\$38.09	\$1.94	\$12.96	\$0.18	\$3.31

Table J.1. Facility Details and Costs

Process	#	Ammonia Removal (Nitrification)	Phosphorus Removal (Denitrification)	Filtration	Disinfection	Flow (mgd)	Present Worth Cost (\$M)	Unit Present Cost (\$M/mgd)	Adjusted Construction Cost (\$M)	Construction Cost (\$M/mgd)	Unit Annual O&M Cost (\$M)	Adjusted Annual O&M Cost (\$M)	Unit Annual O&M Cost (\$/1000 gal)
	24					1,000	\$6.76	\$6.76	\$4.01	\$4.01	\$0.13	\$0.36	
	25					0.160					\$0.37	\$6.34	
	26	Yes				0.065	\$4.46	\$68.56	\$1.37	\$21.06	\$0.15	\$6.27	
	27	Yes			Yes	0.840	\$49.30	\$58.69	\$10.20	\$12.14	\$1.88	\$6.14	
	28	Yes			Yes	0.150	\$3.30	\$22.02	\$0.78	\$5.20	\$0.12	\$2.22	
	29	Yes			Yes	0.100	\$11.59	\$115.89	\$5.59	\$55.86	\$0.29	\$7.92	
	30	Yes			Yes	0.240	\$11.94	\$49.74	\$10.44	\$43.50	\$0.07	\$0.82	
	31	Yes			Yes	0.200	\$7.45	\$37.23	\$1.76	\$8.79	\$0.27	\$3.75	
	32	Yes			Yes	0.060	\$20.43	\$340.49	\$5.67	\$94.57	\$0.71	\$32.44	
	33	Yes			Yes	0.230	\$4.78	\$20.80	\$1.59	\$6.90	\$0.15	\$1.83	
A.2) Extended Aeration	34	Yes		Yes	Yes	1,000	\$22.71	\$22.71	\$3.50	\$3.50	\$0.93	\$2.53	
	35	Yes				0.400	\$12.27	\$30.67	\$1.57	\$33.92	\$0.52	\$3.53	
	36	Yes				0.200	\$5.42	\$27.11	\$1.00	\$4.98	\$0.21	\$2.92	
	37	Yes			Yes	0.125	\$15.49	\$123.95	\$7.78	\$62.25	\$0.37	\$8.14	
	38				Yes	0.100					\$0.16	\$4.38	
	39				Yes	0.490					\$0.57	\$3.19	
	40				Yes	0.400					\$0.32	\$2.22	
	41					1,000					\$1.51	\$4.15	
	42					0.220					\$0.50	\$6.22	
	43	Yes			Yes	0.294	\$54.67	\$185.86	\$17.49	\$59.44	\$1.79	\$16.68	
A.3) Intermittent Aeration	44	Yes	Yes			2,000			\$12.32	\$6.16			
	45	Yes	Yes		Yes	0.839	\$21.76	\$25.95	\$10.05	\$11.99	\$0.56	\$1.84	
A.4) A/O	46	Yes	Yes	Yes	Yes	1,500	\$65.63	\$43.76	\$26.14	\$17.43	\$1.90	\$3.47	
	47	Yes	Yes	Yes	Yes	2,000	\$92.46	\$46.23	\$34.64	\$17.32	\$2.78	\$3.81	
A.5) A2/O	48	Yes	Yes		Yes	3,500			\$8.72	\$2.49			
	49	Yes	Yes		Yes	2,500			\$9.66	\$3.87			
A.6) Bardenpho	50	Yes	Yes			1,500					\$1.17	\$2.13	
	51	Yes	Yes	Yes	Yes	3,000			\$16.23	\$5.41			

Table J.1. Facility Details and Costs

Process	#	Ammonia Removal (Nitrification)	Phosphorus Removal (Denitrification)	Filtration	Disinfection	Flow (mgd)	Present Worth Cost (\$M)	Unit Present Cost (\$M/mgd)	Adjusted Construction Cost (\$M)	Unit Construction Cost (\$M/mgd)	Adjusted Annual O&M Cost (\$M)	Unit Annual O&M Cost (\$/1000 gal)
	52	Yes	Yes			3,000	\$18.06	\$6.02				
	53	Yes	Yes	Yes	Yes	4,000	\$15.11	\$11.32	\$2.83	\$2.36	\$1.62	
	54	Yes	Yes	Yes		5,000			\$42.11	\$8.42		
	55	Yes	Yes	Yes		5,000			\$29.88	\$5.98		
	56	Yes	Yes	Yes		2,250	\$51.32	\$22.81	\$18.73	\$8.33	\$1.57	\$1.91
	57	Yes	Yes	Yes		1,700	\$24.22	\$14.25	\$12.25	\$7.21	\$0.58	\$0.93
	58	Yes	Yes		Yes	4,000	\$42.99	\$10.75	\$23.54	\$5.89	\$0.94	\$0.64
	59	Yes	Yes			5,000			\$42.11	\$8.42		
	60	Yes	Yes	Yes	Yes	0,800					\$10.67	\$13.34
	61	Yes	Yes	Yes	Yes	1,000					\$20.54	\$20.54
A.7) BNR	62	Yes	Yes	Yes	Yes	1,000					\$4.30	
	63	Yes	Yes	Yes	Yes	1,000					\$13.48	
	64	Yes	Yes	Yes	Yes	1,500					\$12.05	\$8.04
	65	Yes			Yes	2,660	\$48.07	\$18.07	\$14.76	\$5.55	\$1.60	\$1.65
	66	Yes				1,600	\$40.14	\$25.09	\$6.08	\$3.80	\$1.64	\$2.81
	67	Yes			Yes	1,000					\$9.21	\$9.21
	68	Yes				2,500					\$13.75	\$5.50
	69	Yes				3,000					\$20.02	\$6.67
A.8) MLE	70	Yes				0,500					\$4.15	\$8.30
	71	Yes				2,300					\$25.42	\$11.05
A.9) Schreiber N&D	72	Yes	Yes	Yes		Yes	0.500	\$32.31	\$64.61	\$7.56	\$15.12	\$1.19
A.10) In-Channel Denitrification	73	Yes	Yes			Yes	1,200	\$34.95	\$29.12	\$5.87	\$4.89	\$1.40
	74	Yes	Yes			Yes	0.500	\$31.02	\$62.04	\$3.72	\$7.43	\$1.31
	75	Yes	Yes			Yes	1,200				\$7.99	\$6.66
A.11) ICEAS	76	Yes					2,800				\$18.89	\$6.75
	77	Yes				Yes	0.350	\$21.73	\$62.07	\$0.99	\$2.84	\$1.00
	78	Yes	Yes			Yes	1,500	\$26.01	\$17.34	\$1.17	\$0.78	\$1.20
												\$2.18

Table J.1. Facility Details and Costs

Process	#	Ammonia Removal (Nitrification)	Phosphorus Removal (Denitrification)	Filtration	Disinfection	Flow (mgd)	Present Worth Cost (\$M)	Present Cost (\$M)	Adjusted Construction Cost (\$M)	Construction Cost (\$M/mgfd)	Unit O&M Cost (\$/1000 gal)	Annual O&M Cost (\$M)	Unit Annual O&M Cost (\$/1000 gal)
	79	Yes	Yes		Yes	1,500	\$26.99	\$17.99	\$9.37	\$6.24	\$0.85	\$1.55	
	80	Yes	Yes			0,213	\$13.91	\$65.33	\$4.47	\$20.97	\$0.45	\$5.85	
A.12) Trickling Filter	81	Yes		Yes		1,000					\$0.53	\$1.46	
	82	Yes		Yes		0,200	\$17.96	\$89.82	\$9.58	\$47.92	\$0.40	\$5.53	
A.13) RBC	83	Yes			Yes	0,300					\$0.28	\$2.55	
	84	Yes			Yes	0,100	\$4.63	\$46.26	\$0.59	\$5.89	\$0.19	\$5.32	
	85	Yes	Yes		Yes	0,230	\$24.25	\$105.44	\$6.76	\$29.38	\$0.84	\$10.03	
B.1) Package Plant	86	Yes				0,025	\$3.65	\$145.99	\$2.78	\$111.15	\$0.04	\$4.60	
	87	Yes				0,150	\$4.13	\$27.53	\$3.42	\$22.79	\$0.03	\$0.63	
	88	Yes				0,090	\$5.25	\$58.38	\$4.13	\$45.89	\$0.05	\$1.65	
	89					0,016					\$0.09	\$14.98	
	90	Yes	Yes	Yes	Yes	0,750	\$19.28	\$25.71	\$8.24	\$10.98	\$0.53	\$1.94	
	91	Yes	Yes			0,050	\$15.43	\$308.63	\$9.84	\$196.84	\$0.27	\$14.75	
	92	Yes	Yes			0,500	\$9.21	\$18.42	\$3.44	\$6.88	\$0.28	\$1.52	
	93	Yes	Yes			0,500			\$6.19	\$12.38			
	94	Yes	Yes	Yes		0,350	\$9.73	\$27.80	\$5.19	\$14.83	\$0.22	\$1.71	
	95	Yes	Yes			0,250			\$8.31	\$33.24			
	96	Yes	Yes		Yes	0,400	\$11.36	\$28.39	\$6.80	\$16.99	\$0.22	\$1.50	
	97	Yes	Yes			0,260			\$2.91	\$11.19			
	98	Yes	Yes			0,498	\$14.04	\$28.19	\$7.36	\$14.77	\$0.32	\$1.77	
	99	Yes	Yes			1,000	\$16.78	\$16.78	\$13.97	\$13.97	\$0.14	\$0.37	
B.2) SBR	100	Yes	Yes			0,250	\$13.73	\$54.92	\$10.80	\$43.21	\$0.14	\$1.54	
	101	Yes	Yes		Yes	0,594	\$13.29	\$22.37	\$3.42	\$5.75	\$0.48	\$2.19	
	102	Yes	Yes			1,500			\$5.38	\$3.59			
	103	Yes	Yes	Yes		2,000			\$18.11	\$9.05			
	104	Yes	Yes			2,400			\$11.87	\$4.95			
	105	Yes	Yes			3,000			\$15.27	\$5.09			
	106	Yes	Yes			1,000			\$24.13	\$24.13			
	107	Yes	Yes			3,600	\$19.37	\$5.38	\$8.45	\$2.35	\$0.53	\$0.40	

Table J.1. Facility Details and Costs

Process	#	Ammonia Removal (Nitrification)	Nitrogen Removal (Denitrification)	Phosphorus Removal	Filtration	Disinfection	Flow (mgd)	Present Worth Cost (\$M)	Unit Present Cost (\$M/mgd)	Adjusted Construction Cost (\$M)	Construction Cost (\$M/mgd)	Unit Annual O&M Cost (\$M)	Annual O&M Cost (\$/1000 gal)
	108	Yes	Yes				1,000			\$3.43	\$3.43		
	109	Yes	Yes				0.500	\$12.38	\$24.75	\$7.10	\$14.20	\$0.25	\$1.39
	110	Yes	Yes	Yes	Yes	Yes	2,250			\$11.27	\$5.01		
	111	Yes	Yes	Yes	Yes	Yes	1,250	\$22.47	\$17.98	\$9.82	\$7.85	\$0.61	\$1.34
	112	Yes	Yes			Yes	1,860	\$112.96	\$60.73	\$40.32	\$21.68	\$3.50	\$5.15
	113	Yes	Yes			Yes	1,400	\$21.30	\$15.21	\$18.18	\$12.98	\$0.15	\$0.29
	114	Yes	Yes			Yes	0.350	\$8.58	\$24.50	\$4.16	\$11.89	\$0.21	\$1.66
	115	Yes	Yes			Yes	2,600			\$22.65	\$8.71		
	116	Yes	Yes			Yes	0.250	\$10.85	\$43.41	\$6.64	\$26.57	\$0.20	\$2.22
	117	Yes	Yes			Yes	0.400	\$10.32	\$25.81	\$2.34	\$5.86	\$0.38	\$2.63
	118	Yes	Yes			Yes	1,000	\$11.58	\$11.58	\$4.18	\$4.18	\$0.36	\$0.98
	119	Yes	Yes			Yes	0.260	\$12.40	\$47.69	\$2.98	\$11.48	\$0.45	\$4.78
	120	Yes	Yes			Yes	0.250	\$7.39	\$29.57	\$1.60	\$6.39	\$0.28	\$3.06
	121	Yes	Yes			Yes	1,000	\$155.57	\$155.57	\$28.40	\$28.40	\$6.12	\$16.77
	122	Yes	Yes			Yes	0.498	\$30.53	\$61.30	\$10.54	\$21.16	\$0.96	\$5.29
	123					Yes	0.101	\$6.87	\$67.97	\$2.65	\$26.24	\$0.20	\$5.50
	124						1,000					\$1.37	\$3.75
	125	Yes				Yes	0.900	\$10.54	\$11.71	\$4.15	\$4.61	\$0.31	\$0.94
	126	Yes	Yes	Yes		Yes	4,000	\$39.76	\$9.94	\$23.77	\$5.94	\$0.77	\$0.53
	127	Yes				Yes	0.175	\$6.45	\$36.83	\$1.46	\$8.32	\$0.24	\$3.76
	128	Yes					1,200			\$6.61	\$5.51		
	129	Yes					1,000	\$12.05	\$12.05	\$7.13	\$7.13	\$0.24	\$0.65
B.3) OD	130	Yes				Yes	1,800			\$25.71	\$14.29		
	131	Yes				Yes	0.773	\$43.31	\$56.03	\$10.49	\$13.57	\$1.58	\$5.60
	132	Yes					1,900	\$24.63	\$12.96	\$9.22	\$4.85	\$0.74	\$1.07
	133	Yes	Yes	Yes		Yes	0.990			\$7.90	\$7.98		
	134	Yes				Yes	1,980	\$38.62	\$19.51	\$30.09	\$15.20	\$0.41	\$0.57
	135	Yes				Yes	0.500	\$11.82	\$23.65	\$5.35	\$10.69	\$0.31	\$1.71
	136	Yes				Yes	0.275	\$9.47	\$34.44	\$1.63	\$5.92	\$0.38	\$3.76

Table J.1. Facility Details and Costs

Process	#	Ammonia Removal (Nitrification)	Phosphorus Removal (Denitrification)	Filtration	Disinfection	Flow (mgd)	Present Worth Cost (\$M)	Present Cost (\$M/mgd)	Adjusted Construction Cost (\$M)	Construction Cost (\$M)	Unit O&M Cost (\$/1000 gal)	Annual O&M Cost (\$M)	Unit Annual O&M Cost (\$/1000 gal)
	137	Yes				0.400	\$20.97	\$52.42	\$5.84	\$14.60	\$0.73	\$4.99	
	138	Yes				1.142	\$15.05	\$13.18	\$2.47	\$2.16	\$0.61	\$1.45	
	139	Yes				0.200	\$11.47	\$57.33	\$2.88	\$14.41	\$0.41	\$5.66	
	140	Yes			Yes	2.500			\$8.30	\$3.32			
	141	Yes			Yes	1.500	\$46.62	\$31.08	\$6.34	\$4.23	\$1.94	\$3.54	
	142	Yes				0.800	\$49.90	\$62.38	\$25.03	\$31.29	\$1.20	\$4.10	
	143	Yes	Yes	Yes		1.740	\$39.09	\$22.47	\$12.55	\$7.21	\$1.28	\$2.01	
B.4) Biological Filtration	144	Yes		Yes	Yes	0.017			\$0.85	\$49.94			
	145	Yes		Yes	Yes	0.120			\$1.02	\$8.50			
	146	Yes		Yes	Yes	0.090			\$2.45	\$27.23			
	147	Yes		Yes	Yes	0.300	\$6.43	\$21.43	\$2.48	\$8.28	\$0.19	\$1.74	
	148	Yes		Yes	Yes	0.400			\$6.28	\$15.70			
	149	Yes		Yes	Yes	0.040			\$2.42	\$60.52			
	150	Yes		Yes	Yes	0.150			\$1.66	\$11.04			
	151	Yes		Yes	Yes	0.300			\$7.61	\$25.38			
	152	Yes		Yes	Yes	0.370			\$12.18	\$32.92			
	153	Yes		Yes	Yes	0.370			\$13.43	\$36.29			
	154	Yes		Yes	Yes	0.400			\$4.77	\$11.93			
	155	Yes		Yes	Yes	0.500			\$6.68	\$13.35			
	156	Yes		Yes	Yes	0.500			\$15.16	\$30.31			
C.1) MBR	157	Yes		Yes	Yes	0.600			\$7.71	\$12.85			
	158	Yes		Yes	Yes	0.670			\$7.01	\$10.47			
	159	Yes		Yes	Yes	0.700			\$24.95	\$35.64			
	160	Yes		Yes	Yes	0.750			\$10.17	\$13.57			
	161	Yes		Yes	Yes	0.900			\$10.21	\$11.35			
	162	Yes		Yes	Yes	1.000			\$16.04	\$16.04			
	163	Yes		Yes	Yes	0.025	\$11.11	\$444.59	\$9.63	\$385.06	\$0.07	\$7.85	
	164	Yes		Yes	Yes	0.900	\$19.99	\$22.22	\$17.78	\$19.76	\$0.11	\$0.32	
	165	Yes		Yes	Yes	1.100	\$18.69	\$16.99	\$15.05	\$13.68	\$0.18	\$0.44	

Table J.1. Facility Details and Costs

Process	#	Ammonia Removal (Nitrification)	Phosphorus Removal (Denitrification)	Filtration	Disinfection	Flow (mgd)	Present Worth Cost (\$M)	Unit Present Cost (\$M/mgd)	Adjusted Construction Cost (\$M)	Construction Cost (\$M/mgd)	Unit Annual O&M Cost (\$M)	Adjusted Annual O&M Cost (\$M)	Unit Annual O&M Cost (\$/1000 gal)
	166	Yes	Yes	Yes	Yes	1,100	\$11.36	\$10.33					
	167	Yes	Yes	Yes	Yes	2,500	\$19.12	\$7.65					
	168	Yes	Yes	Yes	Yes	2,500	\$43.90	\$17.56	\$20.30	\$8.12	\$1.14	\$1.25	
	169	Yes	Yes	Yes	Yes	3,810			\$33.12	\$8.69			
	170	Yes	Yes	Yes	Yes	4,000			\$28.94	\$7.24			
	171	Yes	Yes	Yes		1,000	\$21.25	\$21.25	\$7.77	\$7.77	\$0.65	\$1.78	
	172	Yes	Yes	Yes		0,1117	\$50.13	\$40.06	\$34.76	\$0.09	\$2.03		
	173	Yes	Yes			0,750	\$23.75	\$31.67	\$7.54	\$10.05	\$0.78	\$2.85	
	174	Yes	Yes	Yes	Yes	1,000	\$17.91	\$17.91	\$4.40	\$4.40	\$0.65	\$1.78	
	175	Yes	Yes	Yes		0,300	\$17.07	\$56.90	\$8.49	\$28.31	\$0.41	\$3.77	
D.1) Pond	176	Yes	Yes	Yes		2,000	\$17.94	\$8.97	\$14.30	\$7.15	\$0.18	\$0.24	
	177	Yes	Yes	Yes		0,220					\$0.14	\$1.79	
	178	Yes	Yes	Yes		0,020	\$1.39	\$69.40	\$0.56	\$28.06	\$0.04	\$5.45	
	179	Yes	Yes	Yes		0,165	\$8.57	\$51.95	\$2.86	\$17.33	\$0.28	\$4.57	
	180	Yes	Yes	Yes		0,060	\$7.30	\$121.62	\$2.85	\$47.54	\$0.21	\$9.77	
	181	Yes	Yes	Yes		0,100	\$6.57	\$65.72	\$2.62	\$26.21	\$0.19	\$5.21	
	182	Yes	Yes	Yes		0,180			\$3.24	\$17.99			
	183	Yes	Yes	Yes		0,020	\$3.55	\$177.56	\$2.78	\$139.15	\$0.04	\$5.07	
	184	Yes	Yes	Yes		1,000			\$5.96	\$5.96			
	185	Yes	Yes	Yes		0,490	\$4.16	\$8.48	\$1.10	\$2.25	\$0.15	\$0.82	
	186	Yes	Yes	Yes		0,350					\$0.08	\$0.65	
	187	Yes	Yes	Yes		0,260					\$0.39	\$4.08	
	188	Yes	Yes	Yes		0,250					\$0.27	\$2.95	
	189	Yes	Yes			0,750					\$0.29	\$1.06	
D.2) Lagoon	190	Yes	Yes	Yes		0,175	\$8.67	\$49.54	\$2.41	\$13.77	\$0.30	\$4.72	
	191	Yes	Yes	Yes		0,100	\$2.91	\$29.12	\$0.78	\$7.76	\$0.10	\$2.82	
	192	Yes	Yes	Yes		0,104	\$1.30	\$12.50	\$0.62	\$5.93	\$0.03	\$0.87	
	193	Yes	Yes	Yes		0,387	\$21.16	\$54.67	\$1.56	\$4.03	\$0.94	\$6.68	
	194	Yes	Yes			0,240			\$1.21	\$5.06			

Table J.1. Facility Details and Costs

Process	#	Ammonia Removal (Nitrification)	Phosphorus Removal (Denitrification)	Filtration	Disinfection	Flow (mgd)	Present Worth Cost (\$M)	Unit Present Cost (\$M/mgd)	Adjusted Construction Cost (\$M)	Construction Cost (\$M/mgd)	Unit Annual O&M Cost (\$M)	Adjusted Annual O&M Cost (\$M)	Unit Annual O&M Cost (\$/1000 gal)
	195	Yes	Yes			0.120	\$3.63	\$30.28	\$1.31	\$10.91	\$0.11	\$2.55	
	196	Yes	Yes			0.350	\$30.12	\$86.06	\$2.79	\$7.97	\$1.32	\$10.30	
	197	Yes	Yes		Yes	0.040	\$4.67	\$116.80	\$1.07	\$26.68	\$0.17	\$11.89	
	198	Yes	Yes			0.750	\$9.62	\$12.82	\$1.46	\$1.94	\$0.39	\$1.43	
	199	Yes	Yes			0.750							
	200	Yes	Yes			0.007							
	201	Yes	Yes			0.010							
	202	Yes	Yes			0.009							
	203	Yes	Yes			0.009							
	204	Yes	Yes			0.007							
	205	Yes	Yes			0.016							
	206	Yes	Yes			0.006							
	207	Yes	Yes			0.009							
	208	Yes	Yes			0.066							
	209	Yes	Yes			0.054							
	210	Yes	Yes			0.019							
	211	Yes	Yes			0.010							
	212	Yes	Yes			0.999							
D.3) Wetland	213	Yes	Yes			1.000							
	214	Yes	Yes			0.280							
	215	Yes	Yes			0.050							
	216	Yes	Yes			0.075							
	217	Yes	Yes			0.100							
	218	Yes	Yes			0.065							
	219	Yes	Yes			0.240							
	220	Yes	Yes			0.100							
	221	Yes	Yes			0.680							
	222	Yes	Yes			1.000							
	223	Yes	Yes			0.360							

Table J.1. Facility Details and Costs

Process	#	Ammonia Removal (Nitrification)	Nitrogen Removal (Denitrification)	Phosphorus Removal	Filtration	Disinfection	Flow (mgd)	Present Worth Cost (\$M)	Present Cost (\$M)	Adjusted Construction Cost (\$M)	Construction Cost (\$M/mgfd)	Unit Construction Cost (\$/M/mgfd)	Annual O&M Cost (\$M)	Adjusted Annual O&M Cost (\$/1000 gal)
	224	Yes	Yes	Yes			0.180			\$0.59		\$3.30		
	225	Yes	Yes	Yes			0.040			\$0.38		\$9.41		
	226	Yes	Yes	Yes			0.060			\$1.42		\$23.65		
	227	Yes	Yes	Yes			1.180	\$9.34	\$7.92	\$7.20		\$6.10	\$0.10	\$0.24
	228	Yes	Yes	Yes			0.100			\$2.75		\$27.53		
	229	Yes	Yes	Yes			0.040	\$3.61	\$90.24	\$1.94		\$48.43	\$0.08	\$5.51
	230	Yes	Yes	Yes			0.080	\$5.95	\$74.41	\$2.96		\$37.05	\$0.14	\$4.93
E.1) LM	231	Yes	Yes	Yes			1.000	\$32.26	\$32.26	\$16.66		\$16.66	\$0.75	\$2.06
	232	Yes	Yes	Yes			0.040	\$3.37	\$84.33	\$1.80		\$44.95	\$0.08	\$5.19
	233	Yes	Yes	Yes			0.080	\$5.56	\$69.54	\$2.75		\$34.39	\$0.14	\$4.64
	234	Yes	Yes	Yes			1.000	\$28.45	\$28.45	\$14.80		\$14.80	\$0.66	\$1.80

Table J.2. Construction Costs

Process	#	State Zip Code	Utility Zip Code	R.S. Means Location Factor	Date of Construction	Raw Construction Cost (\$)	ENR Construction Cost Index (CCI)	Adjusted Construction Cost with ENR Index and Location Factor	Filtration Cost	UV Cost	Total Construction Cost
1	CA	950	1,125	6/1/1995	\$10,000,000	5432	\$13,992,800				\$13,992,800
2	NH	033	0,913	6/1/2005	\$1,463,200	7415	\$1,848,156		\$12,369		\$1,860,524
3	AZ	852	0,878	10/5/1986	\$2,100,000	4342		\$4,710,336			\$4,710,336
4	FL	323	0,813	6/1/1974	\$5,948,366	2126	\$29,428,002				\$29,428,002
5	FL	336	0,939	11/1/1988	\$19,923,000	4567	\$39,726,018		\$161,208	\$1,174,998	\$41,062,224
6	CO	800	0,969	9/1/1986	\$2,365,500	4333		\$4,817,563	\$52,140		\$4,869,703
7	MD	210	0,943	1/1/1986	\$3,000,000	4205	\$6,469,347		\$118,067	\$1,020,069	\$7,607,484
8	GA	315	0,761	1/21/1986	\$143,495	4205	\$383,445		\$16,893	\$444,592	\$844,930
9	CO	816	1,079	6/1/1980	\$8,055,000	3193	\$19,992,269		\$112,174		\$20,104,443
10	CO	315	0,932	6/1/1981	\$10,610,000	4201		\$23,172,009	\$110,717		\$23,282,727
11	AR	718	0,735	6/1/2006	\$604,200	7700	\$912,892		\$171,959	\$1,209,946	\$2,294,798
12	GA	302	0,913	6/1/2008	\$7,111,111	8185		\$8,137,011	\$24,492	\$490,512	\$8,652,016
13	FL	324	0,798	6/1/2001	\$2,511,398	6318		\$4,259,415	\$44,245		\$4,303,659
14	FL	324	0,798	6/1/2006	\$4,533,020	7700	\$6,308,279		\$90,942		\$6,399,222
15	FL	323	0,813	6/1/2005	\$3,489,000	7415		\$4,948,985	\$78,460		\$5,027,446
16	FL	338	0,860	6/1/2006	\$3,117,600	7700		\$4,025,762	\$56,725		\$4,082,488
17	GA	302	0,913	6/1/2008	\$3,438,206	8185		\$3,934,226	\$0		\$3,934,226
18	TN	373	0,804	6/1/2001	\$955,000	6318		\$1,607,624	\$42,644		\$1,650,268
19	TN	373	0,804	6/1/2008	\$575,000	8586		\$712,259	\$42,644		\$754,903
20	TN	370	0,882	6/1/2002	\$3,396,000	6532		\$5,040,456	\$98,765	\$940,659	\$6,079,879
21	TN	370	0,882	6/1/2001	\$850,000	6318		\$1,304,330	\$21,651	\$474,763	\$1,800,745
22	TN	371	0,882	6/1/2008	\$1,494,000	8185		\$1,769,621	\$37,696		\$1,807,317
23	TN	377	0,799	6/1/2006	\$1,095,100	7700		\$1,522,065	\$12,435	\$409,967	\$1,944,467
24	FL	338	0,860	6/1/2005	\$2,401,900	7415		\$3,220,789	\$56,725	\$731,304	\$4,008,818
25	GA	302	0,913	6/1/2007		7939					
26	CA	961	1,079	6/1/2007	\$1,021,063	7939		\$1,019,254	\$6370	\$343,451	\$1,369,074
27	CA	945	1,148	6/1/2001	\$8,500,000	6238		\$10,149,592	\$49,340		\$10,198,932
28	CA	932	1,066	6/1/2001	\$597,387	6238		\$768,192	\$12,435		\$780,627
29	CA	953	1,173	6/1/2008	\$6,262,206	8185		\$5,577,346	\$8990		\$5,586,336

A.2) Extended Aeration

Table J.2. Construction Costs

Process	#	State	Utility Zip Code	R.S. Means Location Factor	Date of Construction	Raw Construction Cost (\$)	ENR Construction Cost Index (CCI)	Adjusted Construction Cost with ENR Index and Location Factor	Filtration Cost	UV Cost	Total Construction Cost
	30	AR	725	0.733	6/1/2008	\$7,006,700	8185	\$9,986,373		\$452,857	\$10,439,230
	31	GA	318	0.823	6/1/2001	\$1,060,000	6318	\$1,743,184	\$15,653		\$1,758,837
	32	GA	304	0.734	6/1/2003	\$3,264,358	6709	\$5,668,405	\$5974		\$5,674,379
	33	NC	284	0.773	6/1/1997	\$831,800	5860	\$1,570,214	\$17,505		\$1,587,718
	34	NC	284	0.773	6/1/1999	\$1,909,651	6039	\$3,498,052			\$3,498,052
	35	TN	371	0.882	6/1/1999	\$645,000	6039	\$1,035,483	\$27,254	\$504,576	\$1,567,313
	36	TN	378	0.799	6/1/1995	\$429,200	8432	\$544,753	\$15,653	\$435,711	\$996,117
	37	AR	725	0.733	6/1/2000	\$3,950,000	6238	\$7,386,941		\$394,445	\$7,781,386
	38	GA	318	0.823	6/1/2002		6532				
	39	GA	308	0.805	6/1/2002		6532				
	40	GA	304	0.734	6/1/2002		6532				
	41	TN	373	0.804	6/1/2007		7939				
	42	FL	339	0.822	6/1/1998		4525				
	43	CA	954	1.121	6/1/1996	\$12,813,907	5597	\$17,463,752	\$21,312		\$17,485,065
A.3) Intermittent Aeration	44	GA	310	0.811	6/1/1970	\$1,477,400	1381	\$11,279,776	\$98,765	\$940,659	\$12,319,199
	45	PA	180	1.041	2/1/1988	\$5,475,000	4473	\$10,054,290			\$10,054,290
A.4) A/O	46	NJ	079	1.104	11/20/1989	\$15,677,576	4645	\$26,142,134			\$26,142,134
	47	NJ	786	0.809	11/19/1990	\$15,665,847	4780	\$24,641,315			\$34,641,315
	48	TX	780	0.777	1/1/1987	\$3,445,000	4349	\$8,717,575			\$8,717,575
A.5) A2/O	49	TX	786	0.809	5/22/1990	\$4,039,099	4473	\$9,544,518	\$118,067		\$9,662,585
	50	NH	038	0.962	8/7/1986		4330				
	51	FL	336	0.939	3/29/1986	\$8,300,000	4697	\$16,091,956	\$136,607		\$16,228,564
	52	IN	477	0.956	5/22/1989	\$8,614,000	4578	\$16,830,154	\$136,607	\$1,089,904	\$18,056,666
	53	FL	346	0.939	4/1/1983	\$4,900,000	4001	\$11,152,670	\$171,959		\$11,324,629
	54	FL	327	0.919	1/1/1988	\$19,923,000	4567	\$40,590,567	\$205,567	\$1,312,091	\$42,108,225
	55	MO	630	1.037	6/11/1989	\$15,820,000	4599	\$28,364,898	\$205,567	\$1,312,091	\$29,882,555
	56	FL	329	0.954	8/7/1986	\$8,523,628	4330	\$17,644,328	\$108,523	\$981,772	\$18,734,623
	57	AZ	855	0.836	12/27/1982	\$4,356,000	3950	\$11,279,800	\$86,723	\$886,741	\$12,253,265
	58	AZ	960	1.100	7/1/1991	\$14,700,000	4854	\$23,541,915			\$23,541,915

Table J.2. Construction Costs

Process	#	State	Utility Zip Code	R.S. Means Location Factor	Date of Construction	Raw Construction Cost (\$)	ENR Construction Cost Index (CCI)	Adjusted Construction Cost with ENR Index and Location Factor	Filtration Cost	UV Cost	Total Construction Cost
	59	FL	327	0.919	1/1/1988	\$19,923,000	4567	\$40,590,567	\$205,567	\$1,312,091	\$42,108,225
	60	AZ	852	0.878	6/4/2003	\$7,350,000	6709	\$10,669,693			\$10,669,693
	61	AZ	853	0.836	4/3/1997	\$11,643,889	5799	\$20,537,878			\$20,537,878
A.7) BNR	62	CA	930	1.091	9/30/2004	\$4,000,000	7298	\$4,295,842			\$4,295,842
	63	CA	928	1.086	1/26/2000	\$10,497,896	6130	\$13,484,314			\$13,484,314
	64	CA	930	1.091	8/3/1995	\$8,468,000	5506	\$12,054,156			\$12,054,156
	65	TX	719	0.722	2/1/1980	\$3,872,000	3134	\$14,632,417	\$124,075		\$14,756,491
	66	TX	719	0.722	5/1/1973	\$920,083	2126	\$5,125,585	\$882,618	\$867,430	\$6,075,633
	67	FL	327	0.919	2/27/1988	\$4,400,000	4473	\$9,152,825	\$556,725		\$9,209,551
A.8) MLE	68	KY	416	0.796	11/25/1982	\$4,600,000	3917	\$12,615,605	\$118,067	\$1,020,069	\$13,753,742
	69	FL	336	0.939	6/22/1987	\$9,052,271	4387	\$18,790,625	\$136,607	\$1,089,904	\$20,017,137
	70	FL	320	0.864	10/14/1990	\$1,731,000	4771	\$3,590,797	\$32,580	\$528,984	\$4,152,361
	71	MO	658	0.908	6/26/1988	\$11,686,000	4525	\$24,320,828	\$110,448	\$989,641	\$25,420,917
A.9) Schreiber N&D	72	PA	155	0.940	5/13/1988	\$3,719,000	4493	\$7,529,720	\$32,580		\$7,562,300
A.10) In-Channel Denitrification	73	NY	125	1.087	6/1/1983	\$3,000,000	4066	\$5,804,185	\$65,633		\$5,869,818
	74	IN	473	0.930	4/1/1990	\$1,876,840	4685	\$3,683,423	\$32,580		\$3,716,003
	75	AZ	850	0.895	6/1/1988	\$3,750,000	4519	\$7,928,350	\$65,633		\$7,993,983
A.11) ICEAS	76	PA	179	0.943	3/8/1994	\$10,500,000	5381	\$17,694,224	\$129,272	\$1,062,933	\$18,886,428
	77	PA	154	0.973	1/5/1995	\$600,000	5443	\$968,762	\$24,492		\$993,254
	78	PA	180	1.041	6/30/1988	\$600,000	4525	\$1,089,178	\$78,460		\$1,167,638
	79	NC	286	0.678	4/20/1995	\$4,000,000	5432	\$9,287,257	\$78,460		\$9,365,717
	80	PA	172	0.933	4/1/1989	\$2,000,000	4572	\$4,009,212	\$16,462	\$441,559	\$4,467,233
A.12) Trickling Filter	81	TN	385	0.756	6/1/2000		6238				
	82	TN	377	0.799	6/1/1992	\$4,496,516	5260	\$9,148,724	\$435,711		\$9,584,435
A.13) RBC	83	FL	320	0.864	6/1/2002		6532				
B.1) Package Plant	84	AR	727	0.718	6/1/2007	\$392,500	7939	\$588,798			\$588,798
	85	CA	953	1.173	6/1/1994	\$5,000,000	5408	\$6,739,881	\$17,505		\$6,757,386
	86	NC	273	0.787	6/1/2008	\$1,879,630	8185	\$2,495,145	\$2966	\$280,553	\$2,778,664

Table J.2. Construction Costs

Process	#	State	Utility Zip Code	R.S. Means Location Factor	Date of Construction	Raw Construction Cost (\$)	ENR Construction Cost Index (CCI)	Adjusted Construction Cost with ENR Index and Location Factor	Filtration Cost	UV Cost	Total Construction Cost
	87	WV	267	0.929	6/1/2008	\$2,664,400	8185	\$2,996,277	\$12,435	\$409,967	\$3,418,679
	88	FL	338	0.860	6/1/2000	\$2,355,283	6238	\$3,754,189	\$8264	\$367,946	\$4,130,399
	89	WV	251	0.984	6/1/1994		5408				\$8,237,621
	90	FL	339	0.822	6/1/1998	\$4,668,104	5895	\$8,237,621			
	91	NV	984	0.998	10/1/2004	\$8,119,601	7314	\$9,511,939	\$5164	\$324,895	\$9,841,998
	92	OH	433	0.915	3/1/1994	\$1,603,000	5200	\$2,880,885	\$32,580	\$528,984	\$3,442,450
	93	TN	380	0.893	3/1/1993	\$3,000,000	5106	\$5,626,080	\$32,580	\$528,984	\$6,187,644
	94	NH	031	0.969	1/12/1988	\$2,610,060	4459	\$5,165,426	\$24,492		\$5,189,918
	95	ME	039	0.855	4/1/1993	\$4,000,000	5106	\$7,834,837	\$18,712	\$456,788	\$8,310,337
	96	MI	480	1.009	4/15/1987	\$3,482,486	4360	\$6,769,064	\$27,254		\$6,796,318
	97	GA	302	0.913	10/1/1990	\$1,237,779	4771	\$2,429,852	\$19,309	\$460,596	\$2,909,757
	98	IA	506	0.835	8/24/1981	\$2,400,000	3616	\$6,796,937	\$32,476	\$528,535	\$7,357,948
	99	NV	894	0.998	12/1/2007	\$12,443,190	8090	\$13,179,342	\$56,725	\$731,304	\$13,967,372
	100	GA	301	0.913	6/1/1998	\$6,500,000	5895	\$10,327,036	\$18,712	\$456,788	\$10,802,536
	101	AZ	853	0.836	6/1/2000	\$2,084,000	6238	\$3,417,142			\$3,417,142
	102	MA	012	1.048	8/1/1992	\$2,750,000	5032	\$4,459,105	\$78,460	\$847,333	\$5,384,899
	103	MN	559	1.065	10/1/1987	\$10,000,000	4459	\$18,006,522	\$98,765	\$0	\$18,105,286
	104	AZ	852	0.878	5/1/1995	\$6,000,000	5433	\$10,755,583	\$114,274	\$1,005,057	\$11,874,913
	105	OK	731	0.839	1/1/1987	\$6,000,000	4354	\$14,044,872	\$136,607	\$1,089,904	\$15,271,383
B.2) SBR	106	CT	63	1.067	7/1/1993	\$15,300,000	5252	\$23,346,361	\$56,725	\$731,304	\$24,134,391
	107	IA	522	0.941	11/1/1992	\$6,500,000	8293	\$7,122,443	\$158,059	\$1,164,520	\$8,445,022
	108	GA	301	0.913	9/27/1989	\$1,297,000	4606	\$2,637,316	\$56,725	\$731,304	\$3,425,345
	109	GA	317	0.806	8/25/1988	\$2,800,000	4542	\$6,540,226	\$32,580	\$528,984	\$7,101,790
	110	PA	183	0.978	4/1/1995	\$7,000,000	5432	\$11,267,208			\$11,267,208
	111	PA	159	0.965	6/1/1991	\$5,300,000	4818	\$9,747,622	\$67,812		\$9,815,434
	112	AZ	853	0.895	8/1/2008	\$35,000,000	8293	\$40,322,760			\$40,322,760
	113	PA	179	0.943	6/1/1993	\$10,500,000	5260	\$18,101,258	\$74,247		\$18,175,506
	114	AR	729	0.798	6/1/2003	\$2,591,266	6709	\$4,138,741	\$24,492		\$4,163,233
	115	CT	063	1.067	6/1/2005	\$20,000,000	7415	\$21,615,801	\$1,034,704	\$22,650,505	
	116	FL	323	0.813	6/1/2002	\$3,841,200	6532	\$6,185,105	\$456,788	\$6,641,893	

Table J.2. Construction Costs

Process	#	State	Utility Zip Code	R.S. Means Location Factor	Date of Construction	Raw Construction Cost (\$)	ENR Construction Cost Index (CCI)	Adjusted Construction Cost with ENR Index and Location Factor	Filtration Cost	UV Cost	Total Construction Cost
	117	FL	323	0.813	6/1/2005	\$1,632,000	7415	\$2,314,917	\$27,254		\$2,342,170
	118	GA	308	0.805	6/1/2003	\$2,602,650	6709	\$4,120,776	\$56,725		\$4,177,501
	119	NC	285	0.681	6/1/2000	\$1,482,357	6238	\$2,983,851			\$2,983,851
	120	TN	378	0.799	6/1/2000	\$654,000	6238	\$1,122,025	\$18,712	\$456,788	\$1,597,525
	121	WV	254	0.901	6/1/2007	\$23,102,000	7939	\$27,616,961	\$56,725	\$731,304	\$28,404,991
	122	NC	284	0.773	6/1/1999	\$5,752,633	6039	\$10,537,536			\$10,537,536
	123	AR	170	0.996	7/10/1991	\$1,493,242	4854	\$2,641,119	\$9062		\$2,650,181
	124	FL	338	0.860	6/1/2001		6318				
	125	PA	189	1.058	1/22/1993	\$2,572,048	5071	\$4,099,366	\$52,140		\$4,151,506
	126	FL	327	0.919	7/1/1991	\$12,308,555	4854	\$23,594,387	\$171,959		\$23,766,346
	127	AR	726	0.740	6/1/2005	\$933,760	7415	\$1,455,155			\$1,455,155
	128	AZ	856	0.872	4/1/1993	\$3,000,000	5106	\$5,761,570	\$65,633	\$781,370	\$6,608,573
	129	FL	327	0.919	1/1/1984	\$2,800,000	4109	\$6,340,497	\$56,725	\$731,304	\$7,128,526
	130	CA	934	1.054	11/20/2003	\$21,534,000	6794	\$25,714,345			\$25,714,345
	131	MI	483	1.009	7/1/1986	\$5,339,000	4332	\$10,444,730	\$46,166		\$10,490,896
	132	FL	338	0.860	12/31/1985	\$3,472,000	4208	\$8,203,939	\$94,794	\$923,297	\$9,222,030
	133	FL	348	0.833	3/2/1993	\$3,900,000	5106	\$7,840,716	\$56,271		\$7,896,987
B.3) OD	134	GA	348	0.833	8/1/1989	\$13,500,000	4606	\$30,087,198			\$30,087,198
	135	FL	320	0.864	6/1/2008	\$4,422,000	8185	\$5,346,914			\$5,346,914
	136	NC	275	0.788	6/1/2008	\$1,213,027	8185	\$1,608,209	\$20,195		\$1,628,404
	137	TN	377	0.799	6/1/2006	\$3,819,175	7700	\$5,308,221	\$27,254	\$504,576	\$5,840,050
	138	TN	377	0.799	6/1/2005	\$1,135,700	7415	\$1,639,165	\$63,083	\$767,436	\$2,469,684
	139	TN	377	0.799	6/1/2004	\$1,615,000	7108	\$2,431,617	\$15,653	\$435,711	\$2,882,982
	140	FL	341	0.822	6/1/1999	\$4,752,000	6039	\$8,185,713	\$118,067		\$8,303,780
	141	NC	275	0.788	6/1/2003	\$3,873,458	6709	\$6,265,155	\$78,460		\$6,343,615
	142	CA	955	1.038	2/1/1988	\$13,250,000	4473	\$24,402,624	\$47,451	\$584,325	\$25,034,401
	143	WI	531	1.024	7/1/1986	\$6,000,000	4332	\$11,565,909	\$88,352	\$894,263	\$12,548,524
	144	OR	971	1.058	1/1/2002	\$691,000	6578	\$849,015			\$849,015
B.4) Biological Filtration	145	OR	970	1.058	2/1/2007	\$997,000	7903	\$1,019,611			\$1,019,611
	146	AR	727	0.718	6/1/2001	\$1,300,000	6318	\$2,450,508			\$2,450,508

Table J.2. Construction Costs

Process	#	State	Utility Zip Code	R.S. Means Location Factor	Date of Construction	Raw Construction Cost (\$)	ENR Construction Cost Index (CCI)	Adjusted Construction Cost with ENR Index and Location Factor	Filtration Cost	UV Cost	Total Construction Cost
	147	CO	801	0.969	6/1/2004	\$2,000,000	7108	\$2,482,994			\$2,482,994
	148	NC	275	0.788	8/1/2008	\$4,800,000	8293	\$6,280,877			\$6,280,877
	149	MA	012	1.048	6/1/2005	\$2,200,000	7415	\$2,420,846			\$2,420,846
	150	MO	633	0.957	4/1/2004	\$1,300,000	7017	\$1,655,377			\$1,655,377
	151	MA	781	0.837	6/30/1999	\$4,500,000	6039	\$7,612,704			\$7,612,704
	152	WA	980	1.059	5/1/2006	\$11,600,000	7691	\$12,178,565			\$12,178,565
	153	WA	981	1.059	5/19/2006	\$12,790,000	7691	\$13,427,918			\$13,427,918
	154	FL	330	0.917	6/30/1997	\$3,000,000	5860	\$4,773,877			\$4,773,877
	155	CA	953	1.173	2/1/2004	\$6,250,000	6825	\$6,675,691			\$6,675,691
	156	CA	954	1.121	6/1/1999	\$12,000,000	6039	\$15,157,498			\$15,157,498
C.1) MBR	157	CA	922	1.032	2/1/2004	\$6,350,000	6825	\$7,709,182			\$7,709,182
	158	AZ	853	0.895	12/1/2002	\$4,800,000	6538	\$7,014,395			\$7,014,395
	159	CA	953	1.173	1/31/2007	\$26,967,471	7880	\$24,947,837			\$24,947,837
	160	CA	953	1.173	1/21/2003	\$9,320,000	6678	\$10,174,684			\$10,174,684
	161	WA	980	1.059	1/21/2004	\$9,000,000	7115	\$10,213,828			\$10,213,828
	162	WA	985	1.019	12/1/2004	\$13,600,000	7115	\$16,040,087			\$16,040,087
	163	GA	301	0.913	1/1/2005	\$7,500,000	7297	\$9,626,381			\$9,626,381
	164	GA	301	0.913	1/1/2003	\$13,500,000	6581	\$17,784,299			\$17,784,299
	165	GA	301	0.913	1/1/2008	\$13,000,000	8090	\$15,050,155			\$15,050,155
	166	CA	928	1.086	6/30/2000	\$9,000,000	6238	\$11,360,154			\$11,360,154
	167	CA	945	1.148	6/1/1999	\$15,500,000	6039	\$19,117,966			\$19,117,966
	168	GA	300	1.000	6/1/2001	\$15,000,000	6319	\$20,298,307			\$20,298,307
	169	CA	344	0.810	12/1/2003	\$20,950,000	6678	\$33,120,892			\$33,120,892
	170	CA	954	1.121	8/1/2006	\$29,300,000	7722	\$28,943,371			\$28,943,371
	171	CA	954	1.121	1/1/2003	\$6,025,679	6581	\$6,984,341			\$6,984,341
D.1) Pond	172	CA	933	1.066	5/1/1996	\$2,544,100	5572	\$3,662,478	\$10,183	\$388,855	\$4,061,516
	173	GA	310	0.811	6/1/2006	\$5,052,600	7700	\$6,918,632	\$45,064	\$576,396	\$7,540,092
	174	CA	954	1.121	6/1/2004	\$4,100,965	7108	\$4,400,985			\$4,400,985
	175	GA	317	0.806	6/1/2005	\$5,589,750	7415	\$7,997,663	\$21,651	\$474,763	\$8,494,077
	176	GA	301	0.913	6/1/2003	\$9,500,000	6709	\$13,262,089	\$98,765	\$940,659	\$14,301,512

Table J.2. Construction Costs

Process	#	State	Utility Zip Code	R.S. Means Location Factor	Date of Construction	Raw Construction Cost (\$)	ENR Construction Cost Index (CCI)	Adjusted Construction Cost with ENR Index and Location Factor	Filtration Cost	UV Cost	Total Construction Cost
	177	GA	315	0.761	6/1/2001		6318				
	178	AR	724	0.778	6/1/2005	\$196,400	7415	\$291,117	\$2481	\$267,608	\$561,206
	179	AR	724	0.778	6/1/2005	\$1,920,500	7415	\$2,846,692	\$13,420		\$2,860,112
	180	AR	724	0.778	6/1/2005	\$1,920,500	7415	\$2,846,692	\$5974		\$2,852,666
	181	GA	306	0.806	6/1/2007	\$1,673,377	7939	\$2,236,196	\$8990	\$376,245	\$2,621,431
	182	AZ	864	0.836	1/31/2001	\$1,718,500	6281	\$2,798,559	\$14,388	\$426,100	\$3,239,027
	183	NV	894	0.998	3/8/2008	\$2,378,330	8109	\$2,512,992	\$2481	\$267,608	\$2,783,081
	184	CA	936	1.087	6/1/1991	\$3,170,000	4818	\$5,175,828	\$56,725	\$731,304	\$5,963,857
	185	CA	936	1.087	6/1/2001	\$438,000	6,318	\$545,358	\$32,058	\$526,726	\$1,104,142
	186	CA	936	1.087	6/1/1997		5860				
	187	NC	285	0.681	6/1/1994		5408				
	188	TN	385	0.756	6/1/1992		4973				
	189	WV	261	0.982	6/1/2007		7,939				
	190	CA	932	1.066	6/1/1997	\$1,749,800	5860	\$2,395,248	\$14,067		\$2,409,315
D.2) Lagoon	191	CA	932	1.066	6/1/1975	\$228,853	2393	\$767,138	\$8990		\$776,129
	192	AR	721	0.826	6/1/2005	\$170,000	7415	\$237,342			\$379,382
	193	NC	283	0.780	6/1/2000	\$603,000	6238	\$1,059,728			\$1,560,787
	194	TN	380	0.893	6/1/2008	\$635,000	8185	\$742,883	\$18,111	\$452,857	\$1,213,852
	195	WV	255	0.969	6/1/2007	\$817,000	7939	\$908,133	\$10,402	\$391,051	\$1,309,586
	196	GA	305	0.781	6/1/2008	\$1,700,000	8185	\$2,274,030	\$24,492	\$490,512	\$2,789,034
	197	NC	278	0.690	6/1/1999	\$517,895	6039	\$1,062,783	\$4319		\$1,067,102
	198	TN	384	0.773	6/1/2007	\$600,000	7939	\$836,032	\$45,064	\$576,396	\$1,457,492
	199	TN	385	0.756	6/1/2002		6532				
	200	MN	564	1.000	6/1/2000	\$381,189	6238	\$522,531	\$1022	\$211,655	\$735,208
	201	MN	560	1.006	6/1/2000	\$657,133	6238	\$895,420	\$1429	\$231,273	\$1,128,122
	202	MN	557	1.090	6/1/2001	\$247,331	6318	\$307,107	\$1308	\$225,891	\$534,305
D.3) Wetland	203	MN	563	1.103	6/1/2001	\$304,819	6318	\$374,028	\$1338	\$227,281	\$602,647
	204	MN	557	1.090	6/1/2001	\$704,263	6318	\$874,471	\$1055	\$213,419	\$1,088,946
	205	MN	553	1.138	6/1/2003	\$419,405	6709	\$469,732	\$2032	\$253,848	\$725,612
	206	MN	561	0.885	6/1/2003	\$410,048	6709	\$590,542	\$923	\$206,004	\$797,468

Table J.2. Construction Costs

Process	#	State	Utility Zip Code	R.S. Means Location Factor	Date of Construction	Raw Construction Cost (\$)	ENR Construction Cost Index (CCI)	Adjusted Construction Cost with ENR Index and Location Factor	Filtration Cost	UV Cost	Total Construction Cost
207	MN	553	1.138	6/1/2004	\$618,054	7108	\$653,362	\$1338	\$227,281	\$881,981	
208	WI	550	1.126	6/1/2004	\$2,996,500	7108	\$3,201,440	\$6472	\$344,901	\$3,552,813	
209	MN	562	0.913	6/1/2004	\$1,281,762	7108	\$1,688,908	\$5526	\$330,773	\$2,025,207	
210	MN	563	1.103	6/1/2005	\$349,743	7415	\$365,662	\$2383	\$264,778	\$632,822	
211	MN	550	1.126	6/1/2005	\$406,281	7415	\$416,096	\$1459	\$232,548	\$650,104	
212	CA	955	1.039	4/1/2008	\$3,309,596	8019	\$3,396,692	\$56,680	\$612,461	\$4,065,833	
213	AZ	859	0.848	6/1/1998	\$561,975	5852	\$968,386	\$56,725	\$731,304	\$1,756,416	
214	SD	574	0.806	6/1/1998	\$580,000	5852	\$1,051,527	\$20,488	\$467,879	\$1,539,895	
215	SD	570	0.822	6/1/1998	\$52,048	5852	\$92,525	\$5164	\$324,895	\$422,583	
216	SD	573	0.764	6/1/1998	\$117,048	5852	\$223,871	\$7142	\$354,015	\$585,028	
217	SD	573	0.764	6/1/1998	\$124,364	5852	\$237,864	\$8990	\$376,245	\$623,099	
218	SD	570	0.822	6/1/1998	\$63,536	5852	\$112,947	\$6370	\$343,451	\$462,767	
219	AL	360	0.838	6/1/1998	\$487,009	5852	\$849,220	\$18,111	\$452,857	\$1,320,189	
220	SD	570	0.822	6/1/1998	\$136,908	5852	\$243,380	\$8990	\$376,245	\$628,615	
221	OR	971	1.058	6/1/1998	\$785,424	5852	\$1,084,791	\$41,666	\$564,563	\$1,691,021	
222	CO	814	0.911	6/1/1998	\$1,224,768	5852	\$1,964,550	\$56,725	\$731,304	\$2,752,579	
223	WY	825	0.783	6/1/1998	\$116,769	5852	\$217,919	\$25,051	\$493,446	\$736,416	
224	MD	210	0.943	6/1/1998	\$98,923	5852	\$153,290	\$14,388	\$426,100	\$593,778	
225	MD	207	0.908	6/1/1998	\$38,604	5852	\$62,126	\$4319	\$309,904	\$376,349	
226	MI	490	0.921	6/1/1998	\$677,580	5852	\$1,075,050	\$5974	\$337,680	\$1,418,704	
227	CA	955	1.038	6/1/1982	\$3,309,596	4290	\$6,355,317	\$64,756	\$776,614	\$7,196,688	
228	SD	571	0.822	6/1/1998	\$1,332,204	5852	\$2,368,244	\$8990	\$376,245	\$2,753,479	
E.1) LM	229	MD	217	0.910	\$1/2000	\$1,077,777	6223	\$1,627,439	\$309,904	\$1,937,342	
230	VT	054	0.902	5/1/2000	\$1,710,280	6223	\$2,605,420		\$358,885	\$2,964,305	
231	VT	054	0.902	5/1/2000	\$10,457,542	6223	\$15,930,895		\$731,304	\$16,662,199	
232	MD	217	0.910	5/1/2000	\$985,391	6223	\$1,487,936		\$309,904	\$1,797,840	
233	VT	054	0.902	5/1/2000	\$1,570,246	6223	\$2,392,094		\$358,885	\$2,750,979	
234	VT	054	0.902	5/1/2000	\$9,232,257	6223	\$14,064,311		\$731,304	\$14,795,615	

Note: ENR Construction Cost Index in 12/2008 = 8551

Table J.3. O&M Costs - Material Costs

Process	#	Current Annual O&M Cost	Testing Costs	Chemical Costs	Materials (Supplies)	Maintenance Material Cost	Sludge Costs	Total Material Costs	ENR Material Price Index	Adjusted Material Cost with ENR Material Price Index and Location Factor
	1									
	2									
	3									
	4	\$81,395		\$81,760		\$65,700		\$228,855	1371	\$569,765
	5	\$1,245,149		\$27,442		\$25,162		\$1,297,753	1689	\$2,270,700
	6	\$468,515				\$106,135		\$574,650	1639	\$1,004,069
	7									
	8									
	9									
	10									
	11									
	12									
A.1) Activated Sludge	13									
	14									
	15									
	16									
	17	\$4829	\$9646	\$1922		\$19,292		\$35,689	2698	\$136,859
	18									
	19									
	20									
	21									
	22									
	23									
	24	\$5000			\$12,000			\$17,000	2492	\$22,012
	25									
	26	\$5835	\$2163		\$1700		\$12,698	2572	\$12,697	
	27									
	28	\$3478	\$1847		\$4532		\$9857	2572	\$1,882,367	
A.2) Extended Aeration	29	\$1600			\$4000		\$5600	2572	\$9977	
										\$5151

Table J.3. O&M Costs - Material Costs

Process	#	Current Annual O&M Cost	Testing Costs	Chemical Costs	Materials (Supplies)	Maintenance Material Cost	Sludge Costs	Total Material Costs	ENR Material Price Index	Adjusted Material Cost with ENR Material Price Index and Location Factor		
	30	\$2500	\$7500			\$2500	\$12,500	\$2698	\$17,540			
	31	\$3000	\$10000	\$7500		\$11,500	2572		\$15,076			
	32		\$10,143	\$7351	\$2869	\$20,363	2572		\$29,932			
	33	\$2328	\$2000	\$10000	\$6500	\$11,828	2293		\$18,218			
	34		\$7000		\$42,000		\$49,000	2157		\$81,551		
	35			\$26,000			\$26,000	2157		\$37,924		
	36			\$5000	\$10,000		\$15,000	1987		\$26,219		
	37		\$12,000				\$12,000	2572		\$17,663		
	38	\$2000	\$500	\$10000	\$9000	\$4000	\$16,500	2070		\$26,877		
	39			\$4414			\$4414	2070		\$7351		
	40			\$3800		\$8000	\$11,800	2070		\$21,552		
	41		\$30,000				\$30,000	2572		\$40,258		
	42		\$20,000	\$46,150			\$66,150	2178		\$102,533		
	43					\$51,972		\$51,972	2028		\$63,439	
A.3) Intermittent Aeration	44											
	45		\$14,000		\$6000	\$95,000	\$115,000	1686		\$181,825		
A.4) A/O	46	\$766,500	\$32,850	\$16,425		\$815,775	1708		\$1,200,539			
	47	\$912,500	\$36,500		\$21,900	\$970,900	1718			\$1,938,500		
A.5) A2/O	48											
	49											
	50	\$59,003	\$49,039				\$108,042	2219		\$140,450		
	51											
	52											
	53	\$1,099,380	\$138,700		\$75,920		\$1,314,000	1642		\$2,364,937		
A.6) Bardenpho	54											
	55											
	56	\$59,003	\$49,039				\$108,042	1633		\$192,451		
	57											
	58	\$346,750					\$65,000	1547		\$139,470		
	59	\$7300					\$354,050	1708		\$522,934		

Table J.3. O&M Costs - Material Costs

Process	#	Current Annual O&M Cost	Testing Costs	Chemical Costs	Materials (Supplies)	Maintenance Material Cost	Sludge Costs	Total Material Costs	ENR Material Price Index	Adjusted Material Cost with ENR Material Price Index and Location Factor
	59									
	60									
	61									
	62									
A.7) BNR	63									
	64				\$13,593	\$77,672		\$91,265	1,499	\$234,006
	65				\$79,738	\$69,642		\$77,380	1,351	\$220,140
	66									
	67									
A.8) MLE	68									
	69									
	70									
	71									
A.9) Schreiber N&D	72	\$529,250			\$11,863			\$541,113	1698	\$940,773
A.10) In-Channel Denitrification	73									
	74				\$31,000	\$295,000		\$326,000	1714	\$567,527
	75									
	76									
A.11) ICEAS	77	\$300,000			\$3200		\$22,000	\$325,200	2031	\$456,658
	78	\$500,000			\$1000		\$15,000	\$516,000	1699	\$809,596
	79					\$39,600		\$39,600	1999	\$81,080
	80	\$159,700			\$3000		\$4200		\$166,900	\$295,304
A.12) Trickling Filter	81									
	82						\$4100	\$5500	\$9,600	1787
A.13) RBC	83						\$32,676		\$37,825	2070
	84						\$20,000		\$20,000	2572
B.1) Package Plant	85	\$250,000	\$20,000					\$270,000	2083	\$306,648
	86						\$3000	\$12,000	\$21,500	2698
										\$28,099

Table J.3. O&M Costs - Material Costs

Process	#	Current Annual O&M Cost	Testing Costs	Chemical Costs	Materials (Supplies)	Maintenance Material Cost	Sludge Costs	Total Material Costs	ENR Material Price Index	Adjusted Material Cost with ENR Material Price Index and Location Factor
	87									
	88	\$3300	\$761		\$150	\$1643	\$5854	2219	\$8513	
	89				\$3400		\$3400	2083	\$4603	
	90		\$21,855	\$68,699			\$90,554	2120	\$144,199	
	91									
	92	\$48,100		\$8500			\$56,600	2109	\$81,392	
	93									
	94			\$2000		\$8000	\$10,000	1686	\$16,986	
	95									
	96			\$1000		\$8000	\$9000	1655	\$14,956	
	97									
	98	\$55,765		\$500	\$5192		\$61,457	1,523	\$134,106	
	99									
	100	\$80,000	\$15,000	\$20,000			\$115,000	2178	\$160,484	
	101	\$80,000	\$3000				\$83,000	2219	\$124,159	
	102									
B.2) SBR	103									
	104									
	105									
	106									
	107			\$10,000			\$10,000	1777	\$16,595	
	108									
	109	\$29,490		\$6800			\$36,290	1708	\$73,153	
	110									
	111	\$147,240		\$40,000			\$187,240	1691	\$318,413	
	112	\$2,121,337	\$45,000	\$100,000			\$2,266,337	2823	\$2,489,164	
	113			\$40,000			\$40,000	2092	\$56,266	
	114									
	115									
	116	\$4000		\$22,000	\$3000	\$10,000	\$39,000	2070	\$64,308	

Table J.3. O&M Costs - Material Costs

Process	#	Current Annual O&M Cost	Testing Costs	Chemical Costs	Materials Supplies	Maintenance Material Cost	Sludge Costs	Total Material Costs	ENR Material Price Index	Adjusted Material Cost with ENR Material Price Index and Location Factor
	117									
	118			\$5200		\$13,113		\$13,113	2572	\$17,575
	119					\$14,900	\$7300	\$27,400	2120	\$52,666
	120									
	121									
	122					\$7500		\$7500	2120	\$12,700
	123	\$97,210						\$97,210	1708	\$158,572
	124									
	125			\$18,978				\$18,978	1807	\$27,547
	126									
	127					\$28,822		\$28,822	2572	\$42,023
	128									
	129	\$119,711						\$119,711	1622	\$222,859
	130									
	131	\$542,500		\$13,480		\$35,300		\$591,280	1643	\$989,754
	132	\$54,894		\$21,729		\$29,111		\$105,734	1611	\$211,779
B.3) OD	133									
	134			\$8464				\$8,464	1706	\$16,528
	135	\$18,000	\$4000			\$32,500		\$54,500	2570	\$68,110
	136			\$182		\$256,212		\$256,394	2578	\$350,237
	137									
	138					\$40,000		\$40,000	2492	\$55,748
	139					\$4968	\$2707	\$7675	2572	\$10,364
	140									
	141	\$7684	\$30,363	\$56,945		\$76,140	\$87,835	\$258,967	1961	\$465,054
	142			\$67,160		\$61,320		\$128,480	1686	\$203,725
	143	\$549,000		\$0		\$10,000		\$559,000	1643	\$922,013
	144									
	145									
	146									
B.4) Biological Filtration										

Table J.3. O&M Costs - Material Costs

Process	#	Current Annual O&M Cost	Testing Costs	Chemical Costs	Materials (Supplies)	Maintenance Material Cost	Sludge Costs	Total Material Costs	ENR Material Price Index	Adjusted Material Cost with ENR Material Price Index and Location Factor
	147	\$120,405	\$7825					\$128,230	2345	\$156,597
	148								2823	\$0
	149									
	150									
	151									
	152									
	153									
	154									
	155									
	156									
	157									
	158									
	159									
	160									
	161									
	162									
	163	\$80,000	\$15,000	\$1800				\$96,800	2402	\$122,488
	164	\$80,000	\$15,000	\$20,000				\$115,000	2578	\$135,584
	165	\$100,000	\$15,000	\$48,000				\$163,000	2578	\$192,175
	166									
	167									
	168									
	169									
	170									
	171									
	172									
D.1) Pond	173									
	174	\$10,000				\$15,000		\$25,000	2585	\$33,092
	175									
	176	\$100,000	\$15,000	\$48,000		\$3000		\$6000	2492	\$8290
								\$163,000	2578	\$192,175

Table J.3. O&M Costs - Material Costs

Process	#	Current Annual O&M Cost	Testing Costs	Chemical Costs	Materials (Supplies)	Maintenance Material Cost	Sludge Costs	Total Material Costs	ENR Material Price Index	Adjusted Material Cost with ENR Material Price Index and Location Factor
	177	\$6000	\$8400	\$8300				\$22,700	2120	\$39,045
	178				\$5000			\$5000	2585	\$6899
	179									
	180				\$15,000			\$15,000	2345	\$22,816
	181	\$2000	\$1026	\$1038				\$4064	2345	\$5967
	182									
	183									
	184									
	185				\$3500			\$3500	2219	\$4027
	186				\$2214			\$2214	2293	\$2465
	187	\$4000	\$5673	\$930	\$4650			\$15,253	2083	\$29,839
	188		\$3000		\$15,000			\$18,000	1787	\$36,973
	189							\$83,360	2572	\$91,588
	190									
D.2) Lagoon	191									
	192			\$2370				\$2370	2492	\$3195
	193	\$27,700	\$9600	\$46,900	\$20,000	\$104,200		2157		\$171,864
	194									
	195					\$5588		2572		\$6222
	196		\$13,500	\$37,500		\$51,000		2698		\$67,165
	197	\$2251	\$2500	\$7600		\$12,351		2492		\$19,933
	198			\$30,423	\$33,654	\$3562	\$67,639	2572		\$94,408
	199		\$2300		\$12,600		\$14,900	2070		\$26,421
	200									
	201									
	202									
D.3) Wetland	203									
	204									
	205									
	206									

Table J.3. O&M Costs - Material Costs

Process	#	Current Annual O&M Cost	Testing Costs	Chemical Costs	Materials (Supplies)	Maintenance Material Cost	Sludge Costs	Total Material Costs	ENR Material Price Index	Adjusted Material Cost with ENR Material Price Index and Location Factor
	207									
	208									
	209									
	210									
	211									
	212									
	213									
	214									
	215									
	216									
	217									
	218									
	219									
	220									
	221									
	222									
	223									
	224									
	225									
	226									
	227	\$39,000	\$8564					\$47,564	2572	\$49,440
	228									
	229					\$10,248	\$4375	\$14,623	2241	\$19,898
	230					\$14,325	\$8750	\$23,075	2241	\$31,678
E.1) LM	231					\$105,949	\$54,112	\$160,061	2241	\$219,735
	232					\$9025	\$4375	\$13,400	2241	\$18,234
	233					\$12,626	\$8750	\$21,376	2241	\$29,345
	234					\$93,674	\$54,112	\$147,786	2241	\$202,884

Note: ENR Material Price Index in 12/2008 = 2775

Table J.4. O&M Costs - Electricity Costs and Labor Costs

Process	#	Electricity Costs	Average Price of Electricity (\$)	Adjusted Electricity Cost with Average Prices and Location Factor	Total Labor Costs	ENR Skilled Labor Index	Adjusted Labor Cost with ENR Labor Index and Location Factor	Date for O&M Cost
1								06/01/95 \$1,702,000
2								06/01/93 \$44,678
3								10/05/86
4	\$121,545	1.70	\$647,255	\$106,580	\$3077	\$345,396	\$6,183,831	06/01/74 \$1,562,416
5	\$191,944	4.70	\$320,102	\$1,715,434	\$4122	\$3,593,028	09/01/86 \$1,504,744	11/01/88
6	\$59,130	4.93	\$91,099	\$192,540	\$3933	\$409,575	01/01/86	
7								
8								01/21/86
9	\$102,140	3.70	\$188,300	\$81,710	\$3454	\$177,743	06/01/80 \$366,043	
10	\$130,334	4.30	\$239,360	\$114,395	\$3525	\$282,288	06/01/81 \$521,648	
11								
12	\$51,716	6.51	\$64,040	\$489,098	\$7579	\$573,025	06/01/07 \$676,526	
13				\$450,800	\$6981	\$656,030	06/01/05 \$656,030	
14								06/01/06 \$612,117
15								
16	\$55,500	6.41	\$74,099	\$688,109	\$7213	\$899,297	06/01/06 \$1,110,255	
17	\$14,475	7.42	\$15,726	\$124,834	\$7818	\$141,784	06/01/08 \$197,715	
18	\$2640	5.23	\$4621	\$176,684	\$5948	\$299,523	06/01/01 \$312,936	
19	\$50,250	7.42	\$61,995	\$158,215	\$7818	\$204,059	06/01/08 \$295,477	
20	\$40,000	5.03	\$66,359	\$651,184	\$6166	\$970,715	06/01/02 \$1,056,833	
21	\$23,000	5.23	\$36,697	\$77,385	\$5948	\$119,585	06/01/01 \$156,283	
22	\$21,700	7.42	\$24,404	\$484,883	\$7818	\$570,076	06/01/08 \$614,072	
23	\$7,600	6.41	\$10,922	\$115,527	\$7213	\$162,510	06/01/06 \$181,493	
24	\$38,000	5.86	\$55,496	\$40,575	\$6981	\$54,790	06/01/05 \$132,299	
25	\$24,720	6.51	\$30,611	\$289,776	\$7579	\$339,500	06/01/07 \$370,111	
26	\$17,142	6.51	\$17,961	\$119,013	\$7579	\$117,983	06/01/07 \$148,642	
27								
28	\$17,468	6.51	\$18,526	\$92,608	\$7579	\$92,926	06/01/06 \$1,882,367	
29	\$8300	6.51	\$8000	\$202,519	\$7579	\$275,869	06/01/07 \$289,020	

Table J.4. O&M Costs - Electricity Costs and Labor Costs

Process	#	Electricity Costs	Average Price of Electricity (\$)	Adjusted Electricity Cost with Average Prices and Location Factor	Total Labor Costs	ENR Skilled Labor Index	Adjusted Labor Cost with ENR Labor Index and Location Factor	Date for O&M	Total O&M Cost
	30	\$28,300	7.75	\$36,666	\$12,660	\$7818	\$17,910	06/01/08	\$72,115
	31	\$13,700	6.51	\$18,820	\$184,564	\$7579	\$239,881	06/01/07	\$273,777
	32	\$78,567	6.51	\$121,015	\$383,891	\$7579	\$559,449	06/01/07	\$710,396
	33	\$12,300	4.53	\$25,853	\$54,310	\$5203	\$109,473	06/01/07	\$153,843
	34				\$444,050	\$5521	\$843,519	06/01/09	\$925,070
	35	\$48,000	4.43	\$90,416	\$232,315	\$5521	\$386,768	06/01/09	\$515,109
	36	\$20,000	4.66	\$39,534	\$71,259	\$4909	\$147,286	06/01/05	\$213,039
	37	\$18,000	6.51	\$27,763	\$223,337	\$7579	\$325,915	06/01/07	\$371,342
	38	\$14,500	5.03	\$25,780	\$67,200	\$6166	\$107,356	06/01/02	\$160,012
	39				\$345,045	\$6166	\$563,555	06/01/02	\$570,906
	40	\$21,000	5.03	\$41,863	\$145,431	\$6166	\$260,506	06/01/02	\$323,921
	41	\$101,500	6.51	\$142,727	\$1,000,744	\$7579	\$1,331,420	06/01/07	\$1,514,406
	42	\$27,000	4.48	\$53,962	\$185,971	\$5345	\$343,151	06/01/08	\$499,647
	43	\$100,663	4.60	\$143,676	\$1,659,206	\$7579	\$1,583,226	06/01/07	\$1,790,342
A.3) Intermittent Aeration	44							06/01/07	
	45	\$110,000	4.70	\$165,471	\$114,500	\$4122	\$216,325	02/01/88	\$563,621
A.4) A/O	46	\$186,150	4.72	\$262,924	\$251,850	\$4224	\$437,834	11/20/89	\$1,901,297
	47	\$197,100	4.74	\$378,301	\$204,400	\$4387	\$466,901	11/19/90	\$2,783,702
	48							01/01/87	
A.5) A2/O	49							05/22/90	
	50	\$152,457	4.64	\$251,381	\$526,517	\$5735	\$773,685	06/01/00	\$1,165,516
	51							03/29/86	
	52							05/22/89	
	53							04/01/83	\$2,364,937
A.6) Bardenpho	54							11/01/88	
	55							06/11/89	
	56	\$152,457	4.93	\$238,578	\$526,517	\$3933	\$1,137,628	08/07/86	\$1,568,657
	57	\$95,000	5.00	\$167,273	\$100,000	\$3600	\$269,371	12/27/82	\$576,114
	58	\$142,350	4.83	\$197,195	\$131,400	\$4475	\$216,406	07/01/91	\$936,535

Table J.4. O&M Costs - Electricity Costs and Labor Costs

Process	#	Electricity Costs	Average Price of Electricity (\$)	Adjusted Electricity Cost with Average Prices and Location Factor	Total Labor Costs	ENR Skilled Labor Index	Adjusted Labor Cost with ENR Labor Index and Location Factor	Date for O&M	Total O&M Cost
	59							11/01/88	
	60							06/04/03	
	61							04/03/97	
	62							09/30/04	
A.7) BNR	63							01/26/00	
	64							08/03/95	
	65	\$165,053	3.70	\$454,739	\$281,561	\$3454	\$915,320	02/01/80	\$1,604,065
	66	\$61,904	1.30	\$485,418	\$251,485	\$3021	\$934,726	05/01/73	\$1,640,284
	67							02/27/88	
	68							11/25/82	
	69							06/22/87	
A.8) MLE	70							10/14/90	
	71							06/26/88	
A.9) Schreiber N&D	72	\$43,800	4.70	\$72,967	\$84,863	\$4122	\$177,558	05/13/88	\$1,191,298
A.10) In-Channel Denitrification	73							06/01/83	\$1,400,000
	74	\$85,000	4.74	\$141,917	\$295,000	\$4250	\$605,077	04/01/90	\$1,314,521
	75							06/01/88	
	76							03/08/94	
A.11) ICEAS	77	\$260,000	4.66	\$422,039	\$70,000	\$4881	\$119,491	01/05/95	\$998,188
	78	\$100,000	4.70	\$150,428	\$125,000	\$4122	\$236,163	06/30/88	\$1,196,187
	79	\$53,000	4.66	\$123,463	\$264,000	\$4903	\$643,832	04/20/95	\$848,376
	80	\$29,000	4.72	\$48,468	\$54,000	\$4224	\$111,083	04/01/89	\$454,855
A.12) Trickling Filter	81				\$285,650	\$5735	\$534,120	06/01/00	\$534,120
A.13) RBC	82	\$12,000	4.83	\$22,886	\$162,552	\$4558	\$361,852	06/01/92	\$403,396
	83	\$11,742	5.03	\$19,886	\$131,593	\$6166	\$200,251	06/01/02	\$278,826
	84	\$28,000	6.51	\$44,089	\$80,688	\$7579	\$120,208	06/01/07	\$194,351
	85	\$92,000	4.77	\$121,018	\$288,320	\$4806	\$414,623	06/01/94	\$842,288
B.1) Package Plant	86				\$10,500	\$7818	\$13,835	06/01/08	\$41,934
	87							06/01/07	\$34,252

Table J.4. O&M Costs - Electricity Costs and Labor Costs

Process	#	Electricity Costs	Average Price of Electricity (\$)	Adjusted Electricity Cost with Average Prices and Location Factor	Total Labor Costs	ENR Skilled Labor Index	Adjusted Labor Cost with ENR Labor Index and Location Factor	Date for O&M	Total O&M Cost
	88	\$4,000	4.64	\$7378	\$23,260	\$5735	\$38,233	06/01/00	\$54,123
	89	\$12,719	4.77	\$19,944	\$36,706	\$4806	\$62,924	06/01/94	\$87,472
	90	\$29,504	5.23	\$50,511	\$203,216	\$5948	\$336,958	06/01/01	\$531,668
	91							10/01/04	\$269,119
	92	\$53,100	4.77	\$89,543	\$57,400	\$4764	\$106,753	03/01/94	\$277,688
	93							03/01/93	
	94	\$18,000	4.70	\$29,089	\$85,000	\$4122	\$172,523	01/12/88	\$218,598
	95							04/01/93	
	96	\$32,000	4.77	\$48,935	\$78,000	\$4025	\$155,703	04/15/87	\$219,594
	97							10/01/90	
	98	\$27,793	4.30	\$56,972	\$47,400	\$3525	\$130,555	08/24/81	\$321,632
	99							12/01/07	\$135,400
	100	\$72,000	4.48	\$129,557	\$80,000	\$5345	\$132,902	06/01/98	\$140,981
	101	\$30,000	4.64	\$56,921	\$174,000	\$5735	\$294,218	06/01/00	\$475,298
	102							08/01/92	
	103							10/01/87	
	104							05/01/95	
	105							01/01/87	
	106							07/01/93	
	107	\$180,000	4.83	\$291,483	\$115,000	\$4551	\$217,702	11/01/92	\$525,780
	108							09/27/89	
	109	\$6000	4.70	\$11,657	\$69,306	\$4122	\$169,117	08/25/88	\$253,927
	110							04/01/95	
	111	\$72,000	4.83	\$113,694	\$93,760	\$4443	\$177,286	06/01/91	\$609,392
	112	\$500,000	7.61	\$540,306	\$405,816	\$7861	\$467,615	08/01/08	\$3,497,086
	113							06/01/93	\$150,314
	114							06/01/04	\$212,479
	115							06/01/05	
	116	\$23,000	5.03	\$41,395	\$60,000	\$6166	\$97,033	06/01/02	\$202,736
	117							06/01/04	\$384,232

Table J.4. O&M Costs - Electricity Costs and Labor Costs

Process	#	Electricity Costs	Average Price of Electricity (\$)	Adjusted Electricity Cost with Average Prices and Location Factor	Total Labor Costs	ENR Skilled Labor Index	Adjusted Labor Cost with ENR Labor Index and Location Factor	Date for O&M	Total O&M Cost
	118				\$254,944	\$7579	\$338,764	06/01/07	\$356,339
	119	\$8,500	5.23	\$17,565	\$191,405	\$5948	\$383,085	06/01/01	\$453,316
	120				\$157,713	\$5735	\$279,028	06/01/00	\$279,028
	121							06/01/07	\$6,122,462
	122	\$37,500	5.23	\$68,270	\$499,878	\$5948	\$881,401	06/01/01	\$962,371
	123	\$28,997	4.83	\$44,363				07/10/91	\$202,935
	124				\$863,312	\$5948	\$1,368,228	06/01/01	\$1,368,228
	125	\$92,569	4.85	\$132,775	\$89,504	\$4653	\$147,395	01/22/93	\$307,717
	126							07/01/91	\$770,198
	127				\$137,134	\$7579	\$198,226	06/01/07	\$240,249
	128							04/01/93	
	129				\$6000	\$3759	\$14,081	01/01/84	\$236,940
	130							11/20/03	
	131	\$81,000	4.93	\$119,846	\$230,370	\$3933	\$470,621	07/01/86	\$1,580,221
	132	\$71,329	4.97	\$122,826	\$165,958	\$3844	\$406,983	12/31/85	\$741,588
B.3) OD	133							03/02/93	
	134	\$37,807	4.72	\$70,773	\$140,508	\$4224	\$323,737	08/01/89	\$411,039
	135	\$40,900	6.41	\$54,354	\$145,600	\$7213	\$189,405	06/01/06	\$311,869
	136	\$17,443	6.51	\$25,026	\$1683	\$7579	\$2,285	06/01/07	\$377,547
	137				\$517,728	\$7213	\$728,281	06/01/06	\$728,281
	138				\$378,251	\$6981	\$549,763	06/01/05	\$605,511
	139	\$20,694	6.51	\$29,282	\$279,086	\$7579	\$373,628	06/01/07	\$413,274
	140							06/02/07	
	141	\$147,655	5.28	\$261,196	\$764,778	\$6487	\$1,212,901	06/01/03	\$1,939,151
	142	\$20,440	4.70	\$30,836	\$508,080	\$4122	\$962,691	02/01/88	\$1,197,252
	143	\$48,000	4.93	\$69,980	\$142,000	\$3933	\$285,841	07/01/86	\$1,277,834
B.4) Biological Filtration	144							11/01/02	
	145							02/01/07	
	146							06/01/01	
C.1) MBR	147	\$24,000	5.46	\$33,387	\$760			06/01/04	\$189,984

Table J.4. O&M Costs - Electricity Costs and Labor Costs

Process	#	Electricity Costs	Average Price of Electricity (\$)	Adjusted Electricity Cost with Average Prices and Location Factor	Total Labor Costs	ENR Skilled Labor Index	Adjusted Labor Cost with ENR Labor Index and Location Factor	Date for O&M	Total O&M Cost
	148		7.61					08/01/08	
	149		\$0					06/01/05	
	150							04/01/04	
	151							06/30/99	
	152							05/01/06	
	153							05/19/06	
	154							06/30/97	
	155							02/01/04	
	156							06/01/99	
	157							02/01/04	
	158							12/01/02	
	159							01/31/07	
	160							12/01/03	
	161							12/01/04	
	162							12/01/04	
	163	\$35,000	5.23	\$53,948	\$30,000	\$6912	\$38,540	01/01/05	\$71,659
	164	\$72,000	6.27	\$92,570	\$80,000	\$7796	\$91,119	01/01/03	\$106,424
	165	\$52,000	6.27	\$66,856	\$80,000	\$7796	\$91,119	01/01/08	\$175,075
	166							06/30/00	
	167							06/01/99	
	168	\$240,000	4.78	\$369,540	\$300,000	\$6148	\$395,592	06/01/01	\$1,136,387
	169							12/01/03	
	170							08/01/06	
	171							01/01/03	\$648,932
	172							05/01/06	\$86,490
D.1) Pond	173	\$38,700	6.41	\$54,791	\$499,847	\$7213	\$692,724	06/01/06	\$780,607
	174							06/01/06	\$650,636
	175	\$27,000	5.86	\$42,074	\$251,612	\$6981	\$362,526	06/01/05	\$412,889
	176	\$52,000	6.27	\$66,856	\$80,000	\$7796	\$91,119	01/01/08	\$175,075
	177	\$12,000	5.23	\$22,191	\$46,050	\$5948	\$82,477	06/01/01	\$143,713

Table J.4. O&M Costs - Electricity Costs and Labor Costs

Process	#	Electricity Costs	Average Price of Electricity (\$)	Adjusted Electricity Cost with Average Prices and Location Factor	Total Labor Costs	ENR Skilled Labor Index	Adjusted Labor Cost with ENR Labor Index and Location Factor	Date for O&M	Total O&M Cost
	178	\$2680	6.41	\$3955	\$20,040	\$7213	\$28,951	06/01/06	\$39,805
	179							06/01/03	\$275,000
	180	\$9000	5.46	\$15,594	\$112,862	\$6698	\$175,583	06/01/04	\$213,993
	181	\$12,000	5.46	\$20,069	\$109,335	\$6698	\$164,187	06/01/04	\$190,223
	182							01/31/01	
	183							03/08/08	\$36,980
	184							06/01/91	
	185	\$9000	4.64	\$13,133	\$99,812	\$5735	\$129,802	06/01/00	\$146,961
	186	\$7682	4.53	\$11,482	\$48,420	\$5203	\$69,407	06/01/97	\$83,354
	187	\$26,040	4.77	\$59,000	\$120,342	\$4806	\$298,089	06/01/94	\$386,928
	188	\$22,000	4.83	\$44,344	\$79,791	\$4558	\$187,723	06/01/92	\$269,040
	189				\$182,971	\$7579	\$199,305	06/01/07	\$290,893
D.2) Lagoon	190				\$206,220	\$5203	\$301,425	06/01/97	\$301,425
	191							06/01/95	\$102,849
	192	\$2500	5.86	\$3801	\$66,388	\$4909	\$102,849	06/01/95	
	193	\$31,200	4.43	\$66,456	\$18,435	\$6981	\$25,918	06/01/05	\$32,915
	194				\$374,625	\$5521	\$705,252	06/01/99	\$943,573
	195							06/01/08	
	196	\$37,500	7.42	\$47,627	\$904,603	\$7818	\$1,201,079	06/01/07	\$111,907
	197	\$2175	5.86	\$3959	\$88,926	\$6981	\$149,666	06/01/08	\$1,315,870
	198	\$22,625	6.51	\$33,091	\$191,689	\$7579	\$265,256	06/01/05	\$173,558
	199	\$41,300	5.03	\$79,935	\$233,366	\$6166	\$405,856	06/01/07	\$392,755
	200							06/01/02	\$512,213
	201							06/01/00	
	202							06/01/01	
	203							06/01/01	
D.3) Wetland	204							06/01/01	
	205							06/01/03	
	206							06/01/03	
	207							06/01/04	

Table J.4. O&M Costs - Electricity Costs and Labor Costs

Process	#	Electricity Costs	Average Price of Electricity (\$)	Adjusted Electricity Cost with Average Prices and Location Factor	Total Labor Costs	ENR Skilled Labor Index	Adjusted Labor Cost with ENR Labor Index and Location Factor	Date for O&M	Total O&M Cost
	208							06/01/04	
	209							06/01/04	
	210							06/01/05	
	211							06/01/05	
	212							04/01/08	
	213							06/01/98	
	214							06/01/98	
	215							06/01/98	
	216							06/01/98	
	217							06/01/98	
	218							06/01/98	
	219							06/01/98	
	220							06/01/98	
	221							06/01/98	
	222							06/01/98	
	223							06/01/98	
	224							06/01/98	
	225							06/01/98	
	226							06/01/98	
	227	\$47,259	6.51	\$51,473				06/01/07	\$103,387
	228							06/01/98	
	229	\$13,847	4.64	\$24,136	\$23,400	\$5714	\$36,483	05/01/00	\$80,518
	230	\$21,955	4.64	\$38,609	\$46,800	\$5714	\$73,614	05/01/00	\$143,901
E.1) LM	231	\$145,796	4.64	\$256,389	\$174,720	\$5714	\$274,825	05/01/00	\$750,949
	232	\$12,117	4.64	\$21,121	\$23,400	\$5714	\$36,483	05/01/00	\$75,838
	233	\$18,455	4.64	\$32,454	\$46,800	\$5714	\$73,614	05/01/00	\$135,413
	234	\$102,046	4.64	\$179,452	\$174,720	\$5714	\$274,825	05/01/00	\$657,161

Note: Electricity Price (\$) in 12/2008 = \$7.36; ENR Skilled Labor Index on 12/2008 = \$8,107

Table J.5. Effluent Water Quality

Process	#	Effluent Water Quality				Removal Efficiency			
		Effluent BOD (mg/L)	Effluent TSS (mg/L)	Effluent TN (mg/L)	Effluent TP (mg/L)	Removal Efficiency-BOD	Removal Efficiency-TSS	Removal Efficiency-TN	Removal Efficiency-TP
	1	26.9	30.0			85.0%	88.8%	100.0%	
	2								
	3								
	4	1.1	1.2	2.0	0.2	99.2%	99.5%	95.1%	97.0%
	5	1.0	0.4	1.8	0.2				
	6	30.0	30.0	17.5		89.1%	88.0%	41.7%	
	7								
	8	5.0	9.0	0.3		97.0%			
	9								
	10								
	11								
	12								
A.1) Activated Sludge	13	20.0	20.0			91.3%	90.0%	90.0%	
	14	20.0	20.0			91.3%	90.0%	90.0%	
	15								
	16					100.0%	100.0%	100.0%	
	17								
	18	30.0	30.0						
	19								
	20								
	21								
	22								
	23								
	24	25.0	25.0			90.0%	90.0%	90.0%	
	25								
	26	10.0	15.0	9.0		96.7%	94.0%	94.0%	82.0%
A.2) Extended Aeration	27								
	28								
	29								

Table J.5. Effluent Water Quality

Process	#	Effluent Water Quality			Removal Efficiency			
		Effluent BOD (mg/L)	Effluent TSS (mg/L)	Effluent TN (mg/L)	Effluent TP (mg/L)	Removal Efficiency -BOD	Removal Efficiency -TSS	Removal Efficiency -TN
	30	10.0	15.0	4.0		88.0%	88.2%	
	31	30.0	30.0			96.8%	88.0%	94.0%
	32	8.0	30.0	1.5				
	33							
	34	7.5	30.0					
	35							
	36							
	37							
	38							
	39	15.9	8.4	6.4		95.2%	96.4%	
	40							
	41							
	42							
	43							
A.3) Intermittent Aeration	44							
	45	10.0	30.0	3.0		95.0%	85.0%	92.5%
A.4) A/O	46	7.5	7.5	1.5	0.5	97.1%	97.0%	96.3%
	47	7.5	7.5	1.5	0.5	97.2%	96.7%	95.0%
	48	5.0	5.0	1.0	1.0	97.2%	96.9%	95.7%
A.5) A2/O	49							89.1%
	50							
	51							
	52							
	53	1.5	1.5	1.0	0.6			
A.6) Bardenpho	54							
	55							
	56							
	57							
	58	2.0	1.0	5.0		99.2%	99.3%	86.5%

Table J.5. Effluent Water Quality

Process	#	Effluent Water Quality			Removal Efficiency			
		Effluent BOD (mg/L)	Effluent TSS (mg/L)	Effluent TN (mg/L)	Effluent TP (mg/L)	Removal Efficiency -BOD	Removal Efficiency -TSS	Removal Efficiency -TN
	59			0.9				
	60							
	61							
	62							
A.7) BNR	63							
	64							
	65	2.2	10.5	0.2		98.1%	93.3%	98.9%
	66	1.9	6.6	1.1		98.4%	96.6%	90.4%
	67							
A.8) MLE	68							
	69							
	70							
A.9) Schreiber N&D	71							
A.10) In-Channel Denitrification	72	3.6	3.9	0.1	0.7	98.7%	98.6%	98.3%
	73	3.7	1.8	2.9	1.5			
	74	2.8	3.2	0.4		98.2%	97.8%	97.9%
	75							
	76							
A.11) ICEAS	77	13.0	18.0	0.1		91.8%	94.3%	93.0%
	78	2.7	14.0	3.6		97.8%	94.8%	86.5%
	79	3.8	2.9	1.3		98.4%	98.2%	93.5%
	80	3.8	2.9	1.3		98.4%	98.2%	93.5%
A.12) Trickling Filter	81							
	82							
A.13) RBC	83	16	21	16				
	84	10.0	15.0					
B.1) Package Plant	85	3.6				98.9%		
	86							
	87							

Table J.5. Effluent Water Quality

Process	#	Effluent Water Quality			Removal Efficiency		
		Effluent BOD (mg/L)	Effluent TSS (mg/L)	Effluent TN (mg/L)	Effluent TP (mg/L)	Removal Efficiency -BOD	Removal Efficiency -TSS
	88						
	89						
	90						
	91						
	92	10.0	10.0	5.0	1.0	96.0%	95.0%
	93						
	94	5.0	7.0	0.5	0.6	95.0%	93.0%
	95						
	96	10.0	10.0	0.6	0.6	94.2%	94.4%
	97						
	98	2.6	5.4	0.8		98.3%	97.1%
	99						
	100	5.0	5.0			98.6%	98.6%
	101	15.0	18.4			94.6%	95.6%
	102						
	103	10.0	20.0	1.0	2.0	95.6%	91.1%
	104						
	105						
	106	10.0	10.0	3.0	3.0	97.8%	97.7%
	107	10.0	15.0			91.1%	90.5%
	108	6.2	17.2	0.1		95.3%	92.1%
	109						
	110				5.0	100.0%	100.0%
	111	3.0	7.3	0.2	1.3	98.7%	92.8%
	112	6.0		1.0		97.9%	99.5%
	113	10.0	30.0	1.0	1.0	95.5%	99.5%
	114	15.0	20.0	10.0		94.0%	92.0%
	115						
	116	20.0	20.0			92.1%	93.3%
	117			10.0		100.0%	100.0%

Table J.5. Effluent Water Quality

Process	#	Effluent Water Quality			Removal Efficiency			
		Effluent BOD (mg/L)	Effluent TSS (mg/L)	Effluent TN (mg/L)	Effluent TP (mg/L)	Removal Efficiency -BOD	Removal Efficiency -TSS	Removal Efficiency -TN
	118	30.0	30.0	30.0		91.0%	87.2%	
	119	5.0	30.0	2.0				
	120							
	121	10.0	30.0			96.3%	87.5%	
	122	5.0	5.0			98.0%	98.0%	
	123	5.0	6.8			94.7%	96.5%	
	124	10.0	30.00	5				
	125	10.0	15.0	6.0		96.7%	95.0%	85.0%
	126	30.0	30.0		1.0	83.3%	86.4%	100.0%
	127	20.0	22.5					
	128							
	129	10.0	15.0			95.0%	92.5%	100.0%
	130							
	131	2.6	3.1	0.3	0.2	98.4%	97.8%	98.4%
	132	1.0	0.7	0.6		99.1%	99.5%	98.6%
B.3) OD	133	18.0	15.0	12.0	1.0	91.0%	91.7%	65.7%
	134	3.4	3.9	0.3		98.0%	97.7%	98.6%
	135	5.0	5.0	3.0				
	136	16.0	30.0	12.0				
	137							
	138							
	139							
	140							
	141	16.0	30.0					
	142	1.5	1.5	0.3	0.2	99.6%	99.5%	99.3%
	143	3.6	3.8	3.2		98.0%	97.6%	86.2%
B.4) Biological Filtration	144							
	145							
	146							
C.1) MBR	147	4.5	4.5			98.7%	98.1%	

Table J.5. Effluent Water Quality

Process	#	Effluent Water Quality			Removal Efficiency		
		Effluent BOD (mg/L)	Effluent TSS (mg/L)	Effluent TN (mg/L)	Effluent TP (mg/L)	Removal Efficiency -BOD	Removal Efficiency -TSS
	148	4.5	1.5			98.2%	99.5%
	149						100.0%
	150						
	151						
	152						
	153						
	154						
	155						
	156						
	157						
	158						
	159						
	160						
	161						
	162						
	163						
	164	5.0	5.0			98.6%	98.6%
	165	50.0	90.0			85.7%	74.3%
	166						
	167						
	168						
	169						
	170						
	171						
	172						
	173	30.0	30.0				
D.1) Pond	174						
	175	50.0	90.0	15.0	6.0	75.0%	55.0%
	176	5.0	5.0			98.6%	40.0%
	177	29.5	37.0			98.6%	25.0%

Table J.5. Effluent Water Quality

Process	#	Effluent Water Quality			Removal Efficiency			
		Effluent BOD (mg/L)	Effluent TSS (mg/L)	Effluent TN (mg/L)	Effluent TP (mg/L)	Removal Efficiency -BOD	Removal Efficiency -TSS	Removal Efficiency -TN
	178							
	179							
	180	30.0	90.0					
	181	20.0	20.0					
	182							
	183							
	184							
	185	35.0				68.5%		
	186	40.0				64.0%		
	187	11.0	30.0	5.0				
	188							
	189	30.0	30.0					
	190							
D.2) Lagoon	191	93.0	93.0			59.0%	56.7%	
	192							
	193	30.0	90.0					
	194							
	195							
	196							
	197							
	198							
	199							
	200							
	201							
	202							
D.3) Wetland	203							
	204							
	205							
	206							
	207							

Table J.5. Effluent Water Quality

Process	#	Effluent Water Quality			Removal Efficiency			
		Effluent BOD (mg/L)	Effluent TSS (mg/L)	Effluent TN (mg/L)	Effluent TP (mg/L)	Removal Efficiency -BOD	Removal Efficiency -TSS	Removal Efficiency -TN
	208							
	209							
	210							
	211							
	212							
	213							
	214							
	215							
	216							
	217							
	218							
	219							
	220							
	221							
	222							
	223							
	224							
	225							
	226							
	227	35.0	36.0			87.2%	82.0%	
	228							
	229							
	230	5.9	5.3	5.6	2.0	97.4%	97.5%	66.7%
E.1) LM	231							
	232	4.0	2.0	11.0	6.0	98.3%	99.5%	75.0%
	233							45.5%
	234							

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1199 North Fairfax Street, Suite 410
Alexandria, VA 22314 USA
(703) 548-0880
Fax (703) 548-5085
E-mail: Foundation@WateReuse.org
www.WateReuse.org/Foundation